Low-Temperature Thermal Properties of Cyclohexanethiol

and 2,4-Dimethyl-3-thiapentane

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The low-temperature thermal properties of cyclohexanethiol and 2,4-dimethyl-3-thiapentane were measured by adiabatic calorimetry over the ranges 12° to 370° K. and 12° to 380° K., respectively. Values of the molal heat capacity at saturation pressure were obtained for the solid and liquid for each compound. For cyclohexanethiol the heat of fusion, ΔHm , triple-point temperature for zero impurity, T_{tp} , and sample purity were 2390 cal., 189.64° \pm 0.05° K., and 99.978 \pm 0.010 mole %. For 2,4-dimethyl-3-thiapentane these values were 2489 cal., 195.07° \pm 0.02° K., and 99.992 \pm 0.002 mole %. From the above data, the following molal chemical thermodynamic properties were calculated for the condensed phases (values shown are for cyclohexanethiol and 2,4-dimethyl-3-thiapentane at 298.15° K.) at selected temperatures from 0° to 390° K.: Gibbs energy function, 28.61 and 35.05 cal. per degree; enthalpy function, 33.19 and 39.77 cal. per degree; enthalpy, 9896 and 11,856 cal.; entropy, 61.80 and 74.82 cal. per degree; and heat capacity, 46.04 and 55.45 cal. per degree.

THE LOW-TEMPERATURE thermal studies on cyclohexanethiol and 2,4-dimethyl-3-thiapentane (diisopropyl sulfide) were made as a part of a continuing program of thermodynamics research on hydrocarbons and related substances (1). The measurements were made to provide experimental values of the thermodynamic functions for these compounds in the condensed state. The values of the entropy in the liquid state have been combined (11) with values of the heat of vaporization (16) and vapor pressure (9) to provide measured values for the entropy of each compound in the ideal gas state. These have served in part as a basis for calculation of the chemical thermodynamic properties of cyclohexanethiol and 2,4-dimethyl-3-thiapentane in the ideal gas state from spectral and molecular structure data by Scott and Crowder (11).

EXPERIMENTAL

Apparatus and Physical Constants. The low-temperature calorimetric measurements were made with apparatus described by Huffman and coworkers (6, 7, 12). The "1961 International Atomic Weights" (2) and values of the 1963 physical constants (10) were used. Measurements of temperature were made with platinum resistance thermometers calibrated in terms of the International Practical Temperature Scale of 1948, text revision of 1960 (14), from 90° to 400° K., and in terms of the provisional scale of the National Bureau of Standards (5) from 11° to 90° K. Celsius temperatures were converted to Kelvin by the relation, 0°C. = 273.15°K. (13). Measurements of mass, electrical potential, and resistance were made in terms of standard devices calibrated at the National Bureau of Standards. Energy was measured in joules and converted to calories by the relation, 1 cal. = 4.184 joules.

Materials. The samples of cyclohexanethiol and 2,4dimethyl-3-thiapentane used in this research were standard samples of organic sulfur compounds API-USBM 48-34 and 48-38, having purities of 99.978 and 99.992 mole %, respectively. These compounds were synthesized and purified at the Laramie, Wyo., Petroleum Research Center of the Bureau of Mines. The samples, about 55 ml. each, were received sealed in internal breakoff-tip glass ampoules and were transferred to the calorimeter without exposure to air or water. The 2,4-dimethyl-3-thiapentane showed only a very small amount of water, as evidenced by floaters when partially melted, and was used as received. The cyclohexanethiol was dried by a vapor phase transfer through magnesium perchlorate. In each case pure helium at 40-torr pressure and 23° C. was added to the calorimeter to promote thermal equilibration at low temperatures. Helium at this pressure will have a negligible effect on the melting-point temperatures.

