# Cobalt Corrole Catalyst for Efficient Hydrogen Evolution Reaction from H<sub>2</sub>O under Ambient Conditions: Reactivity, Spectroscopy, and Density Functional Theory Calculations

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**S** Supporting Information

[AB](#page-6-0)STRACT: [The feasibilit](#page-6-0)y of a hydrogen-based economy relies very much on the availability of catalysts for the hydrogen evolution reaction (HER) that are not based on Pt or other noble elements. Significant breakthroughs have been achieved with certain first row transition metal complexes in terms of low overpotentials and large turnover rates, but the majority of reported work utilized purified and deoxygenated solvents (most commonly mixtures of organic solvents/acids). Realizing that the design of earth abundant metal catalysts that operate under truly ambient conditions remains an unresolved challenge, we have now developed an electronically tuned Co(III) corrole that can catalyze the HER from aqueous sulfuric acid at as low as  $-0.3$  V vs NHE, with a turnover frequency of 600 s<sup>-1</sup> and  $\gg 10^7$  catalytic turnovers. Under aerobic conditions, using H<sub>2</sub>O from naturally available sources without any pretreatment, the same complex catalyzes the reduction of  $H^+$  with a Faradaic Yield (FY) of 52%. Density functional theory (DFT) calculations indicate that the electron density on a putative hydride species is delocalized off from the H atom into the



macrocycle. This makes the protonation of a [Co(III)-H]<sup>−</sup> species the rate determining step (rds) for the HER consistent with the experimental data.

## 1. INTRODUCTION

Water splitting to its elementals,  $H_2$  and  $O_2$ , may be considered the ultimate approach for storing energy in the form of stable yet reactive chemical bonds.<sup>1</sup> Once obtained, the H<sub>2</sub> may be used in fuel cells as a possible clean and sustainable pathway for meeting the ever-incre[as](#page-6-0)ing global energy need. Many techniques for the production of  $H_2$  from natural gas, methanol, biomass, and other nonrenewable material do exist,<sup>1-8</sup> but its efficient generation from water still remains the crux of a hydrogen-based economy.<sup>1,2</sup> What has held back th[is d](#page-6-0)evelopment for decades is that efficient catalysts for the hydrogen evolution reaction (HER[\) a](#page-6-0)re based on expensive and rare noble metals (mainly  $Pt)$ .<sup>9,10</sup> A practical catalyst must be affordable, operate fast (i.e., large turnover frequencies, TOF) and at low overpotential, a[nd](#page-6-0) also be able to function under aerobic conditions with large turnover numbers ([mol  $H_2$ ]/ [mol catalyst], TON). Thus there has been a flurry of activity in this area over the past decade, and several catalysts based on first row transition metals have been reported.<sup>11</sup> There are several reports of  $H_2$  generation from organic acids by Fe, Co, and Ni dithiolene and thiolate complexes.<sup>12,13</sup> R[ece](#page-6-0)ntly, a few Mo based catalysts (note that Mo is 100 times more earth abundant than Pt) that can generate  $H_2$  fr[om](#page-6-0) water have been reported. $14,15$  Nevertheless, there is still a lack of an efficient catalyst that works in aqueous medium at low overpotential and und[er aer](#page-6-0)obic conditions. One issue that has impeded such developments is the water-insolubility of most of these catalysts, which has been successfully circumvented by absorbing them onto electrodes. Table 1 summarizes literature reports on first-row transition metal catalysts that perform reasonably well in aqueous medium. It revea[ls](#page-1-0) that all reported systems operate under anaerobic conditions and in high purity solvent, and also that there is no catalyst that displays all the desired parameters for the HER: high TON, high TOF, and relatively positive onset potential.<sup>14−20</sup> We now show that the tris(5,10,15-pentafluorophenyl)2,3,7,8,12,13,17,18-octafluorocorrole (Co−F<sub>8</sub>) catalyst (Figur[e 1a\)](#page-6-0) immobilized on graphite electrode can catalyze the HER very efficiently, from water obtained from local sources wit[hou](#page-1-0)t requiring pretreatment, and even under aerobic conditions.

## 2. EXPERIMENTAL DETAILS

1. Materials. Pentafluorobenzaldehyde, dichloro dicyano quinone (DDQ), cobalt acetate  $[Co(OAc)<sub>2</sub>·4H<sub>2</sub>O]$ , octanethiol  $(C<sub>8</sub>SH)$ , potassium hexafluorophosphate  $(KPF_6)$ , and tetrabutylammonium perchlorate (TBAP) were purchased from Sigma-Aldrich. Di-Sodium hydrogen phosphate dihydrate  $(Na_2HPO_4.2H_2O)$  and sulfuric acid (H2SO4, 98%) were purchased from Merck. Edge Plane Graphite (EPG), Au and Ag discs for the Rotating Ring Disc Electrochemistry (RRDE) and Surface Enhanced Resonance Raman Spectroscopy (SERRS) experiments were purchased from Pine Instruments, U.S.A.

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a Generally calculated at 200−400 mV below the onset potential.



Figure 1. (a) Chemical structure of the bis-pyridine Co−F<sub>8</sub> complex. (b) CV of (pyridine)<sub>2</sub>Co(III)-F<sub>8</sub> in pure acetonitrile (blue) and in acetonitrile containing 0.13 M TFA (red). Scan rate 50 mV/s, Glassy Carbon (GC) working, Pt counter and Ag/AgCl reference electrode. The redox potential CV in 0.13 M TFA is shifted because of dissociation of the metal-bound pyridine ligands due to protonation.

