## **Partial Oxidation of Methane by Nitrous Oxide over Molybdenum Oxide supported on Silica**

## **R.-S. biu, M. Iwamoto, and Jack H. Lunsford**

*Department of Chemistry, Texas A* & *M University, College Station, Texas 77843, U.S.A.* 

Methanol and formaldehyde were formed **as** major products at **a** moderate conversion level (I 6%) in the partial oxidation of methane by nitrous oxide in the presence **of** water over molybdenum oxide supported on silica.

The partial oxidation of methane by  $N_2O$  has been studied extensively, $\frac{1}{2}$  principally in the gas phase. Little success has been achieved in obtaining methanol or formaldehyde in substantial amounts and the main products are CO and *CO,* 

even at very low conversion levels. Recent reports<sup>2</sup> have demonstrated that  $N_2O$  is a very effective oxidant in the oxidative dehydrogenation of ethane over supported molybdenum oxides. The  $O^-$  ions, formed by surface decomposition



**Figure 1.** Yield of products as a function of the thermal desorption program following the reaction of CH<sub>4</sub> with O<sup>-</sup> at 25 °C:  $\bullet$ , CH<sub>3</sub>OH;  $\odot$ , CO<sub>2</sub>;  $\bullet$ , CH<sub>4</sub>;  $\blacktriangle$ , C<sub>2</sub>H<sub>6</sub>;  $\triangle$ , C<sub>2</sub>H<sub>4</sub>.

of  $N_2O$ , have been postulated as active species in initiating the catalytic process *via* **a** hydrogen abstraction reaction. Recently e.s.r. studies by Kazanskii and coworkers<sup>3</sup> have shown that  $O^-$  reacts with methane over various supported metal oxides. In an attempt to understand the role of  $O^-$  in the partial oxidation of methane, we investigated both the stoicheiometric reaction of CH<sub>4</sub> with O<sup>-</sup> and the catalytic oxidation of **CH4** with **N20** over molybdenum oxide supported on silica.

The stoicheiometric reaction of  $CH<sub>4</sub>$  with  $O<sup>-</sup>$  was studied in a conventional gas-circulating system with a catalyst prepared by impregnating silica gel with ammonium heptamolybdate at  $pH = 2$ . The catalyst which contained 6.6 wt. % Mo was calcined in air for 16 h at 500 °C, heated in 100 Torr of 0, for 30 min at *SO0* "C, heated *in vucuo* at *SO0 'C*  and reduced in 100 Torr of CO at 500°C for 30min. The partially reduced catalyst contained  $Mo<sup>v</sup>$  on the surface, which upon exposure to  $N_2O$  gave  $O^-$  ions according to reaction (1).

$$
N_2O + Mo^{\nu} \to Mo^{\nu}O^- + N_2 \tag{1}
$$

The  $O^-$  ions, characterized by an e.s.r. spectrum having  $g_{\parallel}$  = 2.002 and  $g_{\perp}$  = 2.019, reacted rapidly with CH<sub>4</sub> at 25 °C and more slowly at  $-196$  °C. No new radicals were detected; however, the reaction products were followed by analysing the gas phase after desorption or decomposition of the surface species, These gas phase products were collected in a cold trap after heating the catalyst for 1 h increments at progressively higher temperatures. The amount of each product, as determined by gas chromatography, is shown in Figure **1.**  Methanol was observed as the main product at desorption temperatures exceeding 300 *"C.* 

The catalytic oxidation was followed in a continuous-flow reactor which was operated **at** 1 atm. The reactor contained **3** g of 1.7 % Mo/SiO, in a *23* mm **i.d.** Vycor tube, which was connected to a 2 mm i.d. tube so that the products  $CH<sub>3</sub>OH$ and  $H_2CO$  could be quenched, thus reducing subsequent gas phase reactions. In the experiment, helium gas was used as a diluent and the flow rate was controlled at **1.33** ml/s.



**a** Conversions were calculated at steady state. **b** Trace amounts of  $C_2H_6$  and  $C_2H_4$  were observed in all cases.

