

m mixture quantity

Superscripts

ID ideal mixture
 ri reference fluid *i*

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Physical Behavior of Some Reaction Media. Density, Viscosity, Dielectric Constant, and Refractive Index Changes of Ethanol-Cyclohexane Mixtures at Several Temperatures

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Viscosities, densities, dielectric constants, and refractive indexes were determined for ethanol-cyclohexane mixtures at 15, 20, 25, 30, 35 °C and over the whole composition range. These properties are represented by means of empirical relations wherein the composition and temperature effects are involved. These equations fit the experimental data with an uncertainty of the same order of magnitude with the corresponding experimental error. The analysis of data evidences the occurrence of changes in the self-association of ethanol with changing composition.

Introduction

This paper is a part of continuing research on the kinetics of S_N2 reactions between ions and dipolar molecules in solvents where the ionic reactant associates to form ion pairs (1-4). In previous papers we studied the kinetics of the reaction of sodium ethoxide and methyl iodide in ethanol-dioxane solvent systems (3), where the mixture of two organic solvents, in various proportions, enabled us to change the physical properties of the reaction media. In these investigations, in agreement with analogous literature data (5), we observed that the corresponding reactions are markedly accelerated as the dielectric constant of the medium is progressively decreased. This effect has been explained by assuming that the nonelectrostatic solute-solvent interactions are more important than the electrostatic ones. Thus, we assumed that the reactant-solvating ability of the medium is changed by the formation of a polar complex between dioxane and ethanol; the formation of such a complex has been detected in previous investigations (6).

In an attempt to supply further evidence for this assumption, we decided to extend our kinetic studies to binary ethanol-cyclohexane solvent systems, where the possibility of formation of polar associates through hydrogen bonds does not exist.

However, one problem, generally encountered in such studies, is to correlate reaction rate data with the physical properties of the corresponding media. It should be noted that, among

the many intensive physical properties of liquids, the dielectric constant (ϵ), the viscosity (η), and the index of refraction (n) remain the common solvent parameters used to interpret medium effects upon mechanisms of reactions for polar and ionic species, as well as upon electrochemical data and ionic equilibria (7-9).

Although extensive tabulation of values of these properties for pure solvents are generally available, literature data for various binary solvent systems are often incomplete and may be reported only as empirical graphs.

This situation has encouraged us to make a series of systematic measurements of density, viscosity, dielectric constant, and refractive index of ethanol-cyclohexane mixtures over the whole composition range and temperatures from 15 to 35 °C. An attempt has been made to express these properties by means of single equations, wherein the temperature and composition effects are involved. Some physical properties of the above-mentioned binary mixtures have been previously reported in the literature (10-14). However, these studies have been made at very different composition or temperature ranges than those used in our kinetic experiments.

Experimental Section

Reagents. Absolute ethanol (Fluka, p.a.) was further purified according to a recommended method (15).

Cyclohexane (Merck GR > 99.5%, bp = 80.7°/760 mmHg) was refluxed and then fractionally redistilled. In all distillations only the middle fraction coming over at the reported boiling point and comprising about 75% was retained. Pure-component physical properties were measured and compared to average literature data to assure that there were no significant effects due to impurities (Table I). Mixtures were gravimetrically prepared on a Mettler analytical balance just before their use. The probable error in the cyclohexane mole fraction X_2 is estimated to be less than 0.0001.

Measurements. The apparatus and procedure for the experimental measurements of density, viscosity, and dielectric constant were identical with those described previously (6).

Refractive index measurements were carried out by means of a thermostated Abbe refractometer (Jena). Values were

