# Role of Lattice Oxygen Atoms in Partial Oxidations of Methane, Ethane and Ethylene over Samarium Oxides

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# Abstract

The contribution of lattice oxygen atoms of  $Sm_2O_3$  catalysts in the oxidative coupling of methane has been examined by comparing the distributions of products and reactivities of the catalysts observed in the presence and absence of oxygen in the gas phase. The products of the reaction of CH<sub>4</sub> with lattice oxygen atoms (without oxygen in the gas phase) at 873–998 K were  $H_2$ , CO,  $C_2H_4$  and  $H_2O$  without a trace of  $C_2H_6$ . The main products  $H_2$  and CO were speculated to be produced from HCHO as the reaction intermediate. The amount of C<sub>2</sub>H<sub>4</sub> did not depend on the reaction temperatures. Direct formation of C<sub>2</sub>H<sub>4</sub> from CH<sub>4</sub> suggested the formation of  $CH_2$  = groups on special active sites on the surface. In contrast, the reation of CH<sub>4</sub> with the adsorbed oxygens (in the presence of gaseous oxygen) gave  $C_2H_6$ ,  $C_2H_4$ ,  $CO_2$ , CO and  $H_2O$ . The selectivity to  $C_2$ -compounds ( $C_2H_6 + C_2H_4$ ) was remarkably high compared to that observed for the lattice oxygen atoms. Thus the adsorbed oxygens are better oxidants for oxidative coupling of CH<sub>4</sub>. The main products observed in the reactions of  $C_2H_6$  and  $C_2H_4$  with lattice oxygen atoms were CO, H<sub>2</sub> and CH<sub>4</sub>. CO<sub>2</sub> was not produced at temperatures below 973 K. In contrast, the reactions with adsorbed oxygens in the presence of gaseous oxygen produced only CO<sub>2</sub>, CO and H<sub>2</sub>O without any H<sub>2</sub> or CH<sub>4</sub>.

The reactivity of the adsorbed oxygen for converting  $CH_4$  was more than three orders of magnitude greater than that of the lattice oxygen atoms. Thus, oxidative coupling of  $CH_4$  in the presence of gaseous oxygen can be ascribed to the role of adsorbed oxygens.

# Introduction

Rare earth metal oxides are active and selective catalysts for converting methane to  $C_2$ -hydrocarbons  $(C_2H_6 + C_2H_4)$  in oxidative dehydrogenation and coupling of methane [1, 2]. Among the oxides tested,

 $Sm_2O_3$  was the most active and selective catalyst for the reaction [1, 2]. Kinetic studies on the reaction over  $Sm_2O_3$  suggested that the oxygen species responsible for activating methane is an adsorbed dioxygen such as  $O_2^{2^-}$ ,  $O_2^-$ , or  $O_2$  on the surface [3].

There are many reports describing the reactivity and behavior of lattice oxygen atoms in metal oxides for the catalytic oxidation of olefins and the other oxidation reactions [4]. The main interest in the present work is to examine whether the lattice oxygen atoms of  $\text{Sm}_2\text{O}_3$  have better catalytic properties, activity and selectivity than the oxygen adsorbed on the surface of  $\text{Sm}_2\text{O}_3$  for the oxidative coupling of CH<sub>4</sub>. The over-all reaction paths for the oxidation of CH<sub>4</sub> can generally be written as follows:



Reactivity and selectivity of the lattice oxygen atoms of  $Sm_2O_3$  for each path (I–VII) will also be examined by using CH<sub>4</sub>,  $C_2H_6$ ,  $C_2H_4$  and CO as the starting reactants.

#### Experimental

The samarium oxide  $(Sm_2O_3)$  used was a reagent grade powder (purity >99.9%) obtained from Asahi Chemical Industry. The BET surface area of the sample calculated from the adsorption of N<sub>2</sub> was 8.4 m<sup>2</sup> g<sup>-1</sup>. The kinetic curve for each oxidation reaction was measured using a conventional gas-circulation apparatus of *ca.* 340 cm<sup>3</sup> volume, capable of achieving a vacuum to  $1.3 \times 10^{-4}$  Pa. The samarium oxide samples were pretreated in an atmosphere of oxygen (13 kPa) at 873 K and degassed for 2 h under a vacuum of  $1.3 \times 10^{-3}$  Pa at the same temperature.