2. Instrumentation. UV-vis data were taken in Agilent technologies spectrophotometer model 8453 fitted with a diode-array detector. All electrochemical experiments were performed using a CH Instruments (model CHI710D Electrochemical Analyzer). Biopotentiostat, reference electrodes, were purchased from CH Instruments. The RRDE set up from Pine Research Instrumentation (E6 series ChangeDisk tips with AFE6M rotor) was used to obtain the RRDE data. Resonance Raman data were collected using a Trivista 555 spectograph (Princeton Instruments) and using 413.1 nm excitation wavelength from a Kr<sup>+</sup> laser (Coherent, Sabre Innova SBRC-DBW-K). The EPR spectrum was recorded on a JEOL instrument.

3. Synthesis of 2,3,7,8,12,13,17,18-Octafluoro-5,10,15-tris- (pentafluorophenyl)corrole. A 0.5 g portion (4.85 mmol) of 3,4-difluoropyrrole  $(1)$  was dissolved in 1 mL of CH<sub>2</sub>Cl<sub>2</sub> and added to a stirred solution of 400  $\mu$ L (3.24 mmol) of pentafluorobenzaldehyde and 50  $\mu$ L of CH<sub>2</sub>Cl<sub>2</sub> containing 10% TFA at 50 °C. The mixture was stirred vigorously for 1 h after which 80 mL of  $CH_2Cl_2$  and 0.6 g (2.64 mmol) of DDQ in 1 mL of THF were added, and the mixture was stirred for further 10 min. The solvent was evaporated, and the product was purified by column chromatography on silica gel (eluent, hexanes/ $CH_2Cl_2$  9:1 which was changed to acetone). The fluorescence fraction was collected and further purified on PTLC of silica (eluent, acetone/hexanes 1:1). The spectral properties of the product were consistent with literature data. (2) <sup>19</sup>F NMR (188 MHz, C<sub>6</sub>D<sub>6</sub>):  $\delta$ , ppm=  $-139.5$  (dd,  $3J(F,F) = 24.5$  Hz,  $4J(F,F) = 7.7$  Hz, 2F; ortho-F),  $-140.0$  (dd,  $^3$ J(F,F) = 24.1 Hz,  $^4$ J(F,F) = 7.5 Hz, 4F; ortho-F), -154.7  $(t, \frac{3}{F}F) = 20.9$  Hz, 2F; para-F), -155.3  $(t, \frac{3}{F}F) = 20.9$  Hz, 1F; para-F), −157.1 (br. s, 2F; β-pyrr-F), −148.0 (d, 4.7 Hz, 2F; β-pyrr-F), −157.8 (d, 4.7 Hz, 2F; β-pyrr-F), −163.6 (br. s, 2F; β-pyrr-F),  $-164.0$  (dt, <sup>3</sup>J(F,F) = 23.7 Hz, <sup>4</sup>J(F,F) = 7.7 Hz, 4F; meta-F), -164.5  $(dt, \, \, \substack{3}{3}J(F,F) = 24.3 \, \text{Hz}, \, \substack{4}{3}J(F,F) = 7.7 \, \text{Hz}, \, \substack{2F; \, meta-F}.$ 

It was difficult to get a pure product (as indicated by TLC), and the almost pure product was used for cobalt metalation.

Synthesis of  $Co-F_8$ . All the amount of the free base corrole that was obtained from the synthesis of 2,3,7,8,12,13,17,18-octafluoro-5,10,15-tris(pentafluorophenyl)corrole was collected and redissolved in 20 mL of pyridine. A 100 mg portion of  $Co(OAc)<sub>2</sub>·4H<sub>2</sub>O$  (0.40 mmol) was added, and the solution was heated to reflux for 20 min. The reaction progress was monitored by TLC examination (silica,  $CH_2Cl_2$ / n-hexane 1:1), and it was stopped when the fluorescent band of the free base corrole disappeared and the red and nonfluorescent band of the cobalt corrole appeared. The solvent was removed under vacuum, and  $Co-F_8$  was isolated as the major product by column chromatography on silica gel 60 (eluent: CH<sub>2</sub>Cl<sub>2</sub>/hexanes/pyridine 2:1:0.001). Solvent evaporations and recrystallization from  $CH_2Cl_2/n$ -hexane mixtures resulted in 50 mg (43.3  $\mu$ mol, 4.0% yield from the starting amount of the aldehyde) of Co−F<sub>8</sub> as red crystals. <sup>19</sup>F NMR (565 MHz, C<sub>6</sub>D<sub>6</sub>):  $\delta$ , ppm=  $-140.7$  (dd,  $^3$ J(F,F) = 24.3 Hz,  $^4$ J(F,F) = 7.9 Hz, 2F; ortho-F),  $-140.9$  (dd,  $3$ J(F,F) = 24.3 Hz,  $4$ J(F,F) = 7.9 Hz, 4F; ortho-F), -147.2 (d, 6.2 Hz, 2F; β-pyrr-F), −148.0 (d, 5.7 Hz, 2F; β-pyrr-F), −149.2 (d, 6.2 Hz, 2F;  $\beta$ -pyrr-F), -151.1 (t, <sup>3</sup>J(F,F) = 20.1 Hz, 2F; para-F),  $-151.9$  (t,  ${}^{3}J(F,F) = 22.0$  Hz, 1F; para-F),  $-153.8$  (d, 6.2 Hz, 2F;  $\beta$ -pyrr-F),  $-162.6$  (dt,  $^3$ J(F,F) = 24.3 Hz,  $^4$ J(F,F) = 7.9 Hz, 4F; meta-F),  $-163.3$  (dt, <sup>3</sup>J(F,F) = 24.3 Hz, <sup>4</sup>J(F,F) = 7.0 Hz, 2F; meta-F). <sup>1</sup>H NMR (200 MHz,  $C_6D_6$ ):  $\delta$ , ppm= 4.92 (t, 6.4 Hz, 2 H; para-H of pyridine), 4.2 (t, 6.2 Hz, 4H; meta-H of pyridine), 1.34 (br. s, 4H; ortho-H of pyridine). UV/vis (benzene):  $\lambda_{\text{max}}$  nm  $(\varepsilon, \text{ M}^{-1} \text{ cm}^{-1})$  = 418 (1.17  $\times$  $10^6$ ), 563 (3.00 × 10<sup>5</sup>). HR(ESI)-MS in negative ion mode (M<sup>-</sup>) (M-2pyridine =  $C_{37}N_{4}F_{15}F_{8}Co$ ): calcd. for  $m/z = 995.9088$ , obsd. 995.9085 (100%). X-ray quality crystals of Co−F<sub>8</sub> were obtained by slow recrystallization from mixtures of benzene/n-heptane (1:1).

