

Figure 1. Solid-liquid phase diagram of the system hydra-zine-1,1-dimethylhydrazine
straightforward. The components were purified by distillation in nitrogen atmosphere in the presence of sodium hydroxide in the case of hydrazine, and at reduced pressure in the presence of calcium hydride in the case of 1,1-dimethylhydrazine (1), collecting the middle fraction and discarding the first and last $25 \%$ of the distillate. Chromatographic runs did not show any appreciable peak owing to impurities in the case of hydrazine. A faint, unidentified peak was always present in the case of 1,1-dimethylhydrazine. The samples were prepared by weighing the pure components. The molar fractions are therefore certain to within $\pm 0.005$. The samples were sealed in borosilicate glass cells (2) in a nitrogen atmosphere and kept in the dark. Thermal analysis of these samples was repeated at intervals over a period of six months with very good reproducibility of results. Samples that were not kept in the dark showed visible signs of decomposition with development of a yellow color and exhibited, in general, depression of the liquidus and solidus points. Thermal analysis was performed following a procedure described elsewhere (2). The temperatures were measured with copper-constanant thermocouples and a recorder with a resolution of

Table I. Solidus and Liquidus Temperatures of the System Hydrazine-1,1-Dimethylhydrazine

| Molar Fraction <br> of 1,1-Dimethyl- <br> hydrazine | Solidus <br> Temp., <br> o K. | Liquidus <br> Temp., <br> o K. |
| :---: | :---: | :---: |
| 0.00 | $\ldots$. | 275 |
| 0.01 | 214 | 275 |
| 0.05 | 214 | 274 |
| 0.20 | 214 | 271 |
| 0.35 | 214 | 269 |
| 0.50 | 214 | 262 |
| 0.55 | 214 | 260 |
| 0.59 | 214 | 257 |
| 0.72 | 214 | 250 |
| 0.83 | 214 | 225 |
| 0.90 | 214 | 220 |
| 0.95 | 214 | 215 |
| 0.99 | $\cdots$ | 216 |
| 1.00 | $\cdots$ | 216 |

$0.2^{\circ} \mathrm{K}$. Since the rates of cooling and warming were always kept well below one degree per minute, the thermal homogeneity of the sample was better than $0.2^{\circ} \mathrm{K}$., which leads to a maximum uncertainty in the temperature of $0.2^{\circ} \mathrm{K}$. Table I displays the solidus and liquidus temperatures for various compositions.

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# Refractive Indices of Some Ternary Systems Containing Naphthalene 

## Binary Solvent Mixtures Containing Hexane or Cyclohexane

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ININ PREVIOUS publications, refractive indices of some ternary systems containing naphthalene have been reported $(4,5)$. Those studies were concerned with the six solvent pairs from among benzene, toluene, ethylbenzene, and carbon tetrachloride (4) and the six solvent pairs of hexadecane with each of benzene, toluene, ethylbenzene, carbon tetrachloride, hexane, and cyclohexane (5). Also included were the pertinent binary subsystems. The first set of ternary systems is

[^0]characterized by a small energy of interaction between the components ( 1,2 ), and relatively small differences in component molar volumes. The second set involved systems containing components of greater dissimilarity.

The present work concludes the study of the set of naphthalene-mixed solvent systems, adding the remaining nine ternaries of the total of 21 possible for naphthalene with these solvent components. All of the present systems contain hexane or cyclohexane as one of the mixed solvent components. As in the previous two works, the question of the suitability of equations used in representing the experimental data is considered.


#### Abstract

Refractive indices have been determined at $25^{\circ} \mathrm{C}$. for ternary systems of naphthalene with nine mixed solvents containing hexane or cyclohexane and for nine of the binary solvent subsystems. Equations are given relating refractive index to solution composition in mole fraction. The average deviations in the ternary systems from predicted refractive indices by these equations range from 4 to $20 \times 10^{-5}$ units among the systems.


## EXPERIMENTAL DATA

Equipment, experimental procedure, and chemicals used have been described previously (4). All present refractive indices $(n)$ refer to $25.00 \pm 0.01^{\circ} \mathrm{C}$. and the sodium D-line, 5893A. Binary solvent system data are given in Table I. Data for the naphthalene-solvent binaries have been reported previously ( 4,5 ).

