

$v$  = linear crystal growth rate, m/s  
 $\bar{v}$  = mean overall linear growth rate, m/s  
 $\eta$  = viscosity (N s/m<sup>2</sup>) 1 cP = 10<sup>-3</sup> N s/m<sup>2</sup>  
 $\eta_s$  = viscosity of saturated solution, N s/m<sup>2</sup>  
 $\theta$  = temperature, °C  
 $\rho_c$  = crystal density, kg/m<sup>3</sup>  
 $\rho_s$  = density of saturated solution, kg/m<sup>3</sup>

Subscripts (100) and (001) refer to the (100) and (001) crystal axes, respectively.

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## Conductivities and Densities of Aqueous Solutions of Quaternary Ammonium Iodides Containing Pentyl and Ethoxyethyl Groups

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**The conductivities and densities of dilute aqueous solutions of the salts R<sub>3</sub>NR'I (R' = pentyl or ethoxyethyl, R = Me or Et) have been measured at 25°C. Analysis of the molar conductivities with the Fuoss-Hsia and Pitts equations shows that all four salts form ion pairs and that the association constants of the ethoxyethyl compounds are lower than those of their pentyl analogs. The higher limiting molar ionic conductivities observed for the ethoxyethyl salts are correlated with their smaller volumes.**

In a previous investigation (10) it was shown that the limiting molar conductivities of small quaternary ammonium iodides depend primarily on the size rather than the shape of the cation, and it was also shown that these salts form ion pairs to an extent which increases with increasing cation size. The purpose of the work reported here was to establish whether these relationships still hold when a methylene group in the cation is replaced by an ether oxygen.

Conductance measurements were made at 25°C on aqueous solutions of the iodides of pentyltrimethylammonium, ethoxyethyltrimethylammonium, pentyltriethylammonium, and ethoxyethyltriethylammonium cations, and their densities (1) were redetermined with a commercial density meter.

#### Experimental

The apparatus and procedure for the conductance measurements have been described (10). The cell was rebuilt and had a cell constant of 0.48644 cm<sup>-1</sup>, determined with potassium chloride solutions for which resistances were calculated using the equation of Lind et al. (9). The solvent conductivity was allowed for. Temperature fluctuations in the oil thermostat bath did not exceed ±0.01°C.

Densities of solutions with concentrations in the range 0.02-0.2 mol kg<sup>-1</sup> were measured with an Anton Parr DMA 02C density meter. The sample temperature was controlled to ±0.05°C with a Haake-type FE thermostat. The density meter was calibrated daily with at least three sodium chloride solutions with molalities in the range

0-0.9 mol kg<sup>-1</sup>. The densities of these solutions were calculated from the equation,

$$d = 0.997046 + 0.0416600m - 0.0014972m^{3/2} - 0.0009876m^2 \quad (1)$$

which is based on densities calculated from the smoothed apparent molal volumes [The value of  $\phi_v^\circ$  for  $m = 0.3$  mol kg<sup>-1</sup> is 17.62(1) cm<sup>3</sup> mol<sup>-1</sup> (18)] for  $m \leq 0.9$  mol kg<sup>-1</sup> of Vaslow (17). It represents these densities to within  $1.4 \times 10^{-6}$  g cm<sup>-3</sup> and those of Millero (12) for  $m \leq 0.51$  mol kg<sup>-1</sup> to within  $12 \times 10^{-6}$  g cm<sup>-3</sup>. All solutions were prepared with boiled distilled water, and vacuum corrections were applied to all weights. The procedure was tested with potassium chloride solutions and the apparent molal volume derived from these measurements was 26.8(2) ± 0.2 (standard error) cm<sup>3</sup> mol<sup>-1</sup> which is in excellent agreement with the literature (13) values (26.8 - 26.9 cm<sup>3</sup> mol<sup>-1</sup>).

The salts were prepared and purified as described previously (1) and were dried in vacuo at 100°C for at least 24 hr before use. All samples had analyses for iodide which showed that they were at least as pure as those used in earlier work (1).