RESULTS

Heat Capacities in the Solid and Liquid States. The heat capacities of cyclohexanethiol and 2,4-dimethyl-3-thiapentane were measured for the solid and liquid states over the ranges 12° to 365°K. and 12° to 383°K., respectively. The observed values of molal heat capacity at saturation pressure, C_s , are given in Table I. The temperature increments used in the measurements were small enough to eliminate the need for corrections to the heat capacity for curvature. The temperature increments, ΔT , used in the regions just below the melting point, are given as footnotes in Table I to permit calculation of corrections to $C_{\rm s}$ for the effects of premelting. The precision uncertainty of the results, as measured by the average deviation from the smooth curve, was less than 0.1%. Below 30° K. the accuracy uncertainty of the individual measurements is as much as 1% near 12° K., although smoothed values should be better than this. From 30° to 250°K., the accuracy uncertainty is less than 0.2%, except in the premelting region. In the premelting region the accuracy uncertainty is 0.5% owing to the imprecision in the assignment of premelting correction. This higher uncertainty will have a

Table	I. Gram-M	olal Heat	Capacity,	Cal. per [Degree
T^{a}	C^{\flat}_s	T^{*}	$C^{\flat}_{ m s}$	T°	C_s^{\flat}
		Cyclohex	anethiol		
		Crys	tal		
$\begin{array}{c} 11.45\\ 11.62\\ 12.93\\ 12.98\\ 14.35\\ 14.73\\ 15.76\\ 16.52\\ 17.33\\ 18.47\\ 19.11\\ 20.58\\ 21.10\\ 22.87\\ 23.41\\ 25.50\\ 26.06\\ 28.57 \end{array}$	$\begin{array}{c} 0.913\\ 0.953\\ 1.256\\ 1.269\\ 1.630\\ 1.752\\ 2.023\\ 2.263\\ 2.503\\ 2.848\\ 3.044\\ 3.488\\ 3.650\\ 4.175\\ 4.335\\ 4.941\\ 5.093\\ 5.758 \end{array}$	$\begin{array}{c} 29.04\\ 32.29\\ 35.75\\ 39.38\\ 43.35\\ 47.74\\ 52.71\\ 53.77\\ 58.38\\ 59.18\\ 65.07\\ 71.06\\ 76.78\\ 82.70\\ 88.84\\ 94.69\\ 96.24\\ 101.82 \end{array}$	5.872 6.679 7.442 8.154 8.844 9.559 10.319 10.467 11.124 11.228 12.046 12.787 13.503 14.279 15.038 15.721 15.910 16.560	$\begin{array}{c} 107.64\\ 112.77\\ 119.63\\ 126.24\\ 132.63\\ 138.82\\ 145.33\\ 152.14\\ 158.74\\ 161.76\\ 162.23\\ 165.16\\ 167.32\\ 168.76\\ 172.73\\ 174.65 \end{array}$	17.243 17.843 18.650 19.409 20.151 20.878 ^c 21.627 ^c 22.444 ^c 23.272 ^c 23.490 ^c 23.675 ^c 24.076 ^c 24.255 ^c 24.507 ^c 24.980 ^c 25.303 ^c
