# Second Virial Coefficients of Eight <br> Compounds in the Range $40^{\circ}$ to $200^{\circ} \mathrm{C}$. 

RAJA F. HAJJAR, ${ }^{1}$ WEBSTER B. KAY, and GLEN F. LEVERETT
Department of Chemical Engineering, Ohio State University, Columbus, Ohio 43210


#### Abstract

The compressibility of n-pentane, $n$-hexane, $n$-heptane, cyclohexane, benzene, acetone, carbon disulfide, and perfluoro-methyl-cyclohexane were determined in the range $40^{\circ}$ to $200^{\circ} \mathrm{C}$. and 200 to 800 mm . of Hg by a technique which is a combination of the constant volume and variable volume methods. The results agree with the virial equation of state $P V / R T=z=A+B / V+\ldots$, from which the second virial coefficients were calculated.


AT SUFFICIENTLY low pressures, a gas may be represented by the relatively simple system of rigid bodies possessing potentials which interact with the potentials of neighboring bodies. The properties of real gases at low pressures may therefore be interpreted in terms of molecular dimensions and interaction potentials. Under these conditions, only the first two terms may be retained in the virial equation of state


Figure 1. Experimental apparatus
A. Calibrated sample tube
B. Silvered vacuum jacket
C. Manometer
D. Block with pressure seals
E. Boiling flask and heater
F. Bellows for adjusting level of mercury
G. Mercury reservoir
H. Platinum resistance thermometer connected to a Mueller bridge

1. Vacuum ballast
T. Calibrated capillary tip in which the quantity of the sample was determined

Present address: Beirut College for Women, P. O. Box 4080, Beirut, Lebanon

$$
\begin{equation*}
\frac{P V}{R T}=z=A+\frac{B}{V}+\ldots \tag{1}
\end{equation*}
$$

where $V$ is the molecular volume, and $A$ and $B$ are the first and second virial coefficients. When Equation 1 applies, a plot of the compressibility $z$ against $1 / V$ at sufficiently low pressures should give a straight line whose intercept is $A$ and whose slope is $B$. As the system pressure approaches zero, the gas approaches ideal behavior and, in the limit, the compressibility $z=A=1$ at all temperatures.


Figure 2. Isotherms for n-pentane


Figure 3. Second virial coefficients for $n$-pentane, $n$-hexane, and $n$-heptane

[^0]Reference (8)

## EXPERIMENTAL

Low-pressure compressibilities are usually determined by the constant volume (9) or the variable volume method (6). Various buoyancy methods have also been used (1, 3 ). The technique developed for this study was a combination of the constant volume and the variable volume methods. This technique afforded precise determination of volume, while eliminating the need for frequent changes in the quantity of the sample.

The determination of the sample volume was carried out in tube A (Figure 1). This consisted of four glass bulbs, $25-\mathrm{mm}$. I.D., interconnected by smaller tubes, $10-\mathrm{mm}$. I.D. Each of these tubes was etched with a line approximately 0.001 mm . wide. The volume of each bulb and that of the capillary tip, T, 1-mm. I.D., were previously calibrated with respect to these etched lines. Sample tube A was maintained at a constant temperature by boiling
a pure liquid in a side-arm flask attached to the silvered vacuum-jacketed tube, B. The pressure of the boiling liquid could be varied between 250 and 760 mm . of Hg , thus covering a temperature range of about $30^{\circ} \mathrm{C}$. The temperature was measured to within $\pm 0.005^{\circ} \mathrm{C}$. with a platinum resistance thermometer. Pressures were computed from the difference in the mercury levels in sample tube $A$ and manometer C. A precision cathetometer reading to 0.01 mm . was used. All pressures were corrected for the vapor pressure of mercury.

