# Distribution of Prostaglandin $E_1$ in Lipid Emulsion in Relation to Release Rate from Lipid Particles

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The distribution style of prostaglandin  $E_1$  (PGE<sub>1</sub>) in injectable lipid emulsion (Lipo-PGE<sub>1</sub>) was analyzed using a three-phase model: an aqueous phase, an oil phase and an oil/water interface. A combination of the oil phase and the oil/water interface was obtained as the particle phase. Initial diffusion rates of PGE<sub>1</sub> from lipid particles to the aqueous phase were determined by the dialysis method, and equilibrium concentrations were calculated by the diffusion rates using an equation derived from Fick's theory. Lipo-PGE<sub>1</sub> enclosed in cellulose tubing was immersed in buffer solutions (pH 5.5, 7.4), then incubated at various constant temperatures. Each concentration of PGE<sub>1</sub> in the aqueous phase was measured at appropriate intervals. By using these values, partition coefficients between the particle phase and the aqueous phase were calculated. It was found that a larger portion of PGE<sub>1</sub> was distributed in the particle phase compared with the aqueous phase in Lipo-PGE<sub>1</sub> at each temperature. Furthermore, actual partition coefficients between oil and aqueous phases were measured. From the results of two partition coefficients, the distribution ratio of PGE<sub>1</sub> in Lipo-PGE<sub>1</sub> was determined as: oil:oil/water interface:water = 0.2:93.1:6.7, that is, 93% PGE<sub>1</sub> was found to be distributed in lipid particles. On the other hand, by diluting PGE<sub>1</sub> one hundred times with transfusion, the distribution ratio of PGE<sub>1</sub> in lipid particles decreased as the pH of the transfusion increased. The ratios after 2 h were 74% and 47% for pH 5.5 and 7.4, respectively.

In conclusion, a large portion of  $PGE_1$  was found to be distributed in the particle phase when Lipo- $PGE_1$  was diluted with transfusion. Since most  $PGE_1$  exists in an oil/water interface, it is considered that it has a strong affinity for phospholipids. Thus, this affinity may contribute to the remarkable increase in activity in clinical treatment.

**Keywords** prostaglandin E<sub>1</sub>; lipid emulsion; distribution; emulsion; lipid particle; partition

Lipid emulsion formulations of prostaglandin  $E_1$  (PGE<sub>1</sub>) show a remarkable increase in activities in the treatment of various vascular disorders, <sup>1-3)</sup> as well as a reduction in side effects such as local irritation near the site of injection following parenteral administration.<sup>4-8)</sup>

But the behavior of PGE<sub>1</sub> in preparation has not been extensively investigated. Since PGE<sub>1</sub> in injectable lipid emulsion (Lipo-PGE<sub>1</sub>) is generally diluted with several kinds of transfusions for treatments, it is important to clarify the distribution of PGE<sub>1</sub> in these transfusions, because it may be released from the lipid particles in the aqueous phase in the transfusion bottle. Minakuchi et al. reported that most of the PGE<sub>1</sub> was released in an aqueous medium immediately after diluting it ten times with a saline or buffer (pH 5.6).9 Based on these results, they reported that Lipo-PGE, might not exert its effect as a lipid emulsion in clinical treatment. Many case studies indicate that Lipo-PGE<sub>1</sub> diluted two hundred times with an aqueous solution exerts high activity in clinical treatment. For example, the activity of Lipo-PGE<sub>1</sub> (3  $\mu$ g) was greater than that of PGE<sub>1</sub>-CD (cyclodextrin inclusion compound of PGE<sub>1</sub>,  $40 \mu g$ ). The purpose of this study is to identify those factors which account for the high efficacy of Lipo-PGE<sub>1</sub> from the pharmaceutical viewpoint, taking the distribution of PGE<sub>1</sub> in lipid emulsion into consideration.

