Reactivity of Surface Intermediates Derived from Al_2O_3 **-Supported** $Ru_3(CO)_{12}$ **in the CO** $+$ H₂ Reaction

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The effect of subcarbonyl surface intermediates resulting from $Ru_3(CO)_{12}$ molecular clusters supported on Al_2O_3 in the CO hydrogenation has been investigated by using an isotope-labeling technique. It has been establ are stabilized in the form of dicarbonyl species, characterized by 2072- and 2001-cm⁻¹ IR frequencies, when temperature-programmed decomposition (TPDE) is carried out in the temperature range between 473 and 573 K. Despite the presence of $Ru^{II}(CO)_2$, free ruthenium sites are responsible for the catalytic activity in the ¹³CO hydrogenation reaction. The high mobility of the CO ligands in the surface ruthenium dicarbonyl species, demonstrated by CO molecular exchange during the reaction, makes the CO from the dicarbonyl species compete successfully with that chemisorbed from the gas phase labeled in the form of '3C0. An explanation for the stability of the highly dispersed ruthenium particles and detailed mechanisms of the surface reactions are given.

1. Introduction

Metal dispersion of the $Ru/Al₂O₃$ catalysts derived from the $Ru_{3}(CO)_{12}$ carbonyl cluster proved to be higher than for those prepared by an incipient wetness method.¹⁻³ Further studies demonstrated that thermal decomposition plays an important role in the formation of active sites; e.g. decomposition in helium yields species of higher activity than decomposition in hydrogen. $4-6$ Generally, when decomposition is performed up to 570 K, a catalyst is produced that is more active than that heated to 770 $K⁷$ This higher activity might be attributed to the presence of dicarbonyl species, as was demonstrated by IR techniques.⁸ This assumption is also supported by other studies. Earlier it was established that Os(II)-dicarbonyl species derived from osmium clusters are the active sites in the $CO + H₂$ reaction.⁹ It was also found that, during decomposition in a mild, nonreductive atmosphere, the cluster framework breaks up and triosmium ensembles are formed whereas under a hydrogen atmosphere, at higher temperature, osmium aggregates are the prevailing species on the support.¹⁰ The triosmium ensembles proved to be stable under the CO hydrogenation conditions, most likely due to the presence of CO ligands.¹¹ For the formation of methane and oxygenates metal aggregates and a mononuclear osmium complex, respectively, were suggested as active sites.

The inactivity of the triruthenium species was also demonstrated in the $Ru_3(CO)_{12}/Cab-O-Sil$ system with use of IR techniques.⁶ However, on an alumina support monoruthenium dicarbonyl species were already apparent after impregnation, and this was ascribed to a more extensive interaction between the cluster framework and the alumina support.¹²⁻¹⁶

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Table I. Quantitative Evaluation of the TPDE Experiments for $Ru_3(CO)_{12}/Al_2O_3$ Samples

		amt of CO, μ mol (g of catalyst) ⁻¹				
		decomposed				
	TPDE.		T < 473 < T < T			
solvent	K.		initial 473 K 573 K 573 K		total	
pentane 770 792		295	198		195 688 ^a (87%)	

Correction is made for the hydrocarbon moieties evolved with CO and determined by FID.

Dicarbonyl species on the catalyst prepared from $Ru_3(CO)_{12}$ supported on alumina and characterized by bands at 2040 and 1960 cm⁻¹ were also observed by Kellner and Bell.¹⁷ However, these bands were shown to be quite stable and the prevailing band of CO during the reaction at higher pressure was observed at 2010 cm-I; this was assigned to a monocarbonyl species. The conclusion from these experiments was that monocarbonyl species chemisorbed on ruthenium metallic sites are the active intermediates during CO hydrogenation.

It is well-known that in CO hydrogenation to form hydrocarbons over metal surfaces CO is dissociated on metallic sites.¹⁸ On these sites the dissociation is preceded by CO chemisorption that is believed to be in linear form as indicated by Kellner and Bell.¹⁷ However, the question to be answered is why the metallic sites become more active when dicarbonyl species are present on the surface.

