## Viscosity of Gaseous Air at Moderate and High Pressures

HING Y. LO, DANIEL L. CARROLL, and LEONARD I. STIEL
Syracuse University, Syracuse, N. Y.


#### Abstract

A viscosity correlation for air has been developed for temperatures up to $600^{\circ} \mathrm{C}$. and pressures to 1000 atm. Experimental viscosities available in the literature were utilized to establish the atmospheric viscosity behavior of air. A linear relationship resulted when, for each experimental high pressure value, the residual viscosity, $\mu-\mu^{*}$, was plotted against the corresponding value of $P_{T} / T$. The high pressure viscosity behavior was confirmed by the use of experimental data for nitrogen and oxygen. This information enabled viscosity values to be established for gaseous air for a complete range of temperatures and pressures.


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The values of the viscosity of gases at moderate and high pressures are required in many important applications. Accurate experimental data are not available for air for the complete range of temperatures and pressures in the dense gaseous region. The only previous correlation for the viscosity of air is that of Granet and Kass (17) which was based on the approximate reduced state correlation of Uyehara and Watson (45), and which is applicable only for pressures to 2000 p.s.i.a. Therefore, in the present study, relationships have been developed for the viscosity of gaseous air at moderate and high pressures for temperatures to $600^{\circ} \mathrm{C}$. and pressures to 1000 atm .

## VISCOSITY BEHAVIOR AT NORMAL PRESSURES

Experimental values of the viscosity at atmospheric pressure, $\mu^{*}$, reported by 37 investigators for air were obtained from the literature and plotted against the corresponding temperature. In Table I, the sources are listed along with the temperature ranges investigated. The data for most of the references were consistent with each other and permitted the moderate pressure viscosity behavior of air to be established with a high degree of accuracy for temperatures up to $2500^{\circ} \mathrm{K}$. In Figure 1, the resulting relationship between viscosity and temperature is presented, with experimental points obtained from the 12 major sources

| Table I. Source of Viscosity Data and Average Deviations for Air at Atmospheric Pressure |  |  |  |
| :---: | :---: | :---: | :---: |
| Source | Number of Points | Temperature <br> Range, ${ }^{\circ} \mathrm{K}$. | $\underset{\%}{\text { Av. Dev., }}$ |
| Bonilla, Brooks, and Walker (7) | 24 | 200-2500 | 0.89 |
| Braune, Basch, and Wentzel (8) | 25 | 293-944 | 1.47 |
| Bremond (10) | 19 | 291-1407 | 1.27 |
| Grindley and Gibson (18) | 57 | 273-373 | 0.70 |
| Johnston and McCloskey (24) | 15 | 90-300 | 0.53 |
| Shilling and Laxton (37) | 36 | 342-1120 | 0.80 |
| Sutherland and Masss (39) | 8 | 79-294 | 1.85 |
| Titani ( 40,41 ) | 11 | 293-550 | 0.36 |
| Trautz and Ludewigs (43) | 17 | 287-524 | 0.23 |
| Trautz and Zink (44) | 48 | 554-1102 | 0.46 |
| Vasilesco (47) | 36 | 273-1845 | 0.57 |
| Williams (48) | 135 | 462-1275 | 1.39 |
| Others | 58 | 250-720 | 0.86 |

Minor sources (less than eight data points) are: (2, 3, 6, 9, 12-15, 19, 21-23, 25-27, 29, 30, 33-36, 42, 46, 49).


Figure 1. Relationship between viscosity and temperature for air at moderate pressure


Figure 2. Relationship between $\mu-\mu^{\star}$ and $P_{T / T}$ for air
listed in Table I. Representative data points from the other sources are also included.

For temperatures in the range $70^{\circ} \mathrm{K} . \leqq T \leqq 250^{\circ} \mathrm{K}$., the curve of Figure 1 can be expressed analytically as follows:

$$
\begin{equation*}
\left(\mu^{*}\right)^{1.3}=(20.11 T-375) \times 10^{-6} \tag{1}
\end{equation*}
$$

where the viscosity is in centipoises. Similarly, for $250^{\circ} \mathrm{K}$.


