## Platinum Hydrosols in the Sensitized Photoreduction of Water

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Summary Pt hydrosols (22 Å diameter) catalyse  $H_2$  evolution from water with nearly 100% efficiency in the light-induced redox reaction which involves the  $\operatorname{Ru}(2,2'$ -bipyridine)<sub>3</sub><sup>2+</sup>-methyl viologen-ethylenediaminetetra-acetate model system; the catalytic step is not rate-determining.

CATALYTIC studies on hydrosols of transition metals and their oxides have been of considerable interest recently because of their relevance to the photochemical decomposition of water. Investigations<sup>1-3</sup> of platinum hydrosols as the fourth component of a  $\operatorname{Ru}(bpy)_3^{2+}-MV^{2+}-EDTA$ (bpy = 2,2'-bipyridine;  $MV^{2+}$  = methyl viologen; EDTA = ethylenediaminetetra-acetate) hydrogen-evolving model system have been contradictory with respect to the effect of particle size on the catalytic activity and the extent of catalytic specificity.

A necessary requirement for a catalyst under fixed conditions to function at maximum effectiveness in a specific conversion process as part of a series of coupled chemical events is that the catalytic step is not rate-determining. In the Ru(bpy)<sub>3</sub><sup>2+</sup>-MV<sup>2+</sup>-EDTA model system the catalytic step is shown to be no longer rate-determining when the mean diameter of Pt colloids is reduced from 50 to 20 Å. Rate data normalized to constant light intensity (*i.e.*, quantum yields) determined from initial rates are consistent with the catalytic step being nearly 100% efficient in converting the reductive power of the electron relay, MV<sup>+</sup>, into H<sub>2</sub>.

Pt hydrosols were synthesized by reducing  $H_2PtCl_6$  with NaBH<sub>4</sub> in basic solution and then buffering to pH 5 or 6. During the preparations, 0.5% polyethyleneglycol (*M* of PEG, 15000—20000) was added. Particle sizes were measured by transmission electron microscopy. Solutions containing  $\operatorname{Ru}(\operatorname{bpy})_{3}^{2+}$ ,  $\operatorname{MV}^{2+}$ , EDTA, and Pt catalyst were irradiated with monochromatic light and the volume of gas evolved was monitored with a gas micro-volumeter.<sup>4</sup> The formation rate of MV<sup>+</sup> (Figure) was determined by monitoring the temporal growth of the 602 nm absorption band (E 11900 mol l<sup>-1</sup> cm<sup>-2</sup>).

The Pt hydrosols consisted of spherical particles with a distribution of diameters between 15 and 30 Å and an average diameter of 22 Å, corresponding to a mean aggregation number of 370 Pt atoms per particle. At a typical

25.4

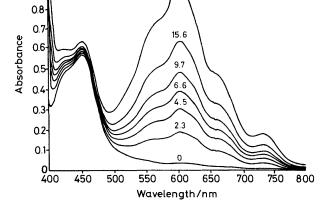


FIGURE. Absorption spectra of photolysed solution (2.0 ml) containing Ru(bpy)<sub>3</sub>Cl<sub>2</sub> (4 × 10<sup>-5</sup> M), methyl viologen (2.0 × 10<sup>-3</sup> M), Na<sub>2</sub>EDTA (0.01 M), and acetate buffer (0.05 M) at pH 5;  $\lambda$  436 ± 5 nm. Duration of photolysis given in seconds on each curve;  $I_0 = 1.27 \times 10^{-7}$  E s<sup>-1</sup>; 23.6 ± 0.1 °C.

atomic Pt concentration of  $6.4 \times 10^{-5}$  mol l<sup>-1</sup>, the colloid concentration was  $1.7 \times 10^{-7} \text{ mol } l^{-1}$  with a contact area of 1500 Å<sup>2</sup> per particle ( $1.3 \times 10^6$  cm<sup>2</sup> g<sup>-1</sup>).

The Pt particles can be considered analogous to microplatinum cathodes.<sup>5</sup> Reduction of the Pt particles by MV<sup>+</sup> results in the establishment of a rapid equilibrium between protons (or water molecules) in solution and the microplatinum electrodes, in a manner similar to those proposed for silver<sup>6</sup> and gold<sup>6,7</sup> hydrosols.

The mechanism of H<sub>2</sub> evolution in the  $Ru(bpy)_{3}^{2+}-MV^{2+}-$ EDTA model system has been well studied.<sup>8</sup> Reaction (1) describes the conversion of MV+ into hydrogen. From

$$MV^{+} + H_{2}O \xrightarrow{} MV^{2+} + \frac{1}{2}H_{2} + OH^{-}$$
(1)  
Pt catalyst

equation (1) it is evident that an upper limit of  $\phi_{\rm H_{\bullet}}$  is  $\phi_{\rm MV^+}/2$ .

As the concentration of atomic Pt is increased, the size of the hydrosol is augmented, and the catalytic activity is reduced. At  $2.6 imes 10^{-4}$  g-atoms l<sup>-1</sup>, Pt particles of 50 Å diameter form as clusters of still larger aggregates. In the case of these 50 Å hydrosols, the value of  $\phi_{\rm H_2}$  (0.0271) at pH 5 is about half that measured for the more dilute solutions (6.4  $\times$  10<sup>-5</sup> g-atoms l<sup>-1</sup>) which contain particles of 22 Å diameter. Besides the concentration effect, low pH,  $H_2$  bubbling, or *in situ* photochemical generation of  $H_2$  tend to produce larger aggregates.

The largest value of  $\phi_{\rm H_2}$ , 0.059  $\pm$  0.006, was obtained with particles of 22 Å diameter at pH 5. While this value is in

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disagreement with an earlier determination,<sup>1</sup> it is consistent with more recent estimates<sup>9</sup> of  $\phi_{H_2}$  0.05 to 0.10. In the determination of  $\phi_{\mathrm{H_2}}$ , the light intensity absorbed by the sensitizer  $\operatorname{Ru}(\operatorname{bpy})_{3}^{2+}$  was corrected for light scattering by the Pt particles.

In separate experiments involving the same system, but without the catalyst,  $\phi_{MV^+}$  was determined to be 0.108  $\pm$ 0.005. Thus, during the initial stages of H<sub>2</sub> evolution, the  $MV^+$  and  $H_2$  production rates are in a ratio (2:1) consistent with reaction (1), indicating that the catalysis is not ratedetermining under the stated experimental conditions. The rate-determining reaction occurs before catalysis and is associated with the net production of MV+. Based on initial mass balance, no evidence exists for the H<sub>2</sub>-competing hydrogenation reaction of methyl viologen reported by others.<sup>2,3</sup> As the reaction proceeds, however, the 2:1 stoicheiometric ratio of  $MV^+$  to  $H_2$  is altered. In part, this change in stoicheiometry must be associated with the accumulation of adsorbed H-atoms on the Pt surface and the competing hydrogenation reaction. Elimination of the MV<sup>+</sup> electron-relay pathway is, consequently, required to improve the long-term H<sub>2</sub> production efficiency.

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