Table IV. Smoothed Values of Excess Enthalpies	of	Mixing of
Tri-n-dodecylamine with Hydrocarbons	at	303.15K
(do Volume Fraction of Hydrocarbon H <sup>E</sup>	: J,	/ml)

$\Phi_2$	n-Octane, H <sup>Eª</sup>	Benzene, H <sup>Eb</sup>	Chloro- benzene, H <sup>E<sup>c</sup></sup>
0.1	0.124	2.564	1.543
0.2	0.190	4.552	2.809
0.3	0.235	6.022	3.651
0.4	0.273	6.967	4.025
0.5	0.303	7.347	3.965
0.6	0.314	7.110	3.553
0.7	0.292	6.218	2.888
0.8	0.228	4.675	2.057
0.9	0.124	2,549	1.103

 $^{a}$   $H^{E} = \Phi_{1}\Phi_{2}(1.214 + 0.455(\Phi_{1} - \Phi_{2}) + 0.257(\Phi_{1} - \Phi_{2})^{2} - 0.714(\Phi_{1} - \Phi_{2})^{2})$  $(\Phi_2)^3$ ].  $\sigma_d = 0.003 \text{ Jml}^{-1}$ .  $\sigma_m = 0.007 \text{ Jml}^{-1}$ .  ${}^{b}H^{E} = \Phi_1 \Phi_2 [29.39 - 1000 \text{ Jml}^{-1}]$  $1.598(\Phi_1 - \Phi_2) - 1.537(\Phi_1 - \Phi_2)^2 + 2.665(\Phi_1 - \Phi_2)^3$ ].  $\sigma_d = 0.162 \text{ Jml}^{-1}\tau$  $\sigma_m = 0.39 \text{ Jm}^{-1}$ .  $^c H^E = \Phi_1 \Phi_2 [15.86 + 5.036(\Phi_1 - \Phi_2) - 1.817(\Phi_1 - \Phi_2)]$  $\Phi_2$ )<sup>2</sup> - 0.310( $\Phi_1 - \Phi_2$ )<sup>3</sup>],  $\sigma_d = 0.08 \text{ Jm}^{-1}$ ,  $\sigma_m = 0.115 \text{ Jm}^{1-1}$ .

cal interactions (3). These reactions are usually endothermic, as are the heats of mixing in the systems under consideration.

The tridodecylamine-octane mixtures are the most ideal, the endothermic heats of mixing being of a comparable magnitude to those of two hydrocarbons, if one of them is slightly polar. The dipole moment of the amine is of the order of 0.3 debyes (7). The substantial difference in the  $H^E$  values between this system and those with the two aromatic hydrocarbons may be taken as fair evidence that the contribution of  $n-\pi$  interactions between the lone-pair electrons of the nitrogen atom and the  $\pi$ electrons of the aromatic ring to the observed heats of mixing is small. That the  $H^E$  values are more endothermic than in the corresponding amine-octane system can best be explained by assuming that the energy needed for breaking the ring-ring bonds is not compensated by the energy of the interaction between the nitrogen of the amine and the  $\pi$ -electrons of the aromatic ring. Chlorobenzene is apparently a less associated liquid than benzene.

We are reporting (5) evidence to show that the strength of  $n-\pi$  interactions is strongly dependent on the length of the hydrocarbon chain in the tertiary amine molecule. Long aliphatic chains screen the nitrogen effectively and thus diminish its availability for interactions with  $\pi$ -electrons.

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# Apparent Molal Volumes of Aqueous NaF, Na<sub>2</sub>SO<sub>4</sub>, KCl, K<sub>2</sub>SO<sub>4</sub>, MgCl<sub>2</sub>, and MgSO₄ Solutions at 0° and 50°C

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The apparent molal volumes,  $\Phi_V$ 's, of dilute (0.002–1*m*) aqueous solutions of NaF, Na<sub>2</sub>SO<sub>4</sub>, KCl, K<sub>2</sub>SO<sub>4</sub>, MgCl<sub>2</sub>, and MgSO<sub>4</sub> are determined at 0° and 50°C from precision density measurements made with a magnetic float densitometer. The infinite dilution apparent molal volumes,  $\Phi_V^{\circ}$ 's, are determined by using the Redlich equation,  $\Phi_V = \Phi_V^{\circ} + S_V c^{1/2} + b_V c$ , where  $S_V$  is the Debye-Hückel limiting law slope, and  $b_V$  is a deviation constant. At 0°C the deviations are positive for all the salts except MgCl<sub>2</sub>. The temperature dependence of the  $b_V$  for all the salts is similar to other common electrolytes ( $\partial b_V / \partial T$  is negative). The effect of temperature on the  ${\Phi_V}^\circ$ 's of all the electrolytes is similar in that  $\partial^2 \Phi_V^{\circ} / \partial T^2$  is negative. The ion-ion and ion-water interactions responsible for the observed behavior of the  $\Phi_V$ 's are briefly discussed.