4. Density Functional Theory Calculations. All of the calculations were performed on the Inorganic-HPC cluster at IACS using the Gaussian 03 software package. The geometries were optimized with the spin-unrestricted formalism using both the BP86 functionals and the 6-311G\* basis set for Co and 6-31G\* basis set for other atoms.

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Frequency calculations were performed on each optimized structure using the same basis set to ensure that it was a minimum on the potential energy surface. Total energy calculations were performed using the 6-311+G\* basis set in water solvent and a convergence criterion of 10<sup>−</sup><sup>10</sup> hartree. Basis-set superposition error has been reported to be minimal (∼1 kcal/mol) for anion binding at this level of theory.

#### 3. RESULTS AND ANALYSIS

In our pursuit of an efficient catalyst that can generate  $H_2$  from  $H<sub>2</sub>O$  electrochemically, we decided to focus on the Co complex of fully fluorinated corrole, which was prepared via metalation of the already reported macrocycle.<sup>21</sup>  $Co-F_8$  was isolated as the bis-pyridine complex, and its characterization by X-ray crystallography (Supporting Inform[ati](#page-6-0)on, Figure S9) revealed quite a perfectly planar macrocycle.<sup>22</sup> Conventional corroles are very electron-ric[h ligands that stabilize metals in high](#page-6-0) oxidation states,<sup>23</sup> while the reactivity of lo[w-v](#page-6-0)alent metallocorroles (i.e., in <2+ oxidation states) has not been thoroughly explored.<sup>24–30</sup> Rece[nt i](#page-6-0)nvestigations have however revealed that halogenation of the eight  $\beta$ -pyrroles in corroles affects the redox prop[ert](#page-6-0)i[es](#page-6-0) of the chelated transition metal ion much more dramatically than in other related macrocycles. This is attributed to the fact that halogenation of corroles (as in  $Co-F_8$ ) does not induce structural deformations that attenuate the electron withdrawing effect of the substituents.<sup>31</sup> Cyclic voltammetry (CV, Figure 1b) of the  $Co-F_8$  in a degassed acetonitrile solution displays a reversible  $Co(II/I)$  redo[x c](#page-6-0)ouple at  $-0.97$  V (Figure 1b, bl[ue](#page-1-0)), almost half a volt more positive than for the nonfluorinated analogue.<sup>32</sup> A large electrocatalytic current was obser[ve](#page-1-0)d when the CV of Co−F8 was performed in the presence of an acid (0.13 M [tri](#page-6-0)fluoroacetic acid (TFA) (Figure 1b, red), which is ascribed to  $H_2$  formation. Spectro-electrochemistry (Supporting Information, Figure S1, S2) of the Co− $F_8$  co[mp](#page-1-0)lex in acetonitrile reveals that it is reduced to its  $Co(I)$  state at  $-0.97$  V, [which is the](#page-6-0) [active form for HER cataly](#page-6-0)sis.

Keeping in mind the goal of HER catalysis in aqueous environments, Co−F<sub>8</sub> was physiabsorbed onto an edge-plane pyrolytic graphite (EPG) electrode, thus allowing for electrochemical investigations of this water-insoluble catalyst in aqueous solutions under heterogeneous conditions. The CV of the Co−F<sub>8</sub> catalyst immobilized on EPG in a pH 7 buffer solution shows that the Co(II/I) couple has shifted to −0.38 V vs Ag/AgCl in aqueous medium relative to −0.97 V vs Ag/AgCl in acetonitrile (Supporting Information, Figure S3). This may possibly be attributed to the greater ability of water to solvate the doubly reduced  $[Co(I)-corrole]^{2-}$  complex (note that the corrole donates 3 negative charges). $33$  The positive shift in the  $Co(II/I)$  potential is very encouraging regarding  $H_2$ generation at relatively low overpotential.