The main goal of the present work is to investigate the formation and the reactivity of the Ru metallic sites and the $Ru(CO)₂$ species formed during the decomposition of $Ru_3(CO)_{12}$. In order to distinguish between the CO species remaining on the surface and those chemisorbed from the gas phase, a 13 C-labeling technique was used along with CO chemisorption to determine the free metallic surface and infrared spectroscopy to study the transformation of the surface dicarbonyl species.

2. Experimental Section

2.1. Materials. $Ru_3(CO)_{12}$ to an extent of 2 wt % metal was deposited on an alumina (Degussa ALON C) surface from pentane solution as described earlier.¹⁹ Prior to impregnation Al_2O_3 was partially dehydroxylated. All gases were carefully purified by using a manganese deoxo unit and a 13X molecular sieve trap. The isotopically labeled CO gas was enriched with ¹³C to a level of 98%.

2.2. Apparatus and Procedure. Temperature-programmed decomposition (TPDE) of the supported cluster was carried out under helium, and

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Figure 1. (a) Temperature-programmed decomposition (TPDE) for $Ru_3(CO)_{12}$ and (b) TPDE-MS analysis for CO and CO₂: (0) CO; $\left(\bullet\right)$ CO2.

the gases evolved were monitored simultaneously by FID and TC detectors. In some cases the effluent gas after the TC detector was analyzed by mass spectrometry at m/e 15, 28, and 44, for CH₄, CO, and CO₂, respectively.

CO chemisorption was measured at room temperature in a pulse system. Separate samples were heated to the required temperature under He and then cooled down to room temperature, and CO chemisorption
was started.
A Fourier transform infrared spectrometer (DIGILAB FTS-20C) was

used ex situ to measure the type and quantity of the CO left on the surface after the different procedures. The catalytic activity of the samples was measured in a tubular flow reactor using a 3:1 H_2/CO mixture with a flow rate of 15 mL min⁻¹. The ¹³C-labeling experiments were performed in an all-glass circulating reactor using a 5:1 $H₂/CO$ mixture. The reactant and the products were analyzed by means of a Packard Type 427 gas chromatograph equipped with a Porapak Q col-
umn. After separation the quantity was determined by FID (CO and
CO₂ were first converted into methane). The isotope content was measured by mass spectrometry with a Du Pont 21-490/B single-focusing instrument interfaced to the gas chromatograph.

3. Results

3.1. Determination of the Surface Species. Before any catalytic reaction, the amount and the structure of the subcarbonyl species must be clarified. The TPDE pattern of $Ru_3(CO)_{12}$ on alumina under He presented in Figure **1** is very similar to that obtained earlier.2 In the lower part of Figure **1** the gas analysis indicates that between **473** and **573 K** there is a minimum in CO evolution. The main peak in this region represents hydrocarbons, mainly methane, which partly results from the pentane remaining on the alumina after impregnation.

From the TPDE results the number of CO ligands retained on the subcarbonyl species in the temperature range mentioned can be estimated as shown in Table I.

The structure of the CO ligands present in the subcarbonyl species in the temperature range between **473** and **573 K** was studied by IR techniques. In Figure **2** the spectra of the impregnated cluster (Figure **2a)** as well as of material decomposed at different temperatures (Figure **2b-f)** are presented. The spectrum of the impregnated sample was taken immediately after the solvent removal. Some bands characteristic of the original cluster (at **2062** and **2032** cm-') were still present, but bands that could be assigned to $Ru^{II}(CO)_2$ species formed from the decomposed cluster were already visible **(2072** sh, **2001 s** cm-1).2J3 In the range between **473** and **573** K, the intensities of these two prevailing bands decreased and disappeared above about **573 K.** Simultaneously, with increasing temperature a single band developed at **1872** cm-' but also disappeared above **573 K.**

During thermal decomposition when partial removal of CO ligands and reconstruction of the metal framework occur, free ruthenium sites are also created. The amount of these surface sites can be estimated by room-temperature CO chemisorption. Chemisorption starts when TPDE is carried out up to a little below **473** K as indicated in Figure **3.** The CO uptake on the sample,

Figure 2. IR spectra for $Ru_3(CO)_{12}/Al_2O_3$ during TPDE under He: (a) after impregnation; (b) at 473 K for 30 min; (c) at 493 K for 30 min; (d) at 523 K for 30 min; (e) at 573 K for 30 min; **(f)** at 773 K for 30 min.