Although there are reliable density and apparent molal volume data for many aqueous electrolyte solutions at 25°C (8), little reliable data are available at other temperatures (14). Recently (11, 13) we had need for reli-<sup>1</sup> To whom correspondence should be addressed.

able apparent molal volume data for some sea salts (NaCl, MgCl<sub>2</sub>, Na<sub>2</sub>SO<sub>4</sub>, MgSO<sub>4</sub>, NaF, KCl, K<sub>2</sub>SO<sub>4</sub>) at temperatures between 0° and 40°C. The present paper contains results of the densities and apparent molal volumes of some of these sea salts at 0° and 50°C from 0.002 to 1 molal.

#### Experimental

All the solutions were made by weight with reagentgrade (Baker Analyzed) chemicals (without further purification) and ion-exchanged water (Millipore Super Q). The concentrations of the KCl, K<sub>2</sub>SO<sub>4</sub>, Na<sub>2</sub>SO<sub>4</sub>, and MgSO<sub>4</sub> stock solutions were analyzed by heating to dryness, whereas the concentrations of the MgCl<sub>2</sub> stock solution were analyzed for  $Cl^-$  by titration with AgNO<sub>3</sub>.

The magnetic float densitometer used to make the density measurements and a review of the development of the magnetic float method were described in detail elsewhere (12). The densitometer consists of a 110-cm<sup>3</sup> solution container which fits into a brass support containing a solenoid. The float (32 cm<sup>3</sup>) is made of borosilicate glass and contains a magnet. The densitometer was calibrated with ion-exchanged water by using the densities (g/ml) tabulated by Kell (7). The density measurements

## Table I. Densities and Apparent Molal Volumes of Aqueous KCl, NaF, Na<sub>2</sub>SO<sub>4</sub>, K<sub>2</sub>SO<sub>4</sub>, MgCl<sub>2</sub>, and MgSO<sub>4</sub> Solutions at 0° and 50°C<sup>a</sup>