Strong indication for  $H_2$  production was obtained by a linear sweep voltammetry (LSV) experiment. When the potential of the Co−F<sub>8</sub> catalyst bearing the EPG electrode was lowered below the  $Co(II/I)$  redox couple in a 0.5 M  $H_2SO_4$  solution, a large electrocatalytic current started to grow (Figure 2a, red) with concomitant gas bubble formation on the surface of the electrode (Figure 2b). The onset potential of this [c](#page-3-0)urrent, indicated by a 10-fold increase of the current with respect to bare EPG, was at a[bo](#page-3-0)ut −0.5 V vs Ag/AgCl (Figure 2a, orange). This implies that catalysis is intimately correlated with the reduction of  $Co(II)$  to  $Co(I)$  in the aqueous aci[dic](#page-3-0) solution. Pronounced catalytic currents were also observed (Figure 2a, blue) with catalyst physiabsorbed on an Au electrode bearing

a self-assembled monolayer (SAM) of octanethiol. Thus the catalyst is capable of HER when physiabsorbed on graphite as well as SAM covered Au/Ag electrodes. This is important for in situ investigations of the catalyst structure under  $H_2$  forming conditions (vide infra) using Surface Enhanced Resonance Raman spectroscopy (SERRS) which can only be performed on SAM covered Au/Ag electrodes and not on EPG electrodes.

Evolution of  $H_2$  was confirmed on both the EPG and Au-SAM electrodes (Figure 2c), using the rotating ring disc electrochemistry (RRDE) technique.<sup>34</sup> The disc bearing the catalyst was rotated at a st[ea](#page-3-0)dy rate that ensures that the hydrodynamic current produced du[e](#page-6-0) to the rotation of the electrode removes any  $H_2$  produced on the disc away from it radially. The Pt ring that encircles the disc electrode was held at an oxidizing potential (0.7 V vs Ag/AgCl), which oxidizes the  $H_2$  back to  $H^+$  and produces a ring current (Supporting Information, Figure S4).<sup>10</sup> The selective detection of  $H_2$ formation by the ring current confirmed that t[he onset of](#page-6-0) H<sub>2</sub> [production by Co](#page-6-0)−F<sub>8</sub> [is](#page-6-0) −0.5 V (−0.3 V vs NHE) on the EPG electrode and −0.3 V (−0.1 V vs NHE) on the Au-SAM electrode.

The reaction was elucidated to be first order with respect to the  $H^+$  concentration (Supporting Information, Figure S5). This implies that the ratio  $i_{cat}/[\tau]$ , between the catalytic current obtained in the presence of substrate  $(i_{cat})$  and the polarographic charge  $([\tau])$  is a measure of the TOF. The TOF in 0.5 M  $H_2SO_4$  under anaerobic condition at room temperature and at  $-0.7$  V and  $-0.8$  V was determined to be 600 s<sup>-1</sup> and 1140 s<sup>-1</sup>, respectively. Electrolysis under anaerobic condition at  $-0.8$  V revealed no decay in the catalyst activity (Figure 2d) for up to 16 h. During this process, 32.16 C was dissipated from the electrode bearing  $4 \pm 0.2 \times 10^{-11}$  moles of Co–F<sub>8</sub> (obtained from integration of the CV current). $35$  This indicates that the TON of the catalyst is  $\gg 10^7$ . .

For in situ investigations of the electro-active [sp](#page-6-0)ecies involved in catalysis during an RRDE experiment under  $H_2$  forming conditions we turned our attention to the Surface Enhanced Resonance Raman Spectroscopy on Rotating Disc Electrode (SERRS-RDE) setup. SERRS-RDE of the Co−F<sub>8</sub> compound absorbed on octanethiol SAM on a roughened Ag disc<sup>36a</sup> that was held at 0 V (i.e., when there is no significant  $H_2$  production) in a pH 7 buffer solution shows a spectrum very similar to that of the Co−F<sub>8</sub> complex in solution (Figure 3a). The vibrations of the Co(II) corrole complex (1350−1400 cm<sup>−</sup><sup>1</sup> and 1530− 1580 cm<sup>−</sup><sup>1</sup> region) were observed on the S[AM](#page-3-0) surface at similar energies and with intensities similar to those observed for the catalyst in acetonitrile solution. This confirms the presence of an intact  $Co-F_8$  catalyst on the electrode after immobilization. Lowering the potential to  $-0.6$  V in a pH 7 buffer solution, where normally  $H_2$  is produced from acidic solutions, caused significant changes in the spectrum in the 300−500  $\text{cm}^{-1}$  region. Although the oxidation and spin state marker bands of Co corroles have not been identified/defined (unlike their porphyrin counterparts), the band at 343 cm<sup>-1</sup> shifts to 341 cm<sup>-1</sup> and loses intensity relative to the band at 385  $cm^{-1}$  (Figure 3b). Identical changes were observed when the Co center in the  $Co-F_8$ complex was reduced to its +1 state by bulk electr[oly](#page-3-0)sis at −1 V in acetonitrile (Figure 3c). These observations indicate that the active form of the catalyst in pH 7 at −0.6 V (i.e., at the potential where  $H_2$  is produced on SAM as well as EPG surfaces from acidic water) has the [Co](#page-3-0) ion in its  $+1$  oxidation state.<sup>36b</sup> In other words, the SERRS-RDE data indicate that the active catalyst on