Figure 3. CO chemisorption at room temperature after TPDE up to the temperature indicated at the abscissa: *(0)* decomposition under He for 15 min; (\blacksquare) decomposition under H_2 for 1 h.

decomposed up to the indicated temperature and held isothermally for **15** min, linearly increases with the TPDE temperature. An enhancement in the amount of the CO chemisorbed could be observed when the hold-on time was increased or the temperature and the atmosphere of TPDE (He to $H₂$) were changed.

The mode of CO chemisorption after full decomposition of $Ru₃(CO)₁₂$ was measured by the IR technique and is presented in Figure **4.** The room-temperature readsorption of CO shows a three-band structure **(2141,2075,** and **2017** cm-I) in agreement with that determined in the $Ru_3(CO)_{12}/Cab-O-Sil$ system⁶ but not with that obtained over a well-reduced $Ru/Al₂O₃$ sample.^{20,21}

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Figure 4. IR spectra of the CO chemisorbed at room temperature: (a) after decomposition in vacuo at 723 K; (b) after hydrogenation at 673 K ; (c) after CO chemisorption at room temperature; (d) with heating up to 473 K after chemisorption; (e) with heating up to 573 K after chemisorption.

In the present system these bands can be assigned to a combination of $Ru^{III}(CO)_2$ (2138 and 2070 cm⁻¹) and $Ru^{II}(CO)_2$ (2070 and 2005 cm⁻¹),¹³ for which the chemisorption bond strength on Ru (111) species is considerably weaker; thus, this band pair disappears after heating the sample to 473 **K.**

3.2. Reactivity of RU(CO)~ Species and Metallic Ru Sites. As previously indicated, in the temperature range between 473 and 573 **K** both metallic sites and ruthenium dicarbonyl species are present. In order to distinguish between the reaction pathways utilizing free ruthenium sites and $Ru(CO)₂$, the catalytic reaction was carried out with a 5:1 $H_2/^{13}CO$ mixture.

First it was established that the rate of methanation on a sample, which had been heated to 473 K, was well below 1×10^{-9} mol **s-l** (g of catalyst)-' at this temperature. The only reaction that could be measured under this condition was molecular isotope exchange between CO ligands in $Ru(CO)_2$ and ¹³CO in the gas phase. It is shown in Figure *5.* The exchange process can be decomposed into a fast initial part followed by a much slower exchange. The kinetic curve shown in Figure *5* can be approximated by a sum of two exponential rate equations,²² and the calculated initial rates designated by k_1 and k_2 are presented in Table 11. One of the exchange reactions is independent of tem-

species at 473 K vs time: **TPDE** up to 473 K.

Figure 6. IR spectra of the ¹³C-substituted dicarbonyl species: (a) at 473 K; (b) at 493 K; (c) at 523 K, (d) at 573 K.

perature whereas the other is strongly temperature-dependent.

Repeated exchange between gaseous **I3CO** and surface I2C0 species results in a change of the two-band IR spectra of the $Ru^{II}(CO)₂$ species. As shown in Figure 6, isotope substitution yields another band pair at 2025 and 1958 cm^{-1} , which can be assigned to the exchanged $Ru^{11}(CO)_2$ species.

However, the band that appears at 1878 cm^{-1} at higher temperature is not affected by isotope substitution. In Figure.6 the frequency range between 1200 and 1600 cm^{-1} is also presented. The bands here could be assigned to surface carboxylate and hydroxy-carboxylate species, $2^{3,24}$ which can most likely be ascribed to a reaction between the *C02* formed from CO ligands and the alumina support.

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Figure 7. ¹²C labeling in CO (\bullet) and in CH₄ (X) during the reaction of $^{13}CO + H_2$ at 493 K. The TPDE temperature was 493 K (\blacksquare stands **for** the sample obtained after extended evacuation).