Figure 3. Relationship between $\left(\mu-\mu^{*}\right) \xi$ and $\left(\partial P_{R} / \partial T_{R}\right)_{V_{R}}$ for nitrogen, oxygen, and air
$\leqq T \leqq 2500^{\circ} \mathrm{K}$., the viscosity dependence on temperature can be expressed as

$$
\begin{equation*}
\mu^{*}=\left(4.38 \times 10^{-2}\right)\left(1.01 \times 10^{-3} T-0.093\right)^{5 / 9} \tag{2}
\end{equation*}
$$

The relationship of Figure 1 has been terminated at $2500^{\circ} \mathrm{K}$., at which point dissociation becomes appreciable. Theoretical values of the viscosity of dissociated air have
been calculated by Bade, Mason, and Yun (1) and are tabulated for temperatures from $3000^{\circ}$ to $8000^{\circ} \mathrm{K}$. and pressures from one to 1000 atm .

Viscosity values calculated with Equations 1 and 2 agree very well with those tabulated by Hilsenrath (20) for air


Figure 4. Viscosity correlation for air in gaseous region
for temperatures below $100^{\circ} \mathrm{K}$. For temperatures below $200^{\circ} \mathrm{K}$., the data of Johnston and McCloskey (24) are slightly higher than those of Sutherland and Maass (39). To establish the viscosity behavior in this region, values of the group $\mu^{*} \xi$ (where $\xi=T_{c}^{1 / 6} / M^{1 / 2} P_{c}^{2 / 3}$ ) for nitrogen, oxygen, and air were plotted against the corresponding reduced temperature. Stiel and Thodos (38) have shown that a unique relationship should result for all nonpolar gases when plotted in this manner. The points of Johnston and McCloskey fell on the curve resulting from the data for oxygen and nitrogen, and, therefore, these data were accepted for use in this study.

The average deviation between experimental viscosities and those calculated from Equations 1 and 2 are presented in Table I. The resulting over-all average deviation is $0.94 \%$ for 489 points.

## VISCOSITY BEHAVIOR IN THE DENSE GASEOUS REGION

The experimental data available for the viscosity of air at elevated pressures are those of Kestin and Wang (27) for $298^{\circ} \mathrm{K}$. and pressures from 2 to 100 atm., Kestin and Leidenfrost (26) for temperatures from $293^{\circ}$ to $298^{\circ} \mathrm{K}$. and pressures from 4 to 70 atm ., Biles and Putnam (5) for $297^{\circ}$ to $543^{\circ} \mathrm{K}$. and 7 to 61 atm., Iwasaki (23) for $323^{\circ}$ to $423^{\circ} \mathrm{K}$. and 10 to 200 atm ., Kellstrom (25) for $293^{\circ} \mathrm{K}$. and 8 to 30 atm ., Golubev (15) for $273^{\circ}$ to $373^{\circ} \mathrm{K}$. and 20 to 300 atm ., Makita (30) for $298^{\circ}$ to $473^{\circ} \mathrm{K}$. and 97 to 775 atm., Nasini and Pastonesi (32) for $287^{\circ} \mathrm{K}$.

Table II. Viscosity Values of Gaseous Air (Centipoises $\times 10^{-5}$ )

