

H <sub>2</sub> O	water
<i>k</i>	Boltzmann's constant
<i>m</i>	number of components in the mixture
MEA	ethanolamine
<i>p</i>	pressure
<i>R</i>	universal gas constant ( $R = 8.3143 \text{ J mol}^{-1} \text{ K}^{-1}$ )
<i>T</i>	temperature
<i>v</i>	molar volume
<i>V</i>	volume
<i>x</i>	mole fraction in liquid phase
<i>y</i>	mole fraction in vapor phase

#### Greek Symbols

$\alpha_i$	polarizability of component <i>i</i>
$\gamma_{i,j}$	activity coefficient for component <i>i</i> dissolved in component <i>j</i>
$\epsilon$	Lennard-Jones energy parameter
$\eta_0, \eta_1,$ $\eta_2, \eta_3$	reduced densities
$\mu$	chemical potential, dipole moment
$\rho$	molar density
$\rho^*$	number density
$\sigma$	Lennard-Jones distance parameter
$\varphi$	fugacity coefficient
$\phi$	volume fraction in liquid phase

#### Subscripts

<i>c</i>	critical value
<i>ij</i>	binary interactions or attractive property between molecules of species <i>i</i> and <i>j</i>
<i>j</i>	component <i>j</i>
H <sub>2</sub>	hydrogen
mix	mixture
pot.	value resulting from intermolecular forces
<i>v</i>	repulsive property

#### Superscripts

exp	experimental value
s	saturated
spt	value calculated from the scaled particle theory
$\infty$	value at infinite dilution
'	liquid phase
"	vapor phase
*	referred to number of particles, reduced
~	solite free
$\ominus$	standard value ( $p^\ominus = 0.1 \text{ MPa}$ )

Registry No. H<sub>2</sub>, 1333-74-0; ethanolamine, 141-43-5.

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## Ultrasonic Speed for Liquid Trichlorofluoromethane and 1,1-Dichloro-2,2,2-trifluoroethane at Temperatures from 283 to 373 K and Pressures up to 75 MPa

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The ultrasonic speeds for liquid trichlorofluoromethane (CCl<sub>3</sub>F) and 1,1-dichloro-2,2,2-trifluoroethane (C<sub>2</sub>HCl<sub>2</sub>F<sub>3</sub>) were measured from 283 to 373 K and from 0.1 MPa or their saturated vapor pressure to about 75 MPa. The measurements were carried out by a ring-around technique operated at a frequency of 2 MHz with the uncertainty of  $\pm 0.2\%$ . The temperature and pressure variation of ultrasonic speed and related properties are discussed.

### Introduction

Trichlorofluoromethane, CCl<sub>3</sub>F (CFC-11), has a high solubility for polymers and is usually used as a solvent in the foam and textile industries. Due to its ability to destroy ozone, its use as a foaming agent and refrigerant is being curtailed. 1,1-Dichloro-2,2,2-trifluoroethane, C<sub>2</sub>HCl<sub>2</sub>F<sub>3</sub> (HCFC-123), is considered

a suitable replacement compound of CCl<sub>3</sub>F (1).

Ultrasonic speeds in fluids, which travel with the compression waves, give a powerful clue for elucidating the thermodynamic properties. In previous papers (2-4), we have been reported the ultrasonic speed of liquid refrigerants at several conditions of temperature and pressure. This paper describes the new experimental results of ultrasonic speeds in the liquid phase of CCl<sub>3</sub>F and C<sub>2</sub>HCl<sub>2</sub>F<sub>3</sub>. The variation of the ultrasonic speed and related thermodynamic properties for these fluids as a function of temperature and pressure are discussed and compared with related properties of tetrachloromethane, CCl<sub>4</sub>.

