

Table IV. Smoothed Values of Excess Enthalpies of Mixing of Tri-*n*-dodecylamine with Hydrocarbons at 303.15K (Φ_2 Volume Fraction of Hydrocarbon H^E J/ml)

Φ_2	<i>n</i> -Octane, H^E ^a	Benzene, H^E ^b	Chlorobenzene, H^E ^c
0.1	0.124	2.564	1.543
0.2	0.190	4.552	2.809
0.3	0.235	6.022	3.651
0.4	0.273	6.967	4.025
0.5	0.303	7.347	3.965
0.6	0.314	7.110	3.553
0.7	0.292	6.218	2.888
0.8	0.228	4.675	2.057
0.9	0.124	2.549	1.103

^a $H^E = \Phi_1\Phi_2[1.214 + 0.455(\Phi_1 - \Phi_2) + 0.257(\Phi_1 - \Phi_2)^2 - 0.714(\Phi_1 - \Phi_2)^3]$, $\sigma_d = 0.003$ J ml⁻¹, $\sigma_m = 0.007$ J ml⁻¹, ^b $H^E = \Phi_1\Phi_2[29.39 - 1.598(\Phi_1 - \Phi_2) - 1.537(\Phi_1 - \Phi_2)^2 + 2.665(\Phi_1 - \Phi_2)^3]$, $\sigma_d = 0.162$ J ml⁻¹, $\sigma_m = 0.39$ J ml⁻¹, ^c $H^E = \Phi_1\Phi_2[15.86 + 5.036(\Phi_1 - \Phi_2) - 1.817(\Phi_1 - \Phi_2)^2 - 0.310(\Phi_1 - \Phi_2)^3]$, $\sigma_d = 0.08$ J ml⁻¹, $\sigma_m = 0.115$ J ml⁻¹.

cal interactions (3). These reactions are usually endothermic, as are the heats of mixing in the systems under consideration.

The tridodecylamine-octane mixtures are the most ideal, the endothermic heats of mixing being of a comparable magnitude to those of two hydrocarbons, if one of them is slightly polar. The dipole moment of the amine is of the order of 0.3 debyes (7). The substantial difference

in the H^E values between this system and those with the two aromatic hydrocarbons may be taken as fair evidence that the contribution of *n*- π interactions between the lone-pair electrons of the nitrogen atom and the π -electrons of the aromatic ring to the observed heats of mixing is small. That the H^E values are more endothermic than in the corresponding amine-octane system can best be explained by assuming that the energy needed for breaking the ring-ring bonds is not compensated by the energy of the interaction between the nitrogen of the amine and the π -electrons of the aromatic ring. Chlorobenzene is apparently a less associated liquid than benzene.

We are reporting (5) evidence to show that the strength of *n*- π interactions is strongly dependent on the length of the hydrocarbon chain in the tertiary amine molecule. Long aliphatic chains screen the nitrogen effectively and thus diminish its availability for interactions with π -electrons.

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Apparent Molal Volumes of Aqueous NaF, Na₂SO₄, KCl, K₂SO₄, MgCl₂, and MgSO₄ Solutions at 0° and 50°C

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The apparent molal volumes, Φ_V 's, of dilute (0.002–1M) aqueous solutions of NaF, Na₂SO₄, KCl, K₂SO₄, MgCl₂, and MgSO₄ are determined at 0° and 50°C from precision density measurements made with a magnetic float densitometer. The infinite dilution apparent molal volumes, Φ_V° 's, are determined by using the Redlich equation, $\Phi_V = \Phi_V^\circ + S_V c^{1/2} + b_V c$, where S_V is the Debye-Hückel limiting law slope, and b_V is a deviation constant. At 0°C the deviations are positive for all the salts except MgCl₂. The temperature dependence of the b_V for all the salts is similar to other common electrolytes ($\partial b_V / \partial T$ is negative). The effect of temperature on the Φ_V° 's of all the electrolytes is similar in that $\partial^2 \Phi_V^\circ / \partial T^2$ is negative. The ion-ion and ion-water interactions responsible for the observed behavior of the Φ_V 's are briefly discussed.