| Pressure, Atm. | $-70^{\circ} \mathrm{C}$. | $-50^{\circ} \mathrm{C}$. | $-25^{\circ} \mathrm{C}$. | $0^{\circ} \mathrm{C}$. | $25^{\circ} \mathrm{C}$. | $50^{\circ} \mathrm{C}$. | $75^{\circ} \mathrm{C}$. | $100^{\circ} \mathrm{C}$. | $150^{\circ} \mathrm{C}$. |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 1 | 1350 | 1455 | 1590 | 1710 | 1820 | 1925 | 2050 | 2160 | 2360 |
| 20 | 1401 | 1500 | 1628 | 1743 | 1850 | 1953 | 2075 | 2183 | 2380 |
| 50 | 1526 | 1604 | 1700 | 1810 | 1912 | 2008 | 2126 | 2227 | 2419 |
| 75 | 1654 | 1726 | 1769 | 1873 | 1966 | 2054 | 2160 | 2266 | 2454 |
| 100 | 1784 | 1856 | 1871 | 1951 | 2033 | 2115 | 2218 | 2312 | 2496 |
| 150 | 2145 | 2122 | 2140 | 2132 | 2188 | 2253 | 2327 | 2410 | 2584 |
| 200 | 2743 | 2540 | 2368 | 2330 | 2349 | 2384 | 2460 | 2504 | 2661 |
| 250 | 3192 | 2918 | 2646 | 2564 | 2551 | 2554 | 2611 | 2635 | 2778 |
| 300 | 3633 | 3297 | 2933 | 2795 | 2741 | 2742 | 2753 | 2761 | 2853 |
| 350 | 4084 | 3654 | 3226 | 3033 | 2954 | 2896 | 2923 | 2897 | 2952 |
| 400 | 4544 | 4016 | 3505 | 3285 | 3163 | 3117 | 3061 | 3042 | 3054 |
| 450 | 4988 | 4385 | 3789 | 3521 | 3375 | 3254 | 3224 | 3183 | 3166 |
| 500 | 5450 | 4737 | 4065 | 3761 | 3577 | 3429 | 3381 | 3245 | 3271 |
| 550 | 5895 | 5093 | 4335 | 4004 | 3777 | 3608 | 3534 | 3463 | 3377 |
| 600 | 6368 | 5442 | 4619 | 4250 | 3987 | 3788 | 3702 | 3607 | 3482 |
| 700 | 7270 | 6150 | 5172 | 4717 | 4390 | 4145 | 4007 | 3889 | 3717 |
| 800 | 8176 | 6788 | 5667 | 5158 | 4794 | 4491 | 4342 | 4169 | 3939 |
| 900 | 9022 | 7363 | 6078 | 5539 | 5164 | 4829 | 4665 | 4448 | 4165 |
| 1000 | 9756 | 7910 | 6458 | 5878 | 5510 | 5152 | 4943 | 4721 | 4409 |
|  | $200^{\circ} \mathrm{C}$. | $250^{\circ} \mathrm{C}$. | $300^{\circ} \mathrm{C}$. | $350^{\circ} \mathrm{C}$. | $400^{\circ} \mathrm{C}$. | $450^{\circ} \mathrm{C}$. | $500^{\circ} \mathrm{C}$. | $550^{\circ} \mathrm{C}$. | $600^{\circ} \mathrm{C}$. |
| 1 | 2570 | 2740 | 2920 | 3090 | 3255 | 3400 | 3550 | 3690 | 3830 |
| 20 | 2588 | 2756 | 2935 | 3104 | 3267 | 3410 | 3559 | 3698 | 3837 |
| 50 | 2621 | 2786 | 2961 | 3126 | 3286 | 3429 | 3576 | 3714 | 3851 |
| 75 | 2648 | 2804 | 2982 | 3145 | 3303 | 3444 | 3591 | 3728 | 3866 |
| 100 | 2679 | 2835 | 3006 | 3165 | 3320 | 3459 | 3605 | 3742 | 3878 |
| 150 | 2742 | 2893 | 3058 | 3205 | 3356 | 3494 | 3636 | 3772 | 3908 |
| 200 | 2807 | 2949 | 3113 | 3256 | 3413 | 3538 | 3671 | 3782 | 3915 |
| 250 | 2893 | 3024 | 31.72 | 3308 | 3456 | 3584 | 3703 | 3826 | 3952 |
| 300 | 2974 | 3096 | 3228 | 3354 | 3497 | 3572 | 3742 | 3859 | 3987 |
| 350 | 3063 | 3179 | 3288 | 3408 | 3546 | 3667 | 3784 | 3916 | 4030 |
| 400 | 3148 | 3251 | 3351 | 3459 | 3590 | 3709 | 3819 | 3946 | 4064 |
| 450 | 3232 | 3320 | 3413 | 3512 | 3642 | 3752 | 3859 | 3976 | 4101 |
| 500 | 3327 | 3387 | 3472 | 3567 | 3693 | 3804 | 3902 | 4023 | 4144 |
| 550 | 3414 | 3456 | 3540 | 3626 | 3744 | 3834 | 3946 | 4059 | 4182 |
| 600 | 3500 | 3537 | 3604 | 3690 | 3793 | 3896 | 3989 | 4112 | 4217 |
| 700 | 3679 | 3687 | 3743 | 3806 | 3897 | 3927 | 4079 | 4183 | 4296 |
| 800 | 3867 | 3855 | 3879 | 3934 | 4010 | 4094 | 4173 | 4279 | 4375 |
| 900 | 4070 | 4025 | 4027 | 4066 | 4124 | 4191 | 4272 | 4365 | 4453 |
| 1000 | 4272 | 4209 | 4173 | 4205 | 4243 | 4298 | 4377 | 4458 | 4524 |