A sample of the pure liquid was confined over mercury in the calibrated tip, $T$, and its quantity determined by measuring its length at a known temperature. The volume determinations were done by vaporizing the liquid sample, and the pressure was adjusted until the vapor was precisely confined within the limits of a calibrated segment of tube A. The precision of the volumetric measurements was established as being better than one part in ten thousand.

| Compound | Purity, Mole \% | roperties | Compounds | udied |  | Source |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | Refractive Index, $20^{\circ} \mathrm{C}$. |  | Vapor Pressure, Mm. Hg |  |  |
|  |  | Exptl. | Lit. | Exptl. | Lit. |  |
| $n$-Pentane | $99.84 \pm 0.16$ | $\ldots$ | $\ldots$ | $\ldots$ | $\ldots$ | ${ }^{\circ}$ |
| $n$-Hexane | $99.85 \pm 0.15$ | ... | ... | $\ldots$ | ... | $\cdots$ |
| $n$-Heptane | $99.93 \pm 0.07$ | $\ldots$ | $\ldots$ | ... | $\ldots$ | ${ }^{\circ}$ |
| Cyclohexane | $99.94 \pm 0.06$ |  |  |  |  | $\bigcirc$ |
| Benzene | $99.93 \pm 0.07$ |  |  |  |  | ${ }^{\circ}$ |
| Acetone | $99.90 \pm 0.05^{d}$ | 1.3591 | 1.3591 (5) | $612.6,50^{\circ} \mathrm{C}$. | 612.6, $50{ }^{\circ} \mathrm{C}$. (5) | ${ }^{6}$ |
| Carbon disulfde | $99.90 \pm 0.05^{d}$ | 1.6276 | 1.6276 (5) | $760.10,46.25^{\circ} \mathrm{C}$. | $760.0,46.25^{\circ} \mathrm{C}$. (5) | ${ }^{\circ}$ |
| Perfluoro-methyl-cyclohexane ${ }^{\text {e }}$ | $99.90 \pm 0.08^{\text {d }}$ | 1.2815 | 1.2816 (2) | $760.0,76.38^{\circ} \mathrm{C}$. | $760.0,76.33^{\circ} \mathrm{C}$. | 。 |

${ }^{a}$ Phillips Petroleum Co., used as received. ${ }^{b}$ Reagent grade chemicals, purified by fractional distillation. ${ }^{\text {e }}$ E. I. DuPont de Nemours Co., purified by fractional distillation. ${ }^{\text {a }}$ Estimated from refractive index and vapor pressure measurements. ${ }^{e}$ Density, $20^{\circ} \mathrm{C}$., 1.8045 gram/cc. exptl. Lit. (2) 1.7996.

Table II. Second Virial Coefficients of Eight Compounds Investigated in the Temperature Range $40^{\circ}$ to $200^{\circ} \mathrm{C}$.

