

Densities, Refractive Indices, and Excess Molar Volumes of Water + Ethanol + 2-Methoxy-2-methylpropane at 298.15 K

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The refractive indices and densities of mixtures of water + ethanol + 2-methoxy-2-methylpropane and ethanol + 2-methoxy-2-methylpropane were determined at 298.15 K. Derived excess molar properties were correlated with the corresponding composition data using the polynomials of Redlich and Kister, Cibulka, and Singh *et al.*

Introduction

As part of our study of aqueous mixtures of alcohols and gasoline additives (Arce *et al.*, 1994, 1995), in this work we examine the systems ethanol + 2-methoxy-2-methylpropane (methyl *tert*-butyl ether or MTBE) and water + ethanol + 2-methoxy-2-methylpropane. For totally miscible mixtures, the excess molar volumes V^E and the molar refractions R were, respectively, calculated from the densities d and refractive indices n_D at 298.15 K, in the latter case employing the Lorentz-Lorenz equation. The V^E data and ΔR —the deviation of R from a mole fraction average of the molar refractions of the pure components—were then correlated with the composition data by means of the polynomials of Redlich-Kister (1948), Cibulka (1982), and Singh *et al.* (1984).

Experimental Section

Materials. Water was purified using a Milli-Q Plus system. Ethanol was supplied by Merck and had a nominal purity >99.5 mass %. 2-Methoxy-2-methylpropane was supplied by Aldrich and was redistilled prior to use, its final purity being >99.7 mass %. Water contents in the ethanol and in the MTBE were 0.08 and 0.03 mass %, respectively (determined with a Metrohm 737 KF coulometer).

Apparatus and Procedure. The mixtures were prepared by mass using a Mettler AE 240 balance that measured to within $\pm 0.000\ 01$ g. Densities were measured to within $\pm 0.000\ 03$ g·cm⁻³ in an Anton Paar DMA 60/602 densimeter (calibrated with air and water) and refractive indices to within ± 0.0001 with an ATAGO RX-1000 refractometer. In both cases, a Hetotherm thermostat was used to maintain the temperature at (298.15 ± 0.02) K.

Table 1 lists the densities and refractive indices measured for the pure components, together with published values for these parameters (Riddick *et al.*, 1986; Obama *et al.*, 1985; Mato *et al.*, 1991).

Results

The measured values of ρ and n_D for the ternary system water + ethanol + MTBE, and the V^E and ΔR values

Table 1. Densities ρ and Refractive Indices n_D of the Pure Components at 298.15 K

component	ρ /(g cm ⁻³)		n_D	
	exptl	lit	exptl	lit
water	0.997 04	0.997 04 ^a	1.3324	1.332 50 ^a
ethanol	0.785 20	0.785 04 ^a	1.3592	1.359 41 ^a
MTBE	0.735 58	0.735 1 ^b 0.735 66 ^c	1.3663	1.366 3 ^b

^a Riddick *et al.* (1986). ^b Obama *et al.* (1985). ^c Mato *et al.* (1991).

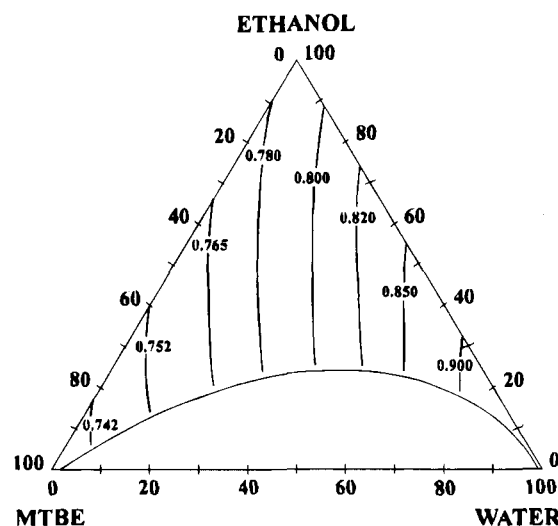


Figure 1. Density isolines for water + ethanol + MTBE at 298.15 K and atmospheric pressure.