Table I. Physical Properties of Pure Components

temp, °C	ρ , g cm ⁻³		η , cP		ϵ		n_D	
	exptl	lit.	exptl	lit.	exptl	lit.	exptl	lit.
Ethanol								
15	0.793 69	0.793 63 (16)	1.3182		26.24		1.3636	1.3633 (28)
20	0.789 22	0.789 40 (16)	1.2050		25.41		1.3616	1.3614 (16)
25	0.785 07	0.785 (13, 14, 17, 18)	1.0856	1.087 (13, 14)	24.55	24.42 (26, 27)	1.3597	1.3595 (16)
30	0.780 76	0.780 79 (19)	0.9892	0.991 (25)	23.80	23.80 (27)	1.3577	
35	0.776 81	0.776 5 (13)	0.9061	0.908 (13)	23.06		1.3557	
Cyclohexane								
15	0.782 84	0.783 1 (20, 21, 16)	1.0626	1.056 (16)	2.028		1.4285	1.4289 (16)
20	0.778 36	0.778 4 (22, 23)	0.9781	0.980 (17)	2.023	2.023 (26)	1.4261	1.42623 (23)
25	0.773 62	0.773 7 (14, 23)	0.8942	0.890 (13, 14)	2.015	2.015 (26)	1.4234	1.42354 (23)
30	0.768 79	0.769 14 (24)	0.8226	0.820 (16)	2.006		1.4206	
35	0.764 01	0.764 5 (13)	0.7592	0.757 (13, 16)	1.999		1.4180	

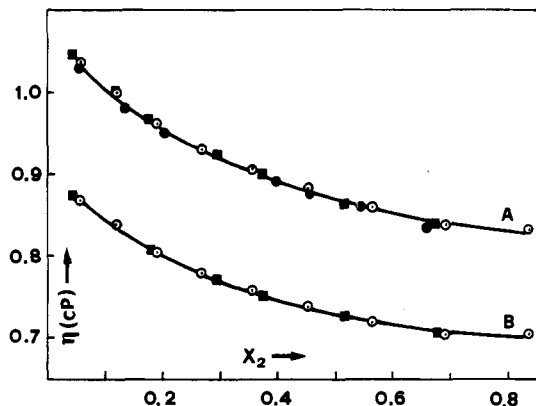


Figure 1. Variation of η (cP) with mole fraction X_2 of cyclohexane for the ethanol-cyclohexane system at (A) 25 °C and (B) 35 °C: (■) data from ref 13; (●) data from ref 14; (○) data of this investigation.

obtained for the sodium D line, with an error of less than 0.0001 unit.

Experiments were generally performed at least in five replicates for each composition, and the results were averaged.

Results and Discussion

The experimental density, viscosity, dielectric constant, and refractive index data at 15, 20, 25, 30, and 35 °C for the ethanol-cyclohexane solvent mixtures are listed in Table II. Only viscosity data of ethanol-cyclohexane mixtures covering the whole composition range at 25 and 35 °C have, to our knowledge, been previously reported (13, 14). These literature data are reported and compared to our values in Figure 1; the agreement is excellent.

Densities. As in the case of the ethanol-dioxane mixtures (6), the polynomial equation

$$\frac{1}{\rho} = \sum_{i=0}^n d_i X_2^i \quad (1)$$

was fitted at each temperature by a least-squares technique. On the basis of careful examination of the results of the fitting and taking into account that as the degree n of the polynomial is increased, the amount of smoothing is decreased, it was decided that the optimum degree n was equal to 4, namely much less than the number of data points. This degree minimizes the standard deviation σ defined by the following equation (29):

$$\sigma = \left[\frac{\sum_i \left(\frac{1}{\rho} \right)_i^{\text{exp}} - \left(\frac{1}{\rho} \right)_i^{\text{est}}{}^2}{N - n - 1} \right]^{1/2} \quad (2)$$

where $(1/\rho)_i^{\text{exp}}$ and $(1/\rho)_i^{\text{est}}$ indicate the experimental and estimated, from regression eq 1, values of $1/\rho$. N is the number

Table II. Experimental Density (ρ), Viscosity (η), Dielectric Constant (ϵ), and Refractive Index (n_D) Data for Ethanol-Cyclohexane Mixtures at 15, 20, 25, 30, and 35 °C