Ternary system data are given in Table II. As previously ( 4,5 ), the data reported in each system have been reduced to 20 points from the total number recorded. The reported data represent the extent of the concentration range covered, and include several points within a few hundredths mole fraction of naphthalene saturation. All data are quite removed in concentration from the binaries, so that rigorous tests of the ternary equations used for data fitting should obtain.

## REPRESENTATION OF DATA BY ANALYTICAL FUNCTIONS

In the binary systems, $n$ has been expressed as

$$
\begin{equation*}
n=n_{1} x_{1}+n_{2} x_{2}+x_{1} x_{2} A_{12} \tag{1}
\end{equation*}
$$

where $n_{1}$ and $x_{1}$ are the refractive index and mole fraction, respectively, of pure component $i . A_{12}$ is a concentration dependent function defined by

$$
\begin{equation*}
A_{12}=B_{12}+C_{12}\left(x_{1}-x_{2}\right)+D_{12}\left(x_{1}-x_{2}\right)^{2} \tag{2}
\end{equation*}
$$

where $B_{12}, C_{12}, D_{12}$ are empirical constants evaluated from experimental $n$ data. The constants of Equation 2 are listed in Table III. Columns 4 and 5 of Table I list the standard and average deviations of experimental $n$ from those predicted with Equation 1.

In representing ternary behavior, the equation has been used:

$$
\begin{align*}
& n=n_{1} x_{1}+n_{2} x_{2}+n_{3} x_{3}+x_{1} x_{2} A_{12}+ \\
& x_{1} x_{3} A_{13}+x_{2} x_{3} A_{23}+A_{123} \tag{3}
\end{align*}
$$

$A_{123}$ is a three component difference term which will be zero if the binary coefficients only are needed to calculate refractive index for the ternary mixtures. The data show that calculation of the refractive index using only the binary coefficients $A_{12}, A_{13}$, and $A_{23}$ leads to large errors in all present ternary systems. For the naphtha-lene-solvent systems, the constants are based upon the assignment of 1.62615 as $n$ of the supercooled state of naphthalene (4).

The difference term $A_{123}$ can be represented by Equation 4:
$A_{123}=B_{123}+C_{193} x_{2}+D_{123} x_{2}+$

$$
E_{123} x_{1}{ }^{2}+F_{123} x_{2}{ }^{2}+G_{123} x_{1} x_{2}
$$

Combining Equations 3 and 4 gives Equation 3a. An attempt to simplify Equation 3a by assigning the value zero to $E_{123}, F_{123}, G_{123}$ gives an Equation 3 b which is less adequate. In using Equation 3a or 3 b it is, of course, understood that the binary coefficients are first calculated using Equation 2 (see Table III). The ternary coefficients are taken from Table IV.

| Table I. Refractive Indices of Binary Systems at $25^{\circ} \mathrm{C}$. |  |  |
| :---: | :---: | :---: |
| System | Mole Fraction First-Named Component | Exptl. Refr. Index |
| Cyclohexane-ethylbenzene | 0.8187 | 1.43550 |
|  | 0.5796 | 1.45232 |
|  | 0.4097 | 1.46431 |
|  | 0.2289 | 1.47690 |
|  | By Eq. 1: Std. and Av. Dev. $10^{5}=2$ |  |
| Cyclohexane-toluene | 0.79051 .43573 |  |
|  | 0.6193 | 1.44704 |
|  | 0.4121 | 1.46176 |
|  | 0.2558 | 1.47361 |
|  | $\begin{gathered} \text { By Eq. 1: St } \\ \text { Dev. } 10^{5}= \end{gathered}$ | and Av. |
| Cyclohexane-benzene | 0.76241 .43590 |  |
|  | 0.5852 | 1.44715 |
|  | 0.4042 | 1.46037 |
|  | 0.2099 | 1.47688 |
|  | By Eq. 1: Std. and Av. |  |
| Cyclohexane-carbon tetrachloride | 0.78071 .42970 |  |
|  | $0.5900 \quad 1.43575$ |  |
|  | 0.42921 .44113 |  |
|  | $\begin{array}{cc} 0.2638 & 1.44708 \\ \text { By Eq. } 1: & \text { Std. and Av. } \\ \text { Dev. } 10^{5}=2 \end{array}$ |  |
|  |  |  |
| Hexane-ethylbenzene | $\begin{array}{ll}0.8137 & 1.39373 \\ 0.5773 & 1.42153\end{array}$ |  |
|  |  |  |
|  | $\begin{array}{ll}0.5773 & 1.42153 \\ 0.4036 & 1.44245\end{array}$ |  |
|  | 0.18441 .46970 |  |
|  | $\begin{aligned} & \text { By Eq. 1: Std. Dev. } \\ & 10^{5}=3, \text { Av. Dev. } 10^{5}= \end{aligned}$ |  |
|  |  |  |
| Hexane-toluene | $0.7684 \quad 1.39587$ |  |
|  | $0.5880 \quad 1.41592$ |  |
|  | 0.41531 .43669 |  |
|  | $0.2351 \quad 1.46027$ |  |
|  | By Eq. 1: Std. and Av. Dev. $10^{5}=2$ |  |
| Hexane-benzene | 0.76441 .39249 |  |
|  | $0.5864 \quad 1.41064$ |  |
|  | 0.40651 .43211 |  |
|  | 0.20071 .46160 |  |
|  | By Eq. 1: Std. and Av. <br> Dev. $10^{5}=2$ |  |
| Hexane-carbon tetrachloride | $0.8118 \quad 1.38459$ |  |
|  | 0.5617 | 1.40308 |
|  | 0.4062 | 1.41600 |
|  | 0.2185 | 1.43368 |
|  | By Eq. 1: Std | $\text { Dev } 10^{5}=$ |
| Cyclohexane-hexane | 0.9102 1.41744 <br> 0.5968 1.39981 <br> 0.3989 1.39001 <br> 0.2157 1.38164 <br> By Eq. 1: Std. and Av. Dev. $10^{5}=1$ |  |
|  |  |  |
|  |  |  |
|  |  |  |
|  |  |  |


