## (Co<sub>2</sub>B)<sub>10</sub>RhH<sub>6</sub> and (Ni<sub>2</sub>B)<sub>10</sub>RhH<sub>15</sub> as Versatile Catalysts for Hydrogenation, Hydrogenolysis, and Methanation Reactions

By ROBERT W. MITCHELL\*† and LOUIS J. PANDOLFI

(Department of Chemistry and Institute of Geophysics, University of California, Los Angeles, California 90024)

and P. CALVIN MAYBURY

(Department of Chemistry, University of South Florida, Tampa, Florida 33620)

Summary The hydrogen adducts  $(Co_2B)_{10}RhH_6$  and  $(Ni_2B)_{10}RhH_{15}$  have been found to be active catalysts for the hydrogenation and hydrogenolysis of *cis*-but-2-ene and also for the reduction of carbon monoxide to methane.

WE have noted<sup>1</sup> that the interaction of cobalt(II) chloride or nickel(II) chloride with NaBH4 leads to products with approximate stoicheiometries (Co2B)5H3 and (Ni2B)2H3 respectively. We have now prepared rhodium containing species whose elemental analyses confirm the stoicheiometries (Co<sub>2</sub>B)<sub>10</sub>RhH<sub>6</sub> and (Ni<sub>2</sub>B)<sub>10</sub>RhH<sub>15</sub>. These substances were obtained by interaction of IM ethanolic Co<sup>II</sup> or  $Ni^{II}$  chloride containing 5 molar % RhCl<sub>3</sub>.3H<sub>2</sub>O with a 4-fold molar excess of NaBH<sub>4</sub> under N<sub>2</sub>. The products were found to be pyrophoric in air when dry, and were stored under ethanol until required for catalytic purposes. It should be noted that treatment of Co<sup>II</sup>, Ni<sup>II</sup> or Rh<sup>III</sup> chloride with  $BH_4^-$  independently does not produce species that are active catalysts in these reactions. Although nickel boride obtained by reduction of Ni<sup>II</sup> salts with BH<sub>4</sub>has been shown to act as a hydrogenation catalyst in liquid phase reactions<sup>2</sup> and in one instance<sup>3</sup> when supported on silica gel for CO reduction, there seems to be no report in the literature where substances obtained by this method

have been used unsupported, as catalysts in gas-phase reactions.

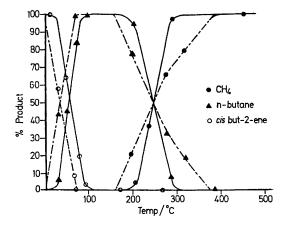


FIGURE Catalytic hydrogenation and hydrogenolysis of cisbut-2-ene (1·2 mole %) in hydrogen by,  $---(Co_2B)_{10}RhH_{6}$ (151 mg),  $----(Ni_2B)_{10}RhH_{15}$  (140 mg). Flow rate 40 cm<sup>3</sup> min<sup>-1</sup>.

We now discuss our preliminary findings on the catalytic nature of the species  $(Co_2B)_{10}RhH_6$  and  $(Ni_2B)_{10}RhH_{15}$ .

† Present address; Monsanto Research S.A., Eggbuhlstrasse 36, CH-8050 Zurich, Switzerland.

For catalytic hydrogenation and hydrogenolysis of gaseous alkenes, notably cis-but-2-ene, the catalysts were supported on a glass wool plug in an 8 mm diameter

## TABLE

Catalytic activity of (Ni<sub>2</sub>B)<sub>10</sub>RhH<sub>15</sub> for the methanation of CO Mole CO conversion

| $T/^{\circ}C$ | $CH_4$ | $C_2H_6$ | $C_2H_4$ | $C_3H_8$ | $C_4H_{10}$ | $C_6H_{14}$ |
|---------------|--------|----------|----------|----------|-------------|-------------|
| 100           | 0.01   | b        |          | b        | b           |             |
| 220           | 0.43   | 0.05     | b        | 0.03     | 0.01        | ь           |
| 300           | 6.63   | 0.14     | -        | 0.02     | b           |             |
| 350           | 27.86  | 0.20     | -        | b        | b           | -           |
| 400           | 34.39  | 0.08     | b        | b        | b           |             |
| 450           | 51.37  | b        | _        |          | -           |             |
| <b>480</b>    | 52.67  | -        | _        | -        | -           | _           |
| 490           | 59.64  | -        | -        | -        | -           | -           |

<sup>a</sup> Includes isobutane, *cis*-and *trans*-but-2-ene and but-1-ene; <sup>b</sup> <0.01%. Feed gas  $H_2$ :CO ratio of 3:1 at 66.7 cm<sup>3</sup> min<sup>-1</sup> at 1 atm. Catalyst weight 410 mg.

Pyrex glass tube and dried in a stream of H<sub>2</sub> at 100 °C for 6 h. A mixture of *cis*-but-2-ene  $(1\cdot 2 \text{ mole } \%)$  in hydrogen was admitted at a flow rate of 40 cm<sup>3</sup> min<sup>-1</sup> at 1 atm pressure. The catalyst temperature was monitored over a wide range (25—500 °C)  $\pm$  1° and the exhaust gas analysed for hydrocarbon content by flame ionisation gas chromatography using a 5 m, 1/8 in diameter Porapak Q column (80-100 mesh) at 140 °C. On no occasion did we find trans-but-2-ene or but-1-ene. At 62 °C the Ni species gave almost 50% hydrogenation to n-butane increasing to ca.

<sup>1</sup> P. C. Maybury, R. W. Mitchell, and M. F. Hawthorne, J.C.S. Chem. Comm., 1974, 534.

<sup>2</sup> R. Paul, P. Buisson, and N. Joseph, Ind. and Eng. Chem., 1952, 44, 1006; C. A. Brown and H. C. Brown, J. Amer. Chem. Soc., 1963, 82, 1005. <sup>8</sup> H. Kurita and Y. Tsutsumi, Nippon Kayku Zasshi, 1961, 82, 1461.

100% at 90 °C. At 200 °C hydrogenolysis started and was quantitative at 300 °C yielding ca. 100% methane (Figure). Both the Co and Ni catalysts showed no loss in activity with time (48 h) and at temperatures up to 500 °C. Unsupported Raney nickel under identical reaction conditions was found to behave similarly, producing ca. 100%  $CH_4$  at 400 °C but below 200 °C apart from n-butane, up to 10 mole % of isomerised trans-but-2-ene and but-1-ene was detected.

For carbon monoxide methanation, the catalysts were supported and dried as above, and carbon monoxide (25 mole %) in hydrogen was admitted at  $66.7 \text{ cm}^3 \text{ min}^{-1}$  at 1 atm pressure. The Co species was ca. 70% as active for methane formation as the Ni species at all temperatures up to 500 °C. The Table gives methanation data using the more active Ni species, showing that mole % CO to CH<sub>4</sub> conversions of up to 60% have been achieved using this catalyst. As noted above, both catalysts showed no loss in activity with time (48 h) at temperatures up to 500 °C.

The species  $(Co_2B)_{10}RhH_6$  and  $(Ni_2B)_{10}RhH_{15}$  have been shown to be effective catalysts for three very important gasphase transformations. More work is required in this field to elucidate the role that the bound hydrogen in these substances plays (if any) in such catalytic reactions involving hvdrogen.

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