and 35 to 200 atm., and Moulton and Beuschlein (31) for $303^{\circ} \mathrm{K}$. and 9 to 300 atm . The data of Moulton and Beuschlein (31) scattered considerably and therefore were not included in this study. The only data available for pressures greater than 300 atm . are those of Makita (30) which were obtained by the rolling-ball method.

Isotherms of the viscosity of a gas against density are parallel, indicating that a unique relationship should exist between $\mu-\mu^{*}$ and density, where $\mu$ is the viscosity of a gas at a certain temperature and pressure and $\mu^{*}$ is the viscosity at the same temperature and atmospheric pressure. When values of $\mu-\mu^{*}$ for each experimental point for air were plotted in this manner against the corresponding density, a single curve did not result for the data of Makita for the high pressure region, indicating that these data may be in error. Since these are the only values available for this region, an alternate procedure was utilized to establish the high pressure viscosity behavior of air.

Golubev (16) has shown through theoretical arguments that the residual viscosity of a gas, $\mu^{\mu-\mu^{*}}$, should be a unique function of $P_{T} / T$, where $P_{T}=T[(\partial P) /(\partial T)]_{V}$ is the thermal pressure. Golubev (16) plotted $\mu-\mu^{*}$ for the dense gaseous and liquid regions vs. $P_{T} / T$ for a number of substances and obtained linear relationships. These linear relationships were confirmed by Lennert and Thodos (28) for the inert gases for the dense gaseous region considered in this paper. The use of the thermal pressure therefore has the advantage that the line resulting from accurate low pressure data can be extrapolated to determine the high pressure values. To obtain values of $P_{T} / T$ for air, thermal pressures were calculated from the derived data of Deming and Shupe (11) for nitrogen. Values of $P_{T R} /$ $T_{R}=P_{r} / P_{c} T_{R}$ were calculated and plotted against reduced temperature for parameters of reduced pressure. A crossplot was then prepared of $P_{T R} / T_{R}$ against $P_{R}$ for values of $T_{R}$ corresponding to the temperatures for which experimental data for air were obtained. Values of $P_{T /} T$ for each experimental point for air were then calculated and plotted vs. $\mu-\mu^{*}$, as shown in Figure 2.

Figure 2 shows that most of the data fall on a single line. The deviations of the experimental points from this line for $P_{T} / T<0.3$ are not significant, since $\mu-\mu^{*}$ represents a viscosity difference. The maximum deviation from the line for this region is about 50 centipoises, which corresponds to a maximum per cent error of approximately $2.5 \%$ between the experimental viscosity and that calculated from the line. However, the experimental points of Makita (30) for $423^{\circ}$ and $473^{\circ} \mathrm{K}$. at high pressures exhibit significant deviations, with a maximum of approximately $10 \%$. The relationship of Figure 2 can be expressed analytically as follows:

$$
\begin{equation*}
\mu-\mu^{*}=5.76 \times 10^{-3}\left(P_{T /} T\right)^{1.28} \tag{3}
\end{equation*}
$$