	NaF, 0°C		N	/IgCl₂, 0°C			NaF, 50°C		N	a₂SO4, 50°C			
m	1000 ∆d	Φι-	m	1000 Δd	$\Phi_V$	m	1000 ∆d	Φι·	m	1000 Ad	$\Phi_{1}$		
0.009715	0.4700	-6.400	0.13720	11,2162	13,315	0.010102	0.4338	1.484	0 002226	0 2804	14 745		
0.029258	1.4109	-6.235	0.17359	14.1197	13.678	0.019600	0.8406	-1.432	0.006220	0 7824	14 905		
0.090096	4,3064	-5.792	0.25072	20,2238	14.262	0.039394	1.6840	-1.290	0.006274	0.7878	15 129		
0.153786	7,2963	-5.424	0.34124	27,2805	14,861	0 079954	3 4070	-1.149	0.012695	1 5905	15.125		
0.243098	11.4628	-5.113	0.42814	33,9473	15 399	0 143533	6 0842	-0.918	0.012095	1 7018	15 /32		
0.268629	12,6310	-4.976	0.50904	40,1183	15 767	0.243280	10 2267	-0.557	0.014500	3 3076	15 012		
0.360703	16.8610	-4.684	0.62437	48.7665	16 311	0 337712	14 1444	-0 400	0.044254	5 4907	16 572		
0.360255	16.8286	-4.653	0.70544	54,7187	16.729	0.430678	17,9545	-0.203	0.044204	10 4949	17 608		
0.497018	23.0247	-4.246	0.82932	63.8230	17.159	0.571046	23.6743	0.029	0 15125	18 3991	18 803		
		-	1.01833	77.4084	17.818	0.803873	32.9935	0.440	0,22660	27.2975	19.811		
0 000507	Na2304, 0 C	2 640	1.01840	77.4134	17.818				0.28814	34.4945	20.415		
0.00356/	0.49/1	2.048							0.41164	48.6398	21.654		
0.008254	1.14/1	3.03/		KCI, 50°C			K₂SO₄, 0°C		0.53857	62.9239	22.637		
0.008301	1.1011	2.9//	0.028720	1.3309	27.496	0.003007	0.4511	24.227	0.69983	80.6510	23.768		
0.0110/3	1.0213	3,120	0.059958	2.7644	28.146	0.004334	0.6501	24.231	0.79824	91.2671	24.386		
0.013031	1.9194	3.23/ 3 101	0.16026	7.3134	28.497	0.005597	0.8387	24.370	1.00476	113.0439	25.583		
0.014650	2.0398	2 201	0.33955	15.2979	28.857	0.007897	1.1835	24.430	1.00476	113.0488	25.578		
0.010009	2.1097	3.301	0.57774 <sub>5</sub>	25.6514	29.215	0.010278	1.5363	24.738		(.SO. 50°C			
0.017661	2.3027	2 200	0.76650	33.6785	29.442	0.014920	2.2738	25.237	0.001004		04 550		
0.017001	2,4497	3.309	1.00327	43.4879	29.743	0.014715	2.1919	25.150	0.001994	0.2/61	24.556		
0.01/808	2.4090	2 202				0.019454	2.8944	25.398	0.003113	0.4304	34./43		
0.01998/	2.7700	3.392	Mg	Cl <sub>2</sub> , 50°C		0.027948	4.1439	25.872	0.004975	0.6861	35,089		
0.020/99	2.0010	2 59/	0.003191	0.2568	13.918	0.034366	5.0833	26.204	0.007964	1.0954	35.438		
0.024100	3.3470	3,304	0.007843	0.6290	14.203	0.036851	5.4457	26.337	0.012674	1./388	35./80		
0.024996	3.4572	3.709	0.010834	0.8671	14.369	0.048361	7.1219	26.800	0.018302	2.0030	30.1/1		
0.024550	3 7232	3 699	0.016475	1.7590	14.449	0.054081	7.9512	27.014	0.027808	3.7003	37.007		
0.020919	1 1948	3 707	0.022025	1.7590	14.531	0.069961	10.2435	27.555	0.035209	4.//3/	37.317		
0.030331	4.1948	4 000	0.026501	2.1108	14.742	0.099044	14.4057	28.399	0.046770	0.0607	37.910 29 176		
0.034703	5 6091	4.000	0.035536	2.8435	14.357	0.13033	18.8196	28.980	0.007613	12 0275	20.170		
0.040147	6 7567	4.511	0.046302	3.6677	15.166	0.15934	22.9357	29.631	0.090042	12.9375	30.004		
0.054676	7 4985	4.841	0.055539	4.3914	15.303	0.21831	31.1124	30.794	0.10092	17 8327	39.014		
0.061606	8,4390	4,998	0.089625	7.0445	15.738	0.28097	39.6358	31.121	0.15585	22 5195	39.210		
0.070549	9.6379	5,359	0.096011	7.5486	15.708	0.36472	50.8675	33.103	0.10333	26 8477	40 013		
0.082529	11.2352	5.822	0.12308	9.6294	16.068				0.20523	29.6710	40.228		
0,099410	13,4818	6.320	0.17339	13.4882	16.453		M~60 000		0.25632	33,6047	40.702		
0.105998	14.3357	6.682	0.24965	19.2903	16.885	0.0051-0	Mg50₄, 0°C		0.31119	40.5636	41.166		
0.126706	17.0637	7.228	0.3/062	28.2/19	1/./16	0.0051/0	0.6822	-11.583	0.36270	46.9749	41.730		
0.147918	19.8493	7.680	0.4/693	36.1026	18,160	0.00/469	0.9800	-10.853	0.36880	47.7854	41.642		
0.177700	23.7353	8.258	0.04005	48.3318	18.8/9	0.014391	1.8805	-10.306	0.52848	67.2859	43.030		
0.259374	34.2313	9.715	0.82033	50.990Z	19.552	0.019090	2.4784	9.450	0.70706	88.5197	44,181		
0.347180	45.2643	11.143	0.99421	72.5900	20.097	0.027767	3.5/84	-8.498					
0.469650	60.3261	12.803	N	lgSO4, 50°C		0.032379	4.1041						
0.557229	70.8333	13.922	0 002420	0001,000	5 016	0.030007	4.0909 5 7127	7 521					
0.705014	88.2276	15.514	0.002439	0.3039	-4 674	0.044002	6 8711	-7 136					
0.921454	112.8616	17.562	0.000403	1 6036		0.053878	8 0435	6 778					
	MgCl <sub>2</sub> , 0°C		0.018164	2.2115	-2 892	0.069471	8.8634	-6.686					
0.008785	0.7386	11,125	0.026523	3.2115	-2.201	0.089133	11.2628						
0.010774	0.9056	11.123	0.040100	4.8309	-1.576	0.100205	12.6247	-5.573					
0.015048	1.2617	11.355	0.064372	7,7068	-0.810	0.11478	14,4291	-5.291					
0.018179	1.5231	11.410	0.10706	12.7219	0.102	0.14239	17.8252	-4.755					
0.025081	2.0935	11.717	0.17204	20.2727	1.092	0.18277	22.7279	-3.915					
0.026659	2.2248	11.732	0.24497	28.6377	2.014	0.24491	30.2141	-2.936					
0.031383	2.6133	11.910	0.35275	40.8393	3.101	0.36328	44.2783	1.474					
0.043333	3.5927	12.258	0.446996	51.3353	3.974	0.49772	59.9735	-0.140					
0.056311	4.6538	12.508	0.58829	66.8730	5.040	0.71312	84.5670	1.623					
0.07966	6.5606	12.778	0.72061	81.2010	5.909	0.89006	104.2264	2.941			25.5/8 24.556 34.743 35.089 35.438 35.786 36.171 37.067 37.317 37.910 38.176 38.604 39.014 39.210 39.777 40.013 40.228 40.702 41.166 41.730 41.642 43.030 44.181		
0.09649	7.9352	12.876	0.88872	99.1366	6.867	0.89033	104.2576	2.941					

