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The formation rate of MeCHO and current for the C_2H_4 | Pd $| H_3PO_4 |$ graphite $| O_2 + NO (NO_2)$ cell are ten times higher **than those for the C₂H₄ | Pd | H₃PO₄ | Pt | O₂ cell.**

The selective synthesis of MeCHO has been demonstrated by a C₂H₄–O₂ cell system that was assembled as $[C_2H_4, H_2O(g)]$ Pd-black/graphite/PTFE anode $|$ aq. H₃PO₄ in silica wool $|$ Ptblack/graphite/PTFE cathode $| O_2 |$.¹ Oxidation of C₂H₄ to MeCHO at the anode [eqn. (1)] and reduction of O_2 to H_2O at the cathode [eqn. (2)] proceeded respectively.

$$
C_2H_4 + H_2O \to MeCHO + 2 H^+ + 2e^-
$$
 (1)

$$
1/2 O_2 + 2 H^+ + 2 e^- \rightarrow H_2O
$$
 (2)

The cell system has several advantages compared with the current Wacker process using a mixture of C_2H_4 and O_2 catalysed by $PdCl_2$ and $CuCl_2$ in HCl solution.² For example, (i) the cell system is chloride free, and (ii) no separation processes for products and catalysts are required. Recent attractive heterogeneous catalytic systems have the same advantages.^{3,4} The cell system has additional advantages, (iii) the reaction rate and the current are easily controlled by variable resistance, and (iv) the danger of explosion is reduced because C_2H_4 and O_2 are separated by the membrane.^{1,5–7} However, the rate of MeCHO formation attained in this $C_2H_4-O_2$ cell system (1 ~ 2 TON per Pd atom in 1 h)¹ has to be improved dramatically. The TON obtained in the current Wacker process is greater than 10.2 Therefore, the purpose of this work is to demonstrate the enhancement of the formation rate of MeCHO by one order of magnitude for the $C_2H_4-O_2$ cell system.

First, the potentials at the anode and the cathode for the $C_2H_4-O_2$ cell were measured at 353 K. The details of electrochemical measurement have been described elsewhere.8 The potentials at the anode and the cathode were +0.26 V (*vs.* Ag $|$ AgCl) and $+0.86$ V respectively under open circuit conditions: the electromotive force (EMF) was 0.60 V. The potentials were changed to +0.65 and +0.67 V under short circuit conditions. The difference in the anode and the cathode potentials under short circuit conditions is due to an Ohm resistance. Thus, the over-potential at the anode was larger than that at the cathode. However, it should be noted that a considerable over-potential existed at the cathode, 32% of the EMF, for the electrochemical reduction of $O₂$.

If the over-potential at the cathode could be decreased by some means, an additional electrochemical potential could be applied at the anode which should increase the formation rate of MeCHO and the current. On the basis of this concept, many trials were performed for improving the rate of MeCHO formation. In conclusion, it is found that the addition of nitric oxide in a stream of O_2 dramatically enhances the current and the formation rate of MeCHO.

Fig. 1 shows a time profile for the formations of MeCHO and $CO₂$ [Fig. 1(*a*)] and for the current [Fig. 1(*b*)] with and without addition of NO into an $O₂$ stream. The apparent surface areas of the electrodes were 2 cm2. The content of Pd in the anode was 120 umol. When the circuit was shorted, a current of 3 mA cm^{-2} flowed and MeCHO was selectively produced ($>97\%$). When NO was added to the stream of O_2 , a drastic increase in the current (35 mA cm^{-2}) and the formation rate of MeCHO were observed. When the NO addition was stopped, the current and the formation rate of MeCHO immediately decreased. Then, the current and the formation rate of MeCHO increased again with the addition of NO. It is clear that the addition of NO to the O_2 stream reversibly accelerates both the current and the formation rate of MeCHO. Although the formation rate of $CO₂$ was also increased by the addition of NO, the selectivity to MeCHO was still quite high $(> 95\%)$.

