

Corrections

Vapor-Liquid Equilibrium Data for Binary Systems of Chlorobenzene with Acetone, Acetonitrile, Ethyl Acetate, Ethylbenzene, Methanol, and 1-Pentene. Patrick J. Maher and Buford D. Smith,* *J. Chem. Eng. Data* **1979**, *24*, 363.

Vapor-Liquid Equilibrium Data for Binary Systems of Aniline with Acetone, Acetonitrile, Chlorobenzene, Methanol, and 1-Pentene. Patrick J. Maher and Buford D. Smith,* *J. Chem. Eng. Data* **1980**, *25*, 61.

Vapor-Liquid Equilibrium for the Binary Systems Propionitrile + Ethylbenzene and Acetonitrile + Ethyl Acetate, + Ethyl Alcohol, and + Toluene. Ol Muthu, Patrick J. Maher, and Buford D. Smith,* *J. Chem. Eng. Data* **1980**, *25*, 163.

In all three papers, the "combined correction term" is defined correctly but, due to an error in the computer program used to tabulate the tables, the numbers listed in all the tables as the "combined correction term" are actually the reciprocal of that term.

In the second paper by Maher and Smith (*J. Chem. Eng. Data* **1980**, *25*, 61) Table XVI is incorrect and must be replaced with the following version:

Table XVI. Calculated Data for the Chlorobenzene (1) + Aniline (2) System at 393.15 K^a

| x_1 | total press., kPa | | mixture fugacity coeff | | y_1 | activity coeff | | G^E , J/mol |
|--------|-------------------|--------|------------------------|--------|--------|----------------|--------|---------------|
| | exptl | calcd | 1 | 2 | | 1 | 2 | |
| 0.0000 | 13.260 | 13.260 | 0.9951 | 0.9919 | 0.0000 | 1.9047 | 1.0000 | 0.00 |
| 0.1000 | 23.617 | 23.617 | 0.9907 | 0.9858 | 0.4872 | 1.6113 | 1.0083 | 180.15 |
| 0.2000 | 31.739 | 31.739 | 0.9873 | 0.9811 | 0.6526 | 1.4450 | 1.0276 | 311.77 |
| 0.3000 | 38.609 | 38.608 | 0.9845 | 0.9772 | 0.7419 | 1.3281 | 1.0568 | 404.63 |
| 0.4000 | 44.511 | 44.510 | 0.9821 | 0.9738 | 0.7996 | 1.2344 | 1.0993 | 461.09 |
| 0.5000 | 49.682 | 49.681 | 0.9800 | 0.9709 | 0.8419 | 1.1577 | 1.1585 | 479.88 |
| 0.6000 | 54.533 | 54.532 | 0.9780 | 0.9682 | 0.8771 | 1.1008 | 1.2320 | 461.26 |
| 0.7000 | 59.179 | 59.178 | 0.9761 | 0.9656 | 0.9083 | 1.0582 | 1.3260 | 406.16 |
| 0.8000 | 63.706 | 63.705 | 0.9743 | 0.9630 | 0.9377 | 1.0269 | 1.4513 | 312.91 |
| 0.9000 | 68.336 | 68.336 | 0.9724 | 0.9605 | 0.9677 | 1.0084 | 1.6084 | 179.92 |
| 1.0000 | 73.021 | 73.021 | 0.9705 | 0.9579 | 1.0000 | 1.0000 | 1.9937 | 0.00 |

^a Liquid molar volumes (cm³/mol): $V_1^L = 125.343$, $V_2^L = 109.245$. Virial coefficients (cm³/mol): $B_{11} = -1318.7$, $B_{12} = -1602.6$, $B_{22} = -1988.9$.