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Figure 2. (a) LSV of EPG with catalyst (red), EPG without catalyst (orange), SAM with catalyst (blue) and SAM without catalyst (cyan). (b) Bubbles formed (highlighted by the blue circle) on the EPG electrode containing the catalyst after a LSV run. (c) Ring currents generated in RRDE experiments with electrodes having no catalyst (orange), with catalyst on EPG (red), and with catalyst on SAM (blue). All the experiments were done in deoxygenated 0.5 M H<sub>2</sub>SO<sub>4</sub>, using Ag/AgCl as reference, Pt wire as counter electrodes, and scan rate of 50 mV/s. (d) Plot of the current obtained at −0.8 V during ∼16 h of electrolysis of EPG with catalyst under aerobic condition (yellow), under Ar atmosphere (green), and without catalyst under Ar atmosphere (red).



Figure 3. (a) Resonance Raman spectra of Co−F<sub>8</sub> electrolyzed at 0 V in acetonitrile (blue), i.e., homogeneous phase and on SAM surface in pH 7 (red). (b) SERRS-RDE data of the catalyst physiabsorbed on the SAM on a roughened Ag disc while electrolyzing it at 0 V (blue) and at −0.6 V (green). (c) Resonance Raman data of the compound in acetonitrile after electrolyzing it at 0 V (blue) and at −1 V (green).

the SAM surface is  $Co(I)$ – $F_8$ , similar to the active catalyst under homogeneous conditions.

Encouraged by the results obtained with the  $Co-F_8$  catalyst so far, we decided to confront another long-standing

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Figure 4. (a) RRDE results of the catalyst on EPG in air saturated 0.5 M H<sub>2</sub>SO<sub>4</sub> showing EPG current (pink), Pt current when ring held at 1.1 V (cyan), and Pt current when ring held at 0.7 V (orange). (b) Enlarged view showing the Pt ring currents. (c) Electrochemical hydrogen production by the catalyst on EPG from H2O obtained from local water bodies in India and Israel. Ag/AgCl and Pt wire were used as reference and counter electrodes respectively.

challenge: to catalyze the formation of  $H_2$  from  $H^+$  in the presence of  $O_2$ . To the best of our knowledge, only some Se-containing naturally occurring hydrogenases and one most recently reported molecular cobalt catalyst are capable of performing that task.<sup>11b,37</sup> The difficulty arises from the fact that any metal-based catalyst capable of generating  $H_2$  from  $H^+$ also readily reacts with  $O_2$ . This is why almost all  $H_2$  evolution experiments, including the ones reported in this study up to here, were performed under strictly anaerobic conditions. In fact, the octabromo analogue of  $Co-F_8$  catalyst has recently been demonstrated to be an excellent  $O<sub>2</sub>$  reducing electrocatalyst.<sup>38</sup> It is hence not surprising that the LSV of the Co $-F_8$ catalyst in air saturated 0.5 M  $H_2SO_4$  shows a strong  $O_2$ reducti[on](#page-6-0) current at 0.2 V (Figure 4a, pink), a potential where the Co(III) is reduced to Co(II) in acidic medium (Supporting Information, Figure S3). Clearly, the Co(II) generated on the electrode reduces  $O_2$  present in the solution. [There was](#page-6-0) [however a further inc](#page-6-0)rease in the current as the potential was swept more negative (Figure 4a, pink). To elucidate the chemistry behind these observations, the Pt ring was poised at 1.1 V, revealing that current increased at around the same potential where  $O_2$  reduction starts (Figure 4b, cyan). The Pt ring oxidizes  $H_2O_2$  and  $O_2^-$  to  $O_2$ , as well as  $H_2$  to  $H^+$  at this potential. But since there was no current on either of the disc or the ring at these potentials in the absence of  $O_2$  in the medium (see Figure 2a), the current detected at the Pt ring is due to oxidation of  $H_2O_2$  produced by incomplete reduction of  $O_2$ in acidic/ar[eo](#page-3-0)bic solutions. The further increase in the ring current below  $-0.6$  V, when the Co(II) is reduced to Co(I), might in principle imply either greater  $H_2O_2$  production by  $Co(I)$  relative to  $Co(II)$  or  $H_2$  generation by  $Co(I)$  in addition to reduction of  $O_2$ . Holding the ring potential (at otherwise identical experimental conditions) at 0.7 V vs Ag/AgCl,

conditions at which Pt oxidizes  $H_2$  to  $H^+$  but not  $H_2O_2$  to  $O_2$ , allowed for the distinction between these two possibilities. No current was detected in the ring at potentials where an  $O_2$ reduction current was observed in the disc (i.e., starting at 0.2 V), but only at potentials lower than −0.6 V (Figure 4b, orange). The experiments performed in the absence of  $O_2$  thus indicate that  $H_2$  is formed on the electrode at these potentials and is detected in the Pt ring when it is held at 0.7 V. We hence conclude that the Co−F<sub>8</sub> catalyst catalyzes  $H_2$  formation from  $H^+$  even in the presence of  $O_2$ .