 $^{\rm a}$  Densities are in units of g/ml, and  $\Phi_{\rm V}$  is in units of ml/mol.

were made by the weight dilution technique (9) and on single stock solutions (12). Duplicate density measurements on the same solution agreed to within  $\pm 2$  ppm. The reproducibility of  $\pm 0.2$  in the apparent molal volumes in the most dilute solutions (0.002) indicates that the density precision within a given experimental run was  $\pm 0.3$  ppm.

The temperature of the bath containing the densitometer was set to  $\pm 0.001^{\circ}$ C with a platinum resistance thermometer (calibrated by NBS) and a G-2 Mueller bridge. The bath was regulated to better than  $\pm 0.001^{\circ}$ C with a Tronac thermal regulator. This temperature variation corresponds to a density uncertainty of  $\pm 0.3$  ppm or  $\pm 0.2$  in the apparent molal volume in the most dilute solutions. During an experimental run, the bath was monitored with a Hewlett-Packard quartz crystal thermometer and recorder.

#### **Results and Discussion**

The densities of dilute aqueous solutions of NaF, Na<sub>2</sub>SO<sub>4</sub>, K<sub>2</sub>SO<sub>4</sub>, MgCl<sub>2</sub>, and MgSO<sub>4</sub> were determined at 0° and 50°C with the magnetic float densitometer. Measurements on KCl solutions were made only at 50°C. The results of the difference ( $\Delta d = d - d^{\circ}$ ) between the density of solutions (d) and the density of water (d°) at various molal concentrations (*m*) are given in Table I. The apparent molal volumes ( $\Phi_V$ 's) of these solutions were calculated from

$$\Phi_V = \frac{1000(d - d^{\circ})}{dd^{\circ}m} + \frac{M}{d}$$
(1)

where *m* is the molality, and *M* is the molecular weight of electrolytes (using the 1969 atomic weights). The  $\Phi_V$ 's of these solutions are given in Table I and are shown in Figures 1-6 as a function of the square root of molar concentrations  $(c)^{1/2}$ . The infinite dilute apparent molal volumes  $(\Phi_V^{\circ} = \bar{V}_2^{\circ})$  for these solutions were obtained by extrapolation with the Redlich (15, 16) equation (below c = 0.2)

$$\Phi_V = \Phi_V^{\circ} + S_V c^{1/2} + b_V c$$
 (2)

where  $S_V$  is the Debye-Hückel limiting law slope (8, 15), c is the molar concentration [ $c = md^\circ 10^3/(10^3 + \Phi_V md^\circ)$ ], and  $b_V$  is an empirical constant. As apparent from Figures 1-6, the  $\Phi_V$ 's of the NaF, Na<sub>2</sub>SO<sub>4</sub>, K<sub>2</sub>SO<sub>4</sub>, and MgCl<sub>2</sub> solutions all approach limiting law behavior in di-



