

Figure 4. Viscosities of water-methanol mixtures, $\eta$, vs. mole per cent methanol

$$
\begin{equation*}
\eta \text { (Millipoises) }=\sum_{i=0}^{4} a_{i} t^{i} \tag{10}
\end{equation*}
$$

This empirical representation by a power series is more precise, within this range of temperature, than that predicted by the theoretically based equations suggested by Gutmann and Simmons (5) for viscosity of liquids in general or by Kampmeyer (10) and by Innes (7) for water and mercury. It is also more precise than that predicted by the equation:

$$
\begin{equation*}
\eta=a /(b+t)^{n} \tag{11}
\end{equation*}
$$

used in the International Critical Tables (9) for methanol. A simple theoretical temperature dependence equation for viscosity of mixtures of liquids has not yet been derived.

## literature cited

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## CORRECTION

In "Critical Properties of Mixtures of Normal Paraffin Hydrocarbons" [Doyle O. Etter and W.B. Kay, J. Chem. Eng. Data 6, 409 (1961)], the legends for Figures 2 and 3 should be reversed.

Equation 5 should read:

$$
P_{\mathrm{c}}=P_{\mathrm{c}_{L}}+\left[9400 M_{L}^{-1.71} x_{L} 2.06 M_{L}^{-0.115}-557 M_{L}-1.265\right]\left(M_{a v .}-M_{L}\right)
$$

Equation 31 should read:

$$
\begin{aligned}
\phi_{4}\left(P_{c d_{4}}, x_{4}\right)= & a_{4}\left(\frac{\left.x_{4}\right]}{1-x_{1}-x_{2}-x_{3}}\right)^{b_{4}} \\
& {\left[\frac{M_{a v}-M_{1} W_{1}-M_{2} W_{2}-M_{3} W_{3}}{1-W_{1}-W_{2}-W_{3}}-M_{4}\right]\left(1-x_{1}-x_{2}-x_{3}\right) }
\end{aligned}
$$