The stability and performance of the catalyst under aerobic conditions may not be assessed by  $i_{\text{cat}}/\lbrack\tau\rbrack$ , since the  $i_{\text{cat}}$ represents both  $O_2$  and H<sup>+</sup> reduction currents and the  $[\tau]$  is enveloped by the  $O_2$  reduction current. Catalyst immobilized on EPG was able to electrolyze an aerated 0.5 M  $H_2SO_4$ solution over a period of 16 h, and no decay of the catalytic current was observed (Figure 2d, yellow). However, the total number of coulombs dissipated was two times the value dissipated under anaerobic conditio[ns](#page-3-0) (Figure 2d, green). The Faradaic yield (FY) under aerobic conditions was evaluated by measuring the v[ol](#page-3-0)ume of  $H_2$  liberated during electrolysis using an inverted buret setup (Supporting Information, Figure S7a). The results were quite revealing: 9.1 mL of  $H_2$  were evolved and 149 C of charge dissip[ated from the electrode after 10 h of](#page-6-0) electrolysis in an aerobic 0.5 M  $H_2SO_4$  solution (Supporting Information, Figure S7b). This implies that the FY for  $H_2$  production at  $-0.8$  V in 0.5 M H<sub>2</sub>SO<sub>4</sub> is 52%. For co[mparison, the sole catalyst](#page-6-0) [that has be](#page-6-0)en demonstrated to work under aerobic conditions provided a FY of 45% and TOF of 0.0042  $s^{-1}$ .<sup>11b</sup> Most . importantly SERRS experiments performed before and after  $H_2$ evolution indicate that the Co− $F_8$  catalyst stays inta[ct o](#page-6-0)n the electrode (Supporting Information, Figure S6) and does not



Figure 5. (A) Calculated electrostatic potential of the  $[Co(III)$ -H]<sup>−</sup> species, and (B) the calculated Mulliken population of the  $[Co(III)$ -H]<sup>−</sup> species.

decay as has been reported to be the case for some other Co catalysts.20

Another aspect that increases the maintenance cost and decrease[s t](#page-6-0)he applicability of a practical  $H_2$  generation setup is the requirement for a clean water source, which is a common practice in research but not in real life. We have thus investigated the ability of Co−F<sub>8</sub> immobilized on EPG to generate  $H_2$ from various available water sources, in contrast to the triply distilled  $H_2O$  used up to here. In all these cases the water was filtered through a laboratory filter paper followed by addition of  $H_2SO_4$  to attain a final concentration of 0.5 M. No other chemical or physical treatments were used. Water from tap water, a local pond (IACS), the Ganges (delta region, high saline content and silt and industrial waste contaminated), the Bay of Bengal (saline and silt bearing), the Dead Sea (most saline containing natural  $H<sub>2</sub>O$  source), and the Sea of Galilee (natural fresh water lake) were used. The data from all the water sources show that both  $O_2$  reduction current (below 0.2 V, Figure 4c green region) and  $H^+$  reduction current (below −0.6 V, H2 detected in situ using Pt ring, Figure 4c cyan [re](#page-4-0)gion) are present. The amount of  $H_2$  generated from all water sources, except that obtained from the Dead Sea was si[gn](#page-4-0)ificant, which demonstrates that  $Co-F_8$  is an efficient HER catalyst under truly reasonable conditions.

The spectroscopic data suggest  $Co(I)$  to be the active form of the catalyst. Additionally, the potential for  $H^+$  reduction coincides with the  $Co(II/I)$  reduction indicating that  $Co(I)$ is the reactive species. The linear dependence of the catalytic current on proton concentration (Supporting Information, Figure S5) indicates that the reaction follows first order kinetics with respect to [H]<sup>+</sup>. Also a substrate diff[usion limited current](#page-6-0) [is not obse](#page-6-0)rved; rather, a kinetic barrier in the catalysis seems to determine the electrocatalytic current. Taken together these facts suggest the following mechanism for  $H_2$  generation.<sup>39</sup>

$$
[Co(I)]^{-2} + H^{+} \rightarrow [Co(III) - H]^{-} + H^{+} \rightarrow Co(III) + H_{2}
$$

Geometry optimized density functional theory (DFT) calculations are performed to evaluate the feasibility of this process. The calculated free energies reflect that the reduction to  $Co(II)$ to Co(I) is the most thermodynamically uphill step with a  $\Delta G$ of +25.74 kCal/mol. This translates into a reduction potential of  $-1.1$  eV. The protonation of the Co(I) species to generate a [Co(III)-H]<sup>−</sup> species and the subsequent protonation of the  $[Co(III)-H]$ <sup>-</sup> species to release H<sub>2</sub> and result in the oxidation of  $Co(I)$  to  $Co(III)$  are calculated to be energetically favorable. Interestingly, while the protonation of the  $Co(I)$  species is

energetically favorable, the protonation of the  $[Co(III)-H]$ <sup>-</sup> is not. The calculated electrostatic potential map (Figure 5A) of this species indicates that the accumulated anionic charge density on the H<sup>−</sup> species is small, and the corresponding Mulliken charge (Figure 5B) on H is calculated to be  $\sim -0.1$ . Alternatively, significant electron density is observed on the fluoride substituents of the corrole ring indicating charge delocalization off the H atom into the macrocycle. This leads to weaker protonation energy (i.e., lower  $pK_a$ ) of this H<sup>-</sup> to liberate  $H_2$ . Taken together, the linear dependence of the catalytic current with  $[H^+]$  (indicating that the rds involved protonation), the calculated free energy of protonation, and the ground state electronic structure of the  $[Co(III)-H]^$ species suggest that the protonation of the  $[Co(III)-H]^$ species is the rds for this catalyst (Scheme 1).

