

Figure 3. Constant  $B_1$  in eq 1 vs. molar fraction of methyl isobutyl ketone.

listed in Table VI. By means of eq 4-15, density, viscosity, and refractive index data for the studied systems in this paper at any temperature and composition, within the experimental ranges, can be predicted. The calculated values through these equations compared well with the experimental data, and the

average percent deviation ( $D$ ) for each property and system is also listed in Table VI.

#### Glossary

$A_1, B_1$	constants in eq 1
$A_2, B_2$	constants in eq 2
$A_3, B_3$	constants in eq 3
$\rho$	density of the mixture, g cm <sup>-3</sup>
$\eta$	viscosity of the mixture, cP
$n_D$	refractive index of the mixture for the sodium D line.
$X_{\text{MIK}}, X$	molar fraction of the MIK
$T$	temperature, K
$t$	temperature, °C
$D$	average percent deviation

Registry No. MIBK, 108-10-1; P<sub>1</sub>, 71-41-0; P<sub>2</sub>, 6032-29-7; IA, 123-51-3; TA, 75-85-4.

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## Isentropic Compressibilities of Binary Liquid Mixtures at 303.15 and 313.15 K

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**Isentropic compressibilities for the binary mixtures of methyl ethyl ketone with benzene, toluene, chlorobenzene, bromobenzene, and nitrobenzene have been determined at 303.15 and 313.15 K, using ultrasonic velocity and density data. Excess isentropic compressibility,  $k_s^E$ , values are negative over the entire range of composition for all the systems and at both temperatures. The behavior of  $k_s^E$  as a function of composition and temperature has been studied. The results have been discussed in terms of dipole-induced dipole and dipole-dipole interactions between dissimilar components.**

Excess isentropic compressibilities have been determined for binary mixtures of methyl ethyl ketone with benzene, toluene, chlorobenzene, bromobenzene, and nitrobenzene in order to study the effect that group substitution on a benzene ring has on the molecular interaction in the presence of a polar component. A literature survey revealed that the excess isentropic compressibilities for these systems have not been reported.

Table I. Pure Component Parameters

com- ponent	T/K	V/ (cm <sup>3</sup> mol <sup>-1</sup> )	K <sub>a</sub> / TPa <sup>-1</sup>	10 <sup>3</sup> α/ K <sup>-1</sup>	C <sub>p</sub> / (J K <sup>-1</sup> mol <sup>-1</sup> )
MEK	303.15	90.77	915	1.256	162.2
	313.15	91.72	1002	1.271	169.1
C <sub>6</sub> H <sub>6</sub>	303.15	89.81	707	1.242	137.4
	313.15	91.08	770	1.258	140.6
C <sub>6</sub> H <sub>5</sub> CH <sub>3</sub>	303.15	107.44	699	1.079	159.9
	313.15	108.61	757	1.091	163.4
C <sub>6</sub> H <sub>5</sub> Cl	303.15	102.75	589	0.985	150.6
	313.15	103.76	634	1.005	152.2
C <sub>6</sub> H <sub>5</sub> Br	303.15	105.98	514	0.896	155.9
	313.15	106.95	554	0.992	157.3
C <sub>6</sub> H <sub>5</sub> NO <sub>2</sub>	303.15	103.16	395	0.818	177.3
	313.15	104.01	426	0.865	173.6

#### Experimental Section

Ultrasonic velocities were measured by using a single-crystal interferometer at a frequency of 2 MHz, and the values were accurate to ±0.1%. Density data for the pure components were measured by using a bicapillary pycnometer, and in the

**Table II. Mole Fraction,  $x_1$ , of Methyl Ethyl Ketone, Density,  $\rho$ , Sound Velocity,  $u$ , Isentropic Compressibility,  $k_s$ , and Excess Isentropic Compressibility,  $k_s^E$** 