Table III. ¹³CO + H_2 Reaction^a

TPDE, K	R_{CH_4} , mol s ⁻¹ $(g \text{ of catalyst})^{-1}$	isotope composition of CH ₄
493 553	5.1×10^{-8} (1st) 8.1×10^{-8} (2nd) 9.0×10^{-8} (3rd) 9.9×10^{-8} (1st) 1.1×10^{-7} (2nd) 1.1×10^{-7} (3rd)	$^{12}CH_4 + ^{13}CH_4$ ${}^{13}C_4$ ${}^{13}CH_4$ $^{13}CH4$ $^{13}CH4$ ${}^{13}CH_4$

 $T_{\text{reacn}} = 493 \text{ K}.$

When decomposition of $Ru_3(CO)_{12}/Al_2O_3$ is performed up to 493 K, the reaction at 493 K with a $H_2 + {}^{13}CO$ mixture takes place to form methane. The isotope fraction of methane and CO vs time is presented in Figure 7. As well as CO exchange, methane is formed initially in nonlabeled form and as the reaction proceeds more and more ¹³CO appears as methane. If more ¹²CO ligands are removed from the Ru subcarbonyl species before the reaction is started, e.g. by extended evacuation, more 13C0 appears in the methane (see Figure 7b).

When the reaction is repeated on the same sample, no ^{12}C labeled methane appears in the gas phase, but this product is fully labeled. This implies that during the first reaction the $Ru(CO)_{2}$ species lost part of the CO ligands. Here it is important to note that under excess of hydrogen as is in the $H_2 + {}^{13}CO$ mixture, at atmospheric pressure, CO ligands can be partly removed. Consequently, after the first reaction more metallic sites are generated and the methanation rate somewhat increases in the subsequent reaction as shown in Table 111.

When decomposition occurs at 573 **K** with most of the CO ligands already removed during decomposition, after the first reaction only ${}^{13}CH_4$ is formed as indicated in the lower part of Table 111. This obviously provides evidence of the participation of CO ligands in the methanation.

On the basis of isotope studies one might assume that CO hydrogenation **takes** place via dicarbonyl species. This is, however, contradicted by the inactivity of the $Ru/Al₂O₃$ sample, which is almost covered by $Ru(CO)_2$ species. The lack of catalytic activity suggests that the reaction is associated with metallic sites. Indeed, if the TPDE temperature is increased and standard conditions are used (flow mode, 5:1 H₂/CO mixture and 493 K temperature), the rate of methanation increases in parallel with the number of Ru metallic sites as determined by *CO* chemisorption as shown in Figure 8. This implies that the methanation is related to the free ruthenium sites.

The question now arising is why metallic ruthenium particles are more active in the presence of dicarbonyl species. The gradual appearance of the band at 1872 cm^{-1} (Figure 6) assigned to bridged-type carbonyl species bound to two ruthenium atoms might be an answer to the question. Here, due to the weakened C-0 bond, dissociation of CO to form reactive carbon may proceed more easily.

Figure 8. Methanation rate (a) vs the decomposition temperature in TPDE and (b) **vs** the amount of the CO chemisorbed at room temperature.

However, this is not supported by the $13CO$ experiments since bridged CO did not participdte in molecular isotope exchange. A similar phenomenon was observed by Zanderighi et al.²⁵ using fully labeled CO in synthesizing $Ru_3(^{13}CO)_{12}$. An extended study of the appearance of this band affected by various parameters showed that it is independent of the pretreatment of the alumina, the solvent used in impregnation, and the presence of air, water vapor, or oxygen at temperatures below 473 K. However, the band is always present if treatment is carried out at temperatures above 473 **K** and a trace quantity of oxygen is present in the helium. A set of experiments is shown in Figure 9. After decomposition of $Ru_3(CO)_{12}$ in unpurified He no dicarbonyl species are left (Figure 9a) but that associated with the band at 1872 cm^{-1} . When the same experiments are carried out in purified He, the opposite effect is observed (Figure 9b). When a switch is made to unpurified He, the original spectrum returns (Figure 9c). Admission of ¹³CO at 553 K (Figure 9d) results in the formations of ¹³CO dicarbonyl species, but no exchange occurs in the bridged species as indicated by the constancy of the band position at 1872 cm-I. Obviously this band is not associated with any carbonyl species on the surface. The suggestion of transformation of $Ru(CO)_{2}$ into bridged CO with higher reactivity by use of free metallic sites can, therefore, be eliminated.