X_2	15 °C	20 °C	25 °C	30 °C	35 °C
ρ , g/cm ³					
0.0565	0.790 37	0.786 26	0.781 94	0.777 70	0.773 40
0.1188	0.787 97	0.783 81	0.779 40	0.775 12	0.770 74
0.1894	0.785 76	0.781 53	0.776 98	0.772 79	0.768 10
0.2674	0.783 83	0.779 81	0.775 29	0.770 84	0.766 13
0.3539	0.782 73	0.778 26	0.773 96	0.769 31	0.764 58
0.4506	0.781 85	0.777 36	0.772 74	0.768 12	0.763 45
0.5626	0.781 30	0.776 68	0.772 22	0.767 30	0.762 53
0.6898	0.781 27	0.776 54	0.771 75	0.766 87	0.761 99
0.8348	0.781 12	0.776 53	0.771 85	0.767 03	0.762 16
η , cP					
0.0565	1.2475	1.1427	1.0369	0.9470	0.8683
0.1188	1.2000	1.0977	0.9995	0.9133	0.8383
0.1894	1.1524	1.0535	0.9602	0.8784	0.8039
0.2674	1.1166	1.0275	0.9303	0.8522	0.7793
0.3539	1.0889	0.9953	0.9067	0.8288	0.7578
0.4506	1.0602	0.9698	0.8821	0.8084	0.7384
0.5626	1.0351	0.9436	0.8589	0.7860	0.7191
0.6898	1.0095	0.9184	0.8388	0.7655	0.7052
0.8348	1.0016	0.9099	0.8319	0.7647	0.7051
ϵ					
0.0565	23.757	22.843	22.204	21.475	20.835
0.1188	21.014	20.329	19.719	19.084	18.584
0.1894	18.263	17.629	17.100	16.524	16.048
0.2674	15.429	14.882	14.423	13.917	13.529
0.3539	12.560	12.062	11.708	11.280	10.977
0.4506	9.693	9.301	8.999	8.704	8.428
0.5626	6.786	6.548	6.344	6.104	5.916
0.6898	4.277	4.180	4.062	3.959	3.867
0.8348	2.619	2.599	2.579	2.556	2.537
n_D					
0.0565	1.3682	1.3660	1.3635	1.3613	1.3590
0.1188	1.3740	1.3712	1.3691	1.3664	1.3636
0.1894	1.3798	1.3772	1.3738	1.3722	1.3687
0.2674	1.3859	1.3832	1.3806	1.3780	1.3747
0.3539	1.3921	1.3893	1.3869	1.3844	1.3821
0.4506	1.3985	1.3964	1.3937	1.3913	1.3886
0.5626	1.4062	1.4036	1.4011	1.3986	1.3960
0.6898	1.4138	1.4116	1.4091	1.4061	1.4038
0.8348	1.4213	1.4194	1.4167	1.4142	1.4117

of experimental data. The values of the adjustable coefficients d_i are summarized in Table III along with the standard deviation σ .

The effect of temperature on the density of the mixtures was examined by assuming the validity of the following equation (27):

$$\rho = \rho_0 - BT \quad (3)$$

Calculated density data, by means of eq 1, were used in the plots of ρ vs T . The mole fraction X_2 was kept as a constant parameter. For each composition and over the temperature range studied, straight lines were obtained ($R^2 > 0.9997$). The

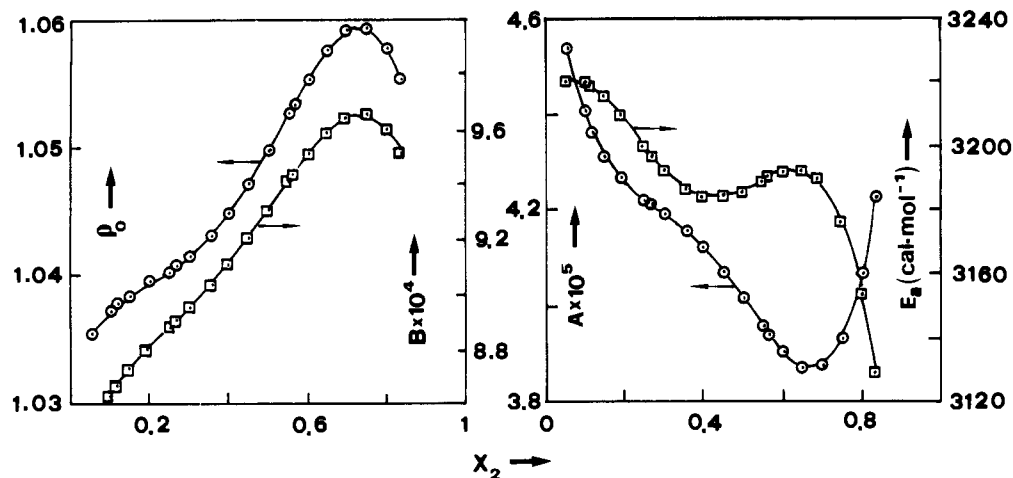


Figure 2. Variation of the constants ρ_0 , B (eq 3) and A , E_v (eq 11) with mole fraction X_2 of cyclohexane.

