# Enthalpies of Reaction of Phosphoric Acid Solutions and Urea at $25^{\circ}$ C and Some Physical Properties of Solutions in System $CO(NH_2)_2-H_3PO_4-H_2O$

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Measurements at 25 °C were made of the compositions of saturated solutions in the system  $CO(NH_2)_2-H_3PO_4-H_2O$ ; the enthalpies of solution of urea orthophosphate in water, in 20.37 % urea, and in 19.99 %  $H_3PO_4$ ; the enthalpies of solution of urea in 49.91 %, 60.12 %, and 75.03 %  $H_3PO_4$ ; the enthalpy of formation of urea orthophosphate; and the densities and heat capacities in the system  $CO(NH_2)_2-H_3PO_4-H_2O$ . The enthalpy of forming crystalline urea orthophosphate from urea and phosphoric acid solutions was calculated from the measurements and published data.

Crystallization of the urea adduct,  $CO(NH_2)_2$ ·H<sub>3</sub>PO<sub>4</sub>, from wet-process phosphoric acid is a promising method for separating the acid from its impurities. Because thermal and physicochemical data are useful in the development of a process for this purpose, measurements at 25°C were made of the compositions of saturated solutions in the system  $CO(NH_2)_2$ -H<sub>3</sub>PO<sub>4</sub>-H<sub>2</sub>O; the enthalpies of solution of urea orthophosphate in water, in 20.37% urea, and in 19.99% H<sub>3</sub>PO<sub>4</sub>; the enthalpies of solution of urea in 49.91%, 60.12%, and 75.03% H<sub>3</sub>PO<sub>4</sub>; the enthalpy of formation of urea orthophosphate; and the densities and heat capacities in the system  $CO(NH_2)_2$ -H<sub>3</sub>PO<sub>4</sub>-H<sub>2</sub>O.

#### Materials

**Urea.** Reagent grade urea was dissolved in water at 70°C. The solution was filtered through fritted glass and cooled slowly to room temperature. The resultant crystals were separated by suction on fritted glass, dried at 57°C for 16 hr, cooled, and ground lightly to pass a 20-mesh screen. The product, when dried to constant weight at 57°C, contained 46.6% N (theoretical, 46.65% N).

**Urea orthophosphate.** Five kg of reagent urea was dissolved in 10 liters of 60% H<sub>3</sub>PO<sub>4</sub> at  $60^{\circ}$ C. The solution was filtered and cooled slowly to room temperature. The coarse crystals were centrifuged, rinsed with cold water, and centrifuged again. The product was air dried on filter paper and then dried under vacuum desiccation over Dehydrite. It then was ground lightly to pass a 20-mesh screen and dried to constant weight under vacuum over Dehydrite. It contained 17.6% N and 44.91% P<sub>2</sub>O<sub>5</sub> (theoretical, 17.72% N and 44.91% P<sub>2</sub>O<sub>5</sub>).

**Phosphoric acid.** The phosphoric acid solutions were prepared by diluting recrystallized reagent phosphoric acid with distilled water.

## Compositions of Saturated Solutions in System $CO(NH_2)_2$ -H<sub>3</sub>PO<sub>4</sub>-H<sub>2</sub>O at 25°C

A determination of the integral enthalpy of solution at saturation requires a knowledge of the composition of the saturated solutions. Twelve saturated solutions were prepared by adding urea orthophosphate to various solutions of urea and

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phosphoric acid at 50°C until no more would dissolve readily. The solutions were cooled slowly to 25°C and held in stoppered flasks for three days, during which time large crystals formed in the bottom of the flasks. The crystals were identified petrographically as urea orthophosphate in each flask. The supernatant liquids were analyzed chemically for P<sub>2</sub>O<sub>5</sub> and N, and the equivalent amounts of H<sub>3</sub>PO<sub>4</sub> and CO(NH<sub>2</sub>)<sub>2</sub>, as calculated from the results, are shown in Table I and Figure 1.

#### **Calorimeter and Procedure**

The solution calorimeter used to determine integral enthalpies of solution was similar to that used by Southard (5). A 900-ml Dewar flask was supported in a constant-temperature water bath by cork rings clamped between stainless-steel plates. A flanged stainless-steel collar that fitted closely around the neck of the Dewar flask was silver soldered to the

Table I. Solutions Saturated with Urea Orthophosphate at 25°C

	Comp	oosition, %
Soin no.	H <sub>3</sub> PO <sub>4</sub>	CO(NH <sub>2</sub> ) <sub>2</sub>
5	28.02	38.65
6	29.37	31.71
3	30.24	28.76
1	32.19	19.73
2	36.33	14.69
4	45.54	9.56
7	46.67	9.90
8	53.49	8.02
9	62.11	6.90
10	69.04	7.18
11	72.20	8.77
12	71.38	15.97



Figure 1. System CO(NH<sub>2</sub>)<sub>2</sub>-H<sub>3</sub>PO<sub>4</sub>-H<sub>2</sub>O at 25°C

top plate. The space between the collar and the neck of the flask was filled with Apiezon W wax. A stainless-steel plate, provided with three small stuffing boxes for the thermometer and heater supports and with a stainless-steel ball bearing guide, 4 in. long, for the stirrer, was clamped to the flanged collar with six spring clamps. A neoprene gasket sealed the cover plate to the collar.

A 4-lead helical constantan heater was mounted in a 5-mm glass tube that had been shaped into a helix. The head of a platinum resistance thermometer was sealed with Apiezon W