The second obvious suggestion would be a change in the mode of CO chemisorption during the reaction, e.g. from $Ru(CO)₂$ species into monoruthenium monocarbonyl species. In Figure 10 the CO stretching region under various conditions is shown. **As** demonstrated in Figure 10, during the reaction dicarbonyl species are maintained on the surface. The only obvious change is that $Ru^{II}(CO)₂$ is transformed into a more reduced form of dicarbonyl species, $Ru^{0}(CO)_{2}$, indicated by a band pair at 2050 and 1975 cm^{-1} (see Figure 10a-d). After evacuation and room-temperature

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Figure 9. IR spectra of $Ru_3(CO)_{12}/Al_2O_3$: (a) after decomposition up to 573 K under He for 30 min; (b) after decomposition under purified He at 573 K for 30 min; (c) after treatment of the sample in (b) under He at 573 K for 30 min; (d) after recarbonylation of the sample in (c) with ¹³CO at 553 K.

CO readmission a band structure similar to that observed without reaction (compare Figure 4 and Figure 10e^{-h}) is visible. However, when $Ru_3(CO)_{12}/Al_2O_3$ is reduced first in hydrogen at 635 K for *5* h after CO adsorption, a single CO band pattern is present (Figure 1Oi-k), similar to what was found by Kellner and Bell."

4. Discussion

We did not aim to carry out a full structural analysis on the interaction between $Ru_3(CO)_{12}$ and Al_2O_3 in the present investigations because it has been done for this system^{12,13,16,26,27} and also for mixed-metal clusters containing ruthenium. $6,14,15,20$ Here merely the conditions under which free ruthenium metal particles and ruthenium subcarbonyl species coexist were determined. Nevertheless, the structure of the subcarbonyl species and the valence state of ruthenium in the $Ru(CO)_2$ entities as determined by IR spectroscopy are still relevant to the present study.

As far as the nature of the active sites of the cluster-derived $Ru/Al₂O₃$ catalyst is concerned, three general conclusions can be drawn from the present investigations. First, metallic sites or free ruthenium atoms are prerequisite for the methanation reaction. Second, the bridged type of chemisorbed CO is not formed on the surface; therefore, it cannot be regarded as an intermediate during the $CO + H_2$ reaction. Finally, the difference in the ¹³C content between CO and CH4 species excludes the identity of the

Figure 10. IR spectra of CO in $Ru_3(CO)_{12}/Al_2O_3$: (a) decomposition up to 523 K under vacuum for 30 min; (b) during $CO + H₂$ reaction of (a) at 493 K after 15 min; (c) (b) under vacuum at 493 K; (d) treatment of (c) between 623 and 723 K under vacuum for 20 min; (e) CO adsorption on (d) at 323 K; **(f)** evacuation of (e); (g) heating of **(f)** up to 473 K under vacuum; (h) heating of **(f)** up to 573 K under vacuum; (i) CO adsorption on (f) at 323 K after treatment at 623 K under H_2 for 5 h; (j) evacuation of (i); (k) heating of (j) up to 573 K.

surface species for the CO ligand exchange and the methanation reaction. This last statement, however, needs some further explanation. When the reaction of $H_2 + {}^{13}CO$ is performed on a surface containing both $Ru(CO)_2$ species and free ruthenium particles, three possibilities exist:

(i) Only Ru metal sites participate in the reaction. In this case the methane formed initially will be completely labeled.

(ii) Methanation proceeds via $Ru(CO)_2$ species. Here, initially ${}^{12}CH_4$ and then ${}^{13}CH_4$ will be produced.

(iii) Fast exchange occurs between ${}^{13}CO$ gas and ${}^{12}CO$ ligands; the reactant and the resulting product will have a constant fraction of labeled molecules.

Although ruthenium sites are required for methanation, the experimental results still clearly indicate that CO ligands in $Ru(CO)$ ₂ also participate in the methanation as will be discussed later. Concerning point ii, the isotope content of CO after a short initial period levels off while that of $CH₄$ during the reaction continuously decreases and is not identical with the 13 C content of CO; it is, therefore, very likely that for molecular exchange and for methanation different sites are needed. Further evidence for this statement is provided by the methanation rate being proportional to the metallic sites measured by the CO molecules chemisorbed on the samples (see Figure 8).

The following questions must also be addressed:

(i) Why is the metallic dispersion measured by CO chemi-

sorption so low compared to that obtained by other measurements? (ii) How can the difference revealed in the activity between the samples decomposed at low and high temperature be explained?