**Figure 1.** Apparent molal volumes,  $\Phi_V$ , of NaF solutions as function of  $\sqrt{c}$  at 0° and 50°C. Straight lines are Debye-Hückel theoretical limiting law slopes (8, 15)



**Figure 2.** Apparent molal volumes,  $\Phi_V$ , of Na<sub>2</sub>SO<sub>4</sub> solutions as function of  $\sqrt{c}$  at 0° and 50°C. Straight lines are Debye-Hückel theoretical limiting law slopes (*8*, *15*)



**Figure 3.** Apparent molal volumes,  $\Phi_V$ , of KCI solutions as function of  $\sqrt{c}$  at 0° and 50°C. 0°C data are taken from Dunn (2). Straight lines are Debye-Hückel theoretical limiting law slopes (8, 15)



**Figure 4.** Apparent molal volumes,  $\Phi_V$ , of K<sub>2</sub>SO<sub>4</sub> solutions as function of  $\sqrt{c}$  at 0° and 50°C. Straight lines are Debye-Hückel theoretical limiting law slopes (8, 15)

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**Figure 5.** Apparent molal volumes,  $\Phi_V$ , of MgCl<sub>2</sub> solutions as function of  $\sqrt{c}$  at 0° and 50°C. Straight lines are Debye-Hückel theoretical limiting law slopes (8, 15)



**Figure 6.** Apparent molal volumes,  $\Phi_V$ , of MgSO<sub>4</sub> solutions as function of  $\sqrt{c}$  at 0° and 50°C. Straight lines are Debye-Hückel theoretical limiting law slopes (8, 15)

lute solutions. The large positive deviations from the limiting law for the MgSO<sub>4</sub> solutions make it difficult to use Equation 2 to obtain an infinite  $\Phi_V^{\circ}$ . We have thus used large plots of the  $\Phi_V$  vs.  $c^{1/2}$  to estimate the  $\Phi_V^{\circ}$ 's for MgSO<sub>4</sub>.

The infinite dilution  $\overline{V_2}^{\circ}$ 's for these solutions at 0° and 50°C are given in Table II along with the results obtained by other workers (1-6, 10, 15-19). Also given in Table II are the  $\overline{V_2}^{\circ}$ 's for these salts at 25°C obtained by other workers (1-6, 8-10, 14, 16).

Our results at 0° and 50°C (except for KCI) cannot be directly compared to the work of others because of the error in extrapolation to infinite dilution made by earlier workers (8, 14). As pointed out elsewhere (8), the errors made by earlier workers are caused by neglecting to use the limiting law as an aid in the extrapolation and by

Table II. Infinite Dilution Partial Molal Volumes of Aqueous NaF, Na<sub>2</sub>SO<sub>4</sub>, KCl, K<sub>2</sub>SO<sub>4</sub>, MgCl<sub>2</sub>, and MgSO<sub>4</sub> Solutions at 0°, 25°, and 50°C

		$\overline{V}_2^{\circ}$ , m	il/mol
Salt	0°C	25°C	50°C
NaF	6.51, <sup>a</sup> 5.72 <sup>b</sup>	2.375	$-1.77,^{a}-1.7^{b}$
Na <sub>2</sub> SO <sub>4</sub>	2.33,ª 3.7°	11.56%	14.09,ª 15.5ª
KCI	23.62 <sup>b</sup>	26.85	27.57,ª 27.66,º 27.64,' 27.9ª
			27.87, <sup>g</sup> 27.12 <sup>h</sup>
K₂SO₄	23.79,ª 22.7 <sup>i</sup>	32.02b	33.63,ª 35.1ª
$MgCl_2$	10.42,ª 12.7,º 11.4/	14.49 <sup>b</sup>	13.40,ª 14.70,′ 15.1ď
MgSO₄	-13.06,ª -10.0°	-7.19 <sup>b</sup>	-8.14, <sup>a</sup> -4.87 <sup>b</sup>

<sup>a</sup> This study. <sup>b</sup> Millero's compilation (14). <sup>c</sup> Zen (19). <sup>d</sup> Ellis (3-5). <sup>e</sup> Scott (18). <sup>f</sup> Root (17). <sup>g</sup> Akerlof and Bender (1). <sup>h</sup> Redlich and Rosenfeld (16). <sup>f</sup> Jones and Calvin (6).