Although there are reliable density and apparent molal volume data for many aqueous electrolyte solutions at 25°C (8), little reliable data are available at other temperatures (14). Recently (11, 13) we had need for reli-

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able apparent molal volume data for some sea salts (NaCl, MgCl₂, Na₂SO₄, MgSO₄, NaF, KCl, K₂SO₄) at temperatures between 0° and 40°C. The present paper contains results of the densities and apparent molal volumes of some of these sea salts at 0° and 50°C from 0.002 to 1 molal.

Experimental

All the solutions were made by weight with reagent-grade (Baker Analyzed) chemicals (without further purification) and ion-exchanged water (Millipore Super Q). The concentrations of the KCl, K₂SO₄, Na₂SO₄, and MgSO₄ stock solutions were analyzed by heating to dryness, whereas the concentrations of the MgCl₂ stock solution were analyzed for Cl⁻ by titration with AgNO₃.

The magnetic float densitometer used to make the density measurements and a review of the development of the magnetic float method were described in detail elsewhere (12). The densitometer consists of a 110-cm³ solution container which fits into a brass support containing a solenoid. The float (32 cm³) is made of borosilicate glass and contains a magnet. The densitometer was calibrated with ion-exchanged water by using the densities (g/ml) tabulated by Kell (7). The density measurements

were made by the weight dilution technique (9) and on single stock solutions (12). Duplicate density measurements on the same solution agreed to within ± 2 ppm. The reproducibility of ± 0.2 in the apparent molal volumes in the most dilute solutions (0.002) indicates that the density precision within a given experimental run was ± 0.3 ppm.

The temperature of the bath containing the densitometer was set to $\pm 0.001^\circ\text{C}$ with a platinum resistance thermometer (calibrated by NBS) and a G-2 Mueller bridge. The bath was regulated to better than $\pm 0.001^\circ\text{C}$ with a Tronac thermal regulator. This temperature variation corresponds to a density uncertainty of ± 0.3 ppm or ± 0.2 in the apparent molal volume in the most dilute solutions. During an experimental run, the bath was monitored with a Hewlett-Packard quartz crystal thermometer and recorder.

Results and Discussion

The densities of dilute aqueous solutions of NaF, Na_2SO_4 , K_2SO_4 , MgCl_2 , and MgSO_4 were determined at 0° and 50°C with the magnetic float densitometer. Measurements on KCl solutions were made only at 50°C . The results of the difference ($\Delta d = d - d^\circ$) between the density of solutions (d) and the density of water (d°) at various molal concentrations (m) are given in Table I. The apparent molal volumes (Φ_V 's) of these solutions were calculated from

$$\Phi_V = \frac{1000(d - d^\circ)}{dd^\circ m} + \frac{M}{d} \quad (1)$$

where m is the molality, and M is the molecular weight of electrolytes (using the 1969 atomic weights). The Φ_V 's of these solutions are given in Table I and are shown in Figures 1-6 as a function of the square root of molar concentrations (c)^{1/2}. The infinite dilute apparent molal volumes ($\Phi_V^\circ = \bar{V}_2^\circ$) for these solutions were obtained by extrapolation with the Redlich (15, 16) equation (below $c = 0.2$)

$$\Phi_V = \Phi_V^\circ + S_V c^{1/2} + b_V c \quad (2)$$

where S_V is the Debye-Hückel limiting law slope (8, 15), c is the molar concentration [$c = md^\circ / (10^3 + \Phi_V md^\circ)$], and b_V is an empirical constant. As apparent from Figures 1-6, the Φ_V 's of the NaF, Na_2SO_4 , K_2SO_4 , and MgCl_2 solutions all approach limiting law behavior in di-