Table II. Observed	Properties o	f Solution of	of Urea	Orthophosphate in	Water at 2	25°C
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Wt %         Density, d. g/ml         Specific heat, s. cal/*C/g         Enthapy of solution           H,PO,         CO(NH), 0         orthophosphate, m         g/ml         Specific heat, s. g/ml         Enthapy of solution           1.30         0.79         0.135         1.0065         0.9853         879.25         7675           2.65         1.63         0.2283         1.0166         0.9662         951.43         7683           3.86         2.37         0.420         1.0256         0.9353         879.25         7675           7.31         4.48         0.8046         1.0509         0.9192         861.55         7577           8.42         5.13         1.004         1.0553         0.8460         941.25         7877           1.645         6.33         1.141         1.0653         0.8460         941.25         7877           1.645         8.36         1.765         1.1011         0.8438         853.57         7839           1.845         8.36         1.765         1.1011         0.8438         854.51         7495           1.845         8.36         1.775         1.1011         0.8438         856.51         7475           1.845         0.8005		Solution conce	ntration				· · · · · · · · · · · · · · · · · · ·	
H_PO_         CO(NH_1)         orthophophate, m         g/mt         cal/ $C/g$ Q, cal/run $\Delta H$ , cal/mol           1.30         0.79         0.135         1.0065         0.9853         879.25         7675           2.65         1.63         0.283         1.0168         0.9642         951.43         7683           3.86         2.37         0.420         1.0256         0.9559         879.29         7696           4.97         3.05         0.552         1.037         0.9435         824.26         7689           6.20         3.80         0.704         1.0424         0.9302         934.39         7675           7.31         4.448         0.846         1.0509         0.9192         861.55         7657           8.46         5.18         1.000         1.0599         0.9059         904.30         7631           9.52         5.83         1.313         1.0777         0.8480         940.28         7587           11.70         7.17         1.627         1.0931         0.8626         83.377         7539           14.55         8.26         1.785         1.101         0.8438         628.25         7459           12.45 <th></th> <th>Wt %</th> <th>Molality urea</th> <th>Density d</th> <th>Specific heat s</th> <th colspan="3">Enthalpy of solution</th>		Wt %	Molality urea	Density d	Specific heat s	Enthalpy of solution		
Solution Series A           0         0         0         0.9983              2.55         1.63         0.2483         1.0168         0.9682         951.43         7633           2.65         1.63         0.2483         1.0168         0.9682         951.29         7659           4.67         3.03         0.552         1.0337         0.8435         824.26         7689           4.67         3.03         0.552         1.0337         0.84852         951.59         7657           7.41         4.48         0.049         1.0599         0.4959         961.59         7657           8.46         5.18         1.000         1.0599         0.4952         961.59         7657           1.70         7.77         1.427         1.0631         0.4700         883.20         7627           1.843         9.46         2.966         1.1160         0.4438         884.39         7617           1.456         8.92         1.042         1.0487         0.4438         884.39         7617           1.456         8.92         1.931         0.4170         885.30         7677           1.456	H <sub>3</sub> PO <sub>4</sub>	CO(NH <sub>2</sub> ) <sub>2</sub>	orthophosphate, m	g/ml	cal/°C/g	Q, cal/run	$\Delta H$ , cal/mol	
$\begin{array}{c c c c c c c c c c c c c c c c c c c $				Solution Seri	ies A			
1.30 $0.79$ $0.135$ $1.0065$ $0.863$ $87925$ $7675$ 2.85 $1.63$ $0.237$ $0.9425$ $0.9569$ $879.29$ $7696$ 4.87 $3.06$ $0.552$ $1.037$ $0.9435$ $824.26$ $7689$ 6.20 $3.80$ $0.704$ $1.04244$ $0.9302$ $934.99$ $7675$ $7.31$ $4.44$ $0.9464$ $0.6509$ $0.9192$ $861.55$ $7657$ $3.46$ $5.18$ $1.000$ $1.0599$ $0.9059$ $904.30$ $7631$ $9.52$ $5.83$ $1.148$ $1.0683$ $0.8740$ $883.20$ $7552$ $12.68$ $7.77$ $1.627$ $1.0931$ $0.6428$ $854.397$ $7539$ $13.55$ $8.36$ $1.785$ $1.1011$ $0.6438$ $828.25$ $7495$ $15.33$ $9.001$ $2.263$ $1.1232$ $0.8266$ $856.51$ $7409$ $15.33$ $0.01$ $2.263$ $1.1232$ $0.8268$ $866.51$ $7409$ $18.54$ $1.662$	0	0	0	0.9958				
2.65         1.63         0.283         1.0168         0.9682         95.1.3         7683           3.86         2.37         0.420         1.0265         0.9559         879.29         7696           4.97         3.05         0.552         1.0337         0.9435         824.26         7695           7.31         4.48         0.846         1.0509         0.9192         861.55         7657           9.52         5.83         1.148         1.0683         0.8952         861.76         7610           10.65         6.53         1.313         1.0777         0.8850         940.28         7587           11.70         7.17         1.471         1.0853         0.8740         83.20         7552           13.65         8.36         1.785         1.1011         0.4438         828.25         7495           14.56         8.92         1.942         1.1087         0.4438         828.25         7495           15.43         9.46         2.096         1.1150         0.8438         828.23         7454           17.25         10.57         2.439         1.311         0.8170         824.84         7429           18.44         1.61	1.30	0.79	0.135	1.0065	0.9853	879.25	7675	
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	2.65	1.63	0.283	1.0168	0.9682	951.43	7683	
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	3.86	2.37	0.420	1.0256	0.9559	879.29	7696	
6.20       3.80       0.704       1.0424       0.3302       93.99 $7675$ 8.46       5.18       1.000       1.0599       0.9099       90.430       7631         9.52       5.83       1.144       1.0663       0.8962       861.76       7610         10.65       6.53       1.313       1.0777       0.8850       940.28       7587         11.70       7.17       1.471       1.0853       0.8740       883.20       7582         12.68       7.77       1.627       1.0931       0.626       853.87       7539         13.65       8.36       1.765       1.1011       0.4338       828.25       7495         16.33       9.46       2.096       1.1160       0.8351       829.257       7454         17.25       10.57       2.439       1.1232       0.8268       856.51       7409         18.44       11.61       2.762       1.1458       0.8005       822.43       7389         18.54       11.61       2.762       1.1458       0.8005       823.43       7389         21.33       13.07       3.129       1.151       0.7854       76.098       7332         21.33 <td>4.97</td> <td>3.05</td> <td>0.552</td> <td>1.0337</td> <td>0.9435</td> <td>824.26</td> <td>7689</td>	4.97	3.05	0.552	1.0337	0.9435	824.26	7689	
7.31       4.48       0.846       1.0509       0.9192       861.55       7651         9.52       5.83       1.148       1.0683       0.8662       861.76       7610         10.65       6.53       1.313       1.0777       0.8850       960.28       7562         12.68       7.77       1.627       1.0931       0.8626       853.57       7539         12.68       7.77       1.627       1.0931       0.8438       854.39       7517         14.56       8.92       1.342       1.1047       0.8438       854.39       7517         14.56       8.92       1.342       1.1047       0.8438       854.39       7517         15.33       9.46       2.096       1.1160       0.8351       852.57       7454         16.33       10.01       2.263       1.122       0.8260       852.57       7454         18.84       11.61       2.782       1.1456       0.8085       856.51       7409         18.12       11.10       2.612       1.1336       0.7923       856.30       7352         2.133       13.07       3.319       1.1652       0.7783       870.59       7333         2.14.02 </td <td>6.20</td> <td>3.80</td> <td>0.704</td> <td>1.0424</td> <td>0.9302</td> <td>934.99</td> <td>7675</td>	6.20	3.80	0.704	1.0424	0.9302	934.99	7675	
$\begin{array}{c c c c c c c c c c c c c c c c c c c $	7.31	4.48	0.846	1.0509	0.9192	861.55	7657	
$\begin{array}{c c c c c c c c c c c c c c c c c c c $	8.46	5.18	1.000	1.0599	0.9059	904.30	7631	
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	9.52	5.83	1.148	1.0683	0.8962	861.76	7610	
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	10.65	6.53	1.313	1.0777	0.8850	940.28	7587	
$\begin{array}{c c c c c c c c c c c c c c c c c c c $	11.70	7.17	1.471	1.0853	0.8740	883.20	7562	
	12.68	7.77	1.627	1.0931	0.8626	853.57	7539	
$\begin{array}{c c c c c c c c c c c c c c c c c c c $	13.65	8.36	1.785	1.1011	0.8438	854.39	7517	
$\begin{array}{c c c c c c c c c c c c c c c c c c c $	14.56	8.92	1.942	1.1087	0.8438	828.25	7495	
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	15.43	9.46	2.096	1.1160	0.8351	802.95	7475	
$\begin{array}{c c c c c c c c c c c c c c c c c c c $	16.33	10.01	2.263	1.1232	0.8260	852.57	7454	
$\begin{array}{c c c c c c c c c c c c c c c c c c c $	17.25	10.57	2.439	1.1311	0.8170	882.48	7429	
$\begin{array}{c c c c c c c c c c c c c c c c c c c $	18.12	11.10	2.612	1.1386	0.8085	856.51	7409	
$\begin{array}{c c c c c c c c c c c c c c c c c c c $	18.94	11.61	2.782	1.1458	0.8005	823.43	7389	
20.52       12.57       3.129       1.1591       0.784       760.98       7352         21.33       13.07       3.319       1.1662       0.7783       875.59       7333         22.10       13.54       3.503       1.1728       0.7700       840.45       7315         22.87       14.02       3.698       1.1798       0.7655       882.61       7278         23.64       14.49       3.899       1.1859       0.7565       882.61       7278         24.40       14.96       4.106       1.1927       0.7496       891.95       7260         25.74       15.77       4.490       1.2054       0.7313       858.62       7212         27.07       16.59       4.903       1.2177       0.7288       822.62       7196         27.71       16.98       5.113       1.2248       0.7200       833.97       7180         28.30       17.35       5.314       1.2312       0.7143       779.86       7163         28.87       17.69       5.512        0.7097       760.22       7149         9.72       0.44       0.074       1.0027       0.9927       478.44       7614         2.01<	19.80	12.13	2.967	1.1533	0.7923	885.30	7369	
$\begin{array}{c c c c c c c c c c c c c c c c c c c $	20.52	12.57	3.129	1.1591	0.7854	760.98	7352	
$\begin{array}{c c c c c c c c c c c c c c c c c c c $	21.33	13.07	3.319	1.1662	0.7783	875.59	7333	
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	22.10	13.54	3.503	1.1728	0.7700	840.45	7315	
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	22.87	14.02	3.698	1.1798	0.7638	870.76	7297	
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	23.64	14.49	3.899	1.1859	0.7565	882.61	7278	
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	24.40	14.96	4.106	1.1927	0.7496	891.95	7260	
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	25.13	15.40	4.313	1.1997	0.7434	875.09	7242	
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	25.74	15.77	4.490	1.2054	0.7382	739.75	7228	
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	26.42	16.19	4.699	1.2119	0.7313	858.62	7212	
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	27.07	16.59	4.903	1.2177	0.7258	822.62	7196	
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	27.71	16.98	5.113	1.2248	0.7200	833.97	7180	
28.87       17.69       5.512        0.7094       760.22       7149         Solution Series B         0       0       0.9971       0.9980           0.72       0.44       0.074       1.0027       0.9927       478.84       7614         2.01       1.23       0.212       1.0123       0.9780       900.98       7709         3.27       2.01       0.353       1.0216       0.9630       908.52       7725         4.65       2.85       0.513        0.9983       1013.03       7713         0.17       0.11       0.018        0.9965       226.05       7345a         0.35       0.22       0.036        0.9965       226.05       7345a         Dilution Series C         31.49       19.30       6.532       1.2622        7128         30.99       18.99       6.324       1.2570       0.6923       37.68       7105         30.47       18.67       6.115       1.2519       0.6965       37.94       7117         29.46       18.05       5.728       1.2419       0.6973	28.30	17.35	5.314	1.2312	0.7143	779.86	7163	
Solution Series B           0         0         0.9971         0.9980             0.72         0.44         0.074         1.0027         0.9927         478.84         7614           2.01         1.23         0.212         1.0123         0.9780         900.98         7709           3.27         2.01         0.353         1.0216         0.9630         908.52         7725           4.65         2.85         0.513          0.9473         1013.03         7713           0.17         0.11         0.018          0.9965         226.05         7345a           0.35         0.22         0.036          0.9965         226.05         7345a           Dilution Series C           31.49         19.30         6.532         1.2622          7094           30.99         18.99         6.324         1.2579         0.6965         37.94         7117           29.95         18.36         5.913         1.2468         0.7011         37.09         7151           29.46         18.05         5.728         1.2419         0.6973         35.40         7	28.87	17.69	5.512		0.7094	760.22	7149	
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$				Solution Seri	es B			
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	0	0	0	0.9971	0.9980			
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	0.72	0.44	0.074	1.0027	0.9927	478.84	7614	
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	2.01	1.23	0.212	1.0123	0.9780	900.98	7709	
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	3.27	2.01	0.353	1.0216	0.9630	908.52	7725	
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	4.65	2.85	0.513		0.9473	1013.03	7713	
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	0.17	0.11	0.018		0.9983	105.74	6983 <i>a</i>	
Dilution Series C31.4919.306.5321.2622709430.9918.996.3241.25700.692337.68710530.4718.676.1151.25190.696537.94711729.9518.365.9131.24680.701137.94712829.4618.055.7281.24190.697335.40713928.9417.735.5371.23660.709437.09715128.4517.435.3641.23130.714834.04716227.9717.145.1991.22690.719833.06717327.4816.845.0351.22230.724333.17718427.0116.554.8841.21820.728231.047194b26.5516.274.7391.20930.727531.17721626.0615.974.5891.20930.727531.17721625.5815.674.4430.741030.817227	0.35	0.22	0.036		0.9965	226.05	7345 <sup>a</sup>	
$31.49$ $19.30$ $6.532$ $1.2622$ $\dots$ $7094$ $30.99$ $18.99$ $6.324$ $1.2570$ $0.6923$ $37.68$ $7105$ $30.47$ $18.67$ $6.115$ $1.2519$ $0.6965$ $37.94$ $7117$ $29.95$ $18.36$ $5.913$ $1.2468$ $0.7011$ $37.94$ $7128$ $29.46$ $18.05$ $5.728$ $1.2419$ $0.6973$ $35.40$ $7139$ $28.94$ $17.73$ $5.537$ $1.2366$ $0.7094$ $37.09$ $7151$ $28.45$ $17.43$ $5.364$ $1.2313$ $0.7148$ $34.04$ $7162$ $27.97$ $17.14$ $5.199$ $1.2269$ $0.7198$ $33.06$ $7173$ $27.48$ $16.84$ $5.035$ $1.2223$ $0.7243$ $33.17$ $7184$ $27.01$ $16.55$ $4.884$ $1.2182$ $0.7282$ $31.04$ $7194b$ $26.55$ $16.27$ $4.739$ $1.2093$ $0.7275$ $31.17$ $7216$ $25.58$ $15.67$ $4.443$ $\dots$ $0.7410$ $30.81$ $7227$				Dilution Seri	es C			
$30.99$ $18.99$ $6.324$ $1.2570$ $0.6923$ $37.68$ $7105$ $30.47$ $18.67$ $6.115$ $1.2519$ $0.6965$ $37.94$ $7117$ $29.95$ $18.36$ $5.913$ $1.2468$ $0.7011$ $37.94$ $7128$ $29.46$ $18.05$ $5.728$ $1.2419$ $0.6973$ $35.40$ $7139$ $28.94$ $17.73$ $5.537$ $1.2366$ $0.7094$ $37.09$ $7151$ $28.45$ $17.43$ $5.364$ $1.2313$ $0.7148$ $34.04$ $7162$ $27.97$ $17.14$ $5.199$ $1.2269$ $0.7198$ $33.06$ $7173$ $27.48$ $16.84$ $5.035$ $1.2223$ $0.7243$ $33.17$ $7184$ $27.01$ $16.55$ $4.884$ $1.2182$ $0.7282$ $31.04$ $7194^{b}$ $26.55$ $16.27$ $4.739$ $1.2093$ $0.7275$ $31.17$ $7216$ $25.58$ $15.67$ $4.443$ $1.093$ $0.72410$ $30.81$ $7227$	31.49	19.30	6.532	1.2622		• • •	7094	
$30.47$ $18.67$ $6.115$ $1.2519$ $0.6965$ $37.94$ $7117$ $29.95$ $18.36$ $5.913$ $1.2468$ $0.7011$ $37.94$ $7128$ $29.46$ $18.05$ $5.728$ $1.2419$ $0.6973$ $35.40$ $7139$ $28.94$ $17.73$ $5.537$ $1.2366$ $0.7094$ $37.09$ $7151$ $28.45$ $17.43$ $5.364$ $1.2313$ $0.7148$ $34.04$ $7162$ $27.97$ $17.14$ $5.199$ $1.2269$ $0.7198$ $33.06$ $7173$ $27.48$ $16.84$ $5.035$ $1.2223$ $0.7243$ $33.17$ $7184$ $27.01$ $16.55$ $4.884$ $1.2182$ $0.7282$ $31.04$ $7194^{b}$ $26.55$ $16.27$ $4.739$ $1.2093$ $0.7275$ $31.17$ $7216$ $25.58$ $15.67$ $4.443$ $1.042$ $0.7410$ $30.81$ $7227$	30.99	18.99	6.324	1.2570	0.6923	37.68	7105	
29.95 $18.36$ $5.913$ $1.2468$ $0.7011$ $37.94$ $7128$ $29.46$ $18.05$ $5.728$ $1.2419$ $0.6973$ $35.40$ $7139$ $28.94$ $17.73$ $5.537$ $1.2366$ $0.7094$ $37.09$ $7151$ $28.45$ $17.43$ $5.364$ $1.2313$ $0.7148$ $34.04$ $7162$ $27.97$ $17.14$ $5.199$ $1.2269$ $0.7198$ $33.06$ $7173$ $27.48$ $16.84$ $5.035$ $1.2223$ $0.7243$ $33.17$ $7184$ $27.01$ $16.55$ $4.884$ $1.2182$ $0.7282$ $31.04$ $7194b$ $26.55$ $16.27$ $4.739$ $1.2093$ $0.7275$ $31.17$ $7216$ $25.58$ $15.67$ $4.443$ $1.042$ $0.7410$ $30.81$ $7227$	30.47	18.67	6.115	1.2519	0.6965	37.94	7117	
29.4618.055.7281.24190.697335.40713928.9417.735.5371.23660.709437.09715128.4517.435.3641.23130.714834.04716227.9717.145.1991.22690.719833.06717327.4816.845.0351.22230.724333.17718427.0116.554.8841.21820.728231.047194b26.5516.274.7391.21390.731729.65720526.0615.974.5891.20930.727531.17721625.5815.674.4430.741030.817227	29.95	18.36	5.913	1.2468	0.7011	37.94	7128	
20.94 $17.73$ $5.537$ $1.2366$ $0.7094$ $37.09$ $7151$ $28.45$ $17.43$ $5.364$ $1.2313$ $0.7148$ $34.04$ $7162$ $27.97$ $17.14$ $5.199$ $1.2269$ $0.7198$ $33.06$ $7173$ $27.48$ $16.84$ $5.035$ $1.2223$ $0.7243$ $33.17$ $7184$ $27.01$ $16.55$ $4.884$ $1.2182$ $0.7282$ $31.04$ $7194b$ $26.55$ $16.27$ $4.739$ $1.2093$ $0.7275$ $31.17$ $7216$ $25.58$ $15.67$ $4.443$ $1.142$ $0.72410$ $30.81$ $7227$	29.46	18.05	5./28	1.2419	0.6973	35.40	7139	
20.4517.435.3641.23130.714834.04716227.9717.145.1991.22690.719833.06717327.4816.845.0351.22230.724333.17718427.0116.554.8841.21820.728231.047194b26.5516.274.7391.21390.731729.65720526.0615.974.5891.20930.727531.17721625.5815.674.4431.140.741030.817227	20.94	17.73	5.53/	1.2366	0.7094	37.09	7151	
27.5717.145.1991.22690.719833.06717327.4816.845.0351.22230.724333.17718427.0116.554.8841.21820.728231.047194b26.5516.274.7391.21390.731729.65720526.0615.974.5891.20930.727531.17721625.5815.674.4431111117227	20.45 27.07	17.43	5.364	1.2313	0.7148	34.04	7162	
27.01       16.55       4.884       1.2182       0.7282       31.04       7194b         26.55       16.27       4.739       1.2139       0.7317       29.65       7205         26.06       15.97       4.589       1.2093       0.7275       31.17       7216         25.58       15.67       4.443       1.11       0.7410       30.81       7227	27.21	1/.14	5.133	1,2209	0.7198	33.06	/1/3	
26.55       16.27       4.739       1.2192       0.7282       31.04       71947         26.06       15.97       4.589       1.2093       0.7217       29.65       7205         25.58       15.67       4.443       1.110       30.81       7227	27.40	10.04	5.055 A 80A	1.2223	0.7243	33.1/	/184	
26.06       15.97       4.589       1.2093       0.7275       31.17       7216         25.58       15.67       4.443       0.7410       30.81       7227	26 55	16.00	4.004 1 720	1 2120	0.7202	31.04	71940	
25.58 15.67 4.443 0.7410 30.81 7227	26.06	15.27	4.735	1 2093	0.7317	23.05 31 17	7205	
	25.58	15.67	4 443	1.2000	0 7410	30.81	7210	