Table III. Coefficients and Standard Deviations σ for Representation of $1/\rho$, $[R]$, ϵ , and n_D of Ethanol-Cyclohexane Mixtures by Equations 1, 9, 17, and 24

	15 °C	20 °C	25 °C	30 °C	35 °C
Equation 1					
d_0	1.260 65	1.267 48	1.273 96	1.281 01	1.287 45
$10^2 d_1$	8.752 56	8.394 53	9.573 49	9.266 02	10.725 2
$-10^2 d_2$	1.423 97	1.227 03	1.735 60	1.482 49	1.996 29
$10^2 d_3$	9.564 58	7.265 88	15.959 7	12.149 6	19.800 6
$-10^2 d_4$	2.043 55	1.347 66	6.215 34	4.535 42	8.431 55
σ	1.44×10^{-4}	1.01×10^{-4}	1.67×10^{-4}	1.72×10^{-5}	1.31×10^{-4}
Equation 9					
R_0	33.7721	33.5898	33.3648	33.1599	32.9732
R_1	26.6902	26.5203	26.4337	26.3836	26.3442
σ	0.022	0.027	0.019	0.026	0.023
Equation 17					
D_0	26.5213	25.2526	24.6268	23.8057	23.0422
$-D_1$	52.0096	43.6174	44.4248	42.4406	39.7009
D_2	59.0154	18.0732	29.4408	23.7134	15.857
$-D_3$	98.8860	1.1087	31.4684	17.2026	3.7800
D_4	106.0846	2.0386	37.0794	21.1404	11.0857
$-D_5$	38.4892	-2.0180	12.7764	6.4230	3.9386
σ	0.018	0.013	0.010	0.024	0.037
Equation 24					
D_0'	1.36224	1.36093	1.35905	1.35617	1.35597
$10^2 D_1'$	11.2587	9.04755	8.01586	9.45031	4.60492
$10^2 D_2'$	-13.9006	-2.27563	1.74911	-8.51751	18.1499
$10^2 D_3'$	22.3897	-3.86612	-9.98956	20.5886	-42.6019
$10 D_4'$	-1.80140	0.905841	1.28391	-2.79601	4.08479
$10^2 D_5'$	4.72971	-5.59917	-6.33486	13.4452	-14.7314
σ	1.4×10^{-4}	1.8×10^{-4}	4.1×10^{-4}	9.4×10^{-5}	3.3×10^{-4}

corresponding constants ρ_0 and B were calculated by the least-squares method. The obtained results are graphically represented in Figure 2. On the basis of these data, the following relations were derived:

$$\rho_0 = \sum_{i=0}^7 C_i X_2^i = 1.03192 + 0.08218X_2 - 0.36871X_2^2 + 0.87062X_2^3 - 0.71997X_2^4 + 0.22572X_2^5 - 0.13718X_2^6 + 0.03460X_2^7 \quad (4)$$

$$\sigma_{\rho_0} = 1.69 \times 10^{-7}$$

$$10^4 B = \sum_{i=0}^7 B_i X_2^i = 8.28438 + 4.68475X_2 - 15.7523X_2^2 + 32.3426X_2^3 - 25.8577X_2^4 + 8.30678X_2^5 - 4.98327X_2^6 + 1.24761X_2^7 \quad (5)$$

$$\sigma_B = 5.5 \times 10^{-10}$$

It follows that the equation relating the density to the temperature, T , and the mole fraction of cyclohexane, X_2 , is

$$\rho = \left(\sum_{i=0}^7 C_i X_2^i \right) - \left(\sum_{i=0}^7 B_i X_2^i \right) T \quad (6)$$

This equation fits the experimental data over the specified range of temperatures (15–35 °C) and compositions ($0.07 < X_2 < 0.85$) with an uncertainty of 8.2×10^{-5} , which is of the same order of magnitude with the experimental error.