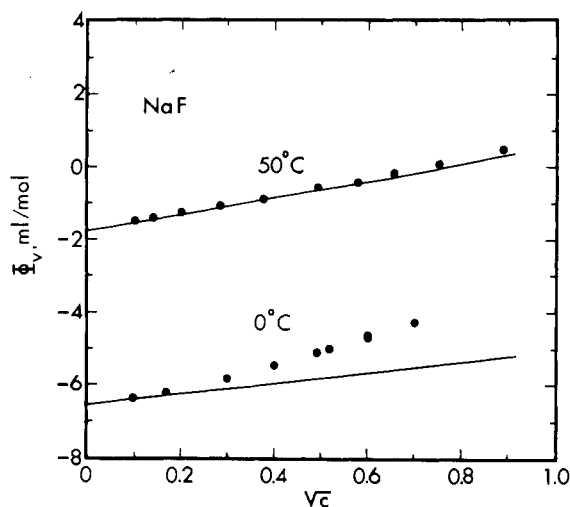


Figure 1. Apparent molal volumes, Φ_V , of NaF solutions as function of \sqrt{c} at 0° and 50°C . Straight lines are Debye-Hückel theoretical limiting law slopes (8, 15)

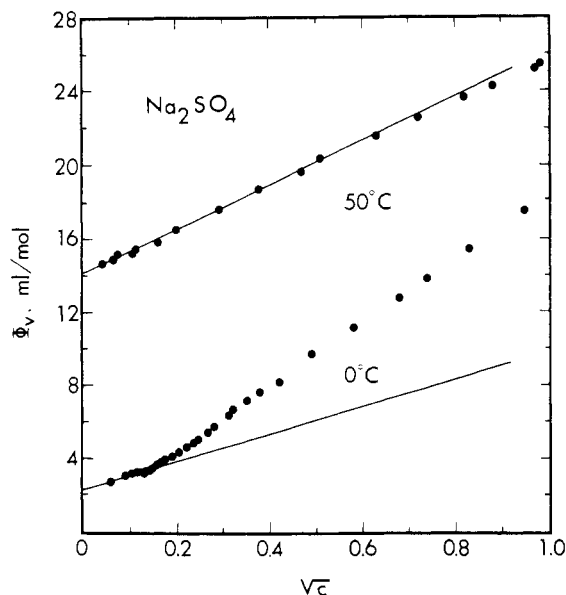


Figure 2. Apparent molal volumes, Φ_V , of Na_2SO_4 solutions as function of \sqrt{c} at 0° and 50°C . Straight lines are Debye-Hückel theoretical limiting law slopes (8, 15)

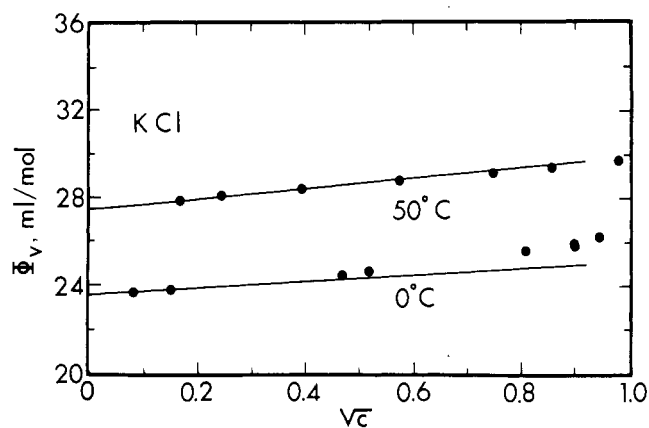


Figure 3. Apparent molal volumes, Φ_V , of KCl solutions as function of \sqrt{c} at 0° and 50°C . 0°C data are taken from Dunn (2). Straight lines are Debye-Hückel theoretical limiting law slopes (8, 15)

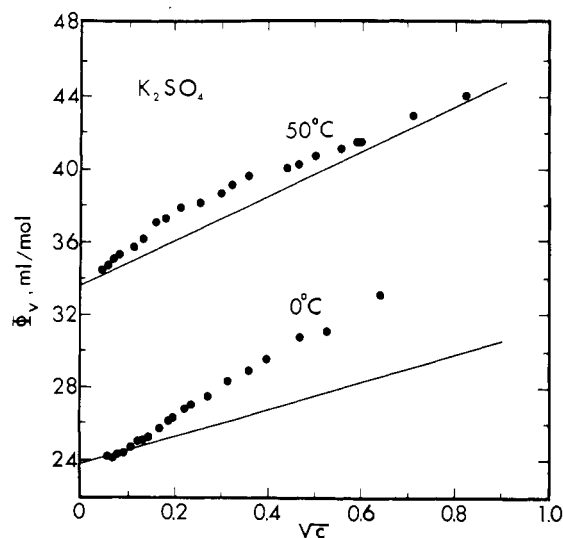


Figure 4. Apparent molal volumes, Φ_V , of K_2SO_4 solutions as function of \sqrt{c} at 0° and 50°C . Straight lines are Debye-Hückel theoretical limiting law slopes (8, 15)