### Experimental Section

**Materials.** Trichlorofluoromethane, CCl<sub>3</sub>F, and 1,1-dichloro-2,2,2-trifluoroethane, C<sub>2</sub>HCl<sub>2</sub>F<sub>3</sub>, were supplied by Daikin Industrials Ltd. Their purities were better than 99.8 wt %, as measured by GLC. Tetrachloromethane, CCl<sub>4</sub>, was a "spectral grade" reagent supplied by Dojin Chemical Ltd.; its purity, de-

Table I. Physical Properties for Each Compound

compound	CCl <sub>4</sub>	CCl <sub>3</sub> F	C <sub>2</sub> HCl <sub>2</sub> F <sub>3</sub>
molecular wt	153.82	137.37	152.93
melting temp/K	250.20	162.15	166.15
boiling temp/K	349.90	296.90	300.15
critical constants <sup>a</sup>			
<i>T<sub>c</sub></i> /K	556.4	471.20	456.85
<i>p<sub>c</sub></i> /MPa	4.56	4.41	3.67
<i>ρ<sub>c</sub></i> /(kg·m <sup>-3</sup> )	558	554	550
dipole moment/(10 <sup>-30</sup> C·m)	0	0.45 <sup>b</sup>	0.8 <sup>c</sup>

<sup>a</sup> Reference 5 for CCl<sub>4</sub> and CCl<sub>3</sub>F; reference 1 for C<sub>2</sub>HCl<sub>2</sub>F<sub>3</sub>.

<sup>b</sup> Reference 6. <sup>c</sup> Estimated by Debye equation (6) using dielectric constant at different temperatures (7).

terminated by GLC, was better than 99.99 mass %. The physical properties of each substance are listed in Table I.

**Apparatus.** The method used for measurement of ultrasonic speed was a ring-around technique employing a fixed-path ultrasonic interferometer, similar to that described previously (2, 8). An acoustic interferometer placed in the high-pressure vessel was immersed in an ethylene glycol bath controlled to within ±0.02 K between 283 and 333 K and to ±0.03 K between 343 and 373 K. The temperature in the bath was measured by a quartz thermometer with a resolution of ±0.001 K. To reduce the temperature variation in the sample caused by the pressure change, the difference in temperature between sample chamber and bath was observed by a T-type thermocouple. The pressure was generated by a hand-operated oil pump and was transmitted to the sample through the moving of a piston, sealed by a Teflon-coated O-ring, in a piston cylinder. The pressure was measured by two strain gauges with ranges of 10 and 100 MPa to within ±0.03 and ±0.08 MPa, respectively.

The ultrasonic speed, *u*, was obtained by measuring the repeat period, *t*, of a short acoustic pulse traveling over the known distance, *L*, between the transducer and reflector. In this work, a new acoustic interferometer made of stainless steel (SUS304) with *L* = 25 mm was used. The acoustic path length was determined by using the speed of sound in pure tetrachloromethane at 298.15 K and 0.1 MPa (924.3 m·s<sup>-1</sup>) reported by Bobic et al. (9). The variation of *L* resulting from temperature and pressure was calculated from the coefficients of expansion and compression of the metal (10).

As preliminary work, the ultrasonic speed, *u*, in CCl<sub>4</sub> was measured. These results, as given in Table II, agree to within ±0.2% with those measured by Bobic et al. (9). Lainez et al. (11) measured the ultrasonic speed at 298.15 K. Their cell was calibrated by using the value in CCl<sub>4</sub> of 920.3 m·s<sup>-1</sup> at 298.15 K and 0.1 MPa; hence their results will be lower. However, the pressure dependence in *u* is in good agreement with the value presented here and in ref 9. The estimated uncertainty in the ultrasonic speeds is ±0.2%, with greater uncertainty for values at pressure close to the saturated vapor pressure.