| System | Table II. Refractive Indices of Ternary Systems at $25^{\circ} \mathrm{C}$. |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | Mole <br> Fraction FirstNamed Component | Mole <br> Fraction SecondNamed Component | Exptl. <br> Refr. <br> Index | System | Mole <br> Fraction FirstNamed Component | Mole <br> Fraction SecondNamed Component | Exptl. Refr. Index |
| Cyclohexane-benzenenaphthalene | 0.0456 | 0.7297 | 1.52951 | Cyclohexane-carbon tetrachloridenaphthalene | 0.1970 | 0.6345 | 1.48420 |
|  | 0.0430 | 0.6876 | 1.53632 |  | 0.1883 | 0.6063 | 1.49193 |
|  | 0.1603 | 0.6282 | 1.51635 |  | 0.1824 | 0.5876 | 1.49687 |
|  | 0.1574 | 0.6168 | 1.51879 |  | 0.2438 | 0.6803 | 1.46400 |
|  | 0.1513 | 0.5928 | 1.52379 |  | 0.2238 | 0.6245 | 1.48026 |
|  | 0.1999 | 0.7525 | 1.48634 |  | 0.3534 | 0.5051 | 1.47252 |
|  | 0.1913 | 0.7201 | 1.49423 |  | 0.3470 | 0.4960 | 1.47576 |
|  | 0.1729 | 0.6511 | 1.51014 |  | 0.3322 | 0.4748 | 1.48323 |
|  | 0.3271 | 0.4918 | 1.49684 |  | 0.3988 | 0.5305 | 1.45696 |
|  | 0.3145 | 0.4728 | 1.50276 |  | 0.3695 | 0.4915 | 1.47179 |
|  | 0.3866 | 0.5698 | 1.46955 |  | 0.5557 | 0.3861 | 1.44864 |
|  | 0.3530 | 0.5203 | 1.48639 |  | 0.5198 | 0.3612 | 1.46190 |
|  | 0.5557 | 0.3969 | 1.45758 |  | 0.5283 | 0.3480 | 1.46213 |
|  | 0.4993 | 0.3565 | 1.47778 |  | 0.5165 | 0.3402 | 1.46638 |
|  | 0.5057 | 0.3419 | 1.47821 |  | 0.4919 | 0.3240 | 1.47510 |
|  | 0.4868 | 0.3292 | 1.48466 |  | 0.7345 | 0.2064 | 1.44270 |
|  | 0.7259 | 0.2263 | 1.44633 |  | 0.6994 | 0.1965 | 1.45254 |
|  | 0.6585 | 0.2053 | 1.46528 |  | 0.7148 | 0.1719 | 1.45348 |
|  | 0.8355 | 0.0547 | 1. 44985 |  | 0.6872 | 0.1653 | 1.46082 |
|  | 0.8066 | 0.0529 | 1.45652 |  | 0.6765 | 0.1627 | 1.46362 |
|  | Std. Dev. $10^{j}$ : 14 (Eq. 3a), 20 (Eq. 3b) Av. Dev. $10^{5}$ : 11 (Eq. 3a), 14 (Eq. 3b) |  |  |  | Std. Dev. 105: 14 (Eq. 3a), 27 (Eq. 3b) Av. Dev. 10i: 10 (Eq. 3a), 20 (Eq. 3b) |  |  |
|  |  |  |  |  |  |  |  |
| Cyclohexane-toluenenaphthalene | 0.1673 | 0.6404 | 1.50925 |  |  |  |  |
|  | 0.1604 | 0.6139 | 1.51454 |  |  |  |  |
|  | 0.1567 | 0.5998 | 1.51735 | Hexane-benzenenaphthalene | 0.0220 | 0.7520 | 1.53079 |
|  | 0.1545 | 0.5913 | 1.51906 |  | 0.0260 | 0.7054 | 1.53830 |
|  | 0.2428 | 0.7062 | 1.48260 |  | 0.0385 | 0.7421 | 1.52684 |
|  | 0.2203 | 0.6408 | 1.49755 |  | 0.0378 | 0.7286 | 1.52902 |
|  | 0.2101 | 0.6110 | 1.50429 |  | 0.0359 | 0.6920 | 1.53540 |
|  | 0.3332 | 0.4899 | 1.49442 |  | 0.1425 | 0.6571 | 1.50556 |
|  | 0.3179 | 0.4674 | 1.50108 |  | 0.1330 | 0.6133 | 1.51566 |