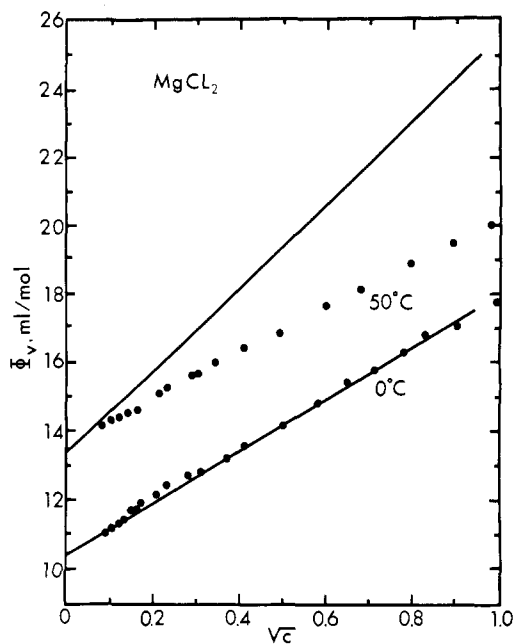


Figure 5. Apparent molal volumes, Φ_V , of MgCl_2 solutions as function of \sqrt{c} at 0° and 50°C. Straight lines are Debye-Hückel theoretical limiting law slopes (8, 15)

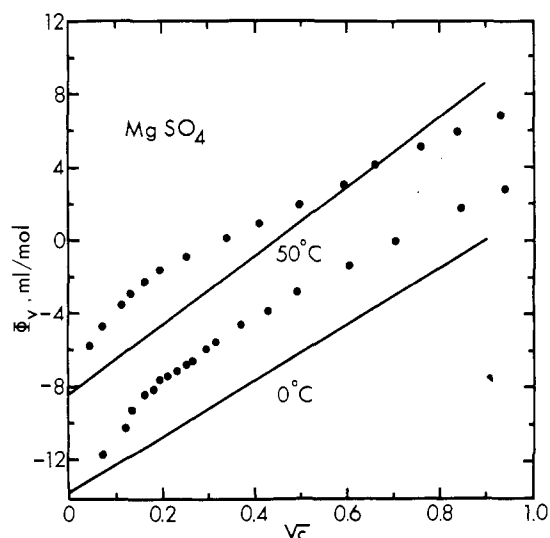


Figure 6. Apparent molal volumes, Φ_V , of MgSO_4 solutions as function of \sqrt{c} at 0° and 50°C. Straight lines are Debye-Hückel theoretical limiting law slopes (8, 15)

lute solutions. The large positive deviations from the limiting law for the MgSO_4 solutions make it difficult to use Equation 2 to obtain an infinite Φ_V° . We have thus used large plots of the Φ_V vs. $c^{1/2}$ to estimate the Φ_V° 's for MgSO_4 .

The infinite dilution \bar{V}_2° 's for these solutions at 0° and 50°C are given in Table II along with the results obtained by other workers (1-6, 10, 15-19). Also given in Table II are the \bar{V}_2° 's for these salts at 25°C obtained by other workers (1-6, 8-10, 14, 16).