<sup>a</sup> Initial solution was water. <sup>b</sup> Calculated from Series A.

wax to a flared 5-mm glass support tube. The heater and the thermometer were suspended from the calorimeter cover by anchoring three sections of  $\frac{1}{4}$ -in. Inconel tubing in the stuffing boxes and sealing the glass tubes to the Inconel tubes with Apiezon W wax. The heater and thermometer leads passed through these tubes. An inert plastic draft tube was fastened inside the glass helix with platinum wire, and the thermometer was located just inside the draft tube. A glass stirrer was sealed to a  $\frac{1}{4}$ -in. stainless-steel tube just below the calorimeter cover with Apiezon W wax so that the impeller blades were only a few millimeters below the tip of the thermometer capsule.

The initial bulk charge of liquid for each experimental run was adjusted to 851 ml at 25°C and weighed. Each incremental addition to the bulk liquid was contained in a thinwalled glass bulb that was suspended from a glass rod inside the hollow stirrer shaft. The bulb was crushed against the bottom of the Dewar flask to start the solution period.

The calorimeter system was calibrated electrically immediately before and after each measurement. The platinum resistance thermometer was calibrated by the National Bureau of Standards. The Wenner potentiometer, Ayrton shunt, and standard resistors used in the energy measurements were calibrated against standard resistors and a potentiometer calibrated by the Redstone Arsenal, Huntsville, Ala., and traceable to the National Bureau of Standards. The defined calorie was taken as 4.1840 absolute joules.

Conventional "normal" and "reverse" readings of the resistance of the platinum resistance thermometer on a Leeds and Northrup G-2 Mueller bridge were made during rating periods to establish heat-leak corrections. Only normal readings were taken during the solution period, and to these were applied both the usual bridge corrections and an adjustment to compensate for the absence of reverse measurements. The observed temperature rise was the difference between the temperatures at the end and at the beginning of the solution period as calculated from linear equations for the rating periods. The correction to the observed temperature for heat leak was calculated by integration by the trapezoidal rule of the heat leak as a function of time from measurements taken at half-minute intervals. The calculation was simplified by the linear relationship of heat leak to temperature over the temperature range of the measurements.

The average temperature during the solution period for each measurement was  $25.00^{\circ} \pm 0.04^{\circ}$ C, and no tempera-

Table III. Integral Enthalpies of Solution of Urea Orthophosphate in Water at 25°C

	Concentration	1	
Wt %		Urea ortho- phosphate	$\Delta H$ , cal/mol urea ortho-
H₃PO₄	$CO(NH_2)_2$	molality, m	phosphate
0.20	0.12	0.02	7050
0.49	0.30	0.05	7510
0.96	0.59	0.1	7660
1.90	1.16	0.2	7730
4.54	2.78	0.5	7690
8.46	5.19	1.0	7620
11.88	7.28	1.5	7550
14.89	9.13	2.0	7490
17.56	10.76	2.5	7430
19.94	12.22	3.0	73 <b>7</b> 0
24.02	14.72	4.0	7270
27.37	16.77	5.0	7190
30.18	18.49	6.0	7120
32.19	19.73	6.83ª	7080

<sup>a</sup> Saturated solution.

ture corrections were necessary. As the water bath around the calorimeter was held at  $28.00^{\circ} \pm 0.02^{\circ}$ C, heat leaks were always in the same direction. Raoult's law was applied to correct for the heat of vaporization of water into the vapor space above the calorimeter liquid for each measurement. A correction for the energy of bulb breaking (1.1 ± 0.1 cal) was based on the results of 10 measurements in which bulbs filled with water were broken in the Dewar flask containing water.

#### Measurements

For enthalpy of solution measurements, the solute was added to the solvent in successive increments; for enthalpy of dilution measurements, the solvent was added to a nearly saturated solution in successive increments.

The observed integral enthalpy of solution of the solute at each final molality was determined by solving the equation

$$\Delta H = \Sigma Q/M \tag{1}$$

where  $\Delta H$  refers to the observed integral enthalpy of solution in cal/mol; Q, the enthalpy change in calories for each measurement of the series to that molality; M, the moles of solute at that molality; and  $\Sigma$  indicates the summation process. Manipulative details in adjusting the final solution from one experimental run to a weighed fixed volume for the following experimental run entailed a loss of 1–2% of the solution; therefore, linear corrections were made in the accumulated weights of solute and solvent and in the accumulated enthalpy changes for each measurement.

The enthalpy of dilution is equal to the difference between the integral enthalpy of solution in the initial  $(\Delta H_i)$  and final  $(\Delta H_F)$  solutions, thus

$$\Delta H_{\rm I} = \Delta H_{\rm F} - Q/M \tag{2}$$

For one solution of the enthalpy of dilution series,  $\Delta H_{\rm E}$  was calculated from an equation for the integral enthalpy of solution as a function of molality for the corresponding enthalpy of solution series. Solving Equation 2 for each dilution gave the observed integral enthalpy of solution for each measurement of the dilution series. These values of the observed integral enthalpies of solution were combined with those from the corresponding enthalpy of solution series, and equations expressing integral enthalpy of solution as a function of molality were fitted to the observed values by the method of least squares. The equations were extrapolated to the molality of the saturated solutions to determine the integral enthalpies of solution at saturation. The concentration of each saturated solution was calculated by solving simultaneously the firstdegree equation of percent solute as a function of percent solvent from pure solvent to pure solute and a similar firstdegree equation between two adjacent points on the saturation isotherm that intersects the first equation.

The total weight of solution in the calorimeter, the temperature rise, and the electrical energy input during the second electrical calibration for each measurement made possible a calculation of the heat capacity, *s*, of each solution at the average temperature of the calibration ( $25.3^{\circ} \pm 0.3^{\circ}$ C). The average water equivalent of the calorimeter was 67.4 ± 0.2 grams, based on 19 determinations.

The initial bulk charge of the liquid for each enthalpy of solution measurement was weighed at room temperature  $(25.0^{\circ} \pm 0.5^{\circ}\text{C})$  in a modified volumetric flask that held  $851.3 \pm 0.2$  ml. From these weights the densities, *d*, of the solutions were determined.

#### **Enthalpies of Solution**

Urea orthophosphate in water. The enthalpies of solution over the concentration range 0-6.53m urea orthophosphate were measured in three series. In Series A, crystalline urea orthophosphate was added to distilled water in successive in-

crements to a final concentration of 5.51m urea orthophosphate. Series B was similar to Series A to a final concentration of 0.51m urea orthophosphate to more clearly define the peak in the integral enthalpy of solution at about 0.4m. Two additional enthalpy of solution measurements were made in which the urea orthophosphate was added to water to more clearly define the slope of the integral enthalpies of solution in the dilute range.