		Liq	uid		
$196.61 \\198.70 \\204.43 \\204.72 \\215.02 \\226.02 \\236.90$	$\begin{array}{c} 41.182 \\ 41.240 \\ 41.398 \\ 41.387 \\ 41.692 \\ 42.058 \\ 42.488 \end{array}$	$\begin{array}{c} 247.67\\ 258.30\\ 268.80\\ 279.16\\ 286.72\\ 289.35\\ 297.99\end{array}$	$\begin{array}{r} 42.980\\ 43.521\\ 44.119\\ 44.743\\ 45.268\\ 45.416\\ 46.042\end{array}$	$\begin{array}{c} 299.40\\ 310.10\\ 322.01\\ 333.71\\ 344.72\\ 355.07\\ 365.27\end{array}$	$\begin{array}{c} 46.129\\ 46.881\\ 47.747\\ 48.636\\ 49.497\\ 50.337\\ 51.114\end{array}$
	2,	4-Dimethyl	-3-thiapent	ane	
		Cry	stal		
$11.59 \\ 11.92 \\ 12.83 \\ 13.18 \\ 14.24 \\ 14.68 \\ 15.84 \\ 16.40 \\ 17.60 \\ 18.30 \\ 19.60 \\ 20.29 \\ 21.79 \\ 22.37 \\ 24.20 \\ 24.57 \\ $	$\begin{array}{c} 1.263\\ 1.361\\ 1.612\\ 1.730\\ 2.060\\ 2.207\\ 2.568\\ 2.748\\ 3.148\\ 3.384\\ 3.384\\ 3.817\\ 4.048\\ 4.554\\ 4.747\\ 5.365\\ 5.491 \end{array}$	$\begin{array}{c} 27.00\\ 27.21\\ 30.34\\ 33.54\\ 36.82\\ 40.72\\ 45.20\\ 50.26\\ 53.46\\ 58.52\\ 64.28\\ 70.41\\ 76.73\\ 82.87\\ 89.11\\ 95.93\\ \end{array}$	$\begin{array}{c} 6.280\\ 6.342\\ 7.309\\ 8.276\\ 9.162\\ 10.153\\ 11.213\\ 12.387\\ 13.087\\ 14.144\\ 15.347\\ 16.541\\ 17.764\\ 18.989\\ 20.173\\ 21.382\\ \end{array}$	$\begin{array}{c} 102.92\\ 110.20\\ 118.19\\ 122.18\\ 128.69\\ 135.47\\ 142.43\\ 150.11\\ 158.12\\ 165.86\\ 175.72\\ 178.81\\ 182.01\\ 185.40\\ \end{array}$	22.589 23.856 25.190 25.836 26.899 27.976 30.271 31.532 32.748^{d} 34.329^{d} 34.850^{d} 35.365^{d} 35.995^{d}
Liquid					
$\begin{array}{c} 203.70\\ 206.61\\ 210.58\\ 214.58\\ 219.35\\ 228.95\\ 238.96\\ 249.46\\ 255.57\\ 259.83 \end{array}$	$\begin{array}{r} 49.801\\ 49.982\\ 50.156\\ 50.343\\ 50.570\\ 51.062\\ 51.601\\ 52.198\\ 52.589\\ 52.858\end{array}$	$\begin{array}{c} 267.25\\ 270.07\\ 279.31\\ 280.19\\ 290.18\\ 291.18\\ 302.88\\ 314.42\\ 325.58\\ 326.29\\ \end{array}$	53.324 53.540 54.173 54.222 54.914 55.019 55.854 56.722 57.569 57.629	330.26 337.83 338.49 340.84 349.86 351.78 361.71 362.55 373.19 383.21	57.936 58.520 58.565 58.746 59.437 59.611 60.374 60.478 61.282 62.026