Viscosities. In order to express the viscosity as a function of X_2 , the rheochor $[R]$ (δ) for various mixtures was calculated from the following equation:

$$[R] = \frac{\bar{M}}{\rho} \eta^{1/8} \quad (7)$$

where

$$\bar{M} = (1 - X_2)M_1 + X_2M_2 \quad (8)$$

M_1 and M_2 being the molecular weights of ethanol and cyclohexane, respectively.

It should be noted that, because of the form of eq 7, even small errors in the experimental values of ρ cause large errors in $[R]$. To avoid these errors, smoothed values of ρ , calculated from eq 1, were substituted in eq 7.

In all temperatures studied, it was found that the plots of $[R]$ vs X_2 are fairly linear ($R^2 > 0.99998$) of the general form:

$$[R] = R_0 + R_1 X_2 \quad (9)$$

whose coefficient R_0 and R_1 are listed in Table III.

By combining eqs 1, 7, and 9, one obtains the following rational function (i.e., the ratio of two polynomials):

$$\eta^{1/8} = \frac{1}{\bar{M}} \frac{R_0 + R_1 X_2}{d_0 + d_1 X_2 + d_2 X_2^2 + \dots + d_4 X_2^4} \quad (10)$$

As previously (δ), it was found in this investigation that, in all cases, eq 10 represents much better the reported data than a simple polynomial. The average deviation of the calculated values from the experimental ones, always less than $\pm 0.25\%$ (approximate experimental accuracy), shows that eq 10 closely represents the experimental viscosity data. A comparison of experimental and calculated η data is presented in Figure 3.

The effect of temperature on the viscosity of the mixtures was examined by assuming the validity of the following equation, first pointed out by Guzman (30):

$$\eta = A \exp\left(\frac{E_v}{RT}\right) \quad (11)$$

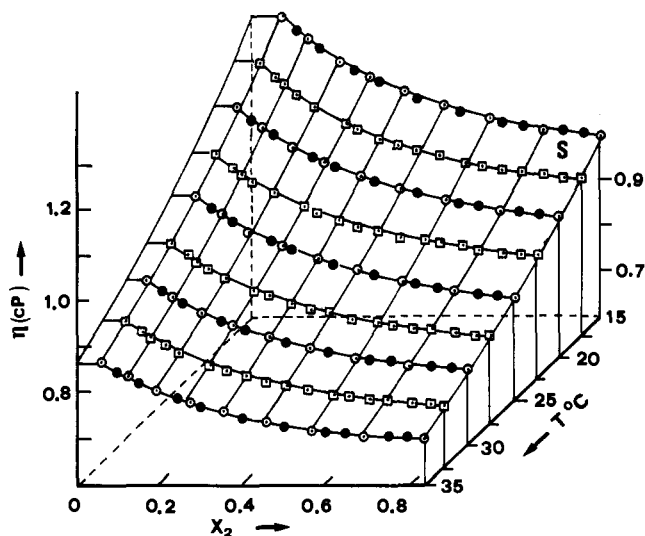


Figure 3. Variation of η (cP) with mole fraction X_2 and temperature T (°C): (○) experimental values; (●) calculated from eq 10 values; (◻) calculated from eq 14 values.

where A is a constant and E_V is the energy barrier that must be overcome before the elementary flow can occur. The term $\exp(E_V/RT)$ can then be interpreted as a Boltzmann factor, giving the fraction of the molecules having the requisite energy to surmount the barrier. Thus, E_V is an activation energy of viscous flow.

Smoothed viscosity data, calculated by means of eq 10, were used in plots of $\ln \eta$ vs $1/T$. Straight lines were obtained for each composition ($R^2 > 0.9992$). The corresponding constants A and E_V were calculated by the least-squares method. The obtained results are graphically presented in Figure 2. The following relations were obtained:

$$10^5 A = \sum_{i=0}^7 A_i X_2^i = 4.8127 - 6.0682X_2 + 24.0534X_2^2 - 41.3531X_2^3 + 7.3541X_2^4 + 54.4976X_2^5 - 61.4387X_2^6 + 24.4315X_2^7 \quad (12)$$