The initial solution of Series C contained 22.74% P2O5 and 9.03% N or 6.53m urea orthophosphate. Successive increments of distilled water were added to this solution to a final concentration of 4.44m urea orthophosphate.

The observed properties of solutions of urea orthophosphate in water are shown in Table II. Equations derived from the observed values are

and

$$\Delta H = 7809 - 15.2m^{-1}, m = 0.02 \text{ to } 0.21$$
 (3)

(0)

$$\Delta H = 7770 - 158m + 8.3m^2, m = 0.21 \text{ to } 6.53 \quad (4)$$

where  $\Delta H$  = integral enthalpy of solution (cal mol<sup>-1</sup>), and m = molality of urea orthophosphate. The observed values fit Equation 3 with a standard deviation of 38 cal mol<sup>-1</sup> and

Table IV. Observed Properties of Solution of Urea Orthophosphate in 20.37% Urea at 25°C

Solution concentration						
Wt %		Molality urea	Density d	Specific heat	Enthalpy	of solution
H₃PO₄	CO(NH <sub>2</sub> ) <sub>2</sub>	orthophosphate, m	g/ml	cal/°C/g	Q, cal/run	$\Delta H$ , cal/mol
			Solution Serie	es D		
0	20.37	0	1 0517			
1 15	20.70	0 1 1 9	1 0598	0.8726	608.40	5692
2 30	21.02	0.243	1.0676	0.8628	689.82	5092
2.50	21.02	0.243	1.0070	0.0020	779.60	5395
1 01	21.30	0.505	1.0701	0.8333	779.00	6136
4.01 5.04	21.74	0.535	1.0000	0.8430	029.01 755.00	6212
7 1 1	22.00	0.870	1 1012	0.8344	755.02	6209
7.11 9.10	22.39	0.019	1,1013	0.8256	807.93	6293
0.15	22.70	0.965	1,1095	0.8194	/6/.18	6312
9.51	23.02	1.11/	1,1104	0.8104	810.72	6326
10.27	23.29	1.257	1,1241	0.8028	722.62	6336
11.20	23.30	1.407	1,1315	0.7955	769.41	6345
12.20	23.84	1.551	1.1389	0.7884	726.70	6351
13.14	24.11	1.702	1.1461	0.7809	752.12	6355
14.00	24.35	1.845	1.1524	0.7742	702.72	6358
14.93	24.62	2.007	1.1595	0.7669	790.04	6361
15.78	24.86	2.160	1.1654	0.7604	/31.15	6362
16.70	25.12	2.332	1.1736	0.7533	809.49	6363
17.61	25.38	2.509	1.1807	0.7468	826.07	6364
			Dilution Serie	es E		
29.52	28.56	5.750	1.2800			6390
28.97	28.41	5.549	1.2750	0.6658	-2.04	6390
28.45	28.26	5.366	1.2701	0.6751	-0.95	6389
27.98	28.13	5.204	1.2660	0.6709	-1.53	6389
27.48	27.99	5.037	1.2615	0.6744	-1.79	6388
27.00	27.86	4.880	1.2578	0.6786	-1.87	6388
26.49	27.72	4.719	1.2541	0.681 <b>8</b>	-2.03	6387
26.01	27.59	4,572	1.2503	0.6858	-1.96	6386
25.59	27.47	4.446	1.2468	0.6884	-1.55	6386
25.17	27.35	4.323	1.2432	0.6917	-1.51	6385
24.75	27.24	4.203	1.2395	0.6950	-1 74	6385
24.31	27.11	4.079	1.2358	0.6981	-2.67	6384
23.86	26.99	3.957	1.2321	0 7011	-2.53	6383
23.43	26.87	3.843	1.2280	0 7042	-2 77	6382
23.02	26.76	3,735	1 2255	0 7075	-2 74	6381
22.59	26.64	3 626	1 2213	0.7106	-2.19	6380
22.20	26.53	3 529	1 2184	0.7136	-2.40	6378
21 78	26.41	3 427	1 2149	0.7163	-2.55	6377
21.36	26.30	3 325	1 2117	0.7194	-2.00	6376
20.96	26.19	3 231	1 2080	0.7248	-2.75	6275
20.50	26.08	3 1 4 5	1,2055	0.7248	-2.00	6375
20.22	25.00	3.062	1 2024	0.7241	-2.27	6374
19.85	25.20	2 980	1 1002	0.7200	-2.01	6750
19 51	25.00	2.000	1 1061	0.7302	-3.03	6270
19 19	25.69	2.304	1 1022	0.7321	-2.97	6370
18.84	25.60	2,330	1 1911	0.7340	-2.59	6267
18.48	25.00	2.702	1 1883	0.7300	-2.00	030/ 6365
18 13	25.00	2.000	1 1856	0.7400	-3.21	6360
17.81	25.31	2.550	1,1000	0.7455	-2.63	6362 <i>a</i>

<sup>a</sup> Calculated from Series D.

Table V.	Integral	Enthalpies	of Solut	ion of	Urea
	Orthoph	nosphate in	20.37%	Urea at	t 25°C

Wt %		Urea ortho- phosphate	$\Delta H$ , cal/mol urea ortho-
H₃PO₄	$CO(NH_2)_2$	molality, <i>m</i>	phosphate
0.96	20.64	0.1	5630
1.90	20.91	0.2	5910
4.54	21.66	0.5	6200
8.46	22.78	1.0	6334
11.88	23.75	1.5	6345
14.89	24.60	2.0	6355
17.56	25.36	2.5	6364
19.94	26.04	3.0	6372
22.08	26.65	3.5	6378
24.02	27.20	4.0	6383
25.77	27.70	4.5	6387
27.37	28.15	5.0	6389
28.83	28.57	5.5	6389
30.18	28.95	6.0	6389
30.24	28.97	6.02 <sup>a</sup>	6388

<sup>a</sup> Saturated solution.

Equation 4 with a standard deviation of 10 cal  $mol^{-1}$ . Integral enthalpies of solution at even values of molality and at saturation as calculated from the equations are shown in Table III.

**Urea orthophosphate in 20.37% urea.** The initial solution of Series D was prepared by dissolving recrystallized urea in distilled water. Chemical analysis showed it to contain 9.50% N or 20.37% urea. Crystalline urea orthophosphate was added to this solution in successive increments to a final concentration of 2.51m urea orthophosphate. The initial solution of Series E was prepared by adding urea orthophosphate to 20.37% urea solution. Chemical analysis showed it to contain 13.32% N and 21.38% P<sub>2</sub>O<sub>5</sub> or 5.75m urea orthophosphate. Successive increments of 20.37% urea orthophosphate.

The observed properties of solutions of urea orthophosphate in 20.37% urea are shown in Table IV. Equations derived from the observed values are

 $\Delta H = 5179 + 5533m - 11578m^2 + 11206m^3 - 4006m^4, m < 1$  (5)

$$\Delta H = 6306 + 30.4m - 2.77m^2, m > 1$$
 (6)

Table VI	Observed	Properties o	f Solutions	of Urea	Orthophosphate	in	19.99% H.PO.	at 25°C
Iddie VI.	Observed	i Fronei lies u	ເວບເບເບເທ					

Solution concentration							
Wt %		Molality urea	Density d	Specific heat s	Enthalpy of solution		
H₃PO₄	CO(NH <sub>2</sub> ) <sub>2</sub>	orthophosphate, m	g/ml	g/ml cal/°C/g	Q, cal/run	$\Delta H$ , cal/mol	
			Solution Seri	es F			
19.99	0	0	1.1122				
20.80	0.73	0.125	1.1193	0.8402	905.75	7682	
21.65	1.50	0.260	1.1277	0.8303	964.97	7658	
22.53	2,30	0.407	1.1363	0.8210	1032.66	7639	
23.33	3.02	0.546	1.1431	0.8115	955.05	7615	
24.05	3.67	0.676	1.1514	0.8032	875.79	7594	
24.82	4.37	0.821	1.1588	0.7949	958.11	7573	
25.50	4.99	0.955	1.1655	0.7872	871.21	7554	
26.21	5.63	1.100	1.1724	0.7800	920.28	7532	
26.95	6.29	1.256	1.1803	0.7715	967.40	7505	
27.62	6.90	1.405	1.1869	0.7646	918.58	7487	
28.26	7.48	1.550	1.1935	0.7577	873.13	7469	
28.92	8.07	1.707	1.2003	0.7508	932.57	7450	
29.54	8.64	1.861	1.2064	0.7433	892.81	7431	
30.09	9.14	2.003	1.2122	0.7374	813.69	7414	
30.60	9.60	2.138	1.2180	0.7324	756.48	7398	
31.14	10.08	2.285	1.2235	0.7267	809.32	7381	
31.69	10.59	2.443	1.2295	0.7212	861.90	7363	
32.22	11.06	2.598	1.2355	0.7158	826.51	7346	
32.76	11.55	2.762	1.2417	0.7101	861.98	7327	
33.23	11.98	2.912		0.7064	767.42	7310	
			Dilution Seri	es G			
35.95	14.34	3.835	1.2758		• • •	7235	
35.57	14.09	3.730	1.2738	0.6828	22.42	7244	
35.30	13.85	3.629	1.2704		19.89	7252	
35.03	13.60	3.528	1.2671	0.6863	19.91	7260	
34.75	13.35	3.429	1.2643	0.6906	19.47	7268	
34.49	13.12	3.335	1.2613	0.6931	18.37	7275	
34.20	12.86	3.235	1.2581	0.6973	20.17	7284	
33.93	12.60	3.140	1.2549	0.6989	19.01	7292	
33.66	12.36	3.050	1.2523	0.7013	17.83	7300	
33.41	12.14	2.971	1.2499	0.6963	15.44	7307	
33.16	11.91	2.889		0.7068	16.20	7315 <sup>a</sup>	

<sup>a</sup> Calculated from Series F.

The observed values fit Equation 5 with a standard deviation of 10 cal  $mol^{-1}$  and Equation 6 with a standard deviation of 3 cal  $mol^{-1}$ . Integral enthalpies of solution at even values of molality and at saturation as calculated from the equations are shown in Table V.

**Urea orthophosphate in 19.99** %  $H_3PO_4$ . In Series F, urea orthophosphate was added to 19.99%  $H_3PO_4$  in successive increments to a final concentration of 2.91*m* urea orthophosphate. The initial solution of Series G was prepared by adding urea orthophosphate to 19.99%  $H_3PO_4$ . Chemical analysis showed it to contain 6.69% N and 26.04%  $P_2O_5$  or 3.84*m* urea orthophosphate. Successive increments of 19.99%  $H_3PO_4$  were added to this solution to a final concentration of 2.89*m* urea orthophosphate.

The observed properties of solutions of urea orthophos-

Orthophosphate in 19.99% H<sub>3</sub>PO₄ at 25°C

Table VII. Integral Enthalpies of Solution of Urea

phate in 19.99%  $H_3PO_4$  are shown in Table VI. The equation derived from the observed values is

$$\Delta H = 7704 - 171.0m + 12.72m^2 \tag{7}$$

The observed values fit Equation 7 with a standard deviation of 2 cal  $mol^{-1}$ . Integral enthalpies of solution at even values of molality and at saturation as calculated from Equation 7 are shown in Table VII.

**Urea in 49.91%**  $H_3PO_4$ . In Series H and I, crystalline urea was added to 49.91%  $H_3PO_4$  in successive increments to final concentrations of 1.73 and 1.65*m* urea, respectively.