Our results at 0° and 50°C (except for KCl) cannot be directly compared to the work of others because of the error in extrapolation to infinite dilution made by earlier workers (8, 14). As pointed out elsewhere (8), the errors made by earlier workers are caused by neglecting to use the limiting law as an aid in the extrapolation and by

Table II. Infinite Dilution Partial Molal Volumes of Aqueous NaF , Na_2SO_4 , KCl , K_2SO_4 , MgCl_2 , and MgSO_4 Solutions at 0°, 25°, and 50°C

Salt	\bar{V}_2° , ml/mol		
	0°C	25°C	50°C
NaF	-6.51, ^a -5.72 ^b	2.37 ^b	-1.77, ^a -1.7 ^b
Na_2SO_4	2.33, ^a 3.7 ^c	11.56 ^b	14.09, ^a 15.5 ^d
KCl	23.62 ^b	26.85 ^b	27.57, ^a 27.66, ^e 27.64, ^f 27.9 ^d 27.87, ^g 27.12 ^h
K_2SO_4	23.79, ^a 22.7 ⁱ	32.02 ^b	33.63, ^a 35.1 ^d
MgCl_2	10.42, ^a 12.7, ^c 11.4 ^f	14.49 ^b	13.40, ^a 14.70, ^f 15.1 ^d
MgSO_4	-13.06, ^a -10.0 ^c	-7.19 ^b	-8.14, ^a -4.87 ^b

^a This study. ^b Millero's compilation (14). ^c Zen (19). ^d Ellis (3-5). ^e Scott (18). ^f Root (17). ^g Akerlof and Bender (1). ^h Redlich and Rosenfeld (16). ⁱ Jones and Calvin (6).

Table III. Partial Molal Expansibilities at Infinite Dilution for NaF , Na_2SO_4 , KCl , K_2SO_4 , and MgSO_4 at 12.5° and 37.5°C

Salt	$\Phi_E^\circ = \bar{E}^\circ$, ml/mol ⁻¹ deg ⁻¹	
	12.5°C	37.5°C
NaF	0.1656	0.0240
NaCl ^a	0.1488	0.0484
Na_2SO_4	0.3716	0.0988
KCl	0.1288	0.0288
K_2SO_4	0.3280	0.0656
MgCl_2	0.1628	-0.0436
MgSO_4	0.2352	-0.0384

^a Millero (10).

using unreliable Φ_V 's at low concentrations (i.e., unreliable densities). Note that an improper extrapolation to infinite dilution can give Φ_V° 's that are in error by as much as 3 ml/mol (8) for a 1-1 electrolyte.

By linearly extrapolating Dunn's (2) work at 45° and 55°C, one obtains Φ_V° (KCl) = 27.57 ml/mol, which is in excellent agreement with our extrapolated values.

The internal consistency of our values for Φ_V° can be tested by using the additivity principle. The differences between Φ_V° (1/2 K_2SO_4) and Φ_V° (1/2 Na_2SO_4) are 10.73 and 9.77 ml/mol, respectively, at 0° and 50°C compared to 10.68 and 9.87 obtained from the Φ_V° 's of KCl and NaCl (2, 8, 10). The Φ_V° of MgSO_4 can be calculated by the additivity principle using the Φ_V° 's of MgCl_2 , Na_2SO_4 , K_2SO_4 , NaCl, and KCl. The additivity method gives Φ_V° (MgSO_4) = -13.05 and -13.03 ml/mol at 0° and -8.17 and -8.11 ml/mol at 50°C, respectively, from the Na^+ and K^+ salts.

The infinite dilution partial molal expansibilities, $\Phi_E^\circ = \bar{E}_2^\circ = \partial\Phi_V^\circ/\partial T$ at 12.5° and 37.5°C for these electrolytes, are given in Table III, along with the results for NaCl (10). The \bar{E}_2° 's for all of the electrolytes decrease with increasing temperature (i.e., $\partial\bar{E}_2^\circ/\partial T$ is negative). As discussed elsewhere (8, 14), the decrease in \bar{E}_2° for electrolytes or the maximum in the \bar{V}_2° can be attributed to the decrease in volume owing to the increase in electrostriction with increasing temperature.

The deviations from the limiting law (b_V) of the Φ_V 's at 0°C for all of the electrolytes, with the exception of MgCl_2 , are positive. At 50°C, the positive deviations become smaller (MgSO_4 and K_2SO_4) or close to zero (NaF and Na_2SO_4). The deviations of Φ_V 's for the MgCl_2 solu-

tions are near zero at 0° and negative at 50°C. The effect of temperature on the b_V 's for all the electrolytes is similar in that $\partial b_V/\partial T$ is negative. The large positive deviations for most of the electrolytes at 0° and K_2SO_4 and $MgSO_4$ at 50°C may be due to cation-anion ion pair formation (10). The large negative deviations for $MgCl_2$ solutions at 50°C are what one might expect from the extended Debye-Hückel equation or if cation-cation and anion-anion interactions are more important than cation-anion interactions (10).