#### Results

The experimental errors in the density measurements arise from the uncertainty in the sample temperature (±0.05°C) and from the solution handling procedures. The maximum error in the values given in Table I is estimated to be  $3 \times 10^{-5}$  g cm<sup>-3</sup>. The densities can be represented to within this experimental error by the empirical equation

$$d = d_0 + a_1m + a_2m^2 \quad (2)$$

in which  $d_0$  is the density of pure water (0.997046 g cm<sup>-3</sup>) and  $a_1$  and  $a_2$  have the values given in Table II. The molarities,  $c$ , calculated from the observed densities are related to the molalities,  $m$ , by the equation

$$c = m (d_0 + A_1m + A_2m^2) \quad (3)$$

in which  $A_1$  and  $A_2$  are empirical constants given in Table II. The apparent molal volumes  $\phi_v$  calculated from the observed densities were fitted to the equation (1, 2)

$$\phi_v = \phi_v^\circ + S_v c^{1/2} + j c \quad (4)$$

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**Table I. Densities at 25°C**

Pent-NMe <sub>3</sub> I		EtOCH <sub>2</sub> CH <sub>2</sub> NMe <sub>3</sub> I	
10 <sup>3</sup> m/mol kg <sup>-1</sup>	d/g, cm <sup>-3</sup>	10 <sup>3</sup> m/mol kg <sup>-1</sup>	d/g, cm <sup>-3</sup> <sup>a</sup>
33.585	0.999300	57.507	1.001597 ± 1
61.279	1.001147	82.189	1.003527 ± 2
161.68	1.007667	109.09	1.005610 ± 2
		192.44	1.011938 ± 6
Pent-NEt <sub>3</sub> I		EtOCH <sub>2</sub> CH <sub>2</sub> NEt <sub>3</sub> I	
10 <sup>3</sup> m/mol kg <sup>-1</sup>	d/g, cm <sup>-3</sup> <sup>a</sup>	10 <sup>3</sup> m/mol kg <sup>-1</sup>	d/g, cm <sup>-3</sup> <sup>a</sup>
63.866	1.001243 ± 1	25.554	0.999057
134.77	1.005754 ± 3	49.127	1.000874 ± 4
143.65	1.006315 ± 4	73.344	1.002719 ± 7
215.67	1.010775 ± 6	97.810	1.004574 ± 15
		184.74	1.011023 ± 2

<sup>a</sup> Errors are in ppm and represent the deviation from the mean of duplicate measurements on different samples of the same solution.

**Table II. Constants for Equations 2, 3, and 4<sup>a</sup>**

Salt	$\phi_v^{\circ b}$	$j^b$	$a_1$	$a_2$	$A_1$	$A_2$
Pent-NMe <sub>3</sub> I	189.66 ± 0.12	-3.8 ± 1.0	0.067550	-0.011397	-0.188787	0.035317
Pent-NEt <sub>3</sub> I	232.91 ± 0.06	-4.1 ± 0.4	0.066515	-0.013537	-0.231585	0.051450
EtOCH <sub>2</sub> CH <sub>2</sub> NMe <sub>3</sub> I	179.16 ± 0.04	-3.2 ± 0.3	0.079911	-0.013071	-0.178346	0.031073
EtOCH <sub>2</sub> CH <sub>2</sub> NEt <sub>3</sub> I	222.68 ± 0.12	-3.2 ± 0.9	0.078776	-0.017414	-0.221412	0.046104

<sup>a</sup> The units of  $\phi_v^{\circ}$ ,  $j$ ,  $a_1$ ,  $a_2$ ,  $A_1$ , and  $A_2$  are consistent with  $\phi_v$  in cm<sup>3</sup> mol<sup>-1</sup>,  $d$  in g cm<sup>-3</sup>,  $c$  in mol dm<sup>-3</sup>, and  $m$  in mol kg<sup>-1</sup>. <sup>b</sup> Errors are stan-

standard errors; the maximum errors in  $\phi_v^{\circ}$  and  $j$  are estimated to be ±0.5 cm<sup>3</sup> mol<sup>-1</sup> and ±3 cm<sup>3</sup> dm<sup>3</sup> mol<sup>-2</sup>, respectively.