Lennert and Thodos (28) have also shown that a single line should result when the group $\left(\mu-\mu^{*}\right) \xi$ is plotted vs. $P_{T R} / T_{R}$ for substances having a similar nature. Therefore, to confirm the high pressure viscosity behavior of air represented by Equation 3, values of $\left(\mu-\mu^{*}\right) \xi$ for nitrogen and oxygen calculated from the data of Golubev and Petrov (16) were plotted against $P_{\tau R} / T_{R}$, as shown in Figure 3. The nitrogen data covered temperatures to $523^{\circ} \mathrm{K}$. Equation 3 for air was expressed in the following reduced form by the use of the critical constants of air:

$$
\begin{equation*}
\left(\mu-\mu^{*}\right) \xi=5.25 \times 10^{-5}\left(P_{T_{R}} / T_{R}\right)^{1.126} \tag{4}
\end{equation*}
$$

Equation 4 was also included in Figure 3. Figure 3 shows that Equation 4 represents well the viscosity behavior of oxygen, nitrogen, and air.

Equation 3 was used in conjunction with the atmospheric viscosity relationship of Figure 1 and the plots for $P_{T R} /$ $T_{R}$ to establish viscosity values for air for temperatures
to $873^{\circ} \mathrm{K}$. and pressures to 1000 atm . These viscosity values were plotted against the corresponding temperatures and pressures to produce the viscosity correlation for air presented in Figure 4. Viscosity values for even intervals of temperature and pressure are presented in Table II. Viscosity values for air can also be calculated from Equation 3 by the use of an appropriate equation of state such as the Beattie-Bridgeman equation (4), to establish values of $P_{T} / T$.

## NOMENCLATURE

| $M$ | $=$ molecular weight |
| ---: | :--- |
| $P$ | $=$ pressure, atm. |
| $P_{c}$ | $=$ critical pressure, atm. |
| $P_{T}$ | $=$ thermal pressure, $T[(\partial P) /(\partial T)]_{v,}$, atm. |
| $P_{T_{R}}$ | $=$ reduced thermal pressure, $T_{R}\left(\left(\partial P_{R}\right) /\left(\partial T_{R}\right)\right]_{V}$ |
| $T$ | $=$ temperature, ${ }^{\circ} \mathrm{K}$. |
| $T_{c}$ | $=$ critical temperature, ${ }^{\circ} \mathrm{K}$. |
| $T_{R}$ | $=$ reduced temperature, $T / T_{c}$ |

## Greek Letters

$\mu=$ viscosity, centipoises
$\mu^{*}=$ viscosity at moderate pressures ( $0.2-5 \mathrm{~atm}$.), centipoises
$\xi=$ viscosity, parameter, $T_{c}^{1 / 6} / M^{1 / 2} P_{c}^{2 / 3}$

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# Latent Heat of Vaporization 

D. S. VISWANATH and N. R. KULOOR<br>Department of Chemical Engineering, Indian Institute of Science, Bangalore, India

IIn A PREVIOUS PAPER (3), a correlation was presented for calculating latent heats of vaporization at the normal boiling point. The authors at that time missed the excellent papers by Fishtine (1). It is the purpose