The observed properties of solutions of urea in 49.91% H<sub>3</sub>PO<sub>4</sub> are shown in Table VIII. The equation derived from the observed values is

$$\Delta H = 613 + 270.3m_1 - 30.2m_1^2 \tag{8}$$

Table IX. Integral Enthalpies of Solution of Urea in 49.91% H<sub>3</sub>PO<sub>4</sub> at 25°C

	Concentration	า		
Wt %		Urea ortho-	$\Delta H$ , cal/mol	
H₃PO₄	$CO(NH_2)_2$	molality, m	phosphate	
20.64	0.59	0.1	7687	
21.28	1.16	0.2	7670	
23.07	2.78	0.5	7622	
25.72	5.19	1.0	7546	
28.04	7.28	1.5	7476	
30.08	9.13	2.0	7413	
31.89	10.76	2.5	7356	
33.50	12.22	3.0	7306	
34.95	13.53	3.5	7261	
36.23	14.69	3.99 <sup>a</sup>	7224	

	Concentration	ı	
Wt %		l Irea	AH cal/mol
H₃PO₄	CO(NH <sub>2</sub> ) <sub>2</sub>	molality, m	urea
49.61	0.60	0.1	639
49.32	1.19	0.2	665
48.45	2.92	0.5	740
47.08	5.67	1.0	853
45.79	8.26	1.5	950
45.19	9.45	1.74 <i>a</i>	991
<sup>a</sup> Saturat	ed solution.		

<sup>a</sup> Saturated solution.

#### Table VIII. Observed Properties of Solutions of Urea in 49.91% H<sub>3</sub>PO<sub>4</sub> at 25°C

Solution concentration						
	Wt %	Urea	Density, d.	Specific heat, s.	Enthalpy	of solution
H₃PO₄	$CO(NH_2)_2$	molality, m	g/ml	cal/°C/g	Q, cal/run	$\Delta H$ , cal/mol
			Solution Serie	s H		
49.91	0	0	1.3296			
49.38	1.06	0.179	1.3296	0.6416	134.22	664
48.72	2.39	0.407	1.3303	0.6396	198.12	726
48.24	3.35	0.576	1.3308	0.6408	156.25	759
47.77	4.29	0.747	1.3310	0.6410	169.30	792
47.34	5.14	0.902	1.3293	0.6406	166.86	826
46.89	6.04	1.071	1.3310	0.6403	188.28	860
46.41	7.01	1.256	1.3308	0.6397	218.40	897
45.95	7.94	1.436	1.3320	0.6390	223.00	932
45.49	8.86	1.619	1.3322	0.6385	235.50	966
45.21	9.42	1.732		0.6385	150.08	987
			Solution Serie	es l		
49.91	0	0	1.3295			
49.65	0.53	0.088	1.3288	0.6418	62.60	626
49.13	1.57	0.266	1.3297	0.6413	142.47	684
48.64	2.53	0.433	1.3300	0.6409	147.04	725
48.17	3.49	0.601	1.3303	0.6408	161.87	766
47.72	4.39	0.765	1.3300	0.6401	168.46	804
47.23	5.36	0.944	1.3310	0.6400	196.06	844
46.72	6.39	1.136	1.3314	0.6394	223.73	885
46.28	7.27	1.306	1.3310	0.6399	205.21	918
45.81	8.22	1.490	1.3316	0.6391	236.27	955
45.42	9.00	1.646	• • •	0.6400	206.63	986

Table X. Observed Properties of Solutions of	f Urea in 60.12% H <sub>3</sub>	PO₄ at 25°C
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Solution concentration							
Wt %			Density d	Specific heat a	Enthalpy of solution		
H₃PO₄	$CO(NH_2)_2$	molality, m g/ml		cal/°C/g	Q, cal/run	$\Delta H$ , cal/mo	
			Solution Seri	es J			
60.12	0	0	1.4216				
59.55	0.95	0.160	1.4212	0.5765	-89.22	-461.6	
59.04	1.80	0.305	1.4193	0.5762	-63.54	-415.5	
58.48	2.73	0.468	1.4181	0.5767	-52.13	-365.6	
57.89	3.71	0.642	1.4182	0.5767	-34.56	-312.2	
57.31	4.67	0.816	1.4186	0.5774	-13.41	-259.7	
56 <i>.</i> 76	5.59	0.986	1.4179	0.5775	6.32	-209.3	
56.17	6.57	1.170		0.5783	26.21	-156.6	
55.64	7.44	1.339	•••	0.5776	41.73	-108.9	

Table XI. Integral Enthalpies of Solution of Urea in 60.12% H<sub>3</sub>PO<sub>4</sub> at 25°C

	Concentratio	n	
	Wt %	l Irea	$\Delta H$ cal/mol
H₃PO₄	CO(NH <sub>2</sub> ) <sub>2</sub>	molality, m	urea
59.41	1.19	0.2	-448.9
58.71	2.35	0.4	-386.1
58.03	3.48	0.6	-324.6
57.36	4.58	0.8	-264.5
56.71	5.67	1.0	-205.6
56.08	6.72	1.2	-148.1
55.45	7.77	1.40 <sup>a</sup>	-91.1

<sup>a</sup> Saturated solution.

where  $m_1$  = molality urea. The observed values fit Equation 8 with a standard deviation of 6 cal mol<sup>-1</sup>. Integral enthalpies of solution at even values of molality and at saturation as calculated from Equation 8 are shown in Table IX.

Urea In 60.12%  $H_3PO_4$ . In Series J, crystalline urea was added to 60.12%  $H_3PO_4$  in successive increments to a final concentration of 1.34m urea.

The observed properties of solutions of urea in 60.12%  $H_3 PO_4$  are shown in Table X. The equation derived from the observed values is

$$\Delta H = -513.0 + 323.9m_1 - 16.44m_1^2 \tag{9}$$

The observed values fit Equation 9 with a standard deviation of 0.3 cal mol<sup>-1</sup>. Integral enthalpies of solution at even values of molality and at saturation as calculated from Equation 9 are shown in Table XI.

**Urea in 75.03** %  $H_3PO_4$ . In Series K crystalline urea was added to 75.03%  $H_3PO_4$  in successive increments to a final concentration of 0.61*m* urea. The initial solution of Series L was prepared by adding urea to 75.03%  $H_3PO_4$ . Chemical analysis showed it to contain 50.41% N and 3.36%  $P_2O_5$  or 1.29*m* urea. Successive increments of 75.03%  $H_3PO_4$  were added to this solution to a final concentration of 0.65*m* urea.

The observed properties of solutions of urea in  $75.03\,\%$   $H_3PO_4$  are shown in Table XII. The equation derived from the observed values is

$$\Delta H = -2805 + 494m_1 - 49m_1^2 \tag{10}$$

The observed values fit the equation with a standard deviation of 5 cal  $mol^{-1}$ . Integral enthalpies of solution at even values of molality and at saturation as calculated from Equation 10 are shown in Table XIII.

#### **Enthalpy of Formation of Urea Orthophosphate**

The standard enthalpy of formation of urea orthophosphate was determined from the enthalpy of Reaction 11 ( $\Delta H_{11}$ ) at 25°C

$$CO(NH_2)_2(c) + H_3PO_4 \cdot 1.00H_2O(I) = CO(NH_2)_2 \cdot H_3PO_4(c) + 1.00H_2O(I) \quad (11)$$

in combination with published values for the enthalpy of formation of  $CO(NH_2)_2$  and  $H_3PO_4 \cdot 1.00H_2O$ , the enthalpy of dilution of phosphoric acid solutions, and the integral enthalpy of solution of urea orthophosphate in  $H_2O$  at 25°C.

The phosphoric acid solution contained 61.15% P<sub>2</sub>O<sub>5</sub>. The calorimetric solvent was distilled water.

The enthalpy of reaction for Equation 11 was determined by the scheme:

Ampul H3PO4•1.00H2O + solvent = solution A
$$\Delta H_x$$
Ampul CO(NH2)2 + solution A = solution B $\Delta H_y$ Ampul CO(NH2)2•H3PO4 + solvent = solution B $\Delta H_z$  $\Delta H_{11} = \Delta H_x + \Delta H_y - \Delta H_z$ 

The enthalpies of solution of ampuls of urea in the solvent to which the stoichiometric amounts of  $H_3PO_4 \cdot 1.00H_2O$  had been added,  $\Delta H_y$ ; the enthalpies of solution of the stoichiometric amounts of  $H_3PO_4 \cdot 1.00H_2O$ ,  $\Delta H_x$ , calculated from the data of Egan and Luff (2); and the enthalpies of solution of the stoichiometric amount of CO(NH<sub>2</sub>)<sub>2</sub>·H<sub>3</sub>PO<sub>4</sub>,  $\Delta H_z$ , calculated from Equation 4; and the enthalpy of Reaction 11 are listed in Table XIV.

The standard enthalpies of formation from the elements at 25°C (4) are  $H_3PO_4$ •1.00 $H_2O$ ,  $-304.69 \pm 0.1$ ; and  $CO(NH_2)_2$ ,  $-79.56 \pm 0.1$  kcal mol<sup>-1</sup>. Substitution of these values, along with the enthalpy of reaction of Equation 11 (-7799 cal), in the equation

$$\Delta H_{\rm f}^{\circ} CO(\rm NH_2)_2 \cdot H_3 PO_4(c) = \Delta H_{\rm f}^{\circ} H_3 PO_4 \cdot 1.00 H_2 O(l) + \Delta H_{\rm f}^{\circ} CO(\rm NH_2)_2(c) + \Delta H_{\rm R} \quad (12)$$

gives  $-392.05 \pm 0.14$  kcal mol<sup>-1</sup> for the standard enthalpy of formation of CO(NH<sub>2</sub>)<sub>2</sub>·H<sub>3</sub>PO<sub>4</sub> at 25°C.