| $n$-Pentane |  | $n$-Hexane |  | Benzene |  | Acetone |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| Temp., ${ }^{\circ} \mathrm{C}$. | -B liters/ mole | Temp., ${ }^{\circ} \mathrm{C}$. | -B liters/ mole | Temp., ${ }^{\circ} \mathrm{C}$. | -B liters/ mole | Temp., ${ }^{\circ} \mathrm{C}$. | -B liters/ mole |
| 40.00 | 1.050 |  |  | 40.00 | 1.565 | 40.00 | 1.575 |
| 50.00 | 0.960 | 42.00 | 1.750 | 50.00 | 1.350 | 50.00 | 1.375 |
| 63.00 | 0.875 | 50.00 | 1.590 | 58.00 | 1.215 | 64.00 | 1.200 |
| 80.00 | 0.785 | 62.00 | 1.450 | 62.00 | 1.150 | 80.00 | 1.065 |
| 95.00 | 0.715 | 80.00 | 1.205 | 80.00 | 0.945 | 95.00 | 0.920 |
| 109.00 | 0.655 | 95.00 | 1.090 | 95.00 | 0.840 | 109.00 | 0.800 |
| 125.00 | 0.575 | 109.00 | 0.995 | 109.00 | 0.765 | 125.00 | 0.700 |
| 140.00 | 0.535 | 130.00 | 0.850 | 125.00 | 0.720 | 140.00 | 0.630 |
| 154.00 | 0.500 | 154.00 | 0.730 | 140.00 | 0.645 | 155.00 | 0.555 |
| 180.00 | 0.445 | 179.97 | 0.615 | 154.00 | 0.610 | 180.00 | 0.455 |
| 200.00 | 0.400 | 200.00 | 0.530 | 180.00 | 0.550 | 200.00 | 0.400 |
|  |  |  |  | 200.00 | 0.510 |  |  |
| $n$-Heptane |  | Cyclohexane |  | Carbon Disulfide |  | Perfluoro <br> Methyl Cyclohexane |  |
|  |  |  |  |  |  |  |  |
| Temp., ${ }^{\circ} \mathrm{C}$. | -B liters/ mole | Temp., ${ }^{\circ} \mathrm{C}$. | -B liters/ mole | Temp., ${ }^{\circ} \mathrm{C}$. | -B liters/ mole | Temp., ${ }^{\circ} \mathrm{C}$. | -B liters/ <br> mole |
| Temp., |  | . |  |  |  |  |  |
| 40.00 | 3.735 | 43.43 | 1.625 | 40.00 | 0.810 | 40.00 | 2.610 |
| 50.00 | 2.765 | 52.92 | 1.365 | 50.00 | 0.700 | 50.00 | 2.140 |
| 63.00 | 2.240 | 63.25 | 1.225 | 64.00 | 0.605 | 64.00 | 1.595 |
| 80.00 | 1.760 | 80.00 | 1.045 | 80.00 | 0.480 | 80.00 | 1.370 |
| 95.00 | 1.555 | 95.00 | 0.940 | 95.00 | 0.430 | 95.00 | 1.145 |
| 109.00 | 1.385 | 108.85 | 0.885 | 109.00 | 0.380 | 109.00 | 1.065 |
| 125.00 | 1.265 | 123.48 | 0.795 | 125.00 | 0.335 | 125.00 | 0.905 |
| 154.00 | 1.045 | 137.90 | 0.690 | 140.00 | 0.310 | 140.00 | 0.815 |
| 180.00 | 0.880 | 155.00 | 0.625 | 154.00 | 0.270 | 154.00 | 0.730 |
| 200.00 | 0.775 | 180.00 | 0.540 | 180.00 | 0.230 | 180.00 | 0.600 |
|  |  | 200.00 | 0.490 | 200.00 | 0.195 | 200.00 | 0.505 |

The over-all precision in the compressibility was better than six parts in ten thousand.

Liquid samples were transferred to the capillary tip by sealing the calibrated sample tube, A, to a high-vacuum line. The sample tube was then heated to ensure that its inside surface was free from adsorbed gases. A small quantity of the deaerated sample was distilled into the capillary tip for rinsing purposes, then distilled out and discarded. The tip was rinsed twice before a final sample was retained. Mercury was then distilled over the sample, the sample tube disconnected from the vacuum line, and mounted in the apparatus, as shown in Figure 1. The sources and purities of the compounds used in this investigation are given in Table I.

## RESULTS AND DISCUSSION

$P-V-T$ measurements on the vapor of eight compounds were made covering the temperature range $40^{\circ}$ to $200^{\circ} \mathrm{C}$. and the pressure range 160 to 1000 mm . of Hg . When the compressibility, $z$, was calculated and plotted against $1 / V$, it was evident that the plots were linear; hence, the third virial coefficient and all higher coefficients were small enough to be neglected. The isotherms did not converge to unity, but to a slightly higher value ranging between 1.001 and 1.004 . This was the case with all eight compounds investigated. Figure 2 shows a typical plot. This consistent error of about $0.2 \%$ in the value of the mean intercept showed no temperature or pressure correlation. Further investigation showed that this could not be due to the solubility of the sample in mercury, leading to the conclusion that the determination of the mass of all the samples was in error by about $0.2 \%$, probably due to an erroneous meniscus correction. The authors had assumed that the