Kinetic measurements for the reactions of lattice oxygen atoms of Sm<sub>2</sub>O<sub>3</sub> with CH<sub>4</sub>, C<sub>2</sub>H<sub>6</sub>, C<sub>2</sub>H<sub>4</sub> and CO were carried out using 5.00 g of the catalyst placed at the bottom of a quartz reactor (25 mm i.d. and 30 mm height). Oxidations of CH<sub>4</sub>, C<sub>2</sub>H<sub>6</sub>, C<sub>2</sub>H<sub>4</sub> and CO in the presence of  $O_2$  in the gas phase were carried out using 10 mg Sm<sub>2</sub>O<sub>3</sub>. The reactions were initiated by circulating the reactants over the catalysts. Small amounts of gaseous products were removed to analyse the composition of the products by gas-chromatography at appropriate time intervals. The column packings were a series of MS13X (1 m) and active carbon (2 m) for the separation of  $CH_4$ , CO,  $O_2$  and  $H_2$ ; and Gaskuropack 54 (2 m) for the separation of CO<sub>2</sub>, C<sub>2</sub>H<sub>6</sub>, C<sub>2</sub>H<sub>4</sub> and H<sub>2</sub>O. Typically a 95% carbon mass balance was achieved by quantitative analysis of the products.

#### Results

## Oxidation of CH<sub>4</sub>

# (a) Reaction with lattice oxygen atoms

The measurement of oxygen adsorption on  $\text{Sm}_2\text{O}_3$  at temperatures above 823 K showed that the adsorption of oxygen was reversible with increasing and decreasing the pressure of oxygen. The adsorption isotherm could be expressed by a Henry's equation. These observations indicate that there is no measurable oxygen adsorbed on  $\text{Sm}_2\text{O}_3$  after pretreatment of the sample under a vacuum at 873 K. Thus, we consider that the oxidation of CH<sub>4</sub> by contacting CH<sub>4</sub> with  $\text{Sm}_2\text{O}_3$  is caused by the lattice oxygen atoms of the oxides.

The reaction between  $CH_4$  and the lattice oxygen atoms of  $Sm_2O_3$  has been carried out at 873, 923,



Fig. 1. Oxidation of methane by lattice oxygen atoms of  $Sm_2O_3$  at 873 K.



Fig. 2. Oxidation of methane by lattice oxygen atoms of  $Sm_2O_3$  at 923 K.



Fig. 3. Oxidation of methane by lattice oxygen atoms of  $Sm_2O_3$  at 973 K.

973 and 998 K at an initial pressure of CH<sub>4</sub> 12.0 kPa. The kinetic curves observed at 873, 923 and 973 K, for example, are shown in Figs. 1, 2 and 3, respectively. The products observed at 873 and 923 K were H<sub>2</sub>, CO,  $C_2H_4$  and  $H_2O$ . CO<sub>2</sub> was produced at >973 K, but the rate was very slow compared to the formation of CO. The results in Figs. 1-3 show that the main products are H<sub>2</sub> and CO at any temperature. The H<sub>2</sub>: CO ratio observed at 873 K was about 2 (except the initial points), but the ratio decreased as the temperature was raised. The formation of H<sub>2</sub>O was not observed at 873 K, but it was clearly observed above 923 K. The quantity of H<sub>2</sub>O formed, however, could not be measured accurately because of a large experimental error in the quantitative analysis of H<sub>2</sub>O. It is to be noted that  $C_2H_4$  is the only coupling product of CH<sub>4</sub> without a trace of C<sub>2</sub>H<sub>6</sub>. The formation of C<sub>2</sub>H<sub>4</sub> was complete within 60 min at all temperatures. The final amounts of C<sub>2</sub>H<sub>4</sub> formed did not change with temperature (0.38  $\pm$  0.04  $\mu$ mole/g-cat).

#### (b) Reaction with adsorbed oxygens

When the weight of catalyst used was decreased to 10 mg, the products of the reaction between CH<sub>4</sub> (12.0 kPa) and the lattice oxygen atoms were too small to be measured at <1023 K. However, fast oxidation of CH<sub>4</sub> took place after adding oxygen (1.8 kPa) to the gas phase. The reaction for the CH<sub>4</sub> and O<sub>2</sub> mixture did not take place at all in the absence of the catalyst at <1023 K. Thus we can consider that the reaction observed for the mixture of CH<sub>4</sub> and O<sub>2</sub> in the presence of Sm<sub>2</sub>O<sub>3</sub> is caused by the adsorbed oxygen on the catalyst.