|  | 0.3102 | 0.4562 | 1.50443 |  | 0.1914 | 0.7625 | 1.47143 |
|  | 0.3887 | 0.5544 | 1.47247 |  | 0.1715 | 0.6832 | 1.49167 |
|  | 0.3695 | 0.5270 | 1.48108 |  | 0.1650 | 0.6572 | 1.49808 |
|  | 0.5889 | 0.3621 | 1.45696 |  | 0.3212 | 0.4721 | 1.47903 |
|  | 0.5559 | 0.3418 | 1. 46749 |  | 0.3133 | 0.4605 | 1.48329 |
|  | 0.5256 | 0.3232 | 1.47704 |  | 0.3893 | 0.5684 | 1.44201 |
|  | 0.7253 | 0.1922 | 1.45297 |  | 0.3724 | 0.5437 | 1.45149 |
|  | 0.6964 | 0.1846 | 1.46057 |  | 0.3408 | 0.4975 | 1.46917 |
|  | 0.6931 | 0.1811 | 1. 46154 |  | 0.5615 | 0.3960 | 1.42092 |
|  | 0.6704 | 0.1751 | 1.46744 |  | 0.5107 | 0.3602 | 1.44179 |
|  | 0.6584 | 0.1720 | 1.47051 |  | 0.4943 | 0.3447 | 1.44895 |
|  | Std. Dev. $10^{5}$ : 10 (Eq. 3a), 21 (Eq. 3b) Av. Dev. $10^{5}$ : 8 (Eq. 3a), 15 (Eq. 3 b ) |  |  |  | 0.7354 | 0.2267 | 1.40181 |
|  |  |  |  | 0.6720 | 0.2071 | 1.42231 |
|  |  |  |  | Std. Dev. $10^{\text {º }}: 27$ (Eq. 3a), 44 (Eq 3b) Av. Dev. 10 ${ }^{\text {it }} 20$ (Eq. 3a), 35 (Eq. 3b) |  |  |
|  | 0.1656 | 0.6346 | 1.50885 |  |  |  |  |
| Cyclohexane-ethyl-benzene-naphthalene | 0.1580 | 0.6054 | 1.51428 |  | - |  |  |
|  | 0.1540 | 0.5904 | 1.51708 |  |  |  |  |
|  | 0.2164 | 0.7289 | 1.48562 |  |  |  |  |
|  | 0.2025 | 0.6820 | 1.49496 | Hexane-toluenenaphthalene | 0.1645 | 0.6228 | 1.50143 |
|  | 0. 1897 | 0.6390 | $1.50353$ |  | 0.1609 | 0.6093 | 1.50439 |
|  | 0.3302 | 0.4966 | 1.49407 |  | 0.1560 | 0.5906 | 1.50845 |
|  | 0.3166 | 0.4760 | 1.49972 |  | 0.2231 | 0.7258 | 1.46979 |
|  | 0,3093 | 0.4651 | 1.50278 |  | 0.2137 | 0.6953 | 1.47709 |
|  | 0.3857 | 0.5558 | 1.47429 |  | 0.2028 | 0.6597 | 1.48554 |
|  | 0.3615 | 0.5209 | 1.48427 |  | 0.1917 | 0.6236 | 1. 49396 |
|  | 0.3459 | 0.4984 | 1.49058 |  | 0.3385 | 0.4942 | 1.47134 |
|  | 0.5426 | 0.3936 | 1.46410 |  | 0.3312 | 0.4835 | 1.47494 |
|  | 0.4996 | 0.3522 | 1.47901 |  | 0.3182 | 0.4646 | 1. 48140 |
|  | 0.4823 0.4694 | 0.3400 0.3309 | 1.48432 1.48831 |  | 0.3934 | 0.5538 | 1.44743 |
|  | 0.7730 | 0.1711 | 1.44688 |  | 0.3742 0.5334 | 0.5268 0.2737 | 1.45704 1.43646 |
|  | 0.7335 | 0.1624 | 1.45680 |  | 0.5105 | 0.3577 | 1.44489 |
|  | 0.7473 | 0.1396 | 1. 45700 |  | 0.5041 | 0.3470 | 1.44798 |
|  | 0.7192 | 0.1344 | 1.46380 |  | 0.4936 | 0.3397 | 1.45193 |
|  | Std. Dev. 3b) Av. | $\begin{aligned} & 10^{5}: 8 \text { (Eq } \\ & \text { Dev. } 10^{5}: \end{aligned}$ | $\begin{aligned} & 3 \mathrm{3a}, 19 \text { (Eq. } \\ & \text { (Eq. 3a), } \end{aligned}$ |  | 0.4832 | 0.3325 | 1.45591 |

