Partial Oxidation of Methane by Nitrous Oxide over Molybdenum Oxide supported on Silica

R.-S. Liu, M. Iwamoto, and Jack H. Lunsford

Department of Chemistry, Texas A & M University, College Station, Texas 77843, U.S.A.

Methanol and formaldehyde were formed as major products at a moderate conversion level (16%) in the partial oxidation of methane by nitrous oxide in the presence of water over molybdenum oxide supported on silica.

The partial oxidation of methane by N_2O has been studied extensively,¹ principally in the gas phase. Little success has been achieved in obtaining methanol or formaldehyde in substantial amounts and the main products are CO and CO₂ even at very low conversion levels. Recent reports² have demonstrated that N_2O is a very effective oxidant in the oxidative dehydrogenation of ethane over supported molyb-denum oxides. The O^- ions, formed by surface decomposition

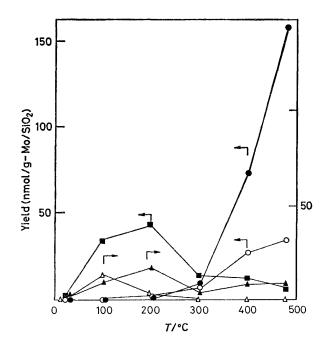


Figure 1. Yield of products as a function of the thermal desorption program following the reaction of CH₄ with O⁻ at 25 °C: \bullet , CH₃OH; \bigcirc , CO₂; \blacksquare , CH₄; \blacktriangle , C₂H₆; \triangle , C₂H₄.

of N_2O , have been postulated as active species in initiating the catalytic process *via* a hydrogen abstraction reaction. Recently e.s.r. studies by Kazanskii and coworkers³ have shown that O⁻ reacts with methane over various supported metal oxides. In an attempt to understand the role of O⁻ in the partial oxidation of methane, we investigated both the stoicheiometric reaction of CH₄ with O⁻ and the catalytic oxidation of CH₄ with N₂O over molybdenum oxide supported on silica.

The stoicheiometric reaction of CH₄ with O⁻ was studied in a conventional gas-circulating system with a catalyst prepared by impregnating silica gel with ammonium heptamolybdate at pH = 2. The catalyst which contained 6.6 wt. % Mo was calcined in air for 16 h at 500 °C, heated in 100 Torr of O₂ for 30 min at 500 °C, heated *in vacuo* at 500 °C and reduced in 100 Torr of CO at 500 °C for 30 min. The partially reduced catalyst contained Mo^v on the surface, which upon exposure to N₂O gave O⁻ ions according to reaction (1).

$$N_2O + MO^V \rightarrow MO^{VI}O^- + N_2 \tag{1}$$

The O⁻ ions, characterized by an e.s.r. spectrum having $g_{\parallel} = 2.002$ and $g_{\perp} = 2.019$, reacted rapidly with CH₄ at 25 °C and more slowly at -196 °C. No new radicals were detected; however, the reaction products were followed by analysing the gas phase after desorption or decomposition of the surface species. These gas phase products were collected in a cold trap after heating the catalyst for 1 h increments at progressively higher temperatures. The amount of each product, as determined by gas chromatography, is shown in Figure 1. Methanol was observed as the main product at desorption temperatures exceeding 300 °C.

The catalytic oxidation was followed in a continuous-flow reactor which was operated at 1 atm. The reactor contained 3 g of 1.7% Mo/SiO₂ in a 23 mm i.d. Vycor tube, which was connected to a 2 mm i.d. tube so that the products CH₃OH and H₂CO could be quenched, thus reducing subsequent gas phase reactions. In the experiment, helium gas was used as a diluent and the flow rate was controlled at 1.33 ml/s.

Table 1. Conversion and selectivity during methane oxidation.										
			-		-	~	Selectivity/% ^b			
	Mo/SiO		<i>P</i> /To			Conv.		~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~		
	wt %	CH_4	N_2O	H_2O	∕°C	/%ª	CH₃OH	H₂CO	CO	CO_2
	1.7	72	277	0	600	14.8	0.9	14.1	59.7	25.3
		72	277	93	600	16.5	13.7	18.1	51.6	16.6
		72	277	145	600	15.7	19.3	20.4	45.6	14.7
		72	277	195	600	15.6	28.0	20.1	40.2	11.7
		72	277	266	600	16.4	46.8	19.0	26.0	8.2
		72	277	266	580	12.5	55.1	23.9	15.6	5.4
		72	277	266	560	8.1	60.5	24.1	12.6	2.8
	6.6	72	277	266	560	12.7	34.2	20.4	39.6	5.8
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 a Conversions were calculated at steady state. b Trace amounts of C_2H_6 and C_2H_4 were observed in all cases.

Water was introduced from a syringe pump and evaporated in a preheater oven. Results are summarized in Table 1. Under the experimental conditions, silica gel was an order of magnitude less active. The combined 60% selectivity to CH₃OH and H₂CO at 16% conversion is considerably better than results reported in the literature.⁴ The 6.6 wt. % Mo/SiO₂ catalyst gave qualitatively similar results, although selectivities for CH₃OH and H₂CO were less.

As shown in Table 1, water is required to maintain the selectivities for CH₃OH and H₂CO. The amounts of CH₃OH and H₂CO increased with increasing amounts of water, and no decrease in activity has been observed in the presence of water. The role of water may be twofold. Pernicone *et al.*⁵ reported that water retards the oxidation of CH₃OH to H₂CO by O₂ over iron molybdate catalysts. The retardation effect by the water in the partial oxidation of CH₃OH by N₂O over Mo/SiO₂ has also been observed in our laboratory;⁶ thus, water may inhibit secondary reactions of both CH₃OH and H₂CO.

In addition, the stoicheiometric results demonstrate that the reaction between O⁻ and CH₄ on Mo/SiO₂ catalysts leads to the formation of CH₃OH. This may involve CH₃O⁻ ions, and indeed alkoxide ions are formed when C₂—C₄ alkanes react with O⁻ ions on MgO.⁷ The formation of methanol may result from the reaction of these CH₃O⁻ ions with water or surface protons. One cannot, however, exclude the possibility that at elevated temperatures hydroxyl radicals derived from water or Si-OH groups react with CH₃• radicals to form CH₃OH.

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