The reaction between CH<sub>4</sub> and the adsorbed oxygen on  $Sm_2O_3$  has been examined at 873, 923 and 973 K. The reaction was carried out at 12.0 (1.63  $\times$  $10^{-3}$  mol) and 1.8 kPa (0.24 ×  $10^{-3}$  mol) for CH<sub>4</sub> and O<sub>2</sub>, respectively, using 10 mg of Sm<sub>2</sub>O<sub>3</sub>. Since the kinetic features of the reaction carried out using a gas-flow system have already been described elsewhere [2, 3], only the results at 923 K are shown in Fig. 4 for comparison with Fig. 2. The kinetic curves in Fig. 4 indicate that  $C_2H_6$  is the initial coupling compound, in contrast to the results for the reaction of CH<sub>4</sub> with lattice oxygen atoms. Only a trace of hydrogen was observed, suggesting that the most of the hydrogen produced was oxidized quickly to H<sub>2</sub>O by adsorbed oxygen.  $CO_2$  was the main carbon oxide formed in the reaction with adsorbed oxygen (Fig. 4). In contrast to this observation, the lattice oxygen atoms oxidized CH<sub>4</sub> only to CO and further oxidation to  $CO_2$  was very slow (Figs. 1–3).

The rates of conversion of  $CH_4$  were also quite different between the reaction of  $CH_4$  with the adsorbed oxygen and the reaction with lattice oxygen atoms. The initial rate per gram of the catalyst for the former reaction is more than three orders of magnitude greater than the rate for the latter (see Figs. 2 and 4). Thus, there are large differences between the reactivities of the adsorbed oxygens and the lattice oxygen atoms for the reaction with  $CH_4$ .



Fig. 4. Oxidation of methane by adsorbed oxygens on  $Sm_2O_3$  at 923 K.



10, mol

reactant T

Б

5

Amount

0.5

product 1.0

0 50 100 150 Reaction time ∕min

Fig. 5. Oxidation of ethane by lattice oxygen atoms of  $Sm_2O_3$  at 873 K.



Fig. 6. Oxidation of ethane by adsorbed oxygens on  $Sm_2O_3$  at 873 K.

#### Oxidation of $C_2H_6$

#### (a) Reaction with lattice oxygen atoms

The reaction of the lattice oxygen atoms with  $C_2H_6$  has been examined at 823, 873 and 973 K at the initial pressure of  $C_2H_6$  of 1.2 kPa. The products were H<sub>2</sub>, CO,  $C_2H_4$ , CH<sub>4</sub> and H<sub>2</sub>O. H<sub>2</sub>O was only a trace at <873 K. The kinetic curves observed at 873 K, for example, are shown in Fig. 5. CO<sub>2</sub> was not observed at the experimental temperatures. This observation shows that further oxidation of CO is difficult for the lattice oxygen atoms, which is coincident with the observations in Figs. 1–3.

## (b) Reaction with adsorbed oxygens

Oxidation of  $C_2H_6$  in the presence of oxygen in the gas phase was observed at 873 and 973 K. The features of the kinetic curves are indicated in Fig. 6 for the reaction at 873 K. Very rapid oxidation of  $C_2H_6$  to CO<sub>2</sub> was observed at the initial stage of the reaction. Oxygen in the gas phase was consumed within 30 min. The product distributions shown in Figs. 5 and 6 are quite different.  $CO_2$  is the main product in Fig. 6 and the formation of  $CH_4$  was not observed at all, in contrast to the results in Fig. 5. It is to be noted that only a trace of  $C_2H_4$  was formed in Fig. 6. This observation suggests that the  $CO_2$  is not produced from  $C_2H_4$  but directly from  $C_2H_6$ . The kinetic curves in Fig. 6 show that the conversion of  $C_2H_6$  and the formation of CO still continue after complete consumption of oxygen in the gas phase. These observations may be explained in terms of the reaction of  $C_2H_6$  with  $H_2O$ . However, because of the difficulty in the quantitative analysis of  $H_2O$ , this reaction will not be discussed further.

Rough estimation for the initial rates of conversion of  $C_2H_6$  per gram catalyst in the presence and absence of oxygen in the gas phase indicated that the reactivity of adsorbed oxygens is at least two orders of magnitude greater than that of lattice oxygen atoms on the surface.