tained for fixed values of  $a$  which were chosen on the basis of the  $\phi_v^{\circ}$  values so as to be consistent with those used in earlier work (4, 11). The values obtained for  $\Lambda^{\infty}$  (Table IV) did not change by more than 0.01 ohm<sup>-1</sup> cm<sup>2</sup> mol<sup>-1</sup> when 10<sup>10</sup>  $a/m$  was increased from 3 to 7 or when the F-H or the P versions of Equation 5 were used. The maximum uncertainty in the  $\Lambda^{\infty}$  values based on the errors from all identified sources is ±0.2 ohm<sup>-1</sup> cm<sup>2</sup> mol<sup>-1</sup>. The duplicate runs with pentyltriethylammonium iodide give  $\Lambda^{\infty}$  values which agree to well within this error limit. As expected (3, 10) the values obtained for  $K_A$  depend on that chosen for the ion size parameter,  $a$ . This is shown in Figure 1 for association constants calculated with the F-H equation. Those obtained with the P equation lie above those in Figure 1 at low  $a$  values and slightly below them for high  $a$  values. The P and F-H equations give identical  $K_A$  values when 10<sup>10</sup>  $a \approx 6m$ . The error in the association constants given in Table IV other than that arising from the choice of conductance equation and ion size parameter is probably ±0.5 dm<sup>3</sup> mol<sup>-1</sup>. Table IV also contains the standard deviations  $\sigma_A$

in which  $\phi_v^{\circ}$  is the limiting apparent molal volume,  $S_v$  is a theoretical constant (= 1.868 cm<sup>3</sup> mol<sup>-3/2</sup> dm<sup>3/2</sup>) (16) and  $j$  is an empirical constant. The values of  $\phi_v^{\circ}$  and  $j$  given with their standard errors in Table II were obtained by a least-squares procedure in which the points were weighted in proportion to their concentrations so as to allow for the dependence of errors in  $\phi_v$  on the reciprocal of the concentration (11). The maximum errors in the values of  $\phi_v^{\circ}$  and  $j$  are estimated to be ±0.5 cm<sup>3</sup> mol<sup>-1</sup> and ±3.0 cm<sup>3</sup> dm<sup>3</sup> mol<sup>-2</sup>, respectively. All of the  $\phi_v^{\circ}$  values agree with those obtained by pycnometry (1) to within experimental error.

The observed molar conductances  $\Lambda$  are given in Table III. The values were fitted to the equation,

$$\Lambda = \alpha[\Lambda^{\infty} - (B_1\Lambda^{\infty} + B_2)(c\alpha)^{1/2} + E(c\alpha) \ln(c\alpha) + J_1(c\alpha)^{1/2} - J_2(c\alpha)^{3/2}] \quad (5)$$

using expressions (5, 6) for  $J_1$  and  $J_2$  (which are functions of the ion size parameter  $a$ ) based on the treatments of Pitts [P] (14, 15) and Fuoss and Hsia [F-H] (7, 8). The degree of dissociation of the ion pairs,  $\alpha$ , is related to their association constant,  $K_A$ , by the expression

$$K_A = (1 - \alpha)/c\alpha^2 y_{\pm}^2 \quad (6)$$

where  $y_{\pm}$  is the molar activity coefficient given by the Debye-Hückel equation,

$$\log_{10} y_{\pm} = -A(c\alpha)^{1/2}/[1 + Ba(c\alpha)^{1/2}] \quad (7)$$

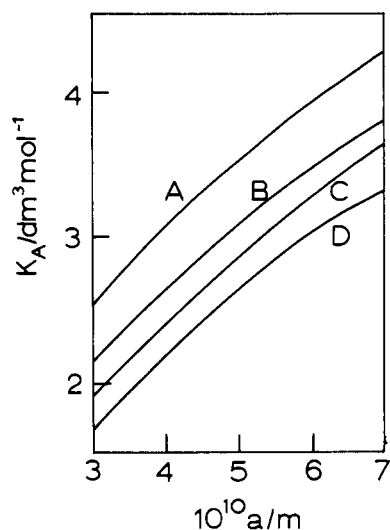
The best fit values of the molar conductivity at infinite dilution  $\Lambda^{\infty}$  and the association constant  $K_A$  were ob-