## Scheme 1. Mechanism for  $H_2$  Evolution Catalyzed by a Molecular Cobalt Corrole Complex



## 6. CONCLUSION

In summary, we report a Co-based electrocatalyst that can reduce H<sup>+</sup> from H<sub>2</sub>O to form H<sub>2</sub> with an onset at −0.3 V vs NHE on a graphite electrode and close to its thermodynamic potential on a thiol monolayer covered Au electrode (onset at −0.1 V vs NHE). In situ SERRS confirms successful immobilization of the intact catalyst on electrodes and further indicates that the Co in Co−F8 is reduced to Co(I) at potentials where it produces  $H_2$ . The catalyst has a turnover frequency of 600 s<sup>-1</sup> at -0.5 V vs NHE in 0.5 M H<sub>2</sub>SO<sub>4</sub> and a turnover number of  $\gg 10^7$ . It is also capable of reducing  $H_2$  in the presence of  $O_2$  with a FY of 52% and TON comparable to those observed under anaerobic conditions. An additional feature is that the Co−F<sub>8</sub> catalyst is capable of producing  $H_2$  <span id="page-6-0"></span>from a variety of local and global water sources without the need for any pretreatment. Electronic structure calculations and  $[H]^{+}$  dependence of the catalytic activity suggests that the protonation of a putative [Co(III)-H]<sup>−</sup> species is the rds of the HER catalyzed by this complex.

### ■ ASSOCIATED CONTENT

#### **S** Supporting Information

Crystallographic data, absorption, and EPR spectra of the complex related to catalysis, experiments related to  $H_2$ detection and quantification, and related electrochemical data. This material is available free of charge via the Internet at http://pubs.acs.org.

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#### Notes

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#### ■ REFERENCES

(1) Cook, T. R.; Dogutan, D. K.; Reece, S. Y.; Surendranath, Y.; Teets, S. T.; Nocera, D. G. Chem. Rev. 2010, 110, 6474−6502.

(2) Lubitz, W.; Tumas, W. Chem. Rev. 2007, 107, 3900−3903.

(3) Esswein, A. J.; Nocera, D. G. Chem. Rev. 2007, 107, 4022−4047.

(4) Holladay, J. D.; Wang, Y.; Jones, E. Chem. Rev. 2004, 104, 4767− 4790.

(5) Kodama, T.; Gokon, N. Chem. Rev. 2007, 107, 4048−4077.

(6) R. M. Navarro, M. A.; Peñ a, J. L.; Fierro, G. Chem. Rev. 2007, 107, 3952−3991.

(7) Palo, D. R.; Dagle, R. A.; Holladay, J. D. Chem. Rev. 2007, 107, 3992−4021.

(8) Reece, S. Y.; Hamel, J. A.; Sung, K.; Jarvi, T. D.; Esswein, A. J.; Pipers, J. J. H.; Nocera, D. G. Science 2011, 334, 645−648.

(9) Du, P.; Eisenberg, R. Energy Environ. Sci. 2012, 5, 6012−6021.

(10) Le Goff, A.; Artero, V.; Jousselme, B.; Tran, P. D.; Guillet, N.; Metaye, R.; Fihr, A.; Palacin, S.; Fontecave, M. Science 2009, 326, 1384−1387.

(11) (a) Helm, M. L.; Stewart, M. P.; Bullock, R. M.; DuBois, M. R.; DuBois, D. L. Science 2011, 333, 863−866. (b) Lakadamyali, F.; Kato, M.; Muresan, N. M.; Reisner, E. Angew. Chem., Int. Ed. 2012, 51, 9381−9384. (c) Singh, W. M.; Baine, T.; Kudo, S.; Tian, S.; Na, X. A. N.; Zhou, H.; DeYonker, N. J.; Pham, T. C.; Bollinger, J. C.; Baker, D. L.; Yan, B.; Webster, C. E.; Zhao, X. Angew. Chem., Int. Ed. 2012, 51, 5941−5944. (d) Lee, C. H.; Dogutan, D. K.; Nocera, D. G. J. Am. Chem. Soc. 2011, 133, 8775−8777. (e) Roubelakis, M. M.; Bediako, D. K.; Dogutan, D. K.; Nocera, D. G. Energy Environ. Science 2012, 5, 7737−7740.

(12) (a) Baffert, C.; Artero, V.; Fontecave, M. Inorg. Chem. 2007, 46, 1817−1824. (b) Razavet, M.; Artero, V.; Fontecave, M. Inorg. Chem. 2005, 44, 4786−4795. (c) McCormick, T. M.; Han, Z.; Weinberg, D. J.; Brennessel, W. W.; Holland, P. L.; Eisenberg, R. Inorg. Chem. 2011, 50, 10660−10666.

(13) (a) Rose, M. J.; Gray, H. B.; Winkler, J. R. J. Am. Chem. Soc. 2012, 134, 8310−8313. (b) McNamara, W. R.; Han, Z.; Alperin, P. J.; Brennessel, W. W.; Holland, P. L.; Eisenberg, R. J. Am. Chem. Soc.

2011, 133, 15368−15371. (c) Han, Z.; McNamara, W. R.; Eum, M. S.; Holland, P. L.; Eisenberg, R. Angew. Chem., Int. Ed. 2012, 51, 1667− 1670.