## Results and Discussion

The experimental results of the ultrasonic speed, *u*, in the liquid phase of CCl<sub>3</sub>F and C<sub>2</sub>HCl<sub>2</sub>F<sub>3</sub> at pressure, *p*, are listed

Table II. Comparison of the Observed Ultrasonic Speed *u*/(m·s<sup>-1</sup>) in Tetrachloromethane, CCl<sub>4</sub>, and Trichlorofluoromethane, CCl<sub>3</sub>F<sup>a</sup>

<i>p</i> /MPa	CCl <sub>4</sub>						CCl <sub>3</sub> F		
	<i>T</i> /K = 298.15			<i>T</i> /K = 343.15		<i>T</i> /K = 373.15		<i>T</i> /K = 353.15	
	this work	ref 9	ref 11	this work	ref 9	this work	ref 9	this work	ref 15
0.1	924.3	924.3	920.3	786.9	786.3			594.9*	590.2*
20	998.7	998.1	994.8	878.2	877.8	803.4	803.4	692.9	690.5
40	1062.2	1061.7	1058.7	953.1	952.7	886.6	886.9	789.8	787.5
60	1118.2	1116.5	1114.9	1017.0	1017.2	956.4	956.5	867.6	865.3

<sup>a</sup> Values marked with an asterisk were measured at 5 MPa.

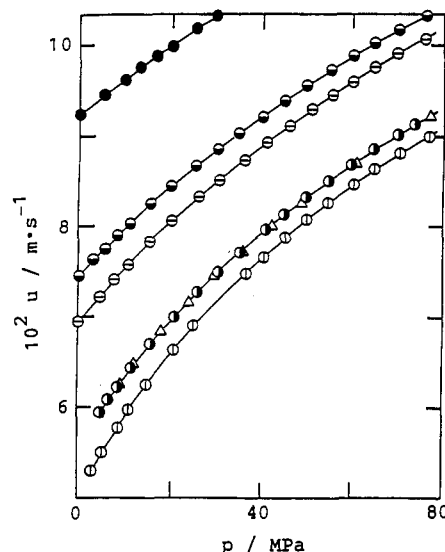


Figure 1. Pressure dependence, *p*, of ultrasonic speed, *u*. CCl<sub>4</sub>: ●, 298.15 K; CCl<sub>3</sub>F: ○, 298.15 K; △, 353.15 K. C<sub>2</sub>HCl<sub>2</sub>F<sub>3</sub>: ○, 298.15 K; ◊, 353.15 K.

in Table III and are shown graphically in Figure 1. The variation in *u* as a function of temperature and pressure can be represented by the polynomial equation

$$u/(m\cdot s^{-1}) = \sum_{j=0}^2 \sum_{i=0}^4 a_{ij}(T/K)(p/MPa)^i \quad (1)$$

The values of the coefficients *a<sub>ij</sub>*, calculated by least-squares analysis of all experimental data, are presented in Table IV. The maximum and standard deviations of the experimental results from this equation are 0.11 and 0.055% for CCl<sub>3</sub>F, and 0.17 and 0.065% for C<sub>2</sub>HCl<sub>2</sub>F<sub>3</sub>, respectively.

The ultrasonic speed in the liquid phase, *u<sub>p</sub>*, at saturation pressure, *p<sub>s</sub>*, was calculated from eq 1. *p<sub>s</sub>* was derived from the equation reported by Downing (12) for CCl<sub>3</sub>F and by Weber (13) for C<sub>2</sub>HCl<sub>2</sub>F<sub>3</sub>. The results are presented in Table III and Figure 2. For C<sub>2</sub>HCl<sub>2</sub>F<sub>3</sub>, these values can be represented by the following equation:

$$u_{p_s}/(m\cdot s^{-1}) = 693.7 - 3.4580t + 3.6659 \times 10^{-4}t^2 + 1.0649 \times 10^{-5}t^3 \quad (2)$$

where *t* = (*T*/K) - 298.15. This equation reproduced the extrapolated values to within a maximum deviation of 0.02%.