Figure 4. Second virial coefficient for cyclohexane, $\mathrm{C}_{6} \mathrm{H}_{12}$


Figure 5. Second virial coefficient for benzene, $\mathrm{C}_{6} \mathrm{H}_{6}$
This study
Reference (4)
meniscus formed a segment of a sphere. This error was insignificant in relation to the volume of the vapor in the bulbs of tube A, but was appreciable in relation to the volume of the liquid sample in tip T .

This error was corrected for by subtracting from the computed value of the compressibility the difference between the mean value of the intercept and unity. This procedure essentially amounted to adjusting the ordinate, or the compressibility value, downward so that the mean intercept was equal to unity. The $B$ values were then determined by a least squares method, taking the intercept as unity as an experimental point. The corrected results are given in Table II and plotted in Figures 3 to 8.


Figure 6. Second virial coefficient for acetone, $\mathrm{C}_{3} \mathrm{H}_{6} \mathrm{O}$

O This study

- Reference (7)


Figure 7. Second virial coefficient for carbon disulfide, $\mathrm{CS}_{2}$


Figure 8. Second virial coefficient for perfluoro-methyl-cyclohexane, $\mathrm{C}_{7} \mathrm{~F}_{14}$

Table III. Literature Values of the Second Virial Coefficients $\begin{array}{cccc} & \text {-B Liters/ } & & \\ \text { Temp., }{ }^{\circ} \mathrm{C} . & \text { Mole } & \text { Temp., }{ }^{\circ} \mathrm{C} . & \text {-B Liters/ } \\ \text { Mole }\end{array}$

$$
n \text {-Heptane (8) }
$$

| 25.0 | 1.194 |
| ---: | ---: |
| 32.9 | 1.117 |
| 44.9 | 1.011 |
| 55.8 | 0.923 |
| 65.8 | 0.863 |
| 75.8 | 0.800 |
| 84.8 | 0.758 |
| 95.4 | 0.701 |
| 105.7 | 0.652 |
| 115.2 | 0.612 |
| 127.8 | 0.578 |
| 140.4 | 0.517 |

$n$-Hexane (8)
1.598

| 44.8 | 1.598 |
| ---: | ---: |
| 55.8 | 1.419 |
| 64.5 | 1.338 |
| 74.8 | 1.235 |
| 85.3 | 1.144 |
| 97.4 | 1.050 |
| 104.5 | 0.992 |
| 113.5 | 0.928 |
| 122.7 | 0.880 |
| 136.9 | 0.800 |


| 76.2 | 1.819 |
| ---: | ---: |
| 85.1 | 1.691 |
| 95.3 | 1.560 |
| 104.9 | 1.446 |
| 115.9 | 1.325 |
| 127.6 | 1.212 |
| 140.5 | 1.108 |
| Benzene (4) |  |
| 70.0 | 1.035 |
| 80.0 | 0.971 |
| 100.0 | 0.852 |
| 100.0 | 0.839 |
| 125.0 | 0.733 |
|  | Acetone $(7)$ |
| 46.2 | 1.644 |
| 56.3 | 1.527 |
| 61.8 | 1.406 |
| 67.8 | 1.362 |
| 68.2 | 1.342 |
| 78.0 | 1.257 |
| 88.0 | 1.134 |
| 95.2 | 0.965 |
| 111.8 | 0.854 |
| 132.4 | 0.651 |

A few checks on the calculated values of $B$ were made by using

$$
\operatorname{Lim}_{V \rightarrow x}(z-A) V
$$

The quantity $(z-A) V$ was plotted against $1 / V$. The values of $B$, as given by the intercepts, were in agreement with the values obtained as explained above. The horizontal slope indicated that the third virial coefficient was, within the experimental error, equal to zero.