## **Theoretical**

Derivation of the Diffusion Rate Equations in Relation to Equilibrium Concentrations Fick's theory was applied to explain the transport of a drug in lipid emulsion. The amount, M, of drug flowing through a unit cross section, S, of a membrane in unit time, t, is known as the flux, J,

in Fick's first law.

$$J = \frac{dM}{S \cdot dt} \tag{1}$$

The flux, in turn, is proportional to the concentration gradient, dC/dx:

$$J = -D\frac{dC}{dx} \tag{2}$$

in which D is the diffusion coefficient of a drug, since the solubility of a drug in the particle phase is different from that in the aqueous phase, and the concentration of the drug is not the same. Accordingly,  $C_{\rm wmax}$  is defined as the equilibrium concentration of a drug in the aqueous phase at an infinite time. Then, the concentration gradient dC/dx can be represented as  $(C_{\rm wmax}-C_{\rm w})/h$ . Hence, Eq. 2 can be rewritten as:

$$\frac{dM}{dt} = \frac{D_{\rm m} \cdot S \cdot K}{h} \left( C_{\rm wmax} - C_{\rm w} \right) \tag{3}$$

where dM/dt is the amount of gradient of drug in the aqueous phase,  $D_{\rm m}$  is the diffusion coefficient of the drug in the interfacial membrane, S is the surface area of the interfacial membrane and the partition coefficient between the interfacial membrane and the aqueous phase, h is the thickness of the interfacial membrane, and  $C_{\rm w}$  is the concentration in the aqueous phase at time t. Permeability P is defined as:

$$P = \frac{D_{\rm m} \cdot S \cdot K}{h} \tag{4}$$

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and, a rearrangement of Eq. 3 shows that

$$\frac{V_{\mathbf{w}} \cdot dC_{\mathbf{w}}}{dt} = P \cdot (C_{\mathbf{w}_{\mathbf{max}}} - C_{\mathbf{w}}) \tag{5}$$

in which  $V_{\rm w}$  is the volume in the aqueous phase. Then, Eq. 5 can be integrated to give:

$$\ln\left(1 - \frac{C_{\mathbf{w}}}{C_{\mathbf{wmax}}}\right) = -\frac{P}{V_{\mathbf{w}}} \cdot t \tag{6}$$

$$\frac{C_{\rm w}}{C_{\rm wmax}} = 1 - \exp\left(-\frac{P}{V_{\rm w}} \cdot t\right) \tag{7}$$

Since the equilibrium concentration as well as the solubility of the oil phase is different from the equilibrium concentration of the aqueous phase,  $C_{\rm wmax}$  can be written as:

$$C_{\text{wmax}} = \frac{M_{\text{t}} - C_{\text{d}} \cdot V_{\text{o}}}{V_{\text{w}} + V_{\text{o}}} \tag{8}$$

where the  $C_{\rm d}$  is the difference between the equilibrium concentrations in the oil phase and the aqueous phase,  $M_{\rm t}$  is the amount of the drug, and  $V_{\rm o}$  is the volume of the oil phase. By substituting Eq. 8 into Eq. 7,  $C_{\rm w}$  can be written as follows:

$$C_{\mathbf{w}} = \frac{M_{\mathbf{t}} - C_{\mathbf{d}} \cdot V_{\mathbf{o}}}{V_{\mathbf{w}} + V_{\mathbf{o}}} \cdot \left(1 - \exp\left(-\frac{P}{V_{\mathbf{w}}} \cdot t\right)\right) \tag{9}$$

## Experimental

Materials The PGE<sub>1</sub> used was synthesized at Taisho Pharmaceutical Co., Ltd. A Palux Injection® was used to administer Lipo-PGE<sub>1</sub>. Prostaglandin A<sub>1</sub> (PGA<sub>1</sub>) of analytical standard was obtained commercially from Funakoshi Co., Ltd. Soybean oil was obtained commercially from Ajinomoto, Co., Inc. All other chemicals were of reagent grade. Cellulose tubing (pore size: 24Å, thickness: 0.03 mm, diameter: 20 mm) used for dialysis was purchased from Viskase Sales Corp. Buffer solutions (pH 3, 4.5, 5.5) were prepared with 0.2 m citric acid and 0.1 m Na<sub>2</sub>HPO<sub>4</sub>. Other buffer solutions (pH 6.5, 7.4) were prepared using 0.2 m KH<sub>2</sub>PO<sub>4</sub> and 0.2 m NaHCO<sub>3</sub>. The ionic strength of each buffer solution was adjusted to 0.15 with NaCl.