**Table III. Molar Conductivities at 25°C**

Pent-NMe <sub>3</sub> I		EtOCH <sub>2</sub> CH <sub>2</sub> NMe <sub>3</sub> I	
10 <sup>3</sup> c/mol dm <sup>-3</sup>	$\Lambda$ /ohm <sup>-1</sup> cm <sup>2</sup> mol <sup>-1</sup>	10 <sup>3</sup> c/mol dm <sup>-3</sup>	$\Lambda$ /ohm <sup>-1</sup> cm <sup>2</sup> mol <sup>-1</sup>
0.5321	106.38	0.6567	107.25
1.1619	105.28	1.2518	106.35
1.8410	104.45	1.8497	105.60
2.4984	103.77	2.3690	105.06
3.2287	103.12	2.8944	104.61
3.8674	102.60	3.5314	104.09
4.9840	101.80	4.0710	103.70
Pent-NEt <sub>3</sub> I (Run 1)		EtOCH <sub>2</sub> CH <sub>2</sub> NEt <sub>3</sub> I	
10 <sup>3</sup> c/mol dm <sup>-3</sup>	$\Lambda$ /ohm <sup>-1</sup> cm <sup>2</sup> mol <sup>-1</sup>	10 <sup>3</sup> c/mol dm <sup>-3</sup>	$\Lambda$ /ohm <sup>-1</sup> cm <sup>2</sup> mol <sup>-1</sup>
0.2714	101.69	0.6967	101.55
0.5122	101.12	0.9909	101.05
0.7535	100.68	1.3033	100.64
0.9755	100.34	1.5993	100.29
1.1739	100.03	1.8708	99.99
1.4122	99.75		
1.6253	99.50		
Pent-NEt <sub>3</sub> I (Run 2)			
10 <sup>3</sup> c/mol dm <sup>-3</sup>		$\Lambda$ /ohm <sup>-1</sup> cm <sup>2</sup> mol <sup>-1</sup>	
0.3531		101.63	
0.7314		100.88	
1.1168		100.27	
1.5002		99.75	
1.8506		99.34	
2.1886		99.00	
2.4367		98.72	

**Table IV. Parameters Derived from Molar Conductivities**

Salt	$10^{10} a/m$	$\Lambda^\infty/\text{ohm}^{-1} \text{cm}^2 \text{mol}^{-1}$	$K_A/\text{dm}^3 \text{mol}^{-1}$		$10^2 \frac{\sigma_A}{\text{ohm}^{-1} \text{cm}^2 \text{mol}^{-1}}$
			F-H	P	
Pent-NMe <sub>3</sub> I	5.64	108.4 <sub>1</sub>	3.3 <sub>5</sub>	3.3 <sub>6</sub>	2.4
Pent-NEt <sub>3</sub> I (Run 1)	5.99	103.1 <sub>2</sub>	3.5 <sub>3</sub>	3.5 <sub>8</sub>	1.1
Pent-NEt <sub>3</sub> I (Run 2)	5.99	103.2 <sub>9</sub>	3.9 <sub>2</sub>	3.9 <sub>5</sub>	1.0
EtOCH <sub>2</sub> CH <sub>2</sub> NMe <sub>3</sub> I	5.55	109.5 <sub>1</sub>	2.8 <sub>4</sub>	2.8 <sub>7</sub>	2.8
EtOCH <sub>2</sub> CH <sub>2</sub> NEt <sub>3</sub> I	5.91	103.8 <sub>6</sub>	3.2 <sub>3</sub>	3.2 <sub>7</sub>	1.9



**Figure 1.** Association constants obtained with Fuoss-Hsia conductance equation for different values of the ion size parameter  $a$   
 A, Pent-NEt<sub>3</sub>I (Run 2); B, Pent-NMe<sub>3</sub>I; C, EtOCH<sub>2</sub>CH<sub>2</sub>NEt<sub>3</sub>I; D, EtOCH<sub>2</sub>CH<sub>2</sub>NMe<sub>3</sub>I

based on the observed  $\Lambda$  and that calculated with the best fit values of  $\Lambda^\infty$  and  $K_A$ . The differences between  $\sigma_A$  values obtained with the F-H and P equations and with ion size parameters between  $3 \times 10^{-10} - 7 \times 10^{-10} \text{ m}$  were always less than  $0.01 \text{ ohm}^{-1} \text{ cm}^2 \text{ mol}^{-1}$  and could not be used to choose between the equations or the  $a$ -parameters.