303.15 K					313.15 K				
$x_1$	$\rho$ /(g cm <sup>-3</sup> )	$u$ /ms <sup>-1</sup>	$k_s$ /TPa <sup>-1</sup>	$k_s^E$ /TPa <sup>-1</sup>	$x_1$	$\rho$ /(g cm <sup>-3</sup> )	$u$ /ms <sup>-1</sup>	$k_s$ /TPa <sup>-1</sup>	$k_s^E$ /TPa <sup>-1</sup>
Methyl Ethyl Ketone + Benzene									
0.0000	0.86851	1276	707		0.0000	0.85799	1230	770	
0.1126	0.86043	1269	722	-9	0.1126	0.85015	1226	783	-14
0.2249	0.85236	1260	739	-16	0.2249	0.84223	1217	802	-22
0.3113	0.84612	1253	753	-20	0.3113	0.83609	1210	817	-27
0.4163	0.83841	1244	771	-25	0.4163	0.82859	1201	837	-32
0.5232	0.83042	1234	791	-27	0.5232	0.82084	1191	859	-35
0.6045	0.82423	1225	809	-26	0.6045	0.81496	1182	878	-35
0.7148	0.81565	1212	835	-22	0.7148	0.80633	1169	908	-30
0.8265	0.80692	1197	865	-15	0.8265	0.79771	1154	941	-22
1.0000	0.79439	1173	915		1.0000	0.78441	1128	1002	
Methyl Ethyl Ketone + Toluene									
0.0000	0.85770	1291	699		0.0000	0.84844	1248	757	
0.1367	0.85093	1281	716	-9	0.1367	0.84166	1240	773	-14
0.2214	0.84643	1274	728	-13	0.2214	0.83709	1233	786	-19
0.3435	0.83968	1263	746	-19	0.3435	0.83033	1222	807	-25
0.4318	0.83442	1255	761	-23	0.4318	0.82515	1214	822	-31
0.5406	0.82767	1243	782	-25	0.5406	0.81847	1202	846	-33
0.6267	0.82194	1232	801	-25	0.6267	0.81282	1191	867	-34
0.7122	0.81606	1219	824	-21	0.7122	0.80686	1178	893	-30
0.8178	0.80815	1203	855	-15	0.8178	0.79906	1162	927	-24
1.0000	0.79439	1173	915		0.0000	0.78441	1128	1002	
Methyl Ethyl Ketone + Chlorobenzene									
0.0000	1.09550	1245	589		0.0000	1.08468	1206	634	
0.1068	1.06731	1238	611	-9	0.1068	1.05711	1197	660	-9
0.1972	1.04319	1235	629	-19	0.1972	1.03314	1194	679	-21
0.3202	1.00903	1229	656	-28	0.3202	0.99933	1188	709	-33
0.4174	0.98114	1224	680	-35	0.4174	0.97149	1183	736	-41
0.5576	0.93945	1218	718	-41	0.5576	0.92981	1177	776	-52
0.6242	0.91987	1213	740	-43	0.6242	0.90951	1172	801	-52
0.7288	0.88576	1201	782	-37	0.7288	0.87623	1160	848	-45
0.8531	0.84470	1187	840	-22	0.8531	0.83588	1146	911	-31
1.0000	0.79439	1173	915		1.0000	0.78441	1128	1002	
Methyl Ethyl Ketone + Bromobenzene									
0.0000	1.48150	1146	514		0.0000	1.46803	1109	554	
0.1221	1.40917	1144	542	-14	0.1221	1.39687	1104	587	-15
0.1917	1.36704	1141	562	-20	0.1917	1.35469	1101	609	-21
0.2946	1.30323	1139	591	-30	0.2946	1.29103	1099	641	-32
0.4069	1.23075	1142	623	-41	0.4069	1.21899	1102	676	-44
0.5335	1.14512	1146	665	-48	0.5335	1.18402	1106	721	-55
0.6748	1.04472	1152	721	-50	0.6748	1.08419	1112	782	-59
0.8126	0.94160	1155	796	-35	0.8126	0.98172	1115	863	-44
1.0000	0.79439	1173	915		1.0000	0.78441	1128	1002	
Methyl Ethyl Ketone + Nitrobenzene									
0.0000	1.19341	1456	395		0.0000	1.18352	1408	426	
0.0986	1.15909	1426	424	-19	0.0986	1.15066	1386	452	-24
0.2098	1.12039	1388	463	-35	0.2098	1.11194	1348	494	-44
0.3268	1.07787	1354	506	-50	0.3268	1.06904	1314	542	-63
0.4182	1.04339	1336	537	-66	0.4182	1.03446	1296	575	-79
0.5212	1.00311	1312	579	-77	0.5212	0.99451	1272	621	-92
0.6458	0.95265	1277	642	-80	0.6458	0.94313	1239	691	-94
0.7512	0.90751	1241	715	-63	0.7512	0.89894	1201	771	-77
0.8119	0.88061	1223	759	-52	0.8119	0.87193	1183	819	-66
1.0000	0.79439	1173	915		1.0000	0.78441	1128	1002	