$$\sigma_A = 2.8 \times 10^{-9}$$

$$E_V = \sum_{i=0}^7 E_i X_2^i = 3210.301 + 291.191X_2 - 2431.58X_2^2 + 5296.57X_2^3 - 3779.91X_2^4 + 531.597X_2^5 - 338.593X_2^6 + 84.5555X_2^7 \quad (13)$$

$$\sigma_{E_V} = 4.37 \times 10^{-3}$$

Consequently, the following equation expresses η as a function of X_2 and T :

$$\eta = \left(\sum_{i=0}^7 A_i X_2^i \right) \exp \left(\frac{\sum_{i=0}^7 E_i X_2^i}{RT} \right) \quad (14)$$

Equation 14 explicitly represents the surface S in Figure 3. This equation predicts the experimental data with an overall uncertainty of ± 0.0021 cP.

The molar quantity E_V is known to be sensitive to molar associations (30–32). If the mixtures studied behave ideally, this quantity could be calculated for each composition by applying the additivity rule

$$E_V^M = (1 - X_2)E_1 + X_2E_2 \quad (15)$$

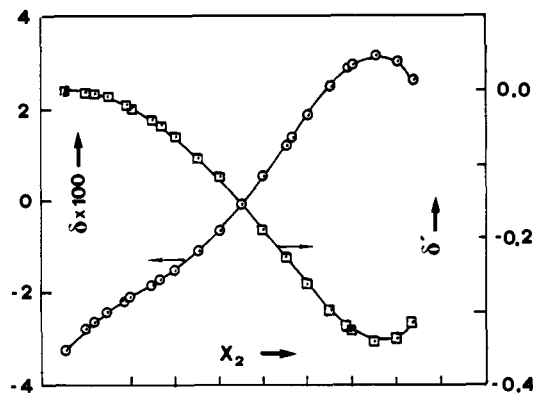


Figure 4. Variation of δ (eq 16) and δ' (eq 19, 35 °C) with mole fraction X_2 of cyclohexane.

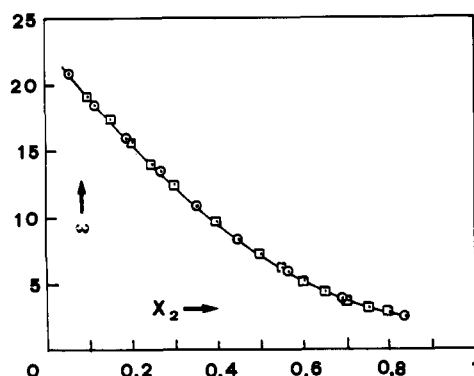


Figure 5. Variation of experimental (○) and calculated (◻) dielectric constants with mole fraction X_2 of cyclohexane for the ethanol-cyclohexane system at 35 °C.

E_1 and E_2 being the activation energies of pure ethanol and cyclohexane, respectively.

So, the values of the parameter

$$\delta = \frac{E_V - E_V^M}{E_V^M} = \frac{E_V^E}{E_V^M} \quad (16)$$

give an adequate approach to estimate molar associations. It was found that the maximum values of δ occurs at $X_2 \approx 0.75$ (Figure 4).

However, it has been well-known, for a long time, that alcohols in solutions in nonpolar solvents associate by means of hydrogen bonds into a series of n -mers (10–13, 33–41). In very dilute solutions the predominant species are the unassociated (monomeric) molecules, while in more concentrated solutions both linear (acyclic) and (cyclic) n -mers coexist. Finally, at concentrated solutions of alcohols only linear n -mers can be considered. On the other hand, Huyskens et al. showed that in solutions around the composition $X_2 \approx 0.8$ the predominant hydrogen-bonded species of ethanol in cyclohexane is the cyclic trimer (13). It has been also postulated in this investigation that the cyclic species present greater viscosity than the linear ones.

Consequently, taking into account all these assumptions, we could attribute the observed values of δ to all these effects.