#### Table III. Partial Molal Expansibilities at Infinite Dilution for NaF, Na<sub>2</sub>SO<sub>4</sub>, KCl, K<sub>2</sub>SO<sub>4</sub>, and MgSO<sub>4</sub> at 12.5° and 37.5°C

	$\Phi_E^\circ = \overline{E}^\circ, ml$	$\Phi_E^\circ = \overline{E}^\circ, \text{ ml/mol}^{-1} \text{ deg}^{-1}$			
Salt	12.5°C	37.5°C			
NaF	0.1656	0.0240			
NaCl⁰	0.1488	0.0484			
Na₂SO₄	0.3716	0.0988			
KCI	0.1288	0.0288			
K₂SO₄	0.3280	0.0656			
MgCl <sub>2</sub>	0.1628	-0.0436			
MgSO4	0.2352	-0.0384			

<sup>a</sup> Millero (10).

using unreliable  $\Phi_V$ 's at low concentrations (i.e., unreliable densities). Note that an improper extrapolation to infinite dilution can give  $\Phi_V$ 's that are in error by as much as 3 ml/mol (8) for a 1-1 electrolyte.

By linearly extrapolating Dunn's (2) work at 45° and 55°C, one obtains  $\Phi_V^{\circ}$  (KCl) = 27.57 ml/mol, which is in excellent agreement with our extrapolated values.

The internal consistency of our values for  $\Phi_V^{\circ}$  can be tested by using the additivity principle. The differences between  $\Phi_V^{\circ}$  (1/2 K<sub>2</sub>SO<sub>4</sub>) and  $\Phi_V^{\circ}$  (1/2 Na<sub>2</sub>SO<sub>4</sub>) are 10.73 and 9.77 ml/mol, respectively, at 0° and 50°C compared to 10.68 and 9.87 obtained from the  $\Phi_V^{\circ}$ 's of KCl and NaCl (2, 8, 10). The  $\Phi_V^{\circ}$  of MgSO<sub>4</sub> can be calculated by the additivity principle using the  $\Phi_V^{\circ}$ 's of MgCl<sub>2</sub>, Na<sub>2</sub>SO<sub>4</sub>, K<sub>2</sub>SO<sub>4</sub>, NaCl, and KCl. The additivity method gives  $\Phi_V^{\circ}$  (MgSO<sub>4</sub>) = -13.05 and -13.03 ml/mol at 0° and -8.17 and -8.11 ml/mol at 50°C, respectively, from the Na<sup>+</sup> and K<sup>+</sup> salts.

The infinite dilution partial molal expansibilities,  $\Phi_E^{\circ} = \bar{E}_2^{\circ} = \partial \Phi_V^{\circ} / \partial T$  at 12.5° and 37.5°C for these electrolytes, are given in Table III, along with the results for NaCl (10). The  $\bar{E}_2^{\circ}$ 's for all of the electrolytes decrease with increasing temperature (i.e.,  $\partial \bar{E}_2^{\circ} / \partial T$  is negative). As discussed elsewhere (8, 14), the decrease in  $\bar{E}_2^{\circ}$  for electrolytes or the maximum in the  $\bar{V}_2^{\circ}$  can be attributed to the decrease in volume owing to the increase in electrostriction with increasing temperature.

The deviations from the limiting law  $(b_V)$  of the  $\Phi_V$ 's at 0°C for all of the electrolytes, with the exception of MgCl<sub>2</sub>, are positive. At 50°C, the positive deviations become smaller (MgSO<sub>4</sub> and K<sub>2</sub>SO<sub>4</sub>) or close to zero (NaF and Na<sub>2</sub>SO<sub>4</sub>). The deviations of  $\Phi_V$ 's for the MgCl<sub>2</sub> solu-

tions are near zero at 0° and negative at 50°C. The effect of temperature on the  $b_V$ 's for all the electrolytes is similar in that  $\partial b_V / \partial T$  is negative. The large positive deviations for most of the electrolytes at 0° and K<sub>2</sub>SO<sub>4</sub> and MgSO4 at 50°C may be due to cation anion ion pair formation (10). The large negative deviations for MgCl<sub>2</sub> solutions at 50°C are what one might expect from the extended Debye-Hückel equation or if cation-cation and anion-anion interactions are more important than cationanion interactions (10).