Table I. Comparison of Calculated $\lambda_{b}$ Values

| Compound | $\lambda_{b}$ Calcd., Cal./G. | $\%$ Dev. |
| :---: | :---: | :---: |
| Acetaldehyde | 145.5 | -0.20 |
| Acetic anhydride | 94.5 | -1.40 |
| Benzaldehyde | 96.0 | -1.16 |
| Benzyl alcohol | 115.2 | -2.58 |
| Bromobenzene | 58.0 | -0.70 |
| iso-Butyl iso-butyrate | 62.8 | 0.80 |
| iso-Butyl $n$-butyrate | 65.3 | -1.24 |
| Carvacrol | 82.0 | 0.61 |
| Chlorobenzene | 77.0 | 0.80 |
| $o$-Chlorotoluene | 73.0 | -0.55 |
| $p$-Chlorotoluene | 73.5 | -0.50 |
| Di-iso-butylamine | 71.0 | -2.60 |
| Diethyloxalate | 73.7 | 0.0 |
| Dimethylamine | 137.2 | 2.14 |
| Dimethylaniline | 85.3 | -1.91 |
| Dimethyloxalate | 85.6 | 1.39 |
| Diphenylsulfide | 67.5 | -1.51 |
| Ethyl phenyl ether | 80.5 | 0.88 |
| Furfural | - 106.0 | 1.45 |
| 1-Heptanol | 101.0 | 3.71 |
| Hydroquinone | 140.0 | 3.09 |
| Methylamine | 198.0 | 0.25 |
| Methylmercaptan | $1 ? 1.0$ | 0.82 |
| Methyl sulfide | 104.5 | -0.87 |
| Napthalene | 80.5 | 0.38 |
| $o$-Nitrobenzaldehyde | 89.5 | 4.20 |
| Nitrobenzene | 90.2 | -1.80 |
| Nitromethane | 141.0 | -4.50 |
| o-Nitrophenol | 83.2 | -2.60 |
| 1-Octanol | 94.0 | -3.60 |
| Phenylacetonitrile | 98.6 | -0.61 |
| Phthalic anhydride | 89.2 | -1.02 |
| $\alpha$-Picolene | 91.5 | 1.92 |
| Piperdine | 96.5 | -1.47 |
| Pipernol | 86.0 | -2.74 |
| Pyridine | 104.5 | 2.60 |
| Salicylaldehyde | 89.2 | 3.24 |
| 2,3,4,6 Tetrachlorophenol | 58.0 | -0.20 |
| 1,2,3 Trichlorobenzene | 59.2 | -1.71 |
| 1,3,5 Trichlorobenzene | 58.0 | -3.57 |
| 2,3,5 Trimethylacetophenone | 74.5 | 2.10 |
| Trimethylamine | 95.0 | -2.48 |
| 2,4 Xyaldehyde | 83.2 | -1.58 |

Average deviation of the 43 compounds $=1.7 \%$.
of the present work to show that the correlation presented earlier is comparable to the modified Kistiakowsky relation proposed by Fishtine.

The equation proposed earlier (3) is

$$
\begin{equation*}
\lambda_{b}=\frac{4.7 T_{c}\left(1.0-P r_{b}\right)^{0.59} \log P r_{b}}{\left(1-1 / T r_{b}\right)} \tag{1}
\end{equation*}
$$

Earlier, this equation was used to predict $\lambda_{t}$ for about 90 substances with an average deviation of about $1.8 \%$. Equation 1 is used to predict $\lambda_{b}$ values for substances considered by Fishtine and the results are shown in Table
I. The input data used are those listed by Fishtine. In Table I, the first values after each substance give the calculated value of $\lambda_{b}$, and the second give per cent deviation defined as $\left(\lambda_{F}-\lambda_{b}\right) 100 / \lambda_{F}$ where $\lambda_{F}$ is the value given by Fishtine in his final paper under the column "Author's Choice".

In a recent paper (2), Fishtine has compared the different methods of predicting latent heat at the normal boiling point, but the author has not used the present methodEquation 1-in such a comparison. From Table I of the previous paper (3), the following table is prepared. In the case of a total of 143 substances tested, the present method gives an average deviation of $1.75 \%$.

| Table II. Comparison of Latent Heat Correlations at $T_{b}$ |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: |
|  | $\begin{aligned} & \text { No. of } \\ & \text { Sub- } \\ & \text { stances } \end{aligned}$ | Present | Riedel's | Giacolone's |
| Compound Group | Tested | Method | Method | Method |
| Inorganic | 8 | 1.45 | 2.20 | 2.00 |
| Hydrocarbons | 18 | 2.45 | 1.92 | 2.44 |
| All substances | 51 | 1.70 | 2.27 | 2.20 |

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