## Oxidation of $C_2H_4$

## (a) Reaction with lattice oxygen atoms

Gas-solid reaction between  $C_2H_4$  and  $Sm_2O_3$  gave CO,  $H_2$ ,  $CH_4$ ,  $C_2H_6$  and  $H_2O$  at the temperatures 773, 823, 873 and 973 K.  $H_2O$  was only a trace at <873 K. Kinetic curves for the reaction at 873 K at 1.2 kPa of the initial pressure of  $C_2H_4$  are given in Fig. 7 as examples. The quantities of the carbon compounds produced were in the order of  $CO > CH_4 >$  $C_2H_6$  irrespective of the experimental temperatures. CO<sub>2</sub> was not observed here either.



Fig. 7. Oxidation of ethylene by lattice oxygen atoms of  $Sm_2O_3$  at 873 K.

# (b) Reaction with adsorbed oxygens

The reaction of  $C_2H_4$  with adsorbed oxygen atoms was examined at 773, 823, 873 and 973 K. In contrast to the results observed for the reaction with



Fig. 8. Oxidation of ethylene by adsorbed oxygens on  $Sm_2O_3$  at 873 K.

lattice oxygen atoms, there were neither  $CH_4$ ,  $C_2H_6$ , nor  $H_2$  produced. The products were only  $CO_2$ , COand  $H_2O$ . The kinetic curves observed at 873 K are shown in Fig. 8 as examples.

The rate of the initial conversion of  $C_2H_4$  per gram catalyst estimated from Fig. 8 is at least three orders of magnitude greater than that estimated from Fig. 7. This shows that the oxidation power of adsorbed oxygens is much greater than that of lattice oxygen atoms.

#### Oxidation of CO

The kinetic curves of  $CO_2$  formation in the oxidation of CO with lattice oxygen atoms and with adsorbed oxygens at 873 K are shown in Fig. 9. The initial pressure of CO was 12.0 kPa. The kinetic curve *a* in Fig. 9 shows that oxidation of CO with lattice oxygen atoms is very slow at 873 K, which is coincident with the observation that  $CO_2$  was not produced in the reactions of  $CH_4$ ,  $C_2H_6$  and  $C_2H_4$ with lattice oxygen atoms at <923 K. On the other hand, oxidation of CO with adsorbed oxygen was



Fig. 9. Oxidations of CO by: (a) lattice oxygen atoms, and (b) adsorbed oxygens, at 873 K.

very fast (kinetic curve b in Fig. 9). Since the weight of catalyst used for this reaction was 1/500 of that used for the reaction with lattice oxygen atoms, the rates of oxidation per gram of catalyst are four to five orders of magnitude greater for the former than the latter. The fast conversion of CO to  $CO_2$  in the presence of  $O_2$  in the gas phase explains the observation that  $CO_2$  was the main carbon oxide in the oxidations of CH<sub>4</sub> and  $C_2H_6$  with adsorbed oxygens.

## Discussion

The amount of lattice oxygen atoms on the surface per 5.00 g Sm<sub>2</sub>O<sub>3</sub> are roughly  $1.2 \times 10^{-3}$  mol on the basis of the lattice parameters of the oxide and the surface area of the sample. The amounts of CO produced by the reactions of lattice oxygen atoms with CH<sub>4</sub>, C<sub>2</sub>H<sub>6</sub> and C<sub>2</sub>H<sub>4</sub> were less (<20%) than that of surface lattice oxygen atoms. However, this cannot preclude the idea that the lattice oxygen atoms in the bulk would also contribute to the reaction because the diffusion of lattice oxygen atoms in the bulk at 873 K is very fast compared to the gas—solid reactions described above. The fast diffusion of the lattice oxygen atoms has been confirmed by measuring the rate of  ${}^{18}O_2(gas)-{}^{16}O(lattice)$  exchange reaction (to be published).

#### **Reaction Schemes**

As described earlier, the product distributions observed were quite different between the reaction with lattice oxygen atoms and the reaction with adsorbed oxygens for each hydrocarbon (CH<sub>4</sub>, C<sub>2</sub>H<sub>6</sub> and C<sub>2</sub>H<sub>4</sub>). The reactivity of the adsorbed oxygens was two to five orders of magnitude greater than that of the lattice oxygen atoms. These observations strongly suggest that the reaction mechanisms for the oxidations of the hydrocarbons caused by the two oxygen species are quite different. Furthermore, we can conclude that the contribution of lattice oxygen atoms to the oxidations of CH<sub>4</sub>, C<sub>2</sub>H<sub>6</sub>, C<sub>2</sub>H<sub>4</sub> and CO can be neglected when oxygen is present in the gas phase.

