

# Partial Pressures of Hydrogen Sulfide over Aqueous Diethanolamine Solutions

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The solubility of hydrogen sulfide in aqueous solutions of diethanolamine was determined at temperatures between 25° and 120°C in two solutions, 0.5N and 5N DEA. Partial pressures of H<sub>2</sub>S ranged from 0.1 to 258 psia. The results were combined with earlier data, and smoothed values are presented.

As an extension of our previous work (1), the partial pressures of H<sub>2</sub>S over 0.5N and 5N diethanolamine solutions have been measured at temperatures of 25°, 50°, 75°, 100°, and 120°C and at partial pressures from 0.1 to 258 psia. The data are given in Tables I and II (deposited with the ACS Microfilm Depository Service). These data have been combined with our previous results and those of Leibush and Shneerson (2) for smoothing purposes. The smoothed results are presented in Table III and cover the temperature range 25–140°C, the partial pressure range 0.01–300 psia, and solutions of normality ranging from 0.5N to 5N DEA. These results include the conditions of operation of most industrial gas treating units.

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Table III. Smoothed Data for Solubility of H<sub>2</sub>S in DEA Solutions

DEA soln, N	H <sub>2</sub> S partial press, psia	$\alpha$ , mole ratio in liquid, H <sub>2</sub> S/DEA					
		25	50	75	100	120	140
0.5	0.01	0.188	0.083	0.010 <sup>a</sup>	...	...	...
	0.03	0.247	0.121	0.042 <sup>a</sup>	...	...	...
	0.06	0.294	0.159	0.070	...	...	...
	0.1	0.333	0.193	0.091	0.032 <sup>a</sup>	...	...
	0.3	0.432	0.285	0.170	0.088	0.042 <sup>a</sup>	0.020 <sup>a</sup>
	0.6	0.502	0.355	0.231	0.137	0.083	0.048 <sup>a</sup>
	1.0	0.559	0.414	0.286	0.180	0.122	0.071 <sup>a</sup>
	3.0	0.685	0.557	0.423	0.295	0.221	0.160 <sup>a</sup>
	6.0	0.780	0.658	0.522	0.394	0.310	0.238 <sup>a</sup>
	10.0	0.861	0.740	0.613	0.480	0.391	0.317 <sup>a</sup>
30.0	0.094	0.966	0.850	0.722	0.616	0.520 <sup>a</sup>	
	0.144	1.446	1.200	1.066	0.950	0.815	0.705 <sup>a</sup>
	1.00	1.921	1.500	1.278	1.175	1.020	0.900 <sup>a</sup>
	2.00	3.040	2.255	1.765	1.600	1.509	1.390 <sup>a</sup>
	3.00	...	2.250	1.970	1.853	1.780 <sup>a</sup>	
2.0	0.01	0.068	0.028	0.005 <sup>a</sup>	...	...	...
	0.03	0.111	0.066	0.020 <sup>a</sup>	...	...	...
	0.06	0.168	0.100	0.036 <sup>a</sup>	...	...	...
	0.1	0.229	0.136	0.055 <sup>a</sup>	0.023 <sup>a</sup>	...	...
	0.3	0.396	0.222	0.119	0.054 <sup>a</sup>	0.020 <sup>a</sup>	...
	0.6	0.508	0.310	0.178	0.090 <sup>a</sup>	0.048 <sup>a</sup>	0.028 <sup>a</sup>
	1.0	0.587	0.382	0.230	0.120	0.079 <sup>a</sup>	0.046 <sup>a</sup>
	3.0	0.738	0.552	0.370	0.202	0.140	0.100 <sup>a</sup>
	6.0	0.812	0.660	0.469	0.280	0.199	0.150 <sup>a</sup>
	10.0	0.865	0.730	0.546	0.348	0.248	0.190 <sup>a</sup>

Table III. Continued

DEA soln, N	H <sub>2</sub> S partial press, psia	$\alpha$ , mole ratio in liquid, H <sub>2</sub> S/DEA					
		25	50	75	100	120	140
3.5	30.0	0.950	0.870	0.733	0.533	0.413	0.326 <sup>a</sup>
	60.0	1.030	0.936	0.850	0.683	0.560	0.441 <sup>a</sup>
	100	1.190	1.002	0.945	0.808	0.680	0.555 <sup>a</sup>
	200	1.473	1.215	1.107	1.030	0.927	0.808 <sup>a</sup>
	300	1.760	1.400	1.280	1.178	1.102	1.012 <sup>a</sup>
	5.0	0.01	0.040 <sup>a</sup>	0.012 <sup>a</sup>	...	...	...
	0.03	0.081 <sup>a</sup>	0.038 <sup>a</sup>	...	...	...	...
	0.06	0.130	0.070	0.020 <sup>a</sup>	...	...	...
	0.1	0.194	0.087	0.040 <sup>a</sup>	0.020 <sup>a</sup>	...	...
	0.3	0.279	0.154	0.070	0.036 <sup>a</sup>	0.014 <sup>a</sup>	...
6.0	0.6	0.361	0.226	0.109	0.057	0.031 <sup>a</sup>	...
	1.0	0.452	0.278	0.146	0.078	0.050	0.029 <sup>a</sup>
	3.0	0.630	0.417	0.252	0.148	0.092	0.055 <sup>a</sup>
	6.0	0.707	0.522	0.338	0.220	0.134	0.086 <sup>a</sup>
	10.0	0.755	0.620	0.423	0.282	0.175	0.122 <sup>a</sup>
	30.0	0.849	0.773	0.652	0.465	0.332	0.246 <sup>a</sup>
	60.0	0.940	0.851	0.765	0.615	0.479	0.365 <sup>a</sup>
	100	1.020	0.920	0.830	0.712	0.600	0.482 <sup>a</sup>
	200	1.155	1.040	0.945	0.840	0.747	0.653 <sup>a</sup>
	300	1.278	1.138	1.040	0.926	0.846	0.762 <sup>a</sup>
10.0	0.01	0.020 <sup>a</sup>	...	...	...	...	...
	0.03	0.062 <sup>a</sup>	0.027 <sup>a</sup>	...	...	...	...
	0.06	0.108	0.050	0.017	...	...	...
	0.1	0.152	0.072	0.028	0.010 <sup>a</sup>	...	...
	0.3	0.281	0.143	0.061	0.024 <sup>a</sup>	...	...
	0.6	0.373	0.203	0.087	0.040	0.017 <sup>a</sup>	...
	1.0	0.444	0.251	0.114	0.055	0.027	...
	3.0	0.609	0.381	0.211	0.112	0.061	0.031 <sup>a</sup>
	6.0	0.716	0.490	0.298	0.171	0.099	0.054 <sup>a</sup>
	10.0	0.779	0.580	0.379	0.227	0.138	0.080 <sup>a</sup>
30.0	30.0	0.870	0.780	0.595	0.415	0.283	0.180 <sup>a</sup>
	60.0	0.918	0.848	0.738	0.600	0.453	0.287 <sup>a</sup>
	100	0.988	0.890	0.805	0.702	0.560	0.431 <sup>a</sup>
	200	1.140	1.002	0.940	0.811	0.692	0.606 <sup>a</sup>
	300	1.300	1.110	1.010	0.891	0.771	0.694 <sup>a</sup>

<sup>a</sup> Extrapolated values.

## Literature Cited

- (1) Lee, J. I., Otto, F. D., Mather, A. E., *J. Chem. Eng. Data*, **18**, 71 (1973).
- (2) Leibush, A. G., Shneerson, A. L., *Zh. Prik. Khim.*, **23**, 145 (1950).

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