The cathode and anode potentials for the $C_2H_4-(O_2+NO)$ cell system were measured. The cathode potential under open circuit conditions is 1.0 V, which was considerably higher than the value (0.86 V) for the $C_2H_4-O_2$ cell. A separate experiment showed that the cathode potential for the \dot{C}_2H_4 –NO cell was 0.85 V. When NO was added to the $O₂$ stream in the cathode compartment, formation of a dark brown gas was observed, indicating the formation of $NO₂$ [eqn. (3)]. The increase in the cathode potential by the addition of NO and O_2 must be due to the formation of NO_2 , which could be a stronger oxidant than O_2 or NO.

$$
NO + 1/2 O_2 \rightarrow NO_2 \tag{3}
$$

The anode potential under open circuit conditions is 0.26 V. The EMF for the $C_2H_4-(O_2+N\tilde{O})$ cell is 0.74 V, which is larger than the value (0.60 V) for the $C_2H_4-O_2$ cell. When the circuit was shorted, the potentials of the anode and the cathode were changing to 0.88 and 0.93 V, respectively. The over-potentials at the anode and cathode were 0.62 and 0.07 V. The overpotential of 0.07 V at the cathode was smaller than that of 0.19 V for the $C_2H_4-O_2$ cell, although the current was one order of

Fig. 1 Effects of NO addition into the O_2 stream at the cathode on the formation of MeCHO with the C₂H₄–O₂ cell: (\bullet) MeCHO and (\triangle) CO₂. C_2H_4 (39 kPa), H_2O (13 kPa), anode | aq. H_3PO_4 in silica wool | cathode, O2 (51 kPa), He (50 kPa) or NO (50 kPa). *T* = 353 K. Anode: Pd-black/CF/ PTFE, total flow rate = 32 ml min⁻¹. Cathode: Pt-black/graphite/PTFE, total flow rate = 32 ml min⁻¹.

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Fig. 2 Effects of some oxidants of the C_2H_4 –oxidant cell with graphite/ PTFE cathode on the Wacker oxidation. C_2H_4 (39 kPa), H_2O (13 kPa), anode $|$ aq. H₃PO₄ in silica wool $|$ cathode, oxidants. Oxidants: NO₂ (5 kPa), NO (20 kPa), O_2 (50 kPa), NO (50 kPa) + O_2 (51 kPa), and NO (6 kPa) + O_2 (51 kPa). $T = 353$ K.

magnitude larger than that for the $C_2H_4-O_2$ cell. This fact suggests that the electrochemical reduction of $NO₂$ is very easy compared with that of O_2 .

The cathode used so far in this work was Pt-black/graphite/ PTFE. If the reduction of $NO₂$ occurs quite easily, we may exclude Pt-black from the cathode. In fact, a cathode without Ptblack (graphite/PTFE cathode) showed very good electrocatalytic performance; a high current of 40 mA $cm⁻²$ and selective MeCHO formation (3% yield and 8 TON in 1 h). The optimum reaction conditions were studied for the C_2H_4 – (\hat{O}_2+NO) cell using the graphite/PTFE cathode. Then, a maximum yield of 15% and 31 TON in 1 h were obtained, which is fairly good productivity for MeCHO formation.

The results for the oxidation of C_2H_4 using different oxidants are compared in Fig. 2. The cathode in these experiments was graphite/PTFE. A current of 18.5 mA cm⁻² flowed and MeCHO was selectively produced with the $C_2H_4-NO_2$ cell, although the pressure of \overline{NO}_2 was only 5 kPa. A mixture of O_2

and NO was an excellent oxidant but $O₂$ or NO alone were not effective oxidant at the graphite cathode. When P_{NO} was reduced from 50 to 6 kPa for the $C_2H_4-(O_2+NO)$ cell, the formation rate of MeCHO and the current were slightly decreased. The influences of P_{NO} on the formation rate and the current were small. When $NO₂$ (5 kPa) was introduced into the anode compartment, catalytic oxidation of C_2H_4 to CO_2 (1.2) μ mol min⁻¹ cm⁻²) and MeCHO (0.4 μ mol min⁻¹ cm⁻²) proceeded under open circuit conditions. The selective synthesis of MeCHO from C_2H_4 with NO_2 catalysed by the Pd anode does not proceeed. No enhancing effects due to the addition of NO2 into the anode compartment on the formation of MeCHO and the current were observed under short circuit conditions. These facts confirm that NO_2 produced from a mixture of O_2 and NO works as a strong oxidant at the cathode.

The products for the reduction of $NO₂$ and NO at the cathode were trace formation of N_2 and N_2O in the gas phase and a small amount of $NH₂OH$ or $NH₃$ (< 4% current efficiency) in the diaphragm. There are no other products containing nitrogen. These observations suggest that $NO₂$ is being reduced to $NO₂$ and H_2O [eqn. (4)].

$$
NO2 + 2 H+ + 2 e- \rightarrow NO + H2O
$$
 (4)

The NO produced here would regenerate $NO₂$ according to [eqn. (3)]. Thus, NO works as a mediator (or catalyst) for the electrochemical reduction of O₂.

Notes and References

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