

were grouped together as  $K_2$  and the equation for  $(HTU)_S$  for the solid beads could be written as

$$(HTU)_S = K_2(\mu/\rho D_v)^{0.68} \quad (8)$$

with a value of  $K_2$  ranging from 0.017 to 0.03 for the different systems reported in this investigation.

Further work will be necessary on more systems before a more general correlation can be developed. A more extensive study with systems and packings, varied over a wide range of properties, is in progress in these laboratories, and a more general correlation is close at hand.

#### NOMENCLATURE

- $a$  = interfacial contact area per unit tower volume, surface area of packing per cu. ft.  
 $C$  = concentration in lb. moles/cu. ft.  
 $\Delta C$  = over-all concentration difference in lb. moles/cu. ft.  
 $D_v$  = diffusivity  
 $g$  = acceleration due to gravity  
 $x$  = fractional volumetric holdup of dispersed phase, cu. ft./cu. ft.  
 $HTU_{OX}$  = height of over-all transfer unit based on X-phase in ft.  
 $HTU_X$  = height of individual transfer unit of X-phase in ft.  
 $ka$  = individual volumetric mass transfer coefficient in lb. moles/(hr.) (cu. ft.) ( $\Delta C$ )  
 $m$  = slope of equilibrium line =  $dC_c/dC_d$  or  $dC_w/dC_c$   
 $N$  =  $N'/\theta$  = rate of solute transfer in lb. moles/hr.  
 $Re$  = Reynolds' number  
 $U$  = superficial velocity in ft./hr., (flow rate of phase referred in cu. ft./ (hr.) (sq. ft.)  
 $v$  = volume of tower  
 $\epsilon$  or  $F$  = void fraction  
 $\sigma$  or  $\gamma$  = interfacial tension in dynes/cm.  
 $\rho$  = density in lb./cu. ft.  
 $\rho'$  = specific gravity  
 $\mu$  = viscosity in lb./ft.(sec.),  $\mu'$  = viscosity in centipoises  
 $K_1$  = constant in the correlation for ring packings  
 $K_2$  = constant in the correlation for bead packings  
 $\theta$  = time in hours

#### Subscripts

- W or C = water, continuous phase  
 S or D = solvent, dispersed phase  
 K, M, P, T = kerosine, methyl isobutyl ketone, Pegasol, and toluene, respectively  
 l.m. = logarithmic mean  
 av = average

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#### CORRECTION

In "Fall of Liquid Drops in Water. Drag Coefficients, Peak Velocities, and Maximum Drop Sizes" [P.M. Krishna, D. Venkateswarlu, and G.S.R. Narasimhamurty, *J. Chem. Eng. Data* **4**, 340 (1959)] Equations 5, 6, 8, and 9 on page 343 should read as follows

$$(Re/We)_P = 0.3592 Sd^{0.8260} \quad (5)$$

$$U_P = 2.784/Sd^{0.8260} \quad (6)$$

$$(Re/We)_M = 0.6883 Sd^{0.7567} \quad (8)$$

$$U_M = 1.453/Sd^{0.7567} \quad (9)$$

The constants in the equations may be rounded off as

suggested by Markowitz (3) to have the correlations workable and meaningful.

Regarding the Weber number, this dimensionless group is stated as  $D\rho U^2\sigma$  by Hu and Kintner (1) and Johnson and Braida (2). Other workers have defined the Weber number as  $D\rho U^2\sigma g_c$ . If it is necessary to include  $g_c$  to be consistent with the definition of the  $Sd$  group, it can be defined as  $D\rho U^2/\sigma g_c$ .

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