### Integral Enthalpy of Solution at Saturation of Urea Orthophosphate in Concentrated H<sub>3</sub>PO<sub>4</sub> Solutions

Attempts to determine the enthalpy of solution of urea orthophosphate in 40%  $H_3PO_4$  were unsuccessful because of the small temperature change and the low dissolution rate in the solution calorimeter. The integral enthalpy of solution at saturation of urea orthophosphate in more concentrated solutions of  $H_3PO_4$  can be determined by the scheme

$\begin{tabular}{ c c c c c c c c c c c c c c c c c c c$	Solution concentration							
$\begin{array}{c c c c c c c c c c c c c c c c c c c $		Wt %	L Irea	Density d	Specific heat s	Enthalpy of solution		
Solution Series K         75.03       0       0       1.5701            74.35       0.91       0.153       1.5673       0.4966       -560.46       -2746         73.65       1.84       0.312        0.4959       -535.46       -2646         73.03       2.67       0.457        0.4960       -455.47       -2576         72.38       3.54       0.610        0.4961       -460.35       -2513         Dilution Series L         69.60       7.20       1.292       1.5518         -2242         69.75       7.03       1.259       1.5525       0.4998       -22.18       -2256         69.88       6.87       1.227       1.5530       0.4998       -20.55       -2269         69.99       6.72       1.200       1.5529       0.4998       -17.61       -2281         70.09       6.58       1.172       1.5537       0.4994       -17.14       -2292	H₃PO₄	$CO(NH_2)_2$ molality, m		g/ml	cal/°C/g	Q, cal/run	$\Delta H$ , cal/mol	
$\begin{array}{cccccccccccccccccccccccccccccccccccc$				Solution Seri	ies K			
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	75.03	0	0	1.5701				
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	74.35	0.91	0.153	1.5673	0.4966	-560.46	-2746	
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	73.65	1.84	0.312		0.4959	-535.46	-2646	
72.38       3.54       0.610        0.4961       -460.35       -2513         Dilution Series L         69.60       7.20       1.292       1.5518        -2242         69.75       7.03       1.259       1.5525       0.4998       -22.18       -2256         69.88       6.87       1.227       1.5530       0.4998       -20.55       -2269         69.99       6.72       1.200       1.5529       0.4998       -17.61       -2281         70.09       6.58       1.172       1.5537       0.4994       -17.14       -2292	73.03	2.67	0.457		0.4960	-455.47	-2576	
Dilution Series L69.607.201.2921.5518224269.757.031.2591.55250.4998-22.18-225669.886.871.2271.55300.4998-20.55-226969.996.721.2001.55290.4998-17.61-228170.096.581.1721.55370.4994-17.14-2292	72.38	3.54	0.610		0.4961	-460.35	-2513	
69.607.201.2921.5518224269.757.031.2591.55250.4998-22.18-225669.886.871.2271.55300.4998-20.55-226969.996.721.2001.55290.4998-17.61-228170.096.581.1721.55370.4994-17.14-2292				Dilution Seri	es L			
69.757.031.2591.55250.4998-22.18-225669.886.871.2271.55300.4998-20.55-226969.996.721.2001.55290.4998-17.61-228170.096.581.1721.55370.4994-17.14-2292	69.60	7.20	1.292	1.5518			-2242	
69.88         6.87         1.227         1.5530         0.4998         -20.55         -2269           69.99         6.72         1.200         1.5529         0.4998         -17.61         -2281           70.09         6.58         1.172         1.5537         0.4994         -17.14         -2292	69.75	7.03	1.259	1.5525	0.4998	-22.18	-2256	
69.996.721.2001.55290.4998-17.61-228170.096.581.1721.55370.4994-17.14-2292	69.88	6.87	1,227	1.5530	0.4998	-20.55	-2269	
70.09 6.58 1.172 1.5537 0.4994 -17.14 -2292	69.99	6.72	1.200	1.5529	0.4998	-17.61	-2281	
	70.09	6.58	1.172	1.5537	0.4994	-17.14	-2292	
70.21 6.42 1.143 1.5546 0.4995 -17.75 -2305	70.21	6.42	1.143	1.5546	0.4995	-17.75	-2305	
70.32 6.28 1.116 1.5555 0.4990 -15.58 -2316	70.32	6.28	1.116	1.5555	0.4990	-15.58	-2316	
70.42 6.14 1.090 1.5550 0.4991 -14.27 -2326	70.42	6.14	1.090	1.5550	0.4991	-14.27	-2326	
70.53 6.00 1.063 1.5553 0.4990 -15.39 -2338	70.53	6.00	1.063	1.5553	0.4990	-15.39	-2338	
70.63 5.86 1.037 1.5554 0.4987 -13.76 -2348	70.63	5.86	1.037	1.5554	0.4987	-13.76	-2348	
70.73 5.73 1.012 1.5556 0.4987 -12.89 -2358	70.73	5.73	1.012	1.5556	0.4987	-12.89	-2358	
70.83 5.60 0.987 1.5558 0.4986 -12.49 -2368	70.83	5.60	0.987	1.5558	0.4986	-12.49	-2368	
70.93 5.47 0.963 1.5567 0.4985 -12.34 -2378	70.93	5,47	0,963	1.5567	0.4985	-12.34	-2378	
71.02 5.34 0.939 1.5568 0.4984 -11.57 -2388	71.02	5.34	0.939	1.5568	0.4984	-11.57	-2388	
71.11 5.22 0.917 1.5569 0.498210.562397	71.11	5.22	0.917	1.5569	0.4982	-10.56	-2397	
71.20 5.10 0.895 1.5575 0.4982 -9.90 -2405	71.20	5.10	0.895	1.5575	0.4982	-9.90	-2405	
71.29 4.99 0.875 1.5582 0.4981 -8.91 -2413	71.29	4.99	0.875	1.5582	0.4981	-8.91	-2413	
71.37 4.88 0.854 1.5580 0.4980 -9.28 -2422	71.37	4.88	0.854	1,5580	0.4980	-9.28	-2422	
71.45 4.77 0.834 1.5584 0.4979 -8.29 -2429	71.45	4.77	0.834	1.5584	0.4979	-8.29	-2429	
71.53 4.67 0.816 1.5586 0.4981 -7.18 -2436	71.53	4.67	0.816	1.5586	0.4981	-7.18	-2436	
71.60 4.57 0.797 1.5584 0.4977 -7.00 -2443	71.60	4.57	0.797	1,5584	0.4977	-7.00	-2443	
71.68 4.46 0.778 1.5590 0.4979 -8.22 -2451	71.68	4.46	0.778	1.5590	0.4979	-8.22	-2451	
71.75 4.37 0.760 1.5587 0.4981 -7.12 -2458	71.75	4.37	0.760	1.5587	0.4981	-7.12	-2458	
71.82 4.28 0.744 1.5590 0.4979 -5.95 -2465	71.82	4.28	0.744	1.5590	0.4979	-5.95	-2465	
71.89 4.19 0.727 1.5593 0.4976 -6.02 -2471	71.89	4.19	0.727	1.5593	0.4976	-6.02	-2471	
71.96 4.10 0.712 1.5595 0.4978 -5.81 -2477	71.96	4.10	0.712	1.5595	0.4978	-5.81	-2477	
72.02 4.01 0.695 1.55885.69 -2484	72.02	4.01	0.695	1,5588		-5.69	-2484	
72.08 3.93 0.680 1.5598 0.4976 -5.08 -2489	72.08	3.93	0.680	1.5598	0.4976	-5.08	-2489	
72.15 3.84 0.665 1.5592 0.4964 -4.67 -2495	72.15	3.84	0.665	1.5592	0.4964	-4.67	-2495	
72.22 3.75 0.648 0.4976 -5.53 -25014	72.22	3.75	0.648		0.4976	-5.53	$-2501^{a}$	

Table XII. Observed Properties of Solutions of Urea in 75.03% H<sub>3</sub>PO<sub>4</sub> at 25°C

<sup>a</sup> Calculated from Series K.

#### Table XIII. Integral Enthalpies of Solution of Urea in 75.03% H<sub>3</sub>PO<sub>4</sub> at 25°C

	Concentration				
	Wt %	L Irea	$\Delta H$ cal/mol		
H₃PO₄	CO(NH <sub>2</sub> ) <sub>2</sub>	molality, m	urea		
74.14	1.19	0.2	-2708		
73.27	2.35	0.4	-2615		
72.42	3.48	0.6	-2526		
71.59	4.58	0.8	-2441		
70.78	5.67	1.0	-2360		
69.99	6.72	1.2	-2283		
69.48	7.40	1.33 <i>a</i>	-2234		

<sup>a</sup> Saturated solution.

 $H_3PO_4 \cdot aH_2O + bCO(NH_2)_2 = H_3PO_4 \cdot aH_2O \cdot bCO(NH_2)_2$  (13)

 $H_3PO_4 + aH_2O = H_3PO_4 \cdot aH_2O$  (14)

 $H_3PO_4 + a/(1-b)H_2O = H_3PO_4 \cdot a/(1-b)H_2O$  (15)

 $H_3PO_4 + CO(NH_2)_2 = CO(NH_2)_2 H_3PO_4$  (16)

 $\frac{1/b\{(13) + (14) - (1 - b)(15) - b(16)\}}{\{(1 - b)/b\}\{H_3PO_4 \cdot a/(1 - b)H_2O\} + CO(NH_2)_2 \cdot H_3PO_4} = \frac{1/b\{H_3PO_4 \cdot aH_2O \cdot bCO(NH_2)_2\}}{1/b\{H_3PO_4 \cdot aH_2O \cdot bCO(NH_2)_2\}}$ (17)

The value for *a* can be calculated from the concentration of the phosphoric acid solution to which the urea is to be added, and *b* can be calculated from the composition of the phosphoric acid solution saturated with urea. The enthalpy of Reaction 13,  $\Delta H_{13}$ , can be determined from the integral enthalpy of solution of urea in the phosphoric acid to saturation. The value for a/(1 - b) can be calculated from *a* and *b*. The formula H<sub>3</sub>PO<sub>4</sub>•*a*/(1 - *b*)H<sub>2</sub>O gives the concentration of phosphoric acid to which urea phosphate must be added to obtain the saturated solution of the third term of Equation 13. A linear equation for percent phosphoric acid as a function of percent urea from the composition of urea phosphate through the composition of the saturated solution of Equation 13 extrapolated to 0% urea also gives the concentration of phosphoric acid corresponding to H<sub>3</sub>PO<sub>4</sub>•*a*/(1 - *b*)H<sub>2</sub>O.

The enthalpies of Reactions 14 and 15,  $\Delta H_{14}$  and  $\Delta H_{15}$ , respectively, can be calculated from the data of Luff et al. (3) and Egan and Luff (2). The enthalpy of Reaction 16,  $\Delta H_{16}$ ,

#### Table XIV. Observed Enthalpies of Reaction for Equation 11

	Run no.					
	1	2	3	4	5	
Solvent wt, grams	848.0695	848.0445	848.2818	848.3949	848.1967	
Urea wt, grams	12.09067	12.43737	12.91616	13.26962	13.92902	
Stoich, H <sub>2</sub> PO <sub>4</sub> ·1.00H <sub>2</sub> O, grams	23.03708	24.03708	24.96821	25.64553	26.91992	
Molality H <sub>3</sub> PO <sub>4</sub> , final soln	0.2364	0.2431	0.2524	0.2592	0.2721	
$\varphi_{\rm L}$ H <sub>3</sub> PO <sub>4</sub> , <sup><i>a</i></sup> final soln cal mol <sup>-1</sup>	180	182	186	188	193	
$\Delta H_{1}$ , cal mol <sup>-1</sup>	-3571	-3569	-3565	-3563	-3558	
Stoich. CO(NH <sub>2</sub> ) <sub>2</sub> ·H <sub>3</sub> PO <sub>4</sub> , grams	31.81950	32.73192	33.99987	34.92219	36.65756	
Molality CO(NH <sub>2</sub> ) <sub>2</sub> ·H <sub>3</sub> PO <sub>4</sub> , final soln	0.2364	0.2431	0.2524	0.2592	0.2721	
$\Delta H_{3}$ , cal mol <sup>-1</sup>	7733	7732	7730	7729	7727	
$\Delta H_{a}$ , cal mol <sup>-1</sup>	3505	3501	3497	3495	3486	
$\Delta H_{\rm R}$ , Equation 11	-7799	-7800	-7798	-7797	-7799	
	Average $\Delta H$	<sub>R</sub> = -7799 cal				

 ${}^a \varphi_{\rm L}$  (H<sub>3</sub>PO<sub>4</sub>·1.00H<sub>2</sub>O) = 3751 cal mol<sup>-1</sup>.