### Discussion

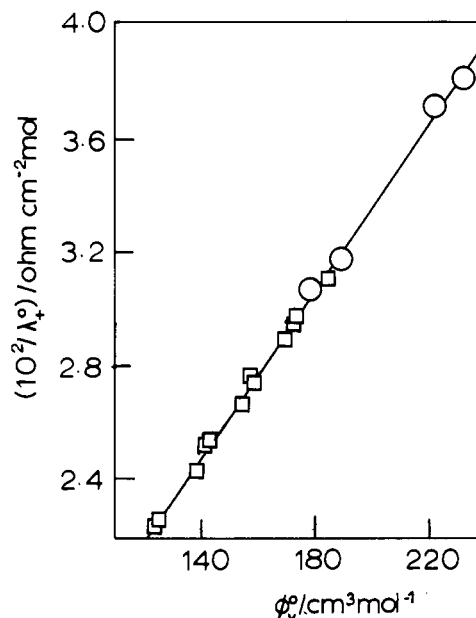
The replacement of  $-\text{CH}_2-$  by  $-\text{O}-$  leads to an increase in  $\Lambda^\infty$  and it is clear from Figure 2 in which the limiting ionic resistivity  $1/\lambda_+^\infty$  is plotted against  $\phi_v^\circ$  that a substantial part of this increase arises from the decrease in cation volume. This is also borne out by the values obtained for  $q [= \lambda_+^\infty (\phi_+^\circ)^{2/3}]$  given in Table V, which are all within experimental error of the value  $868.4 \pm 10.1$  (standard deviation) obtained for cyclic and straight chain cations with sizes between those of Me<sub>4</sub>N<sup>+</sup> and Et<sub>4</sub>N<sup>+</sup> (10).

The association constants obtained for the two ethoxyethyl compounds are both lower than those of their pentyl analogs by  $0.50 \text{ dm}^3 \text{ mol}^{-1}$ . This decrease in  $K_A$  although only just significant is larger than would be ex-

**Table V. Limiting Ionic Molar Conductivities and Apparent Molal Volumes**

Salt	$\lambda_+^\infty/\text{ohm}^{-1} \text{cm}^2 \text{mol}^{-1} \text{ }^a$	$\phi_+^\circ/\text{cm}^3 \text{mol}^{-1} \text{ }^b$	$q^c$
Pent-NMe <sub>3</sub> I	31.4	147.5	877.4
Pent-NEt <sub>3</sub> I	26.2	190.7	868.7
EtOCH <sub>2</sub> CH <sub>2</sub> NMe <sub>3</sub> I	32.5	137.0	864.5
EtOCH <sub>2</sub> CH <sub>2</sub> NEt <sub>3</sub> I	26.9	180.5	858.5

<sup>a</sup> Limiting molar ionic conductivity based on  $\lambda^\circ(\text{I}^-) = 76.98 \text{ ohm}^{-1} \text{ cm}^2 \text{ mol}^{-1}$ . <sup>b</sup> Limiting ionic partial molal volume based on  $\phi_v^\circ(\text{I}^-) = 42.2 \text{ cm}^3 \text{ mol}^{-1}$ . <sup>c</sup>  $q = \lambda_+^\infty (\phi_+^\circ)^{2/3}$ ; mean value =  $867.3 \pm 7.9$ .



**Figure 2.** Reciprocal of the ionic conductivity plotted against the apparent molal volume of the iodide  
 □, results (10, 11) for small straight chain and cyclic quaternary ammonium iodides; O, this work

pected simply from the change in cation size (about  $0.1 \text{ dm}^3 \text{ mol}^{-1}$ ) and probably reflects a difference in the solute-solvent interactions of the pentyl and ethoxyethyl groups. The decrease (about  $0.40 \text{ dm}^3 \text{ mol}^{-1}$ ) in  $K_A$  consequent on the replacement of  $-\text{NEt}_3$  by  $-\text{NMe}_3$  is the same for both pentyl and ethoxyethyl compounds.

### Acknowledgment

We thank R. B. Barlow for providing and purifying the compounds used in this work and for helpful discussions.