These are no previous measurements of the ultrasonic speeds in C<sub>2</sub>HCl<sub>2</sub>F<sub>3</sub>. For CCl<sub>3</sub>F, Chavez et al. (14) obtained the values in the liquid phase along the saturation line from 162 to 458 K by a pulse echo overlap method, given by the dotted line in Figure 2. They give 555.5 m·s<sup>-1</sup> as the ultrasonic speed at 353.15 K and *p<sub>s</sub>*. This value is a little lower than our result: 557.2 m·s<sup>-1</sup>. In the vicinity of the saturation pressure, absorption of the acoustic wave generated in the sample was

**Table III. Ultrasonic Speed,  $u/(m \cdot s^{-1})$ , in the Liquid Phase of Trichlorofluoromethane,  $CCl_3F$ , and 1,1-Dichloro-2,2,2-trifluoroethane,  $C_2HCl_2F_3$ , at Various Pressures,  $p/MPa^a$** 

$p/MPa$	$u/(m \cdot s^{-1})$	$p/MPa$	$u/(m \cdot s^{-1})$	$p/MPa$	$u/(m \cdot s^{-1})$	$p/MPa$	$u/(m \cdot s^{-1})$	$p/MPa$	$u/(m \cdot s^{-1})$	$p/MPa$	$u/(m \cdot s^{-1})$
<b><math>CCl_3F</math></b>											
298.15 K											
0.1056*	743.5*	8.23	786.9	20.32	843.0	35.10	901.9	49.76	953.2	64.83	1000.4
0.132	743.6	11.00	800.4	25.45	864.5	40.27	920.7	55.20	970.8	70.13	1015.9
3.359	761.4	15.66	822.4	30.11	883.0	45.15	937.8	60.31	986.7	74.77	1029.1
5.818	774.5										
313.15 K											
0.1734*	692.4**	8.44	741.1	20.49	801.7	35.24	864.2	50.19	921.3	65.50	968.8
3.202	710.9	11.14	755.7	25.85	825.3	40.71	885.1	55.23	936.1	69.48	980.9
5.725	725.8	15.99	780.3	30.27	843.8	45.95	904.2	60.59	953.4	73.98	994.4
333.15 K											
0.3111*	627.5**	8.78	682.1	20.35	746.6	35.95	817.4	49.87	872.6	64.49	923.3
3.176	645.3	11.01	695.6	25.32	771.2	40.48	836.7	54.95	890.9	69.78	940.2
6.343	666.6	15.59	721.8	30.63	795.3	45.28	855.4	59.79	907.5	74.41	954.6
353.15 K											
0.5192*	557.4**	8.20	619.4	20.89	697.7	35.38	769.6	50.07	830.8	64.94	884.6
4.621	591.7	11.46	641.1	26.01	724.8	40.92	793.8	54.77	848.5	69.91	901.2
6.442	605.7	15.81	668.5	30.55	747.2	44.97	810.7	60.00	867.4	73.86	914.1
<b><math>C_2HCl_2F_3</math></b>											
283.15 K											
0.0506*	745.7**	7.077	785.2	21.00	852.1	36.06	913.6	50.91	966.6	65.69	1014.5
0.1	746.0	9.22	796.5	26.16	874.4	40.86	931.5	55.58	982.3	70.88	1030.1
0.459	748.2	11.77	809.4	31.70	896.7	45.79	949.1	60.76	999.0	75.50	1044.0
4.537	771.6	15.96	829.4								
293.15 K											
0.0756*	711.0**	7.720	756.4	20.36	819.4	35.00	882.0	50.29	938.8	65.30	988.2
0.132	712.1	10.74	722.5	24.85	839.8	40.51	902.9	54.81	954.2	69.00	999.9