The following discussions on the reaction mechanisms will be limited to the reactions with lattice oxygen atoms because the details on the reaction mechanism for the partial oxidation of  $CH_4$  by  $O_2$ over  $Sm_2O_3$  have already been described elsewhere [2, 3]. Moreover, the experimental results obtained in this work for the reactions of  $C_2H_6$  and  $C_2H_4$  with adsorbed oxygens are not adequate to discuss the reaction mechanism. The adsorbed oxygen species responsible for each reaction must also be clarified. Further work is needed on these subjects.

## Oxidation of CH<sub>4</sub> with lattice oxygen atoms

The results shown in Figs. 1–3 indicate that the lattice oxygen atoms of  $Sm_2O_3$  do not convert  $CH_4$ 

into C<sub>2</sub>-hydrocarbons in good selectivity but produce  $H_2$  and CO as the main products. The observation that the ratio of  $H_2$ :CO was about 2 (Fig. 1) implies that CH<sub>4</sub> is oxidized through CH<sub>3</sub>OH and HCHO as reaction intermediates, as follows:



 $CH_3OH(ads) \longrightarrow HCHO(ads) + H_2$ (2)

$$HCHO(ads) \longrightarrow CO + H_2$$
(3)

Where coordination numbers for the surface Sm and oxygen were tentatively written in eqn. (1). The conversion of CH<sub>3</sub>OH(ads) and HCHO(ads) must be very fast since neither CH<sub>3</sub>OH nor HCHO was observed in the gas phase during the reaction. The decrease in the ratio H<sub>2</sub>:CO to below 2 at higher temperatures >923 K (Figs. 2 and 3) can be ascribed to the further oxidation of  $H_2$  by lattice oxygen atoms. The formation of  $C_2H_4$  without a trace of  $C_2H_6$  observed in Figs. 1–3 strongly suggests that  $C_2H_4$  is produced directly from  $CH_4$  (path V in the general scheme for CH<sub>4</sub> oxidation described earlier). This is quite unusual because C<sub>2</sub>H<sub>6</sub> is generally believed to be the precursor of C<sub>2</sub>H<sub>4</sub> in oxidative coupling of  $CH_4$  by  $O_2$  over metal oxides [2, 5–8]. As pointed out earlier, the quantity of  $C_2H_4$  formed was limited to  $0.38 \pm 0.04 \ \mu mol/g-Sm_2O_3$  irrespective of the reaction temperatures. This quantity corresponds to 0.16% of the number of surface oxygen atoms. Thus, the number of active sites converting  $CH_4$  directly into  $C_2H_4$  is very low. Although the nature of the active sites is not known at the moment, we speculate that  $C_2H_4$  may be formed through the dimerization of the  $CH_2$  = groups generated on the active sites (=Sm\*=O) as follows:



$$2(CH_2=) \longrightarrow C_2H_4 \tag{5}$$

Oxidation of  $C_2H_6$  and  $C_2H_4$  with lattice oxygen atoms

Figure 5 indicates that the selectivity of formation of  $C_2H_4$  is quite high at the early stage of the reaction between  $C_2H_6$  and  $Sm_2O_3$ . This observation shows

that the lattice oxygen atoms are efficient oxidants for oxidative dehydrogenation of  $C_2H_6$ . In contrast to this, the adsorbed oxygen oxidizes  $C_2H_6$  quickly to  $CO_2$  (Fig. 6).

The reactions of  $C_2H_6$  and  $C_2H_4$  with lattice oxygen atoms gave many products (Figs. 5 and 7) such as CO, H<sub>2</sub>, CH<sub>4</sub>, C<sub>2</sub>H<sub>4</sub> (from C<sub>2</sub>H<sub>6</sub>) and C<sub>2</sub>H<sub>6</sub> (from C<sub>2</sub>H<sub>4</sub>). These products complicated the situation for discussing the reaction mechanism because several intermediates on the surface could be hypothesized to explain the products. Moreover, we cannot neglect the subsequent reactions of the products. Therefore, further discussions on the reaction mechanism will not be made here. Spectroscopic and more detailed kinetic works are needed to clarify the reaction mechanism.

The adsorbed oxygen did not produce any  $CH_4$ ,  $H_2$  and  $C_2H_6$ , as can be seen in Fig. 8. This observation is explained by the idea that the reaction intermediates for the  $CH_4$ ,  $H_2$  and  $C_2H_6$  must be oxidized rapidly to CO, CO<sub>2</sub> and  $H_2O$  because the reactivity of the adsorbed oxygen is so strong compared to that of lattice oxygen atoms, as described earlier.

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