(iii) What is the explanation for the involvement of surface dicarbonyl species in the methanation reaction?

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It is well-known²⁸⁻³¹ that ruthenium on alumina always forms an oxidic interface and its reduction is rather difficult. Even if the starting material is zerovalent ruthenium as in the case of $Ru_{3}(CO)_{12}$, after partial decomposition a part of the ruthenium becomes oxidized due to the reaction with surface OH^- and O^{2-} species. This is well demonstrated in the spectra of the chemisorbed CO molecule. As Figure **4** shows, a typical three-band spectrum is obtained similar to that observed on recarbonylation of the Cab-0-Sil-supported ruthenium clusters decomposed under hydrogen.⁶ This is due to the formation of $Ru^{\text{III}}(CO)_2$ and $Ru^{II}(CO)₂ species, ^{12–14} which is a result of the partial oxidation$ of the decomposed ruthenium framework under the effect of surface hydroxyl groups. On the other hand, if the decomposition of the Al₂O₃-supported Ru₃(CO)₁₂ cluster occurs under hydrogen at **770** K, larger metal particles are formed and the character of the CO chemisorbed is completely different from that presented in Figure **4.** In this case the characteristic bands are as follows:2o $Ru^{III}(CO)_2$, 2138 and 2070 cm⁻¹; $Ru^{II}(CO)_2$, 2072 and 2001 cm⁻¹ CO on Ru(O), **2050** cm-I.

When the sample temperature is increased after CO chemisorption, decarbonylation of $Ru^{III}(CO)_2$, that is the most weakly bonded dicarbonyl species, occurs similarly to what was observed by Guglielminotti et al.¹² and the appropriate bands appear at 2075 and 2009 cm⁻¹ due to Ru^{II}(CO)₂. These are the same surface species as shown in Figure **2.** Even high-temperature readmission of 13C0 results in this two-band spectrum, indicating the rather high stability of the decarbonylated ruthenium species (see Figure 9d).

Since the surface contains oxidized ruthenium atoms to a large extent, determination of the metallic sites is difficult when no single CO peak at about 2050 cm⁻¹ is present.

However, under the reaction conditions nearly all surface ruthenium species with various oxidation states are converted into highly dispersed $Ru(0)$ species indicated by the appearance of $Ru^{0}(CO)_{2}$ with a band pair at 2050 and 1980 cm⁻¹ (see Figure 10b,c). After reaction and evacuation, the ruthenium species is partly oxidized again, so CO chemisorption results in the appearance of the bands characteristic of $Ru^{III}(CO)$, and $Ru^{II}(CO)$, (see Figure 10e,f). Consequently, determination of metallic dispersion in the presence of dicarbonyl species may not lead to an unambiguous result. Good estimation can only be obtained when CO chemisorption is characterized by a single CO band in the IR spectrum. It does not necessarily mean, however, that proportionality does not exist between the catalytic activity and the number of the CO molecules chemisorbed, but this cannot be utilized in the quantification of the turnover frequency (TOF).

As an explanation for the activity difference between the samples prepared by heating to **573** and **773** K, the most obvious suggestion would be the difference in the modes of CO chemisorption during the reaction. Kellner and Bell¹⁷ already showed that two types of CO exist during the reaction: single-bonded and dicarbonyl species. However, this experiment cannot be related to the present work because, first, the IR spectra were taken under high pressure and, second, Kellner first completely decomposed $Ru_3(CO)_{12}$ and then the reaction was started. In those experiments linearly bound CO was considered to be the reaction intermediate.

In contrast to the experiments of Kellner and Bell,¹⁷ here practically no change was observed in the mode of CO chemisorption during the catalytic reaction except the change in ruthenium valence state. Although some decline in dispersion was experienced, the basic characteristics of the single ruthenium atoms were retained and the morphology of the metallic part was unchanged.

After long treatment at **623** K, which may mimic the decom-

Scheme I

1. $T \le 473$ K; $R_{CH_4}(473$ K) $\le 10^{-9}$ mol s⁻¹ (g of catalyst)⁻¹ (exchange only)

$$
OC \xrightarrow{\text{ROO}} CO + {}^{13}\text{CO(g)} = \xrightarrow{\text{OC}} {}^{13}\text{CO} + {}^{12}\text{CO(g)}
$$

2. $473 K < T < 573 K$; $R_{CH_4} \approx 10^{-7}$ mol s⁻¹ (g of catalyst)⁻¹ **(A** faster than **8)**

position at **770** K, a change in the surface morphology can be observed characterized by CO chemisorption via the appearance of a dominating single CO band at **2050** cm-I. It must be underlined that this morphology change could lead to an alteration in the catalytic activity.