^a T is the mean temperature (in °K.) of each heat capacity measurement. ^bC_s is the heat capacity of the condensed phase at saturation pressure. Values of C_s are not corrected for the effects of premelting caused by impurities. ^{cd} The temperature increments of these measurements are in order of increasing T, °K.: ^c 6.106, 6.916, 6.703, 6.506, 5.623, 7.555, 6.338, 5.484, 5.512, 5.347, 6.277; ^d 7.628, 6.370, 6.172, 6.218, 7.018.

negligible effect on the over-all enthalpy and entropy as the heat of fusion calculations largely compensate for inaccuracy in the heat capacity in the premelting region. From data obtained on other compounds in the range 250° to 370° K., the authors believe that the heat capacities obtained using a platinum sample container are too large. The deviation increases steadily from 0.1% at 250° K. to 0.7% at 370° K. This progressive decline in accuracy with increasing temperature is thought to be related to variations in the temperature profile of the sample container during heating periods and will be discussed in detail in a forthcoming paper (3).

The heat capacity of cyclohexanethiol and 2,4-dimethyl-3-thiapentane in the liquid state is represented by Equations 1 and 2 below, respectively, with maximum deviations of 0.06 and 0.07% and average deviations of 0.02 and 0.03%for the temperature ranges indicated.

$$C_{\rm s} = 58.804 - 0.22268T + 8.2813 \times 10^{-4}T^2$$

$$-7.5521 \times 10^{-7} T^3 215^{\circ} - 365^{\circ} \text{ K.}$$
(1)

 $C_s = 55.912 - 0.12300T + 5.6586 \times 10^{-4}T^2$

 $-5.2975 \times 10^{-7} T^3 206^{\circ} - 383^{\circ} K.$ (2)

Heat of Fusion, Triple-Point Temperature, and Sample Purity. The heat of fusion, ΔHm , for each compound was calculated from the heat capacity data and enthalpy measurements made over temperature intervals that included the triple-point temperature. Correction to the heat of fusion for the effects of premelting owing to impurities was made in each case. For cyclohexanethiol, four measurements of the heat of fusion were made which gave values of 2389.1, 2389.5, 2389.5, and 2392.3 cal. The average value, 2390, was chosen. For 2,4-dimethyl-3-thiapentane, three measurements were made giving values of 2489.0, 2487.9, and 2489.6 cal., and again the average value of 2489 was chosen and used in calculation of the thermodynamic functions.

The triple-point temperature and sample purity for cyclohexanethiol and 2,4-dimethyl-3-thiapentane were determined from a study of the equilibrium melting temperature as a function of the fraction of the sample melted (8, 15). The resulting melting-point summaries are given in Table II. In each case the equilibrium temperature, T_F , was plotted as a function of 1/F, the reciprocal of the fraction of the sample in the liquid state. The triple-point temperature, T_{iF} , was determined by linear extrapolation of T_F to zero value of 1/F.

If impurities form an ideal solution in the liquid phase and are insoluble in the solid phase, the relation between mole fraction of total impurity, N_2^* , and melting-point depression, $\Delta T = T_{tp} - T_F$, is (4)

$$\ln (1 - N_2) = A \Delta T (1 + B \Delta T + \dots)$$
(3)

	Table II. M	elting Point Sumn	naries			
F	1/	F T_F	${T}_{ m Calcd.}$			
	Cyclohexanethiol					
A = 0.03345	deg. ⁻¹ , $B = 0.0$	00291 deg. ⁻¹ , impu	rity = 0.022 mole %			
0.09961 0.25403 0.49676 0.69534 0.89385 1.00000 Pure	$10.039 \\ 3.937 \\ 2.013 \\ 1.438 \\ 1.119 \\ 1.000 \\ 0$	189.6008 189.6193 189.6274 189.6299° 189.6319°	189.5760 189.6142 189.6263 189.6299 189.6319 189.6326 189.6389			
2,4,-Dimethyl-3-thiapentane						
A = 0.03291 deg. ^-1, B = 0.00273 deg. ^-1, impurity = 0.008 mole $\%$						
0.11993 0.27425 0.50594 0.71183 0.91770 1.00000 Pure		195.0520 195.0630 195.068° 195.0679 195.0688°	$195.0524 \\195.0630 \\195.0668 \\195.0681 \\195.0688 \\195.0688 \\195.0690 \\195.0713$			

^aA straight line through these points was extrapolated to 1/F = 0 to obtain triple-point temperature, T_{π} .