Table XV.	Calculation of Integral Enthalpies of Solution
	to Saturation of Urea Phosphate in Phosphoric
	Acid Solutions at 25°C

	$\% H_{3}PO_{4} \sim H_{3}PO_{4} \cdot aH_{2}O$					
	49.91	60.12	75.03			
$\Delta H_{\rm T_1}$ , cal/mol <sup>a</sup>	991	-91.1	-2234			
a <sup>-</sup> ,	5.46	3.61	1.81			
ь	0.34	0.23	0.17			
$\Delta H_{13}$ , cal	337	-21	-380			
$\Delta H_{14}$ , cal	-4399	-3918	-2961			
a/(1-b)	8.29	4.68	2.19			
	$\% H_{3}PO_{4} \sim H_{3}PO_{4} \cdot a/(1-b)H_{2}O$					
	39.63	53.77	71.29			
$\Delta H_{15}$ , cal	-4780	-4230	-3235			
$\Delta H_{16}$ , cal	-9948	-9948	-9948			
$\Delta H_{17}$ , cal b	7280	6983	6089			

<sup>a</sup> Integral enthalpy of solution of urea at saturation in  $H_3PO_4 \cdot aH_2O$ . <sup>b</sup> Integral enthalpy of solution of urea phosphate at saturation in  $H_3PO_4 \cdot a/(1 - b)H_2O$ .

Table XVI. Enthalpy of Producing Crystalline Urea Orthophosphate from Equimolar Amounts of Urea and Phosphoric Acid at 25°C

0/2	*	$\Delta H$	d	$\Delta H$	$\Lambda H$	$\Delta H$
H₃PO₄	х, Eq. 21	cal	u, Eq. 21	cal	cal	cal/g
		Satd s	soln Q. Fi	aure 1		
100	0	-9948	0	0	-9948	-62.94
95	0.2863	-8898	0.0352	250	-8648	-56.72
90	0.6044	-8228	0.0744	527	-7701	-52.64
85	0.9599	-7855	0.1182	837	-7018	-50.36
80	1.3599	-7393	0.1674	1185	-6208	-47.17
75	1.8132	-6985	0.2232	1580	-5405	-44.02
70	2.3312	-6624	0.2870	2032	-4592	-40.75
65	2.9290	-6306	0.3605	2553	-3753	-37.14
60	3.6264	6024	0.4464	3161	-2863	-32.73
55	4.4505	-5775	0.5479	3879	-1896	-26.53
50	5.4396	-5553	0.6696	4741	-813	-15.55
45	6 6483	-5356	0.8185	5795	439	15 29

(-9948 cal) can be calculated by adding the enthalpy of dilution from H<sub>3</sub>PO<sub>4</sub> to H<sub>3</sub>PO<sub>4</sub>•1.00H<sub>2</sub>O (*2*, *3*) (-2149 cal) to the enthalpy of Reaction 11 (-7799 cal). Combining  $\Delta H_{13}$  through  $\Delta H_{16}$  in the manner indicated will give the enthalpy of Reaction 17,  $\Delta H_{17}$ , the integral enthalpy of solution of 1 mole of urea orthophosphate in sufficient phosphoric acid of the concentration expressed in the first term of Equation 17 to form a saturated solution.

Values for the integral enthalpies of solution to saturation  $(\Delta H_{T_1})$  of urea in 49.91, 60.12, and 75.05% H<sub>3</sub>PO<sub>4</sub> along with the calculations of the integral enthalpies of solution to saturation  $(\Delta H_{T_2})$  of urea phosphate in 39.63, 53.77, and 71.29% H<sub>3</sub>PO<sub>4</sub> by use of Equations 13–17 are summarized in Table XV.

## Enthalpy of Crystallization of Urea Orthophosphate from Urea and Phosphoric Acid Solutions at 25°C

Subtracting the enthalpy of Reaction 18 ( $\Delta H_{18}$ )

$$H_3PO_4 \cdot 1.00H_2O + (x - 1)H_2O = H_3PO_4 \cdot xH_2O$$
 (18)

from  $\Delta H_{11}$  (-7799 cal) gives the enthalpy of Reaction 19 ( $\Delta H_{19}$ ).

$$CO(NH_2)_2(c) + H_3PO_4 \cdot xH_2O(l) =$$
  
 $CO(NH_2)_2 \cdot H_3PO_4(c) + xH_2O(l)$  (19)

The value of  $\Delta H_{18}$  was calculated from published data (2, 3).

Part of the urea orthophosphate remains in the saturated solution so

(20)

$$xH_2O(I) + a_1^4CO(NH_2)_2 H_3PO_4(c) = a_1H_3PO_4 a_2CO(NH_2)_2 xH_2O$$

where *d* is the number of moles of urea orthophosphate needed to saturate the water from the phosphoric acid solution (see Table III). The value of  $\Delta H_{20}$  was calculated from the integral enthalpy of solution at saturation of urea orthophosphate in water (7080 cal/mol).

Adding  $\Delta H_{20}$  to  $\Delta H_{19}$  gives  $\Delta H_{21}$ , the enthalpy of Reaction 21

$$CO(NH_{2})_{2}(c) + H_{3}PO_{4} \cdot xH_{2}O(I) = (1 - d)\{CO(NH_{2})_{2} \cdot H_{3}PO_{4}\}(c) + dH_{3}PO_{4} \cdot dCO(NH_{2})_{2} \cdot xH_{2}O \quad (21)$$

and  $\Delta H_{21}/158.05114(1 - d)$  gives the enthalpy of producing crystalline urea orthophosphate ( $\Delta H_c$ ) in calories per gram

from equimolar amounts of urea and phosphoric acid. Values of x,  $\Delta H_{19}$ , d,  $\Delta H_{20}$ ,  $\Delta H_{21}$ , and  $\Delta H_c$  for different concentrations of phosphoric acid are listed in Table XVI.

 $xH_2O + dCO(NH_2)_2(c) = dCO(NH_2)_2 \cdot xH_2O$  (22)

and 23 ( $\Delta H_{23}$ )

Enthalpies of producing crystalline urea orthophosphate from solutions of phosphoric acid and excess urea were determined by adding the enthalpies of Reactions 22 ( $\Delta H_{22}$ )

 $dCO(NH_{2})_{2} \cdot xH_{2}O + e\{CO(NH_{2})_{2} \cdot H_{3}PO_{4}\}(c) = (d + e)CO(NH_{2})_{2} \cdot eH_{3}PO_{4} \cdot xH_{2}O \quad (23)$ 

% H <sub>3</sub> PO <sub>4</sub>	<i>x</i> , Eq. 24	$\Delta H_{19}$ , cal	<i>d</i> , Eq. 24	$\Delta H_{_{22}}$ , cal	<i>e</i> , Eq. 24	$\Delta H_{_{23}}$ , cal	$\Delta H_{{\scriptscriptstyle 24}}$ , cal	$\Delta H_{ m c}$ , cal/g
			Sat	d soln R, Figu	re 1			
100	0	-9948	0	0	0	0	-9948	-62.94
95	0.2863		0.0220	. 74	0.0390	249	-8574	-56.45
90	0.6044	-8228	0.0464	157	0.0824	526	-7545	-52.02
85	0.9599	-7855	0.0737	249	0.1309	836	-6770	-49.28
80	1.3599	7393	0.1044	353	0.1854	1185	-5856	-45.48
75	1.8132	-6985	0.1391	471	0.2472	1579	-4935	-41.48
70	2.3312	-6624	0.1789	605	0.3179	2031	-3988	-36.99
65	2.9290	-6306	0.2248	760	0.3994	2551	-2995	-31.55
60	3.6264	-6024	0.2783	941	0.4945	3159	-1924	-24.08
55	4.4505	-5775	0.3415	1155	0.6069	3877	-743	-11.96
50	5.4396		0.4174	1412	0.7417	4738	597	14.62
45	6.6483	-5356	0.5102	1725	0.9066	5791	2161	146.31

Table XVIII. Enthalpy of Producing Crystalline Urea Orthophosphate from Urea and Excess Phosphoric Acid at 25°C

$H_3PO_4$	<i>x</i> , Eq. 27	$\Delta H_{_19}$ , cal	<i>d</i> , Eq. 27	$\Delta H_{25}$ , cal	<i>e</i> , Eq. 27	$\Delta H_{\rm 26}$ , cal	$\Delta H_{27}$ , cal	$\Delta H_{ m c}$ , cal/g
			Sat	d soln P, Figur	e 1			
100	0	-9948	0	0	0	0	-9948	-62.94
95	0.2863	-8898	0.0133	-57	0.0260	188	-8767	-56.95
90	0.6044	-8228	0.0286	-102	0.0558	403	-7927	-53.12
85	0.9599	-7855	0.0461	-148	0.0901	651	-7352	-51.12
80	1.3599	-7393	0.0666	-183	0.1302	941	-6635	-48.27
75	1.8132	-6985	0.0908	-213	0.1776	1283	-5915	-45.50
70	2.3312	-6624	0.1199	-237	0.2344	1693	-5168	-42.71
65	2.9290	-6306	0.1554	-258	0.3038	2195	-4369	-39.71
60	3.6264	<del>-</del> 6024	0.1998	-276	0.3906	2822	-3478	-36.11
55	4.4505	-5775	0.2569	-290	0.5022	3628	-2438	-30.98
50	5.4396	-5553	0.3331	-302	0.6510	4702	-1153	-20.90
45	6.6483	-5356	0.4396	-313	0.8592	6207	538	24.19
			Sat	d soln O, Figu	re 1			
100	0	-9948	0	0	0	0	-9948	-62.94
95	0.2863	-8898	0.0358	-134	0.0185	135		-57.35
90	0.6044	-8228	0.0787	-241	0.0407	296	-8173	-53.91
85	0.9599	-7855	0.1310	-353	0.0678	494	-7715	-52.36
80	1.3599	-7393	0.1963	-439	0.1016	740	-7092	-49.95
75	1.8132	-6985	0.2801	-511	0.1449	1055	-6441	-47.66
70	2.3312	-6624	0.3915	-574	0.2026	1475	-5723	-45.41
65	2.9290	-6306	0.5467	-627	0.2829	2059	-4874	-43.00
60	3.6264	-6024	0.7782	673	0.4026	2931	-3766	-39.89
55	4.4505	-5775	1.1603	-715	0.6003	4370	-2119	-33.55
50	5.4396	-5553	1.9108	-753	0.9887	7197	892	497.47
			Sat	d soln N, Figu	re 1			
100	0	-9948	0	0	0	0	-9948	-62.94
95	0.2863	-8898	0.0652	-207	0.0193	135	-8971	-57.87
90	0.6044	-8228	0.1484	-373	0.0439	306	-8294	-54.89
85	0.9599	-7855	0.2583	-552	0.0764	533	-7874	-53.94
80	1.3599	-7393	0.4100	-687	0.1212	846	-7233	-52.08
75	1.8132	-6985	0.6332	-802	0.1872	1307	-6480	-50.44
70	2.3312	-6624	0.9939	-900	0.2938	2052	-5473	-49.03
65	2.9290	-6306	1.6758	-985	0.4955	3460	-3832	-48.05
			Sat	d soln M, Figu	re l			
100	0	-9948	0	0	0	0	-9948	-62.94
95	0.2863	-8898	0.1503	-328	0.0316	193	-9034	-59.03
90	0.6044	-8228	0.3810	-577	0.0802	488	-8317	-57.21
85	0.9599	7855	0.7800	-891	0.1642	1000	-7746	-58.64
80	1.3599	-7393	1.6370	-1113	0.3446	2098	-6408	-61.86

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to  $\Delta H_{19}$  to give the enthalpy of Reaction 24 ( $\Delta H_{24}$ )

$$(1 + d)CO(NH_2)_2 + H_3PO_4 \cdot xH_2O = (1 - e) \{CO(NH_2)_2 \cdot H_3PO_4\}(c) + (d + e)CO(NH_2)_2 \cdot eH_3PO_4 \cdot xH_2O$$
(24)

The value d was calculated to make the third term of Equation 22 equivalent to 20.37% urea, and e was calculated to make the third term of Equation 23 equivalent to the saturat-

ed solution given in Table V. The value of  $\Delta H_{22}$  was calculated from published values for the enthalpy of solution of urea (1), and  $\Delta H_{23}$  was calculated from the integral enthalpy of solution at saturation of urea orthophosphate in 20.37% urea solution (6388 cal/mol). The expression  $\Delta H_{24}$ /{158.05114 (1 - e)} gives the enthalpy of crystallization of urea orthophosphate in calories per gram under the conditions of Equation 24. Values of x,  $\Delta H_{19}$ , d,  $\Delta H_{22}$ , e,  $\Delta H_{23}$ ,  $\Delta H_{24}$ , and  $\Delta H_c$  for different concentrations of phosphoric acid are listed in Table XVII.