4.026	735.5	12.96	784.0	30.03	861.9	45.07	920.2	60.09	971.7	74.01	1015.1
6.816	751.4	15.90	798.6								
298.15 K											
0.0913*	693.7**	7.735	740.1	20.55	806.5	36.01	873.5	51.06	930.0	65.06	977.2
0.464	694.9	10.88	757.7	26.15	832.1	41.08	893.3	55.65	945.9	69.88	992.3
4.553	721.3	15.57	782.2	30.77	852.1	45.75	910.8	60.46	962.1	74.44	1006.2
303.15 K											
0.1094*	676.4**	8.99	731.3	21.45	796.3	36.26	861.2	50.81	916.7	66.12	968.7
0.403	677.3	13.20	754.6	26.31	818.9	40.72	879.0	55.37	932.8	70.82	983.6
6.267	715.2	16.59	772.4	30.87	838.8	45.97	898.9	61.17	952.5	75.59	999.1
313.15 K											
0.1543*	641.9**	7.786	694.2	20.21	763.9	36.09	837.1	50.29	893.1	64.71	943.7
0.172	642.6	11.01	713.7	25.44	789.4	40.10	853.5	55.55	912.2	70.22	961.7
3.855	668.2	15.37	738.4	30.53	812.9	44.83	872.3	60.59	929.6	74.64	975.7
5.435	679.1										
323.15 K											
0.2123*	607.7**	6.367	652.6	21.04	741.0	35.83	811.3	50.55	871.0	65.63	925.2
0.487	608.6	12.14	691.2	25.63	764.3	40.70	831.6	55.99	891.0	69.76	939.0
3.827	633.9	15.72	712.2	31.09	790.2	45.18	850.2	61.17	909.5	75.26	956.7
333.15 K											
0.2862*	573.6**	8.95	641.0	21.14	715.8	36.31	790.8	50.36	849.3	65.63	905.7
0.505	574.8	11.74	660.4	25.63	739.7	40.72	809.9	55.70	869.8	70.39	921.6
4.153	605.3	16.01	686.9	31.29	767.6	45.51	830.0	60.82	888.7	75.71	937.9
7.014	627.6										
343.15 K											
0.7760*	539.8**	9.33	614.0	21.22	690.0	35.46	763.2	50.97	830.2	65.79	885.9
4.888	579.5	12.14	633.7	25.58	714.0	40.86	787.8	55.70	848.6	70.60	902.7
7.135	597.5	16.32	660.9	30.99	741.9	45.91	809.4	60.97	868.6	75.14	918.0
353.15 K											
0.4898*	506.4**	8.29	575.9	20.75	661.8	40.88	766.7	55.03	826.4	70.37	883.5
2.961	529.3	11.02	596.9	25.37	688.8	45.63	787.5	60.70	848.4	75.12	899.9
5.165	549.6	14.87	624.4	36.68	747.2	50.42	807.8	65.02	864.4		
363.15 K											
0.6254**	473.4**	9.74	559.2	25.96	668.8	40.72	744.5	55.48	808.2	70.07	864.0
4.784	515.3	15.62	603.5	31.07	696.3	45.67	767.1	60.25	827.3	75.30	882.1
6.932	535.1	20.86	638.3	35.45	719.3	50.61	788.5	65.38	846.9		
373.15 K											
0.7871*	440.9**	11.97	548.7	26.24	647.7	40.70	723.9	55.60	790.0	70.60	847.7
7.473	509.4	15.76	578.1	31.05	674.7	45.40	745.8	60.93	811.3	75.40	864.4
9.26	529.0	20.30	610.0	35.37	697.5	50.36	768.0	65.87	830.1		

<sup>a</sup> Values marked with an asterisk are vapor pressures  $p_v$ , from ref 12 for  $CCl_3F$  and ref 13 for  $C_2HCl_2F_3$ . Those values marked with a double asterisk are extrapolated values at the given  $p_v$ .