Dielectric Constants. The smoothing function

$$\epsilon = \sum_{i=0}^n D_i X_2^i \quad (17)$$

was fitted at each temperature by the least-squares method. In this case it was found that the optimum degree n was equal to 5. Values of the coefficients D_i and the corresponding standard deviations σ are summarized in Table III. The results

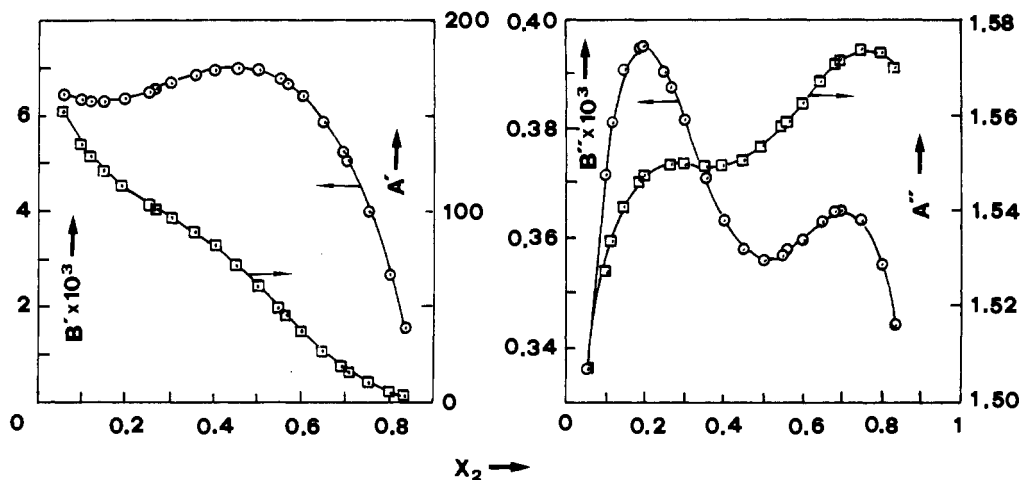


Figure 6. Variation of the constants A' , B' (eq 20) and A'' , B'' (eq 25) with mole fraction X_2 of cyclohexane.

of fitting the data for 35 °C are presented as an example in Figure 5.

In an attempt to study from a different point of view, than was previously studied, the self-association of ethanol, we examined the dielectric constant deviation from ideality. The ideal dielectric constants of the mixtures were calculated by using the Decriocq formula (42) in the most general form:

$$\epsilon^{id} = (1 - Y_2)\epsilon_1 + Y_2\epsilon_2 + 2\left(\frac{1}{\epsilon^{id}} - \frac{(1 - Y_2)}{\epsilon_1} - \frac{Y_2}{\epsilon_2}\right) \quad (18)$$

where ϵ_1 and ϵ_2 are the dielectric constants of pure ethanol and cyclohexane, respectively, and Y_2 is the volume fraction of cyclohexane defined on the partial molar volume basis (43). This quantity has been determined by means of a method described previously (6).

Evidently, the values of the parameter

$$\delta' = \frac{\epsilon - \epsilon^{id}}{\epsilon^{id}} = \frac{\epsilon^E}{\epsilon^{id}} \quad (19)$$

give an adequate approach to estimate molar associations of ethanol.

It was found that ϵ^E values are generally negative, and the corresponding curves $\delta' = f(X_2)$ at each temperature present a pronounced minimum at $X_2 \approx 0.75$ (Figure 4).

A point of interest is that the maximum relative deviations from dielectric ideality occur for all temperatures exactly in the same region of compositions where we observed the maximum value of δ .

At the molecular level, it has been argued that the negative values of ϵ^E for various systems are a consequence of the formation of polar associates of lower dipole moment (36, 41, 44, 45). Thus, it has been postulated that, in pure alcohols or in concentrated solutions of these substances in nonpolar liquids, the formed linear n -mers present a higher dipole moment. This behavior has been attributed to the fact that the O-H bond moment of these aggregates is increased through mutual induction. However, when the nonpolar solvent is added, these associates are broken up and the resulting hydrogen-bonded species have a lower dipole moment. On the other hand, Huyskens et al. (34) showed that in solutions of some alcohols in hexane and cyclohexane the calculated apparent dipole moment of the corresponding alcohols changes with changing composition and passes through a minimum at $X_2 \approx 0.8$. This behavior has been attributed to the formation of nonpolar cyclic trimers.

Consequently, taking into account all these assumptions, we could attribute the observed deviations from dielectric ideality to all these effects.