Assay for PGE<sub>1</sub> PGE<sub>1</sub> was measured by high-performance liquid chromatography (HPLC) with a post-column reaction. <sup>11)</sup> An aqueous solution of PGE<sub>1</sub> (equivalent to 2.5 µg of PGE<sub>1</sub>) was run through a pre-column (Sep pack C18) which had been washed, and eluted with 7 ml of methanol. All of the elution was evaporated at a temperature of not more than 40 °C under vacuum conditions. One ml of the internal standard solution was added to the evaporated sample. This sample was injected to HPLC. The HPLC parameters were as follows: column, TSK gel ODS-LS410; column temperature, about 50 °C; mobile phase, CH<sub>3</sub>CN: aqueous 1/150 м phosphate buffer (pH 6.3) = 28:72; and flow rate, 1 ml/min. Conditions for the post-column reaction were as follows: column, teflon tube; flow rate, 0.5 ml/min; reaction solution, 1 N KOH.

**Preparations of Lipo-PGE**<sub>1</sub> The formulas of Lipo-PGE<sub>1</sub> are shown in Table I. The preparation of Lipo-PGE<sub>1</sub> was as follows: 7 mg of PGE<sub>1</sub>, 18 mg of egg yolk lecithin and 2.4 g of oleic acid were added to 100 g of

TABLE I. Formulas for Lipo-PGE<sub>1</sub>

PGE <sub>1</sub>	7	μg
Soybean oil	100	mg
Egg yolk lecithin	18	mg
Oleic acid	2.4	4 mg
Glycerol		l mg
Sodium hydroxide for pH adjustment to 4.5—6.0		
Water for injection	a.c	7. a)

a) Adjusted to 1 ml. a.q. = adequate quantity.

soybean oil. This mixture was heated and stirred until it was completely clear. Eight hundred ml of water for injection and 22.1 g of glycerol were added to the oil mixture. This total mixture was preemulsified using a Physcotron homogenizer (model NS-60, Niti-on Medical & Physical Instruments MFG. Co., Ltd.) at 8000 rpm for 10 min. The pH of the coarse emulsion was then adjusted to a pH of 4.5—6.0 with sodium hydroxide aqueous solution. Final emulsification was completed by passing the coarse emulsion through a high pressure homogenizer (model 15 M, APV Gaulin, Inc.). The volume of emulsion was adjusted to 1000 ml with water for injection. <sup>12)</sup> In all the processes, nitrogen gas was bubbled into the emulsion. The mean particle size of the Lipo-PGE<sub>1</sub> thus obtained was established as being 0.2  $\mu$ m using a light scattering spectrometer (Nicomp model 370 Submicron particle sizer, Pacific Scientific Instrument Division). The pH of Lipo-PGE<sub>1</sub> was determined to be 5.4 by a pH meter (model HM-30, Toa Denpa Kogyo Co. Ltd.).

**Diffusion Rate** Diffusion rates of PGE<sub>1</sub> from the particle phase to the aqueous phase were obtained by the dialysis method. Four ml of Lipo-PGE<sub>1</sub> enclosed in cellulose tubing was immersed in 36 ml of pH 5.5 or 7.4 buffer solution, and incubated at constant temperatures (5, 20, 37 °C). Each concentration of PGE<sub>1</sub> in the aqueous phase was measured at appropriate intervals by HPLC. Similarly, 2 ml of Lipo-PGE<sub>1</sub> enclosed in cellulose tubing was immersed in 198 ml of pH 5.5 or 7.4 buffer solution and incubated at 20 °C.

**Oil/Water Partition Coefficient** Five-tenths mg of  $PGE_1$  was dissolved in 50 ml of various pH of buffer solutions. Ten ml of each solution was added to 10 ml of soybean oil, and the oil/water mixture was shaken for 3 or 24 h. The mixture was then centrifuged at 3000 rpm for 15 min to separate each layer, and the aqueous layer was assayed for  $PGE_1$  by HPLC.