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Diffusion Coefficients of O_2 , N_2 , and CO_2 in Fluorinated Ethers

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Diffusion coefficients of O_2 , N_2 , and CO_2 in three fluorinated ethers are measured at 25° and 37°C. These coefficients are, in general, about twice as large as those in water.

Large gas solubilities in certain fluorinated ethers have stimulated considerable interest in their use as potential oxygen carriers in liquid breathing (5), in cardiopulmonary bypass machines (3), and as blood substitutes (8). To compute the mass-transfer rate during such processes, the diffusion coefficients of O_2 , N_2 , and CO_2 are needed. We have undertaken to measure these values for gases in fluorinated ethers at 25° and 37°C. The compounds studied were Caroxin-D (perfluoro-1,4 diisopropoxy butane) (Allied Chemical Corp., Morristown, N.J.), Caroxin-F (perfluoro-1-isopropoxy hexane) (Allied Chemical Corp., Morristown, N.J.), and FC-80 (perfluorobutyl perfluorotetrahydrofuran) (3M Co., St. Paul, Minn.).

Experimental

Materials. Minimum purities of O_2 , N_2 , and CO_2 were 99.6%. Caroxin-D and Caroxin-F were of greater than 99.9% purity as supplied, whereas FC-80 contains several isomers (2).

Procedure. Diffusion coefficients were measured with a modified Stokes' diaphragm cell (9). The procedure was described in detail by Tham and Gubbins (11), and we shall present only essential information here. The diaphragms were of porosity D (ASTM 10-20 μm), and stirring was accomplished with magnetic stirrers, rotating at 60 rpm. The diaphragm cells were immersed in a constant temperature bath controlled to within $\pm 0.02^\circ$ of the desired temperature with a proportional controller.

The cells were calibrated with 0.1N HCl, each cell being calibrated twice at the beginning of the work; cell constants were reproducible within $\pm 0.5\%$. [The diffusion coefficients are known accurately for the HCl-H₂O system (10).]

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The solvent-filled diaphragm method was used for both the calibration and diffusion coefficient measurement runs. Diffusion coefficients were calculated from the equation (1, 4)

$$D_{12} = \frac{1}{\beta t} \ln \left[\frac{C_B^\circ}{C_B - C_T} \right] \left[1 - \frac{\lambda}{6} \right] \quad (1)$$

where D_{12} is the differential diffusion coefficient of 1 in 2.

$$C_B^\circ = C_B \left[\frac{V_B + 1/2 V_D}{V_D} \right] + C_T \left[\frac{V_T + 1/2 V_D}{V_B} \right] \quad (2)$$

$$\lambda = \frac{V_D}{V_B + V_T} \quad (3)$$

β is the cell constant derived from calibration with HCl, and t is the time of diffusion; C is the concentration of diffusing substance, and V is the volume. Subscripts B , T , and D refer to bottom and top compartment and diaphragm, respectively.

The cell was first evacuated and then filled with the degassed fluorocarbon. It was equilibrated in a constant temperature bath for 2 hr with constant stirring; then, the bottom chamber was emptied and filled with solution containing the diffusing material. The method of preparing the gas solution and the precautions necessary in filling the cell have been described elsewhere (7, 12).

Solutions containing the dissolved gas were analyzed with a Perkin-Elmer Model 900 gas chromatograph equipped with a thermal conductivity detector. The column was a $1/8$ -in. \times 12-ft Porapak Q column, which was kept at room temperature. The helium carrier gas flow rate was 40 ml/min; injector port and detector temperatures were kept at 100° and 200°C, respectively. Calibration of the chromatograph was done by injecting a known volume of pure gas into the chromatograph and measuring the peak area. Linear response was observed in the range of concentrations of interest. The chromatograph analyses were reproducible to $\pm 0.6\%$.