The simplest interpretation of the activity differences between the Ru/Al₂O₃ samples prepared by decomposition of $Ru_3(CO)_{12}$ at **573** and **773** K is the various dispersions indicated by the mode of CO chemisorption. It is well known that the TOF for methanation over $Ru/Al₂O₃$ catalysts increases with decreasing dispersion. $17,31,32$ If we assume that the total number of ruthenium atoms are constant $(N_t = constant)$, the total rate can be expressed as $R_{\text{CH}_4} = N_t CD(1 - D)$, where R_{CH_4} is the rate of methanation per gram of catalyst, C is a constant, and **D** is the dispersion defined by N_s/N_t . As the temperature used for the decomposition is increased, *D* will decrease and hence *R* should pass a maximum. This explains the activity decrease in the overall rate at lower dispersion.

Here the role of $Ru(CO)_2$ obviously is that metallic dispersion can be stabilized by this species whereas free ruthenium metal atoms formed at high temperature tend to be easily sintered. As is indicated by the easy change in the ruthenium valence state in the $Ru(CO)$ ₂ species, after partial removal of the CO ligands under the reaction conditions the metallic ruthenium remains in a well-dispersed state since the reaction temperature is not high (see Figure **9).**

We still need to explain why ${}^{12}CH_4$ is produced initially from a H₂ + ¹³CO mixture during the catalytic methanation over a sample containing $Ru(CO)_2$ species. As was shown by the high rate of exchange, CO ligands in $Ru(CO)_2$ are already in a preactivated state. Thus, since there are free ruthenium sites on alumina, the CO molecules in CO ligands on the surface, being in a precursor state, might compete successfully for the neighboring Ru sites with the CO molecule arriving from the gas phase. This may be the most plausible explanation why ${}^{12}CH_4$ is the primary product followed by formation of ${}^{13}CH_4$. The lack of activity of a surface fully covered with $Ru(CO)_2$ species can be ascribed to the missing Ru sites, which are utilized for both CO and H_2 dissociation.

A tentative mechanism for the low- and medium-temperature reactivity of $Ru(CO)₂$ is presented in Scheme I.

When negligible numbers of ruthenium sites are present (after decomposition up to **473** K), the main reaction is the molecular CO exchange between the gaseous $13CO$ and the ligands in the $Ru(CO)₂$ species. This indicates that the CO molecules in the ligands are rather mobile. In the temperature range between **473** and **573** K, dicarbonyl species are present along with free ruthenium atoms in various oxidation states. This high ruthenium dispersion is stabilized by the presence of dicarbonyl species, and the valence of ruthenium can be easily converted into the zero state under the reaction conditions, i.e. in the presence of a CO

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 $+ H₂$ mixture. In the presence of metallic or zerovalent ruthenium atoms, CO ligands from the neighboring $Ru(CO)$ ₂ species can easily migrate to the free ruthenium sites, on which they dissociate and form methane.

The metallic ruthenium site is also a center for hydrogen dissociation and is a necessary requirement for the methanation reaction.

When decomposition takes place at high temperature (up to **773 K),** all CO ligands which were required to stabilize single ruthenium atoms in dicarbonyl species are removed and the ruthenium particles tend to migrate on the surface to form large aggregates. On large particles the mode of CO chemisorption is changed; in particular, only a negligible amount of dicarbonyl species is produced.

In conclusion, it can be established that free ruthenium sites

are a necessary requirement for the CO hydrogenation reaction. Initially, the presence of dicarbonyl species in the temperature range in which the reaction takes place is important to stabilize the high dispersion of ruthenium. As soon as free ruthenium sites are also present, the CO molecules from the ruthenium dicarbonyl species indicated by the IR bands at 2072 and 2001 cm^{-1} easily migrate to the free ruthenium sites due to their high mobility and react with hydrogen to produce methane. Since these molecules are already in an activated form, it explains their higher reactivity compared to those chemisorbed from the gas phase, i.e. **I3CO.** This ultimately leads to the initial ¹²CH₄ formation when $H_2 + {}^{13}CO$ is used.