Table III. Gram-Molal Thermodynamic Functions for Condensed \mbox{Phases}^{α}

<i>T</i> , ° K.	$-(G_{s}-H_{0}^{\circ})/T,$ Cal./°K.	$(H_s - H_0^\circ)/T,$ Cal./°K.	$H_s - H_0^{\circ},$ Cal.	$S_{s},$ Cal./° K.	$C_{s},$ Cal./° K.
Cyclohexanethiol					
$\begin{array}{c} 10\\ 12\\ 14\\ 16\\ 18\\ 20\\ 25\\ 30\\ 35\\ 40\\ 45\\ 50\\ 60\\ 70\\ 80\\ 90\\ 100\\ 110\\ 120\\ 130\\ 140\\ 150\\ 160\\ 170\\ 180\\ 189.640 \end{array}$	0.052 0.090 0.141 0.207 0.287 0.381 0.671 1.023 1.420 1.847 2.294 2.753 3.687 4.625 5.554 6.471 7.373 8.259 9.131 9.988 10.832 11.663 12.483 13.293 14.093 14.093 14.857	Cr 0.156 0.265 0.410 0.585 0.786 1.009 1.620 2.261 2.898 3.509 4.086 4.629 5.632 6.545 7.387 8.184 8.942 9.668 10.371 11.056 11.725 12.383 13.033 13.681 14.326 14.947	ystal 1.556 3.181 5.734 9.354 14.155 20.176 40.49 67.84 101.43 140.38 183.87 231.47 337.9 458.1 591.0 736.6 894.2 1063.5 1244.6 1437.3 1641.5 1857.4 2085.3 2325.7 2578.7 2834.5	0.208 0.355 0.551 0.792 1.074 1.390 2.291 3.284 4.318 5.356 6.380 7.382 9.319 11.170 12.942 14.655 16.315 17.928 19.502 21.044 22.557 24.046 25.517 26.974 28.419 29.803	$\begin{array}{c} 0.616\\ 1.028\\ 1.535\\ 2.095\\ 2.706\\ 3.316\\ 4.794\\ 6.118\\ 7.284\\ 8.266\\ 9.119\\ 9.911\\ 11.355\\ 12.658\\ 13.926\\ 15.175\\ 16.346\\ 17.519\\ 18.691\\ 19.845\\ 21.008\\ 22.177\\ 23.416\\ 24.667\\ 25.929\\ 27.125\\ \end{array}$
		Li	quid		
$189.64 \\ 190 \\ 200 \\ 210 \\ 220 \\ 230 \\ 240 \\ 250 \\ 260 \\ 270 \\ 273.15 \\ 280 \\ 290 \\ 298.15 \\ 300 \\ 310 \\ 320 \\ 330 \\ 340 \\ 350 \\ 360 \\ 370 \\ 370 \\ 370 \\ 370 \\ 370 \\ 380 \\ 370 \\ 380 \\ 370 \\ 380 \\ 370 \\ 380 \\ 370 \\ 380 \\ 370 \\ 380 \\ 370 \\ 380 \\ 370 \\ 380 \\ 370 \\ 380 \\ 370 \\ 380 \\ 370 \\ 380 \\ 380 \\ 370 \\ 380 \\ 380 \\ 370 \\ 380 \\ 380 \\ 370 \\ 380 \\ 3$	$\begin{array}{c} 14.857\\ 14.909\\ 16.341\\ 17.735\\ 19.092\\ 20.414\\ 21.702\\ 22.958\\ 24.184\\ 25.381\\ 25.753\\ 26.551\\ 27.696\\ 28.611\\ 28.816\\ 29.914\\ 30.991\\ 32.047\\ 33.085\\ 34.104\\ 35.107\\ 36.093 \end{array}$	$\begin{array}{c} 27.550\\ 27.575\\ 28.254\\ 28.880\\ 29.463\\ 