## **Results and Discussion**

Diffusion Rates of PGE<sub>1</sub> from the Particle Phase The release profiles of PGE<sub>1</sub> from lipid particles are shown in Figs. 1 to 3, when Lipo-PGE<sub>1</sub> was diluted ten times with the buffer solution. A small amount of PGA<sub>1</sub> was yielded during experimentation as a decomposition product (Table II). But since the amount was so small, this effect was considered to be negligible. The plots show the concentrations of PGE<sub>1</sub> in the aqueous phase at appropriate intervals, and the full lines are the theoretical curves obtained from Eq. 9. The values of the characteristic parameter in Eq. 9 are shown in Table III, and the values of  $C_d$  and P were obtained by regressing Eq. 9 to the experimental measurements. Since good correlation was observed between experimental and theoretical data, the values of  $C_d$  and P were considered reasonable. The particle/water partition coefficient could be calculated

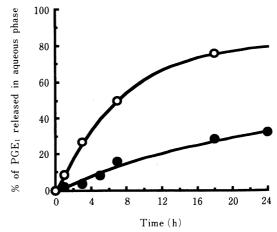


Fig. 1. Release Profiles of PGE  $_1$  from Particles in Lipo-PGE  $_1$  Diluted Ten Times with Buffer Solutions at  $5\,^{\circ}\mathrm{C}$ 

●, pH 5.5; ○, pH 7.4. The full lines are theoretical curves of Eq. 9.

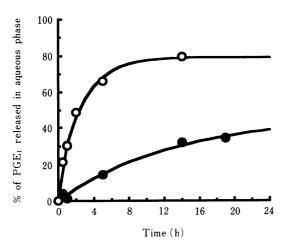


Fig. 2. Release Profiles of  $PGE_1$  from Particles in Lipo-PGE<sub>1</sub> Diluted Ten Times with Buffer Solutions at 20 °C

•, pH 5.5; O, pH 7.4. The full lines are theoretical curves of Eq. 9.

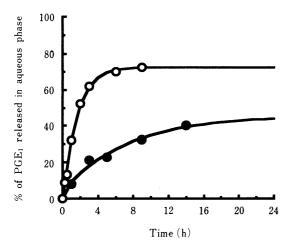


Fig. 3. Release Profiles of PGE  $_1$  from Particles in Lipo-PGE  $_1$  Diluted Ten Times with Buffer Solutions at 37  $^{\circ}{\rm C}$ 

•, pH 5.5; O, pH 7.4. The full lines are theoretical curves of Eq. 9.

Table II. Amount of PGA<sub>1</sub> during Experimentation as a Decomposition Product of PGE<sub>1</sub> (%)

рН		Temperature (°C)	•
	5	20	37
5.5	0.3	1.4	5.3
7.4	0.4	1.8	5.9

from the values of  $C_{\rm d}$  obtained. Each equilibrium concentration of the particle phase and the aqueous phase under the various temperatures was calculated. The results are shown in Table IV. It was found that most of the PGE<sub>1</sub> was distributed in lipid particles independent of temperature, but that the partition coefficient was increased as the pH of the buffer increased. This may be due to the increase of ionic PGE<sub>1</sub> as the pH of the buffer solution increased, since the p $K_{\rm a}$  of PGE<sub>1</sub> was reported to be 5.02. <sup>13)</sup>

The effect of temperature on the distribution ratio between the particle phase and the aqueous phase was

TABLE III. Characteristic Parameters of Lipo-PGE,

	Volume (ml)				
Dilution	Total PGE <sub>1</sub> M <sub>t</sub> (μg)	Lipo-PGE <sub>1</sub> (ml)	Buffer (ml)	Aqueous phase $V_{\rm w}$ (ml)	Oil phase $V_o$ (ml)
× 10	28	4	36	39.56	0.44
$\times 100$	14	2	198	199.78	0.22

a)  $V_o = \text{total oil amount/density of oil (0.91)}$ .