The values of the second virial coefficient, $B$, reported in the literature in the temperature range covered in this study are given in Table III and are plotted in Figures 3,5 , and 6 . There seems to be close agreement with the authors' results, except for acetone at low temperatures.
The calculation of the intermolecular potential parameters will be discussed in a forthcoming paper.

## literature cited

(1) Cawood, W., Patterson, H.S., J. Chem. Soc. (London), 1933, p. 619.
(2) Fowler, R.D., Ind. Eng. Chem. 39, 375 (1947).
(3) Hajjar, R.F., MacWood, G.E., J. Chem. Phys. 49, 4567 (1968).
(4) Hamann, S.D., McManamey, W.J., Ibid., 20, 1341 (1952).
(5) Handbook of Chemistry, N. A. Lang, Ed., Handbook Publ., Sandusky, Ohio, 1949.
(6) Lambert, J.D., Trans. Faraday Soc. 37, 421 (1941).
(7) Lambert, J.D., Roberts, G.A.H., Rowlinson, J.S., Wilkinson, V.J., Proc. Roy. Soc. (London) A196, 113 (1949).
(8) McGlashan, M.L., Potter, D.J.B., Proc. Roy. Soc. (London) A267, 478 (1962).
(9) Russell, J., Maass, O., Can. J. Res, 5, 436 (1931).

Recelved for review October 7, 1968. Accepted April 28, 1969.

# Density, Electrical Conductivity, and Vapor Pressure of Concentrated Phosphoric Acid 

DAVID I. MacDONALD ${ }^{1}$ and JAMES R. BOYACK<br>Direct Energy Conversion Business Section, General Electric Co., West Lynn, Mass. 01905


#### Abstract

Density and specific conductivity for $\mathrm{H}_{3} \mathrm{PO}_{4}$ in the concentration range 86 to 102 $\mathrm{w} t$. \% from room temperature to $170^{\circ} \mathrm{C}$. are presented. The vapor pressure portion gives data for 77 to $102 \mathrm{wt} . \% \mathrm{H}_{3} \mathrm{PO}_{4}$ for temperatures between $130^{\circ}$ and $170^{\circ} \mathrm{C}$. In each case, equations are given which provide a good least squares fit to the experimental data.


$\mathrm{T}_{\text {HE DENSITIES of phosphoric acid solutions have been }}$ determined by others (2,3) at concentrations up to $92 \%$ and at temperatures up to $80^{\circ} \mathrm{C}$. This work concerns the experimental determination of densities at higher concentrations and higher temperatures.

## EXPERIMENTAL

Pycnometers of $25-\mathrm{ml}$. capacity were calibrated against water at $25.00^{\circ} \mathrm{C}$. The cubical coefficient of expansion of borosilicate glass was used to calculate the volumes at higher temperatures. All weights were corrected to vacuum. Temperature was controlled to $0.01^{\circ} \mathrm{C}$. and measured to $0.1^{\circ} \mathrm{C}$. in oil thermostats. Solutions of phosphoric acid were prepared by dehydration of the C.P. grade at $150^{\circ}$ to $175^{\circ} \mathrm{C}$.
${ }^{1}$ Present address: Gillette Safety Razor Co., Boston, Mass.
in ovens. To avoid contamination, preparations were made in FEP bottles (fully fluorinated ethylene-propylene copolymer). The bottles were preconditioned at $150^{\circ}$ to $175^{\circ} \mathrm{C}$. Then, acid of known composition (usually $85.1 \%$, determined by repeated pH titration) was weighed into them. The acid composition was calculated from the weight loss of water after heating. The concentrated phosphoric acid solutions were stored in FEP bottles at room temperature before use. The experimental data is given in Table I.

## CORRELATION OF DENSITY DATA

Plots of the data in Table I reveal the density to be a linear function of the temperature, including the points at $25^{\circ} \mathrm{C}$. Furthermore, the density is also linear in the concentration over the limited range studied here.


[^0]:    This study