### Nomenclature

- A = theoretical constant in Equation 6
- $A_1, A_2$  = empirical constants in Equation 3
- $a$  = ion size parameter
- $a_1, a_2$  = empirical constants in Equation 4
- B = theoretical constant in Equation 6
- $B_1, B_2$  = theoretical constant in Equation 5
- $c$  = molarity,  $\text{mol dm}^{-3}$
- $d$  = density,  $\text{g cm}^{-3}$
- E = theoretical constant in Equation 5
- $J_1, J_2$  = ion size dependent constants in Equation 5
- $j$  = empirical constant in Equation 4

$K_A$  = association constant,  $\text{dm}^3 \text{mol}^{-1}$   
 $m$  = molality,  $\text{mol kg}^{-1}$   
 $S_v$  = theoretical constant in Equation 4  
 $\gamma_{\pm}$  = molar activity coefficient  
 $\alpha$  = degree of dissociation  
 $\Delta$  = molar conductivity,  $\text{ohm}^{-1} \text{cm}^2 \text{mol}^{-1}$   
 $\phi_v$  = apparent molal volume  
 $\sigma_{\Delta}$  = standard deviation between observed and calculated values of  $\Delta$

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## Isothermal Vapor-Liquid Equilibrium Data for System Heptane-2-Pentanone at 90°C

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Isothermal equilibrium vapor and liquid composition measurements have been made for the heptane-2-pentanone system at 90.0°C, using equilibrium samples produced with the aid of a vapor-recirculation equilibrium still. Vaporization equilibrium constants ( $K$  values) and activity coefficients were calculated from the equilibrium compositions, and the thermodynamic consistency was checked by two methods.

Isothermal vapor-liquid equilibrium data at low pressures are useful for studying the thermodynamics of non-ideal solutions and desirable for establishing the vaporization equilibrium constants ( $K$ -values) used for the design of equilibrium stage processes.

A survey of the literature indicates that no such isothermal data have been published for the system heptane-2-pentanone. Because of this, the equilibrium compositions reported here were determined.

#### Experimental

A detailed description of the experimental equipment, procedures, and methods has been given by Lodi and Scheller (5) and by Scheller et al. (10).

Briefly, a modification of the vapor-recirculation equilibrium still described by Hipkin and Myers (3) was used. Pressure in the still was controlled by a Cartesian manostat of the type described by Gilmont (2) and measured with a mercury manometer to  $\pm 0.1$  mm.

Temperature was measured with an iron-constantan thermocouple to  $\pm 0.1^\circ\text{C}$ , using a Model 320 Data Technology Corp. digital voltmeter which could be read to the nearest microvolt. The thermocouple was calibrated at the solid-state transition point of sodium sulfate decahydrate ( $32.384^\circ\text{C}$ ) and also against the boiling point of water. Distilled water was placed in the equilibrium still, the pressure was adjusted to the desired value with the

aid of the Cartesian manostat, and the system was allowed to operate until a constant millivolt reading was obtained on the potentiometer. The temperature was determined from the measured pressure and the steam tables. Twenty-three experimental points between 85.6 and 690.3 mm of Hg ( $48.44^\circ$  and  $97.33^\circ\text{C}$ ) were used in the calibration. A linear equation of temperature as a function of voltage was fitted to these 23 points by the method of least squares. The absolute average deviation between the experimental and calculated temperatures is  $0.13^\circ\text{C}$ . Spot checks of the calibration were made using pure benzene, acetone, and toluene.

Compositions of equilibrium samples were obtained with the aid of a Perkin-Elmer 880 gas chromatograph with a hot-wire detector, a 194B printing integrator, an L&N Speedomax G strip chart recorder, and a stationary phase of diisodecyl phthalate on 80/90 mesh ABS Anakrom packed in a stainless steel tube  $\frac{1}{8}$  in. by 10 ft. long. Helium was used as the elution gas. The chromatograph was calibrated with 12 mixtures of heptane-2-pentanone of known composition by relating the area fraction of the heptane peak to the mole fraction of heptane. The overall precision of the composition analyses was 0.2 mol %.

The heptane and 2-pentanone were obtained from Phillips Petroleum Co. and Eastman Kodak Co., respectively. Because chromatographic analysis indicated small secondary peaks, the reagents were distilled at high reflux in a glass distillation column about 5 ft 6 in. high. A heart cut representing approximately the center 40% of each reagent was collected and displayed no secondary peaks on the chromatograph. Densities, refractive indexes, and normal boiling points were measured and are compared with literature values in Table I.

#### Discussion of Results

Table II contains the experimental  $x$ ,  $y$ ,  $P$  equilibrium data obtained at  $90.0^\circ\text{C}$ . The vaporization equilibrium constants ( $k = y/x$ ) and activity coefficients were calculated and are also tabulated in Table II. The liquid phase

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