		M/troa	Satd soln, wt %		Reactants in soln, %			
% H₃PO₄	Wt urea, g	orthophosphate, g	H₃PO₄	Urea	H <sub>3</sub> PO <sub>4</sub>	Urea	$-\Delta H_{ m c}$ , kcal	
95	506	1290	69.5	7.4	15.8	3.2	76.13	
	547	1411	55.4	7.8	7.9	1.9	81.64	
	562	1452	45.2	9.4	5.2	1.9	83.27	
	575	1473	36.2	14.7	3.9	2.6	83,87	
	582	1478	32.2	19.7	3.5	3.5	83.84	
	595	1472	30.2	29.0	39	6.0	83.12	
90	399	967	69.5	7 4	33.4	8.0	55 31	
50	480	1209	55.4	7.8	16.7	4 A	66 33	
	511	1203	45.2	9.0	11 1	4.1	69.55	
	536	1233	36.2	14.7	8.2	5.6	70 78	
	550	1333	30.2	10.7	7.4	7.4	70.78	
	552	1344	32.2	19.7	7.4	12.2	60.20	
05	202	1332	50.Z	29.0	0.Z	12.5	27.75	
65	293	1000	09.D	7.4	53.0	10.4	57.75	
	414	1006	55.4	7.8	20.0	7.6	54.28	
	461	1130	45.2	9.4	17.0	0.8	59.16	
	498	1192	36.2	14.7	13.0	9.0	60.96	
	521	1209	32.2	19.7	11.8	11.8	50.88	
	559	1191	30.2	29.0	13.1	19.1	58.72	
80	186	321	69.5	7.4	/5.1	34.5	. 19.84	
	348	804	55.4	7.8	37.7	12.1	41.88	
	410	969	45.2	9.4	24.9	10.2	48.40	
	460	1052	36.2	14.7	18.5	13.0	50.79	
	490	1074	32.2	19.7	16.7	16.7	50.68	
	541	1051	30.2	29.0	18.5	26.2	47.80	
75	281	602	55.4	7.8	50.2	18.7	30.37	
	359	808	45.2	9.4	33.2	14.5	38.51	
	421	912	36.2	14.7	24.6	17.8	41.50	
	460	940	32.2	19.7	22.3	22.3	41.36	
	524	911	30.2	29.0	24.7	33.9	37.77	
70	215	400	55.4	7.8	64.6	29.4	19.60	
	308	647	45.2	9.4	42.7	20.3	29.38	
	383	772	36.2	14.7	31.6	23.4	32.96	
	429	805	32.2	19.7	28.7	28,7	32.80	
	506	770	30.2	29.0	31.8	42.1	28.49	
65	149	198	55.4	7.8	81.1	49.5	9.50	
00	258	486	45.2	9.4	53.6	28.3	20.90	
	345	632	36.2	14.7	39.7	30.4	25.08	
	398	670	32.2	19.7	36.1	36.1	24.89	
	488	630	30.2	29.0	39.9	51.0	19.86	
60	207	325	45.2	9.4	66.4	40.3	12.00	
00	306	491	36.2	14.7	49.2	39.1	17 75	
	368	536	32.2	19.7	44.6	44.6	17.53	
	470	489	30.2	29.0	49.4	60.5	11 78	
55	156	164	45.2	9.4	81.5	60.0	5 51	
55	268	351	36.2	14.7	60.4	50.2	10.88	
	200	401	32.2	19.7	5/ 8	54.8	10.60	
	452	3/0	30.2	29.0	60.7	70.7	4 1 7	
50	105	2+5	45.2	2 <i>3</i> .0	99.7	98 G	-1 56	
50	100	5 21 1	70.2	5.4 1/1 7	72 0	65 1	4 / 1	
	200	211	32.2	10 7	67.0	67.0	 A 1A	
	200	200 202	30.2	19.7 20 N	74 2	81 S		
45	102	∠∪0 71	36.2	29.0	00 2	85 G	1 72	
40	192	122	30.2	19.7	90.2 81 8	20.5 g1 g	-2 02	
	416	68	30.2	29.0	90.7	93.8	-9.92	



Figure 2. Enthalpy change and urea orthophosphate crystallized when urea is added to 1000 grams of 75% H<sub>3</sub>PO<sub>4</sub>

Table XX. Heat Capacity, cal °C<sup>-1</sup> g<sup>-1</sup>, of Solutions Containing Phosphoric Acid and Urea at 25°C

	% Urea					
% H₃PO₄	0	5	10	15	20	25
0	1.000	0.971	0.943	0.915	0.887	
5	0.961	0.933	0.906	0.880	0.853	
10	0.923	0.896	0.870	0.845	0.820	
15	0.885	0.860	0.835	0.811	0.787	
20	0.848	0.824	0.801	0.778	0.755	0.733
25	0.812	0.789	0.767	0.745	0.724	0.703
30	0.776	0.755	0.734	0.713	0.693	0.673
35	0.742	0.721	0.702			
40	0.707	0.688	0.670			
45	0.674	0.656				
50	0.641	0.625				
55	0.609	0.594				
60	0.578	0.564				
65	0.547	0.534				
70	0.517	0.505				

Table XXI. Density, g ml<sup>-1</sup>, of Solutions Containing Phosphoric Acid and Urea at 25°C

	% Urea						
% H₃PO₄	0	5	10	15	20	25	
0 5 10 15 20 25 30 35 40 45 50 55 60 65 70	1.001 1.025 1.052 1.080 1.110 1.142 1.176 1.212 1.250 1.289 1.331 1.374 1.420 1.467 1.516	1.015 1.040 1.067 1.097 1.128 1.161 1.196 1.233 1.271 1.312 1.355 1.399 1.445 1.494 1.544	1.028 1.055 1.083 1.113 1.145 1.179 1.215 1.253 1.293	1.041 1.069 1.098 1.129 1.162 1.198 1.234	1.054 1.083 1.113 1.145 1.179 1.215 1.253	1.196 1.233 1.272	

Enthalpies of producing crystalline urea orthophosphate from urea and excess phosphoric acid were determined by adding the enthalpies of Reactions 25 ( $\Delta H_{25}$ )

$$d(H_3PO_4 \cdot xH_2O) + xH_2O = dH_3PO_4 \cdot (x + dx)H_2O \quad (25)$$

and 26 ( $\Delta H_{26}$ )

$$dH_{3}PO_{4}(x + dx)H_{2}O + e\{CO(NH_{2})_{2}H_{3}PO_{4}\}(c) = (d + e)H_{3}PO_{4}eCO(NH_{2})_{2}(x + dx)H_{2}O$$
(26)

to  $\Delta H_{19}$  to give the enthalpy of Reaction 27 ( $\Delta H_{27}$ )

$$CO(NH_{2})_{2} + (1 + d) \{H_{3}PO_{4} \cdot xH_{2}O\} = (1 - e) \{CO(NH_{2})_{2} \cdot H_{3}PO_{4}\}(c) + (d + e)H_{3}PO_{4} \cdot eCO(NH_{2})_{2} \cdot (x + dx)H_{2}O$$
(27)

The value d was calculated to give the phosphoric acid concentration of the third term of Equation 25 in which the integral enthalpies of solution of urea orthophosphate had been determined (19.99%, 39.63%, 53.77%, and 71.29% H<sub>3</sub>PO<sub>4</sub>, respectively), and e was calculated to make the third term of Equation 26 equivalent to the corresponding saturated solutions given in Tables VII, IX, XI, and XIII. The value  $\Delta H_{25}$  was calculated from published values for the enthalpy of dilution of phosphoric acid solutions (2, 3), and  $\Delta H_{26}$  was calculated from the integral enthalpy of solution at saturation of urea orthophosphate in  $19.99\,\%,\ 39.63\,\%,\ 53.77\,\%,\ and\ 71.29\,\%$ H<sub>3</sub>PO<sub>4</sub>. Values of x,  $\Delta H_{19}$ , d,  $\Delta H_{25}$ , e,  $\Delta H_{26}$ ,  $\Delta H_{29}$ , and  $\Delta H_{c}$ under conditions of excess H<sub>3</sub>PO<sub>4</sub> described for different concentrations of phosphoric acid are listed in Table XVIII.

Calculations of material balance and enthalpy change based on the addition of urea to 1000 grams of various concentrations of phosphoric acid solutions to produce crystalline urea orthophosphate are listed in Table XIX. Values for the integral enthalpy of solution at saturation of urea in 75% H<sub>3</sub>PO<sub>4</sub> from Table XIII were combined with the corresponding values from Table XIX for the same acid and are illustrated in Figure 2.

#### **Densities and Heat Capacities** in System CO(NH<sub>2</sub>)<sub>2</sub>-H<sub>3</sub>PO<sub>4</sub>-H<sub>2</sub>O at 25°C

Second-degree equations in weight percent urea and weight percent phosphoric acid were fitted to the observed values of heat capacity, s, and density, d, for the solutions listed in Tables II, IV, VI, VIII, X, and XII.

$$s = 1.000 - 0.00787P - 0.00580U + 0.0000138P^2 + 0.000082U^2 + 0.0000491PU$$
(28)  
$$d = 1.001 + 0.00470P + 0.00279U + 0.00278U + 0.0$$

$$0.0000381P^2 - 0.0000056U^2 + 0.0000400PU$$
 (29)

where s = heat capacity, cal °C<sup>-1</sup> g<sup>-1</sup> of solution; d = density, g ml<sup>-1;</sup> P = weight percent H<sub>3</sub>PO<sub>4</sub>; and U = weight percent urea. The standard deviation of Equation 28 is 0.002 cal  $^{\circ}C^{-1}g^{-1}$  of solution, and that of Equation 29 is 0.001 g ml<sup>-1</sup>. Heat capacities at even values of P and U are shown in Table XX. Densities at even values of P and U are shown in Table XXI.

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