Table IV. Coefficients  $a_{ij}$  of Equation 1

$i$	$j = 0$	$j = 1$	$j = 2$	$j = 3$	$j = 4$
			$\text{CCl}_3\text{F}$		
0	$1.58845 \times 10^3$	$3.44256 \times 10$	$-7.03811 \times 10^{-1}$	$1.08352 \times 10^{-3}$	$4.28663 \times 10^{-6}$
1	-2.32189	$-2.25665 \times 10^{-1}$	$5.15063 \times 10^{-3}$	$-1.82313 \times 10^{-5}$	$-2.04228 \times 10^{-7}$
2	$-1.72525 \times 10^{-3}$	$4.32928 \times 10^{-4}$	$-9.79267 \times 10^{-8}$	$5.16812 \times 10^{-8}$	$1.95805 \times 10^{-10}$
			$\text{C}_2\text{HCl}_2\text{F}_3$		
0	$1.73922 \times 10^3$	3.48051	$5.04164 \times 10^{-1}$	$-1.68721 \times 10^{-2}$	$1.34814 \times 10^{-4}$
1	-3.53052	$-3.42231 \times 10^{-2}$	$-2.27335 \times 10^{-3}$	$9.21730 \times 10^{-5}$	$-7.69574 \times 10^{-7}$
2	$7.34716 \times 10^{-5}$	$1.48980 \times 10^{-4}$	$1.31040 \times 10^{-8}$	$-1.13724 \times 10^{-7}$	$1.04207 \times 10^{-9}$

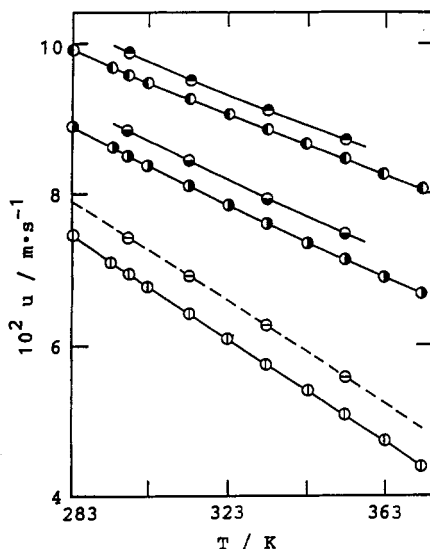


Figure 2. Temperature dependence,  $T$ , of ultrasonic speed,  $u$ .  $\text{CCl}_3\text{F}$ :  $\ominus$ ,-- (ref 14), saturated vapor pressure;  $\bullet$ , 30 MPa;  $\circ$ , 60 MPa.  $\text{C}_2\text{HCl}_2\text{F}_3$ :  $\circ$ , saturated vapor pressure;  $\bullet$ , 30 MPa;  $\circ$ , 60 MPa.

frequently observed, especially in the high-temperature region. This behavior, which appeared as a narrow pulse width in the received signal, gives rise to irregularities in the experimental results. Lainez et al. (15) also measured the ultrasonic speed in liquid  $\text{CCl}_3\text{F}$  using a pulse echo overlap method at temperatures from 353 to 413 K and pressures up to 200 MPa. When the values at saturation were recalculated by using their 12 experimental points up to about 75 MPa at 353.25 K, the value of  $552.8 \text{ m}\cdot\text{s}^{-1}$  was obtained, which is low compared with those presented here and reported by Chavez et al. (14).  $u_p$  values for  $\text{C}_2\text{HCl}_2\text{F}_3$  differ by about  $50 \text{ m}\cdot\text{s}^{-1}$  from the value for  $\text{CCl}_3\text{F}$  over the whole temperature range (see Figure 2). With elevated pressure, the difference of  $u$  between the two substances, derived from eq 1, tends to decrease.