Water was introduced from a syringe pump and evaporated in **a** preheater oven. Results are summarized in Table **1.**  Under the experimental conditions, silica gel was an order of magnitude less active. The combined  $60\%$  selectivity to **CH30fI** and **H2C0** at 16% conversion is considerably better than results reported in the literature.<sup>4</sup> The 6.6 wt.  $\frac{9}{6}$  Mo/SiO<sub>2</sub> catalyst gave qualitatively similar results, although selectivities for CH<sub>3</sub>OH and H<sub>2</sub>CO were less.

**As** shown in Table **1,** water **is** required to maintain the selectivities for CH<sub>3</sub>OH and H<sub>2</sub>CO. The amounts of CH<sub>3</sub>OH and H<sub>2</sub>CO increased with increasing amounts of water, and no decrease in activity has been observed in the presence of water. The role of water may be twofold. Pernicone et al.<sup>5</sup> reported that water retards the oxidation of  $CH<sub>3</sub>OH$  to  $H<sub>2</sub>CO$ by *0,* over iron molybdate catalysts. The retardation effect by the water in the partial oxidation of  $CH<sub>3</sub>OH$  by  $N<sub>2</sub>O$  over  $Mo/SiO<sub>2</sub>$  has also been observed in our laboratory;<sup>6</sup> thus, water may inhibit secondary reactions of both **CH30H** and **H,CO.** 

In addition, the stoicheiometric results demonstrate that the reaction between  $O^-$  and  $CH_4$  on  $Mo/SiO_2$  catalysts leads to the formation of **CH30H.** This may involve **CH30-** ions, and indeed alkoxide ions are formed when  $C_2-C_4$  alkanes react with O<sup>-</sup> ions on MgO.<sup>7</sup> The formation of methanol may result from the reaction of these  $CH<sub>3</sub>O<sup>-</sup>$  ions with water or surface protons. One cannot, however, exclude the possibility that at elevated temperatures hydroxyl radicals derived from water or **Si-OH** groups react with **CH3-** radicals to form  $CH<sub>3</sub>OH.$ 

This work has been supported by the National Science Foundation.

*Received, 10th September 1981; Com. 1080* 

## **References**

- 1 A. A. Borisov, V. **M.** Zanianskii, K. Potmishil, **G.** 1. Skachkov, and **V. A.** Foteenkov, *Kixet. Kurd.,* 1977, **8,** 307; J. **W.**  Falconer, D. E. Hoare, and R. Overend, *Combust. Flame*, 1973, **21,** 339; P. **L.** Robinson and E. J. Smith, *J. Cliem. Soc.,* 1952, **3895.**
- 2 T. J. Yang and J. H. Lunsford, *J. Catal.*, 1980, 63, 505; M. B. Ward, **M.** J. Lin, and J. **H.** Lunsford, *J. Cutai.,* 1977, **50,** 306.
- **3** N. **1.** kipatkina, V, **A.** Shvets, and V. B Kazanskii, *Kinct. Kcllnl.,*  1978, 19, 979; S. L. Kaliaguire, B. N. Shelimov, and V. B. Kazanskii, *J. Catal.,* 1978, *55,* 384.
- V. Ya. Shtern, 'The Gas Phase Oxidation of Hydrocarbons,' Pergamon, Oxford. 1964; B. H. **McConkey** and P. **K.** Wilkenson, *Ind. Eng. Chpm., Process Dey. Dev.,* 1967, **6,** 437; G. **A.**  Luckett and B. Miles. *Cornbust. Flume,* 1976, **26,** 299.
- *5* N. Pernicone, *J. Less-Common Met.,* 1974, **36,** 289; N. Pernicone, F. Lazzerin, G. Liberti, and G. Lanzavecchia, *J. Catal.*, 1969, **14,** 293.
- 6 T. J. Yang and J. H. Lunsford, unpublished results.
- 7 K. Aika and **J.** H. Lunsford, *J. Phys. Chem.,* 1977, **81,** 1393.