30.009\\ 30.525\\ 31.019\\ 31.493\\ 31.952\\ 32.094\\ 32.400\\ 32.839\\ 33.192\\ 33.271\\ 33.699\\ 34.122\\ 34.542\\ 34.959\\ 35.375\\ 35.791\\ 36.205 \end{array}$	5224.5 5239 5651 6065 6482 6902 7326 7755 8188 8627 8767 9072 9523 9896 9981 10447 10919 11399 11399 11886 12381 12885 13396	$\begin{array}{c} 42.407\\ 42.484\\ 44.595\\ 46.615\\ 48.554\\ 50.422\\ 52.227\\ 53.977\\ 55.677\\ 57.333\\ 57.847\\ 58.951\\ 60.535\\ 61.803\\ 62.088\\ 63.613\\ 65.113\\ 66.589\\ 68.044\\ 69.479\\ 70.897\\ 72.298\end{array}$	$\begin{array}{c} 41.020\\ 41.030\\ 41.271\\ 41.536\\ 41.851\\ 42.208\\ 42.623\\ 43.093\\ 43.615\\ 44.188\\ 44.376\\ 44.798\\ 45.463\\ 46.038\\ 46.169\\ 46.874\\ 47.599\\ 48.351\\ 49.125\\ 49.925\\ 50.733\\ 51.500\end{array}$
		2,4-Dimethyl Cr	-3-thiapentane vstal		
$\begin{array}{c} 10\\ 12\\ 14\\ 16\\ 20\\ 25\\ 30\\ 35\\ 40\\ 45\\ 50\\ 60\\ 70\\ 80\\ 90\\ 100\\ 110\\ 120\\ 130\\ 140\\ 150\\ 160 \end{array}$	$\begin{array}{c} 0.073\\ 0.125\\ 0.195\\ 0.282\\ 0.386\\ 0.506\\ 0.864\\ 1.290\\ 1.765\\ 2.276\\ 2.812\\ 3.365\\ 4.501\\ 5.657\\ 6.818\\ 7.976\\ 9.130\\ 10.273\\ 11.407\\ 12.531\\ 13.642\\ 14.742\\ 15.831\\ \end{array}$	$\begin{array}{c} 0.216\\ 0.363\\ 0.550\\ 0.769\\ 1.011\\ 1.272\\ 1.976\\ 2.718\\ 3.467\\ 4.200\\ 4.909\\ 5.593\\ 6.895\\ 8.121\\ 9.285\\ 10.409\\ 11.489\\ 12.532\\ 13.543\\ 14.523\\ 13.543\\ 14.523\\ 15.479\\ 16.412\\ 17.326\end{array}$	$\begin{array}{c} 2.160\\ 4.360\\ 7.700\\ 12.300\\ 18.200\\ 25.430\\ 49.390\\ 81.530\\ 121.33\\ 168.01\\ 220.90\\ 279.66\\ 413.7\\ 568.5\\ 742.8\\ 936.8\\ 1148.9\\ 1378.5\\ 1625.1\\ 1888.0\\ 2167.0\\ 2461.8\\ 2772.2\end{array}$	$\begin{array}{c} 0.289\\ 0.488\\ 0.745\\ 1.051\\ 1.397\\ 1.778\\ 2.840\\ 4.008\\ 5.232\\ 6.476\\ 7.721\\ 8.958\\ 11.396\\ 13.778\\ 16.103\\ 18.385\\ 20.619\\ 22.805\\ 24.950\\ 27.054\\ 29.121\\ 31.150\\ 33.160\end{array}$	$\begin{array}{c} 0.844\\ 1.373\\ 1.981\\ 2.619\\ 3.283\\ 3.951\\ 5.630\\ 7.207\\ 8.680\\ 9.975\\ 11.170\\ 12.327\\ 14.458\\ 16.463\\ 18.418\\ 20.333\\ 22.086\\ 23.820\\ 25.483\\ 27.107\\ 28.693\\ 30.260\\ 31.830\end{array}$