For these fluids, many sets of accurate values for the saturated liquid densities,  $\rho_p$ , have been reported. From the extrapolated values of  $u_p$ , the isentropic compressibility,  $\kappa_S [= (\rho u^2)^{-1}]$  at  $p_s$  was estimated by using the  $\rho_p$  calculated from equations reported by Downing (12) for  $\text{CCl}_3\text{F}$  and Yokoyama and Takahashi (16) for  $\text{C}_2\text{HCl}_2\text{F}_3$ , and the results are shown in Figure 3 as a function of temperature. The saturated liquid densities for both compounds show the same temperature dependence (16), but the values of  $\kappa_S$  for  $\text{C}_2\text{HCl}_2\text{F}_3$  have a larger temperature dependence compared with those for  $\text{CCl}_3\text{F}$  and diverge significantly at higher temperatures. The temperature and pressure dependence of the speed of sound is closely related to the molecular structure in each liquid (17). That is, the speed of sound has a large absolute value for simple molecules having a spherical and/or symmetrical structure, such as  $\text{CCl}_4$ , as shown in Figure 1. The ultrasonic speed is little influenced by pressure changes, because the molecules are packed to high density (18). For hydro- and/or chloro-fluorocarbons, such as  $\text{CCl}_3\text{F}$  and  $\text{C}_2\text{HCl}_2\text{F}_3$ , the van der Waals radius of the fluorine atom is small compared with that for the

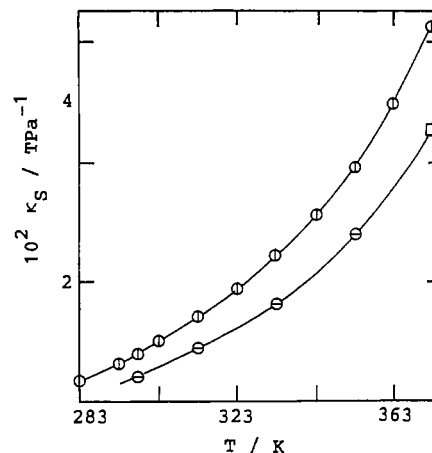


Figure 3. Temperature dependence,  $T$ , of isentropic compressibility,  $\kappa_S$ , at saturated liquid conditions.  $\text{CCl}_3\text{F}$ :  $\ominus$ , this work;  $\square$ , estimated from  $u$  reported in ref 15.  $\text{C}_2\text{HCl}_2\text{F}_3$ :  $\circ$ , this work.

chlorine atom, so these substances will have a larger free volume. The increase of free volume contributes in general to a decrease in the speed of sound and to an increase in the compressibility, and that leads to the strong pressure dependence observed in the case of the nonpolar and weak-polar substances. From these facts,  $\text{C}_2\text{HCl}_2\text{F}_3$  should have a large intermolecular free volume as a result of the complexity of the molecular structure, and the ultrasonic speed and compressibility should be more temperature and pressure dependent than those for  $\text{CCl}_3\text{F}$ .

$\text{C}_2\text{HCl}_2\text{F}_3$ , which is assumed to have to be short atmospheric lifetime, has been recommended as a replacement compound of  $\text{CCl}_3\text{F}$ , since both substances have similar physicochemical properties, such as the critical constants and vapor pressure. However, the present results for the ultrasonic speeds in  $\text{C}_2\text{HCl}_2\text{F}_3$  differs considerably from the values for  $\text{CCl}_3\text{F}$ , especially at higher temperatures. This difference may present some thermodynamic problems in using  $\text{C}_2\text{HCl}_2\text{F}_3$  as a replacement as an alternative compound of  $\text{CCl}_3\text{F}$ .

Registry No.  $\text{CCl}_3\text{F}$ , 75-69-4;  $\text{C}_2\text{HCl}_2\text{F}_3$ , 306-83-2.