The variation of dielectric constant with temperature was studied by means of the following equation (6, 26):

$$\epsilon = A' \exp(-B'T) \quad (20)$$

A similar form of calculation, as described before, was applied. The obtained results are represented in Figure 6. The following equations were obtained:

$$10^{-2}A' = \sum_{i=0}^7 \alpha_i X_2^i = 1.8518 - 7.2757X_2 + 27.8283X_2^2 - 61.5843X_2^3 + 75.8432X_2^4 - 82.5097X_2^5 + 79.8437X_2^6 - 34.3610X_2^7 \quad (21)$$

$$\sigma_{A'} = 0.06$$

$$10^3B' = \sum_{i=0}^7 \beta_i X_2^i = 6.7795 - 7.4941X_2 + 28.343X_2^2 + 33.272X_2^3 - 283.82X_2^4 + 539.52X_2^5 - 506.04X_2^6 + 185.13X_2^7 \quad (22)$$

$$\sigma_{B'} = 8.52 \times 10^{-4}$$

By combining equations 20, 21, and 22, it follows that

$$\epsilon = \left(\sum_{i=0}^7 \alpha_i X_2^i\right) \exp\left(-T \sum_{i=0}^7 \beta_i X_2^i\right) \quad (23)$$

This equation predicts the experimental data with an overall uncertainty of ± 0.025 unit, which is about equal to the experimental error.

Refractive Indexes. The coefficients of the smoothing function

$$n_D = \sum_{i=0}^5 D_i' X_2^i \quad (24)$$

calculated by the least-squares method are listed in Table III.

The effect of temperature on n_D was studied by using the following equation (6):

$$n_D = A'' \exp(-B''T) \quad (25)$$

In all cases it was found that the graphs in n_D vs T were linear ($R^2 > 0.998$). The obtained values of A'' and B'' for

various compositions are graphically shown in Figure 6. The corresponding curves were fitted to the following polynomials:

$$A'' = \sum_{i=0}^7 \alpha_i' X_2^i = 1.465590 + 0.931896X_2 - 3.740238X_2^2 + 6.384525X_2^3 - 3.689626X_2^4 - 1.106555X_2^5 + 1.814415X_2^6 - 5.488909X_2^7 \quad (26)$$

$$\sigma_{A''} = 8.4 \times 10^{-6}$$

$$10^3 B'' = \sum_{i=0}^7 \beta_i' X_2^i = 0.2546 + 1.8833X_2 - 8.6274X_2^2 + 16.068X_2^3 - 12.897X_2^4 + 3.7810X_2^5 - 0.27621X_2^6 - 0.0212X_2^7 \quad (27)$$

$$\sigma_{B''} = 1.5 \times 10^{-6}$$

The equation

$$n_D = \left(\sum_{i=0}^7 \alpha_i' X_2^i \right) \exp\left(-T \sum_{i=0}^7 \beta_i' X_2^i\right) \quad (28)$$

fits the experimental data over the specified range of temperatures and compositions with an uncertainty of ± 0.0001 unit, which is about equal to the experimental error.

Glossary

ρ	density of the mixture, g cm ⁻³
η	viscosity of the mixture, cP
δ	relative excess activation energy of viscous flow of the mixture
ϵ	dielectric constant of the mixture
ϵ_1, ϵ_2	dielectric constants of ethanol and cyclohexane, respectively
ϵ^E	excess dielectric constant of the mixture
ϵ^id	ideal dielectric constant of the mixture
δ'	relative excess dielectric constant of the mixture
n_D	refractive index of the mixture for sodium D line
T	absolute temperature
$[R]$	rheochor of the mixture defined by eq 7
X_2	mole fraction of cyclohexane
Y_2	partial volume fraction of cyclohexane
ρ_0, B	constants in eq 3
M	apparent molecular weight of the mixture
A	constant in eq 11
E_v	activation energy of viscous flow
A', B'	constants in eq 20
A'', B''	constants in eq 25
$d_0 \dots d_4$	coefficient in eq 1
R_0, R_1	coefficient in eq 9
$D_0 \dots D_5$	coefficient in eq 17
$D_0' \dots D_5'$	coefficient in eq 24

Registry No. Ethanol, 64-17-5; cyclohexane, 110-82-7.

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