TABLE IV. Equilibrium Concentrations of Two Phases and Partition Coefficients when Lipo-PGE<sub>1</sub> Was Diluted Ten Times

pH of buffer	Temp.	Particle phase (µg/ml)	Aqueous phase (µg/ml)	Partition particle/ water
5.5	5	35.5	0.3	115
	20	35.1	0.3	110
	37	35.6	0.3	130
7.4	5	10.1	0.6	17
	20	20.5	0.5	43
	37	14.9	0.5	28

Table V. Distribution of  $PGE_1$  in Lipo- $PGE_1$  at Various Temperatures

Temp. (°C)	Particle phase (%)	Aqueous phase (%)
5	93.3	6.7
20	93.2	6.8
37	94.1	5.9

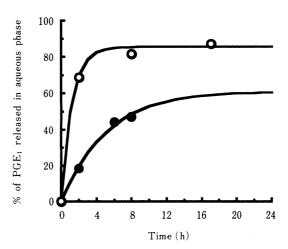


Fig. 4. Release Profiles of PGE  $_1$  from Particles in Lipo-PGE  $_1$  Diluted One Hundred Times with Buffer Solutions at 20  $^{\circ}{\rm C}$ 

•, pH 5.5; O, pH 7.4. The full lines are theoretical curves of Eq. 9.

calculated from the partition coefficient, as shown in Table IV, and the volume ratio (aqueous volume: particle volume = 0.89:0.11). The results are shown in Table V.

Figure 4 shows the release profiles of PGE<sub>1</sub> from lipid particles at 20 °C, where Lipo-PGE<sub>1</sub> was diluted one hundred times with buffer solutions (pH 5.5, 7.4). As shown in this figure, most of the PGE<sub>1</sub> was distributed in the aqueous phase after equilibrium was reached.

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Table VI. Amount of PGE<sub>1</sub> Remaining in Particles when Lipo-PGE<sub>1</sub> Was Diluted One Hundred Times at 20 °C

pН		PGE <sub>1</sub> Time after di		
	Initial	30	60	120
5.5	93.2	87.8	82.9	74.4
7.4	93.2	73.7	60.9	46.9

Table VII. Partition Coefficient of  $PGE_1$  between Soybean Oil and Aqueous Buffers at Various Temperatures

Temp.			pН		
	3.0	4.5	5.5	6.5	7.4
5			0.25		0.02
20	0.63	0.55	0.22	0.01	0.03
37	***************************************		0.24		0.02

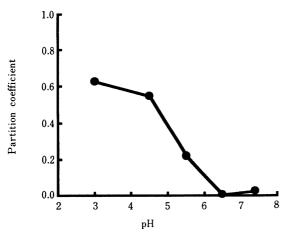


Fig. 5. The pH–Partition Profiles of  $PGE_1$  between Soybean Oil and Water at  $20\,^{\circ}C$ 

However, it took from 6—8 h to reach the equilibrium concentration; and as the dilution ratio as well as the pH of the buffer solution increased, the equilibrium concentration increased. The amount of PGE<sub>1</sub> which remained in lipid particles at appropriate intervals is shown in Table VI. The amounts of PGE<sub>1</sub> remaining in lipid particles were 74% and 47% for pH 5.5 and 7.4, respectively, after 2 h, when Lipo-PGE<sub>1</sub> was diluted one hundred times at 20 °C.

In contrast, Minakuchi et al. reported that 50% and 10% of PGE<sub>1</sub> remained in the lipid particles immediately after being diluted ten times with a saline (pH 5.6) and phosphate buffer solution, respectively. The inconsistency of the data may be due to the different methods used to separate the aqueous solution from the lipid emulsion. That is, cellulose tubing with a pore size of 24 Å was used in this study, whereas an ultrafilter with a pore size equal to a molecular weight 30000 was used by Minakuchi et al. In general, the amount of substance in filtrate is influenced by the pore size of the filter. Since the pore size of the ultrafilter was greater than that of the cellulose tubing, small lipid particles might have been passed

TABLE VIII. Distribution of PGE<sub>1</sub> in Lipo-PGE<sub>1</sub> at Various Temperatures

Temp. (°C)		Oil/water phase (%) (lecithin)	Water phase (%)
5	0.2	93.1	6.7
20	0.2	93.0	6.8
37	0.2	93.9	5.9

through the ultrafilter, which may be the reason why different data were obtained.