(Continued on page 43)


## Table III. Binary System Constants

Constants of Equation $2\left(x_{1}\right.$ is FirstNamed Component)

| System | Named Component) |  |  |
| :---: | :---: | :---: | :---: |
|  | $B_{12}$ | $C_{12}$ | $D_{12}$ |
| Cyclohexane-ethylbenzene | -0.00109 | -0.00086 | -0.00325 |
| Cyclohexane-toluene | -0.01337 | -0.00133 | -0.00061 |
| Cyclohexane-benzene | -0.02948 | 0.00338 | 0.00058 |
| Cyclohexane-carbon tetrachloride | -0.00632 | 0.00064 | -0.00005 |
| Hexane-ethylbenzene | $-0.00841$ | 0.00006 | -0.00016 |
| Hexane-toluene | -0.02833 | 0.00226 | -0.00057 |
| Hexane-benzene | -0.05854 | 0.01336 | -0.00610 |
| Hexane-carbon tetrachloride | -0.02766 | 0.00402 | -0.00119 |
| Cyclohexane-hexane | -0.01195 | $-0.00265$ | -0.00175 |

Columns 5 to 8 of Table II list the standard and average deviations of the experimental $n$ from those predicted with Equations 3 a and 3 b . As was done previously (4, 5), computations in the present work were programmed for a digital computer.

## DISCUSSION

In the present binary solvent-solvent systems, the deviations from Equation 1 resemble more closely those of the first set of systems (4) than the second set (5). The error thus appears to be more dependent upon the difference in molal volumes than upon the molecular interaction between the solvent component pair (1-3) or the difference in $n$ of the pure components.

In the ternary systems, $n$ values calculated with Equation 3 are systematically below the experimental values in all present systems if $A_{123}=0$ is assumed. Both the average and extreme deviations in all present systems are greater by Equation 3b than by 3a. The use of Equations 3a or 3 b yields deviations from experimental results comparable to those found previously $(4,5)$, with no apparent correlation between the error thereby and any of molecular interaction, difference in molal volumes of the pure components or difference in refractive indices of the pure components.

While the usefulness of Equation 3a in the 21 ternary systems considered in these works is limited, it is not markedly affected by increasing dissimilarity between the solvent pair.