(Continued on page 429)

Table III. Gram-Molal Thermodynamic Functions for Condensed Phases^a (Continued)

<i>T</i> , ° K.	$-(G_s - H_0^\circ)/T,$ Cal./°K.	$(H_s - H_0^\circ)/T,$ Cal./°K.	$H_{ m s}-H_{ m \delta}^{ m s}$, Cal.	S_s , Cal./° K.	C_s , Cal./° K.
2,4-Dimethyl-3-thiapentane					
		Cr	ystal		
170 180 190 195.07	$\begin{array}{c} 16.909 \\ 17.976 \\ 19.031 \\ 19.566 \end{array}$	$\begin{array}{c} 18.224 \\ 19.111 \\ 19.995 \\ 20.439 \end{array}$	3098 3440 3799 3987	35.13 37.09 39.03 40.01	$33.39 \\ 35.01 \\ 36.76 \\ 37.54$
Liquid					
$\begin{array}{c} 195.07\\ 200\\ 210\\ 220\\ 230\\ 240\\ 250\\ 260\\ 270\\ 273.15\\ 280\\ 290\\ 298.15\\ 300\\ 310\\ 320\\ 330\\ 340\\ 350\\ 360\\ 370\\ 380\\ \end{array}$	$\begin{array}{c} 19.566\\ 20.391\\ 22.055\\ 23.678\\ 25.248\\ 26.785\\ 28.285\\ 29.756\\ 31.18\\ 31.62\\ 32.58\\ 33.96\\ 35.05\\ 35.05\\ 35.05\\ 35.05\\ 35.05\\ 35.00\\ 36.61\\ 37.90\\ 39.17\\ 40.42\\ 41.63\\ 42.83\\ 44.02\\ 45.17\end{array}$	$\begin{array}{c} 33.20\\ 33.61\\ 34.38\\ 35.10\\ 35.79\\ 36.44\\ 37.06\\ 37.65\\ 38.23\\ 38.41\\ 38.79\\ 39.33\\ 39.77\\ 39.86\\ 40.38\\ 40.89\\ 41.40\\ 41.89\\ 42.39\\ 42.87\\ 43.35\\ 43.83\end{array}$	$\begin{array}{c} 6476\\ 6721\\ 7220\\ 7723\\ 8232\\ 8746\\ 9265\\ 9790\\ 10322\\ 10491\\ 10861\\ 11407\\ 11856\\ 11959\\ 12518\\ 13086\\ 13661\\ 14244\\ 14835\\ 15433\\ 16040\\ 16654 \end{array}$	52.77 54.00 56.44 58.78 61.04 63.23 65.35 67.41 69.41 70.03 71.37 73.29 74.82 75.16 76.99 78.79 80.57 82.31 84.02 85.70 87.37 89.00	$\begin{array}{c} 49.45\\ 49.66\\ 50.13\\ 50.60\\ 51.12\\ 51.66\\ 52.23\\ 52.87\\ 53.51\\ 53.73\\ 54.21\\ 54.91\\ 55.45\\ 55.57\\ 56.35\\ 57.14\\ 57.92\\ 58.68\\ 59.46\\ 60.25\\ 61.03\\ 61.81\end{array}$
370 380 390	$\begin{array}{r} 44.02 \\ 45.17 \\ 46.32 \end{array}$	43.35 43.83 44.30	$16040 \\ 16654 \\ 17276$	87.37 89.00 9.062	61.03 61.81 62.61

^aThe values tabulated are the Gibbs energy function, enthalpy function, enthalpy, entropy, and heat capacity of the condensed phases at saturation pressure.

where $N_2 = N_2^*/F$. The cryoscopic constants, $A = \Delta Hm/RT_{ip}^2$ and $B = 1/T_{ip} - \Delta Cm/2\Delta Hm$, were calculated from the mean value of ΔHm , given above, the triple-point temperature, T_{ip} , given in Table II, and the value of ΔCm , the difference between the heat capacity of the compound in the solid and liquid states at the triple point, obtained from data in Table III. Values of A and B for cyclohexanethiol and 2,4-dimethyl-3-thiapentane are given in Table II. The impurity value given in Table II was calculated using Equation 3 in its simplified form (for N_2^* < 1), $N_2^* = AF\Delta T$.

Chemical Thermodynamic Properties in the Solid and Liquid States. The low-temperature data for cyclohexanethiol and 2,4-dimethyl-3-thiapentane were used in calculating the values of the Gibbs energy function, enthalpy function, enthalpy, entropy, and heat capacity for the liquid and solid states at selected temperatures from 10° to 390° K. The values at 10° K. were calculated from Debye functions whose parameters (for cyclohexanethiol, $\theta = 108.79^{\circ}$ C. and 5.2 degrees of freedom, and for 2,4-dimethyl-3-thiapentane, $\theta = 96.01^{\circ}$ C. and 5.0 degrees of freedom) were calculated from the values of the heat capacity between 11° and 20° K. The values of the thermodynamic properties above 10° K. were calculated from the observed values of the heat and temperature of melting and appropriate numerical integration of smoothed values of C_s at regular intervals. The results, shown in Table III, were corrected for the effects of heterophase premelting. Although the values of impurity of 0.015 mole % for cyclohexanethiol and 0.0075 mole % for 2,4-dimethyl-3-thiapentane used in the corrections for premelting deviated from the impurities calculated from the melting-point studies (Table II), these lower values represented the effective concentrations in the premelting region.

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