**Partition Coefficient of PGE**<sub>1</sub> The partition coefficients of PGE<sub>1</sub> between soybean oil and aqueous buffer solutions were obtained in the range of pH 3.0—7.4 at several temperatures (5, 20, 37 °C). The results are shown in Table VII and Fig. 5. Partition coefficients had no influence on the temperature, but did influence the pH value. That is, when the pH of the buffer solution was lower than 6.5, the partition coefficient decreased as the pH value linearly increased. On the other hand, when the pH of the solution was more than 6.5, the partition coefficient became constant and remained at a low level. Since the  $pK_a$  of PGE<sub>1</sub> is 5.02, the pH–partition coefficient profile in Fig. 5 can be explained from the relationship between the pH and the ionic PGE<sub>1</sub> ratio.

**Distribution of PGE**<sub>1</sub> in Lipo-PGE<sub>1</sub> The distribution style of PGE<sub>1</sub> in Lipo-PGE<sub>1</sub> was analyzed using a three-phase model, that is, PGE<sub>1</sub> distribution in an aqueous phase, an oil phase and an oil/water interface. The schematic model for partition was assumed where  $C_1$ ,  $C_2$  and  $C_3$  were defined as equilibrium concentrations in a water (aqueous) phase, a lecithin (oil/water interface) phase, and an oil phase, respectively. The concentration ratios of the lecithin/water and oil/lecithin are defined as  $P_{(L/W)}$  and  $P_{(O/L)}$ , respectively. If the concentrations of a drug were lower than the solubility in each phase, the values of  $P_{(L/W)}$  and  $P_{(O/L)}$  became constant. Therefore,  $C_2$ ,  $C_3$  can be written as follows:

$$C_2 = C_1 \cdot P_{(L/W)} \tag{8}$$

$$C_3 = C_1 \cdot P_{(O/L)} = C_1 \cdot P_{(L/W)} \cdot P_{(O/L)}$$
(9)

The particle phase is constituted with soybean oil and lecithin. Therefore, by measuring the concentration ratio between the particle phase and the water phase, and the partition coefficient between the oil phase and the water phase, the concentration ratio in the three phases can be obtained.

From the data in Table IV and VII, the partition coefficients of PGE<sub>1</sub> in the three phases (water, lecithin, oil) were calculated. Furthermore, the distribution ratios of PGE<sub>1</sub> in Lipo-PGE<sub>1</sub> were obtained at various temperatures (Table VIII). Most of the PGE<sub>1</sub> in Lipo-PGE<sub>1</sub> was distributed in lecithin and the ratio was not influenced by temperature. Since a large portion of the PGE<sub>1</sub> was found in the oil/water interface, PGE<sub>1</sub> is believed to have a high affinity with phospholipids. These results are considered to be the apparent distribution of the liposome in the lipid emulsion. Teagarden *et al.* reported that the distribution ratio of PGE<sub>1</sub> in the oil/water interface changed under the influence of ionic form.<sup>14</sup>)

In our study, the distribution of PGE<sub>1</sub> was measured at pH 5.5 (pH of Lipo-PGE<sub>1</sub>), but it was considered that the distribution, partition coefficient and release rate were thought to be due to ionic charges and solubilities. Therefore, we are planning to clarify the relationship between pH and distribution of PGE<sub>1</sub>.

In conclusion, a study was carried out of the release rate of  $PGE_1$  from lipid particles to an aqueous solution, when  $Lipo-PGE_1$  was diluted with aqueous solution. The equilibrium concentration was obtained using a modified form of Fick's equation. This method allowed the residual ratio of  $PGE_1$  in the lipid particles to be determined, which clarified the distribution of  $PGE_1$  in the transfusion bottle. This may be one of the factors which explains the high activity in clinical treatment.

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