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## PVT and Vapor Pressure Measurements on 1,1-Dichloro-2,2,2-trifluoroethane (HCFC-123)

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A complete set of *PVT* properties, vapor pressures, and critical parameters of 1,1-dichloro-2,2,2-trifluoroethane (HCFC-123) were measured by a constant-volume method. Values of 134 *PVT* property data were obtained along 19 isochores in a range of temperatures from 311 to 523 K, pressures from 0.5 to 12 MPa, and densities from 95 to 1440 kg·m<sup>-3</sup>, respectively. Results for 68 vapor pressures were obtained at temperatures from 308 K to the critical temperature, while a vapor pressure correlation representing the experimental data within ±0.26% was developed. The critical pressure was determined as 3.6655 ± 0.0030 MPa in the course of developing the vapor pressure correlation. The uncertainties of measurements are less than ±10 mK in temperature, ±2 kPa in pressure, and ±0.01 to ±0.14% in density, respectively. The purity of samples used was 99.8 and 99.82 wt %.

### Introduction

1,1-Dichloro-2,2,2-trifluoroethane (HCFC-123, CHCl<sub>2</sub>CF<sub>3</sub>) is one of the promising substitutes for the conventional refrigerant CFC-11 (CCl<sub>3</sub>F), but studies of the thermodynamic properties of HCFC-123 are rather limited, not only in the quantity of the reported data but also in the range of the measurements up to the present.

In the present study, the vapor pressures and *PVT* properties are reported in extensive temperature, pressure, and density range covering the entire fluid phase. A vapor pressure correlation and the critical pressure have also been derived from the experimental data.

### Experimental Apparatus and Procedure

A constant-volume method was applied for measuring the vapor pressures and *PVT* properties of HCFC-123. Figure 1 shows the experimental apparatus, which is composed of a constant-volume cell immersed in a thermostated bath, a temperature-measurement device, a PID temperature controller, and a pressure-measurement device, etc. We have already measured *PVT* properties of 1,1,1,2-tetrafluoroethane (HFC-134a) (1), and perfluoro-2-methylpentane (2), with this apparatus.

The inner volume of the constant-volume cell was carefully calibrated by using the density of water and its volume change

Table I. Uncertainties of Data and Purities of Samples of HCFC-123

	series	$\Delta T /$ mK	purity/ wt %	$\Delta \rho /$ (kg·m <sup>-3</sup> )	purity/ wt %
vapor pressures		±10	±2		99.8/99.82
<i>PVT</i> properties	a	±10	±2	±0.1	99.82
	b			±0.1	99.8
	c			±0.2	99.82
	d			±0.3	99.82
	e			±0.4	99.82
	f			±0.5	99.8
	g			±0.5	99.8
	h			±0.7	99.82
	i			±0.7	99.82
	j			±0.8	99.82
	k			±0.8	99.82
	l			±0.9	99.82
	m			±0.9	99.82
	n			±0.9	99.82
	o			±0.9	99.82
	p			±0.8	99.82
	q			±0.8	99.82
	r			±0.7	99.82
	s			±0.4	99.82

due to changes in temperature and pressure was calculated by using the thermal expansivity and Young's modulus of stainless steel. The volume was about 139 cm<sup>3</sup> at room temperature. The density of the sample was determined from the inner volume of the cell and the mass of the sample confined in the cell, which was measured by a precision balance. The uncertainty of the cell volume was about ±0.02 to ±0.12%, depending on temperature and pressure, while the uncertainty of the sample mass was ±3 mg.

The temperature of silicon oil filled in a thermostated bath was controlled within ±3 mK by the PID temperature controller. At thermal equilibrium, which was confirmed by the pressure of the sample fluid in the cell being stable, the pressure and the temperature of the sample were measured.

The pressure of the sample was measured by the pressure gauges O1, O2, and O3 in Figure 1. The sample cell is connected with a differential pressure detector (B), which transfers the pressure of the sample to pressure-transfer medium, nitrogen gas. The mechanical behavior of the differential pressure detector (B) was calibrated before and after each series of measurements.

The temperature was measured with a standard platinum resistance thermometer (D in Figure 1), which was located near the sample cell. The platinum resistance thermometer was calibrated according to IPTS-68 at the National Laboratory of Metrology, Ibaraki, Japan.

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