case of mixtures the data were obtained from excess volumes (1) by using the relation

$$\rho = \frac{x_1 M_1 + x_2 M_2}{x_1 V_1 + x_2 V_2 + V^E} \quad (1)$$

Density values obtained from both methods were accurate to  $\pm 5 \times 10^{-5}$  g cm<sup>-3</sup>. All the analytical grade chemicals were further purified by the methods described earlier (1-3). The purity of the samples was checked by comparing the values of density, boiling point, and refractive index with those reported in the literature (4).

## Results

The isentropic compressibilities were calculated indirectly by

using the ultrasonic velocity,  $u$ , and density,  $\rho$ , with the relation

$$k_s = 1/u^2 \rho \quad (2)$$

The values of  $k_s$  were accurate to  $\pm 2$  TPa<sup>-1</sup>. The excess isentropic compressibilities were computed by using the equation

$$k_s^E = k_s^{\text{mix}} - k_s^{\text{id}} \quad (3)$$

where  $k_s^{\text{mix}}$  and  $k_s^{\text{id}}$  are isentropic compressibilities of the actual mixture and ideal mixture. The values of  $k_s^{\text{id}}$  were obtained by using the equation (5, 6)

$$k_s^{\text{id}} = \sum \phi_i [k_{s,i} + TV_i \alpha_i^2 / C_{p,i}] - T(\sum x_i V_i)(\sum \phi_i \alpha_i^2) / (\sum x_i C_{p,i}) \quad (4)$$

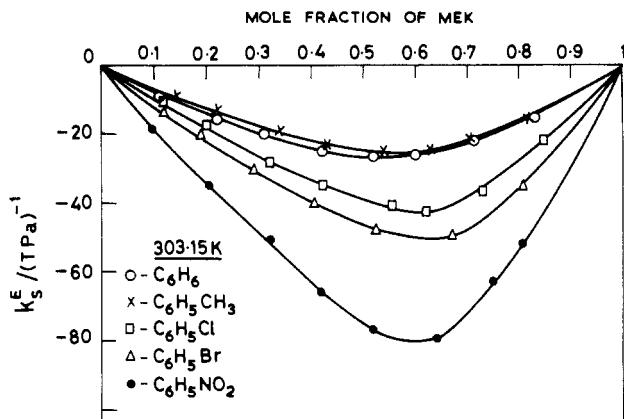


Figure 1. Mole fraction vs. excess isentropic compressibility at 303.15 K.

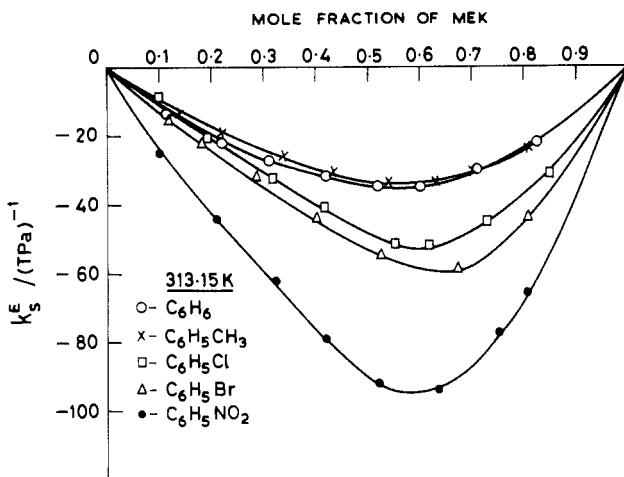


Figure 2. Mole fraction vs. excess isentropic compressibility at 313.15 K.