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## Diffusion Coefficients of O<sub>2</sub>, N<sub>2</sub>, and CO<sub>2</sub> in Fluorinated Ethers

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Diffusion coefficients of O<sub>2</sub>, N<sub>2</sub>, and CO<sub>2</sub> in three fluorinated ethers are measured at 25° and 37°C. These coefficients are, in general, about twice as large as those in water.

Large gas solubilities in certain fluorinated ethers have stimulated considerable interest in their use as potential oxygen carriers in liquid breathing (5), in cardiopulmonary bypass machines (3), and as blood substitutes (8). To compute the mass-transfer rate during such processes, the diffusion coefficients of  $O_2$ ,  $N_2$ , and  $CO_2$  are needed. We have undertaken to measure these values for gases in fluorinated ethers at 25° and 37°C. The compounds studied were Caroxin-D (perfluoro-1,4 diisopropoxy butane) (Allied Chemical Corp., Morristown, N.J.), Caroxin-F (perfluoro-1-isopropoxy hexane) (Allied Chemical Corp., Morristown, N.J.), and FC-80 (perfluorobuty) perfluorotetrahydrofuran) (3M Co., St. Paul, Minn.).

#### Experimental

Materials. Minimum purities of O2, N2, and CO2 were 99.6%. Caroxin-D and Caroxin-F were of greater than 99.9% purity as supplied, whereas FC-80 contains several isomers (2).

Procedure. Diffusion coefficients were measured with a modified Stokes' diaphragm cell (9). The procedure was described in detail by Tham and Gubbins (11), and we shall present only essential information here. The diaphragms were of porosity D (ASTM 10-20  $\mu$ m), and stirring was accomplished with magnetic stirrers, rotating at 60 rpm. The diaphragm cells were immersed in a constant temperature bath controlled to within  $\pm 0.02^{\circ}$  of the desired temperature with a proportional controller.

The cells were calibrated with 0.1N HCl, each cell being calibrated twice at the beginning of the work; cell constants were reproducible within  $\pm 0.5\%$ . [The diffusion coefficients are known accurately for the HCI-H2O system (10).]

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The solvent-filled diaphragm method was used for both the calibration and diffusion coefficient measurement runs. Diffusion coefficients were calculated from the equation (1, 4)

$$D_{12} = \frac{1}{\beta t} \ln \left[ \frac{C_B^{\circ}}{C_B - C_T} \right] \left[ 1 - \frac{\lambda}{6} \right]$$
(1)

where  $D_{12}$  is the differential diffusion coefficient of 1 in 2.

$$C_B^{\circ} = C_B \left[ \frac{V_B + 1/2 V_D}{V_D} \right] + C_T \left[ \frac{V_T + 1/2 V_D}{V_B} \right] \quad (2)$$

$$\lambda = \frac{V_D}{V_B + V_T} \tag{3}$$

 $\beta$  is the cell constant derived from calibration with HCl. and t is the time of diffusion; C is the concentration of diffusing substance, and V is the volume. Subscripts B, T, and D refer to bottom and top compartment and diaphragm, respectively.

The cell was first evacuated and then filled with the degassed fluorocarbon. It was equilibrated in a constant temperature bath for 2 hr with constant stirring; then, the bottom chamber was emptied and filled with solution containing the diffusing material. The method of preparing the gas solution and the precautions necessary in filling the cell have been described elsewhere (7, 12).

Solutions containing the dissolved gas were analyzed with a Perkin-Elmer Model 900 gas chromatograph equipped with a thermal conductivity detector. The column was a  $\frac{1}{8}$ -in. X 12-ft Porapak Q column, which was kept at room temperature. The helium carrier gas flow rate was 40 ml/min; injector port and detector temperatures were kept at 100° and 200°C, respectively. Calibration of the chromatograph was done by injecting a known volume of pure gas into the chromatograph and measuring the peak area. Linear response was observed in the range of concentrations of interest. The chromatograph analyses were reproducible to  $\pm 0.6\%$ .

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