(14) Karunadasa, H. I.; Chang, C. J.; Long, J. R. Nature 2010, 464, 1329−1333.

(15) Karunadasa, H. I.; Montalvo, E.; Sun, Y.; Majda, M.; Long, J. R.; Chang, C. J. Science 2012, 335, 698−702.

(16) Sun, Y.; Bigi, J. P.; Piro, N. A.; Tang, M. L.; Long, J. R.; Chang, C. J. J. Am. Chem. Soc. 2011, 133, 9212−9215.

(17) McCrory, C. C. L.; Uyeda, C.; Peters, J. C. J. Am. Chem. Soc. 2012, 134, 3164−3170.

(18) Berben, L. A.; Peters, J. C. Chem. Commun. 2010, 46, 398−400. (19) Stubbert, B. D.; Peters, J. C.; Gray, H. B. J. Am. Chem. Soc. 2011, 133, 18070−18073.

(20) Anxolabéhère-Mallart, E.; Costentin, C.; Fournier, M.; Nowak, S.; Robert, M.; Savéant, J. M. J. Am. Chem. Soc. 2012, 134, 6104–6107. (21) Lui, H. Y.; Lai, T. S.; Yeung, L. L.; Chang, C. K. Org. Lett. 2003, 5, 617−620.

(22) CCDC 893235 contains the supplementary crystallographic data for Co-F<sub>8</sub>. This data can be obtained free of charge from The Crystallographic Data Centre via www.ccdc.cam.ac.uk/data\_request/ cif.

(23) (a) Watanabe, Y. In Porphyrin Handbook; Kadish, K. M., Kevin, S. M., Guilard, R., Eds.; Academic [Press: New York, 2000;, Vol.](www.ccdc.cam.ac.uk/data_request/cif) 4, pp [97](www.ccdc.cam.ac.uk/data_request/cif)−117. (b) Guildard, R.; Barbe, J. M.; Stern, C.; Kadish, K. M. In Porphyrin Handbook; Kadish, K. M., Kevin, S. M., Guilard, R., Eds.; Academic Press: New York, 2003; Vol. 18, pp 303−349.

(24) Gross, Z. J. Biol. Inorg. Chem. 2001, 6, 733−738.

(25) Aviv, I.; Gross, Z. Chem. Commun. 2007, 1987−1999.

(26) Abu-Omar, M. M. Dalton. Trans. 2011, 40, 3435−3444.

(27) Will, S.; Lex, J.; Vogel, E.; Adamian, V. A.; Caemelbecke, E. V.; Kadish, K. M. Inorg. Chem. 1996, 35, 5577−5583.

(28) Ghosh, A.; Wondimagegn, T.; Parusel, A. B. J. J. Am. Chem. Soc. 2000, 122, 5100−5104.

(29) Meier-Callahan, A. E.; Gray, H. B.; Gross, Z. Inorg. Chem. 2000, 39, 3605−3607.

(30) Gross, Z.; Gray, H. B. Inorg. Chem. 2006, 27, 61−72.

(31) (a) Mahammed, A.; Timanskii, B.; Gross, Z. J. Porphyrins Phthalocyanines 2011, 15, 1276. (b) Mahammed, A.; Botoshansky, M.; Gross, Z. Dalton Trans. 2012, 41, 10938−10940.

(32) Grodkowski, J.; Neta, P.; Fujita, E.; Mahammed, A.; Simkhovich, L.; Gross, Z. J. Phys. Chem. A 2002, 106, 4772−4778.

(33) (a) Barker, J. D.; Eckermann, A. L.; Sazinsky, M. H.; Hartings, M. R.; Abajian, C.; Georganopulou, D.; Ratner, M. A.; Rosenzweig, A. C.; Meade, T. J. Bioconjugate Chem. 2009, 20, 1930−1939. (b) Dey, A.; Jenney, F. E.; Adams, M. W. W.; Babini, E.; Takahashi, Y.; Fukuyama, K.; Hodgson, K. O.; Hedman, B.; Solomon, E. I. Science 2007, 318, 1464−1468.

(34) Bard, A. J.; Faulkner, L. R. Electrochemical Methods; J. Wiley: New York, 1980.

(35) Note that while the CV current is weak, it yields the same coverage over various scan rates, Supporting Information, Figure S10.

(36) (a) Both Ag and Au form stable monolayers with thiols and can physiabsorb the  $Co-F_8$  catalyst, but only Ag can be used as SERRS substrate for 413.1 nm excitation into the Soret band of  $Co-F_8$ . (b) We assume that inferences based on the spectroscopic data obtained on the SAM covered Ag electrode is also applicable to SAM covered Au electrode and EPG electrodes.

(37) Parkin, A.; Goldet, G.; Cavazza, C.; Fontecilla-Camps, J. C.; Armstrong, F. A. J. Am. Chem. Soc. 2008, 130, 13410−13426.

(38) Schechter, A.; Stanevsky, M.; Mahammed, A.; Gross, Z. Inorg. Chem. 2011, 51, 22−24.

(39) (a) Kellet, R. M.; Spiro, T. G. Inorg. Chem. 1985, 24, 2373− 2377. (b) Marinescu, S. C.; Winkler, J. R.; Gray, H. B. Proc. Natl. Acad. Sci. U.S.A. 2012, 109, 15127−15131.