Table IV. Ternary System Constants

|  | Equation 3a |  |  |  |  |  | Equation 3b |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| System | $B_{123}$ | $C_{123}$ | $D_{123}$ | $E_{123}$ | $F_{123}$ | $G_{123}$ | $B_{123}$ | $C_{123}$ | $D_{123}$ |
| Cyclohexane-benzenenaphthalene | 2,5907 | -4.5198 | -4.7043 | 1.8113 | 2.3196 | 4.2806 | 0.9763 | -1.0664 | -0.7895 |
| Cyclohexane-toluenenaphthalene | 2.9673 | -5.5511 | -5.4788 | 2.5181 | 2.6979 | 5.2945 | 1.0205 | -1.1092 | -0.8600 |
| Cyclohexane-ethylbenzenenaphthalene | 2.7167 | -4.8873 | -4.9902 | 2.0938 | 2.5301 | 4.4972 | 1.0100 | $-1.1220$ | -0.8365 |
| Cyclohexane-carbon tetra-chloride-naphthalene | 5.4585 | -10.1942 | -11.3500 | 4.7299 | 6.1260 | 10.7561 | 1.3594 | -1.3802 | -1.3127 |
| Hexane-benzenenaphthalene | 3.1835 | -6.7509 | -6.2560 | 3.6274 | 3.2043 | 6.5781 | 0.8402 | -0.9703 | -0.763 |
| Hexane-toluenenaphthalene | 1.5487 | -2.8260 | -2.9444 | 1.2195 | 1.5036 | 2.7235 | 0.5160 | $-0.5800$ | $-0.4395$ |
| Hexane-ethylbenzenenaphthalene | 1.2323 | -2.2293 | -2.1376 | 0.9425 | 0.9983 | 1.9447 | 0.5049 | -0.5726 | -0.4261 |
| Hexane-carbon tetrachlo-ride-naph thalene | 6.7871 | -13.1284 | $-15.4595$ | 6.4527 | 8.9758 | 14.8240 | 1.0988 | $-1.0474$ | -1.2149 |
| Cyclohexane-hexanenaphthalene | 10.9516 | -23.0937 | -22.3052 | 12.2495 | 11.4918 | 23.7388 | 1.0097 | -1.0103 | -0.9092 |

In applying these constants in Equation 3a or 3 b to a system, subscripts 1, 2, 3, refer to the components in the order listed in column 1 of this table.

## ACKNOWLEDGMENT

The University of Georgia Institute of Statistics provided vital assistance in computation.

## NOMENCLATURE

$$
\begin{aligned}
A_{i j} & =\text { function defined in Equation 2 } \\
A_{i j k} & =\text { function defined in Equation 4 } \\
B_{i j}, C_{i j}, D_{i j} & =\text { constants in Equation 2 } \\
B_{i j k}, C_{i j k}, D_{i j k}, E_{i j k}, & \\
\Gamma_{i j k}, G_{i j k} & =\text { constants in Equation 4 }
\end{aligned}
$$

$n=$ refractive index
$n_{i}=$ refractive index of pure component
$x_{i}=$ mole fraction of component $i$

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# Viscosity of a Mixture of Methane and n-Butane 

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#### Abstract

Measurements of the viscosity of a mixture of methane and $n$-butane containing 0.394 mole fraction methane have been carried out with a couette-type instrument at pressures up to 5000 p.s.i. in the temperature interval between $40^{\circ}$ and $400^{\circ} \mathrm{F}$. Goad agreement with an earlier investigation involving an effusion-type instrument was realized. The present results and comparisons with the earlier data are depicted in both graphical and tabular form.


TTHE VISCOSITY of the paraffin hydrocarbons at atmospheric and elevated pressure has been the subject of many investigations over the past two decades. In the case of methane, the viscosity has been investigated experimentally in some detail (1-4, 6, 7, 10, 13, 14). Likewise, the viscosity of $n$-butane has been investigated rather completely ( $5,9,11,15-18$ ). Satisfactory agreement for both methane and $n$-butane was obtained between
effusion and couette-flow equipment. The agreement as to the viscosity of a particular state as measured with widely different types of equipment lends credence to the accuracy of the absolute values for these compounds.

Recently, the viscosity of four mixtures of methane and $n$-butane was established by Dolan, Ellington, and Lee (8) at pressures as high as 5000 p.s.i.a. in the temperature interval between $70^{\circ}$ and $340^{\circ} \mathrm{F}$. The measurements upon


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