Registry No. $Ru_3(CO)_{12}$ **, 15243-33-1; Ru(CO)₂, 106960-32-1; Ru,** 7440-18-8; CH₄, 74-82-8; H₃C(CH₂)₃CH₃, 109-66-0.

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Cyclotriphosphazenes with Geminal (Trimethylsily1)methyl and Alkyl or Aryl Side Groups'

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The synthesis of a series of organosilyl cyclophosphazenes of formula $\text{gem-}N_3P_3Cl_4(CH_2SiMe_3)(R)$, where $R = C_2H_5$, $i-C_3H_7$, $n-C_4H_9$, $t-C_4H_9$, $neo-C_3H_{11}$, and C_6H_5 , via organometallic reactions, is described. The chlorine atoms in the cyclic trimers were replaced by trifluoroethoxy groups by reactions that led to either retention of th them by methyl groups, depending **on** the reaction conditions. The crystal and molecular structures of gem-N3P3C14- $(CH_2SiMe_3)(t-C_4H_9)$ and the related derivative gem-N₃P₃Cl₄(CH₂SiMe₃)₂ were determined by single-crystal X-ray diffraction methods. Steric hindrance involving the organosilyl units results in a widening of the external angle at the supporting phosphorus atom and a narrowing of the corresponding ring angle at that site. Crystals of gem-N₃P₃Cl₄(CH₂SiMe₃)(t-C₄H₉) are orthorhombic with space group Pbca, with $a = 14.884 (4)$ \AA , $b = 15.815 (4)$ \AA , $c = 16.615 (4)$ \AA , $V = 3910.9$ \AA ³, and $Z = 8$. Crystals of gem-N₃P₃Cl₄(CH₂SiMe₃)₂ are monoclinic with space group P_2/n , with $a = 10.145$ (4) Å, $b = 11.060$ (5) Å, $c = 19.999$ (6) Å, $\beta = 103.56$ (3)°, $V = 2181.4$ Å³, and $Z = 4$.

Introduction

Cyclic and linear high-polymeric phosphazenes are now known that bear a wide variety of inorganic, organic, or organometallic side groups.^{2,3} A recent development has been the synthesis of phosphazenes with organosilicon side units.⁴⁻⁷ At the highpolymeric level⁶ these species are hybrid systems with characteristics that resemble those of both poly(organophosphazenes) and poly(organosiloxanes).

The main method for the preparation of phosphazene high polymers involves the ring-opening polymerization of smallmolecule cyclic phosphazenes. Thus, the synthesis of phosphazene cyclic trimers or tetramers that bear organosilicon side groups is an essential first step in the assembly of hybrid organosiliconorganophosphazene macromolecules. A second reason for the study of small-molecule phosphazene ring systems is that they provide excellent reaction models for the more complex substitution reactions carried out on the corresponding high polymers. The small-molecule cyclic species also provide structural models for the high polymers since their molecular geometries can be deduced

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more easily by X-ray diffraction techniques.

In earlier work⁵ at the cyclic trimer level, we developed a series of organometallic pathways that allowed access to small-molecule cyclotriphosphazenes with siloxane or (trimethylsi1yl)methyl units linked to the phosphazene ring. In several cases, two identical organosilicon units were attached to one skeletal phosphorus atom. In other examples, a ring phosphorus atom bore one organosilicon unit and either a chlorine atom or a methyl group. The remaining four side groups were either chlorine atoms or trifluoroethoxy groups introduced by nucleophilic replacement of chlorine.

In the present work, we have extended the number of accessible structures to the 12 compounds depicted as species **la-f** and **2a-f.** The compounds of formula 1 and 2, where $R = CH_3$, were reported earlier.5 Species **3a-f** are compounds formed during the conversion of **1** to **2** by a pathway that will be discussed.

In this study, we have attempted to answer the following questions: (a) What reaction pathways are available for the sequential replacement of two chlorine atoms in hexachloro-

This is the fourth paper from **our** laboratory on organosilicon-organophosphazene chemistry. For the **first** three papers, see ref **4-6.**