where  $\phi_i$ ,  $k_{s,i}$ ,  $V_i$ ,  $\alpha_i$ , and  $C_{p,i}$  are volume fraction calculated on the basis of ideal density, isentropic compressibility, molar volume, thermal expansivity, and heat capacity of component  $i$ , respectively. The values of these parameters are given in Table I. The values of ultrasonic velocity, density, isentropic compressibility, and excess isentropic compressibility at both the temperatures are given in Table II. The graphs of  $k_s^E$  vs. composition are also presented in Figures 1 and 2. The dependence of  $k_s^E$  on mole fraction has been represented by an empirical equation of the form

$$k_s^E = x_1 x_2 [a_0 + a_1(x_1 - x_2) + a_2(x_1 - x_2)^2] \quad (5)$$

The parameters  $a_0$ ,  $a_1$ , and  $a_2$  are obtained by the method of least squares and are given in Table III along with the standard deviation  $\sigma(k_s^E)$ .

## Discussion

Excess isentropic compressibilities are negative for all the

Table III. Values of the Parameters in Eq 5 and Standard Deviation  $\sigma(k_s^E)$

methyl ethyl ketone +	$T/K$	$a_0/T\text{Pa}^{-1}$	$a_1/T\text{Pa}^{-1}$	$a_2/T\text{Pa}^{-1}$	$\sigma(k_s^E)/T\text{Pa}^{-1}$
benzene	303.15	-109.8	-9.4	25.5	1.2
	313.15	-137.6	-10.6	0.6	1.2
toluene	303.15	-99.1	-15.2	11.6	0.8
	313.15	-137.5	-26.9	17.4	1.4
chlorobenzene	303.15	-163.7	-46.8	59.1	1.9
	313.15	-197.2	-86.7	56.3	1.7
bromobenzene	303.15	-194.6	-65.6	46.3	2.6
	313.15	-222.7	-99.1	23.5	2.9
nitrobenzene	303.15	-302.4	-92.8	67.6	3.9
	313.15	-363.8	-110.9	58.8	4.1

Table IV. Comparison of the Maximum Values of Excess Isentropic Compressibilities  $k_s^E$  and Excess Volumes  $V^E$ , at 303.15 and 313.15 K

methyl ethyl ketone +	303.15 K		313.15 K	
	$k_s^E/T\text{Pa}^{-1}$	$V^E/(cm^3 \text{mol}^{-1})$	$k_s^E/T\text{Pa}^{-1}$	$V^E/(cm^3 \text{mol}^{-1})$
benzene	-27	-0.161	-35	-0.168
toluene	-26	-0.256	-34	-0.245
chlorobenzene	-43	-0.362	-52	-0.376
bromobenzene	-50	-0.405	-59	-0.419
nitrobenzene	-80	-0.601	-94	-0.644

systems over the entire range of composition. The results are attributed to the induced dipole and dipole interaction between  $\pi$  electrons of the benzene ring and carbonyl group of methyl ethyl ketone in the systems methyl ethyl ketone with benzene and toluene. In addition to the above effect a dipole-dipole interaction between the groups  $\text{CO}$  with  $-\text{Cl}$ ,  $-\text{Br}$ , and  $-\text{NO}_2$  may be responsible for the large negative values of  $k_s^E$  in the other three systems. The algebraic values of  $k_s^E$  fall in the order benzene  $\approx$  toluene  $<$  chlorobenzene  $<$  bromobenzene  $<$  nitrobenzene, at both temperatures.

This order is parallel to the dielectric constant values of the noncommon components. A similar trend is also observed with respect to excess volumes, reported in our earlier paper (7). The two properties are compared in Table IV and a remarkable similarity has been observed in their behavior with respect to these systems and at both temperatures. A negative temperature coefficient is observed in all the systems.

Registry No. MEK, 78-93-3;  $\text{C}_6\text{H}_6$ , 71-43-2;  $\text{C}_6\text{H}_5\text{CH}_3$ , 108-88-3;  $\text{C}_6\text{H}_5\text{Cl}$ , 108-90-7;  $\text{C}_6\text{H}_5\text{Br}$ , 108-86-1;  $\text{C}_6\text{H}_5\text{NO}_2$ , 98-95-3.

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