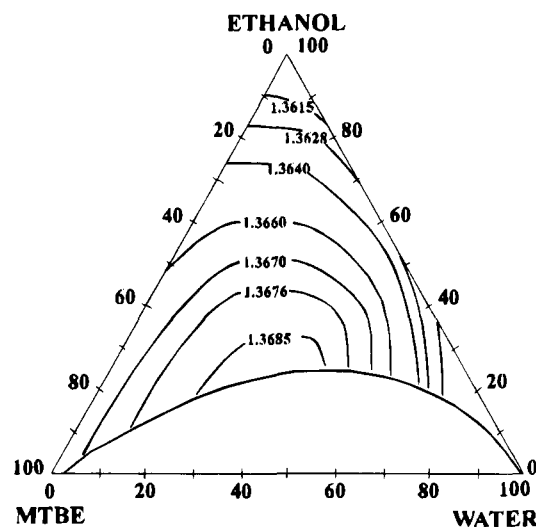


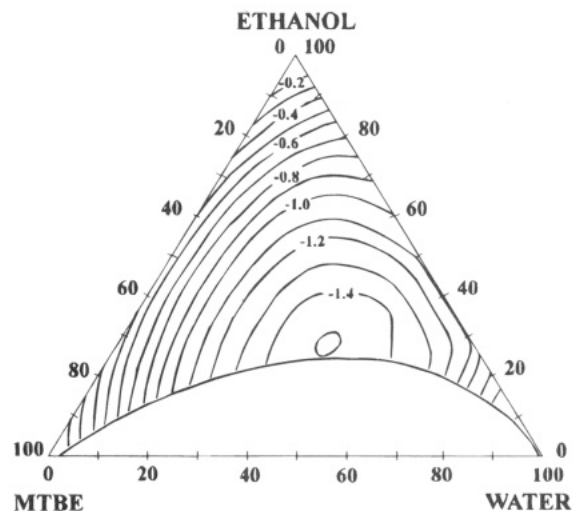
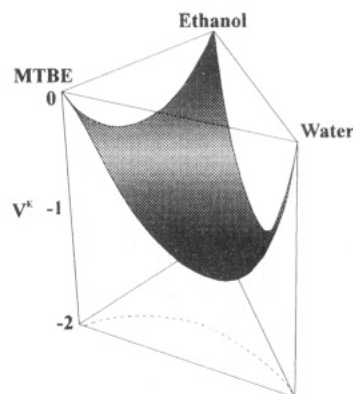
Figure 2. Refractive index isolines for water + ethanol + MTBE at 298.15 K and atmospheric pressure.

derived from them, are given in Table 2, which also includes these data for the binary system ethanol + MTBE. Figures 1 and 2 respectively, show the density and refractive index isolines for the ternary system. Figure 3 shows the dependence of V^E on the mole fractions of water and ethanol and Figure 4 the corresponding V^E isolines.

For the binary system, the V^E and ΔR data were correlated with the composition data using the Redlich-

Table 2. Densities ρ , Refractive Indices n_D , Excess Volumes V^E , and ΔR Values for Water (1) + Ethanol (2) + MTBE (3) at 298.15 K

x_1	x_2	$\rho/(\text{g}\cdot\text{cm}^{-3})$	n_D	$V^E/(\text{cm}^3\cdot\text{mol}^{-1})$	$\Delta R/(\text{cm}^3\cdot\text{mol}^{-1})$
0.0000	0.0414	0.737 24	1.3664	-0.100	-0.004
0.0000	0.1057	0.739 80	1.3666	-0.230	-0.010
0.0000	0.1532	0.741 68	1.3666	-0.308	-0.014
0.0000	0.2005	0.743 57	1.3667	-0.371	-0.016
0.0000	0.2550	0.745 77	1.3666	-0.429	-0.019
0.0000	0.3593	0.750 09	1.3665	-0.499	-0.021
0.0000	0.4082	0.752 20	1.3663	-0.516	-0.021
0.0000	0.4475	0.753 93	1.3662	-0.522	-0.021
0.0000	0.4560	0.754 31	1.3661	-0.523	-0.021
0.0000	0.5057	0.756 58	1.3659	-0.522	-0.020
0.0000	0.5516	0.758 75	1.3656	-0.513	-0.019
0.0000	0.5936	0.760 81	1.3654	-0.499	-0.018
0.0000	0.6522	0.763 80	1.3649	-0.468	-0.016
0.0000	0.6972	0.766 20	1.3645	-0.436	-0.015
0.0000	0.7502	0.769 16	1.3639	-0.389	-0.012
0.0000	0.7943	0.771 73	1.3633	-0.342	-0.010
0.0000	0.8460	0.774 88	1.3625	-0.275	-0.008
0.0000	0.8848	0.777 35	1.3619	-0.218	-0.006
0.0000	0.9471	0.781 50	1.3606	-0.109	-0.003
0.0078	0.0693	0.738 88	1.3665	-0.188	-0.008
0.0216	0.1915	0.745 04	1.3668	-0.454	-0.020
0.0327	0.2901	0.750 40	1.3669	-0.612	-0.027
0.0410	0.3645	0.754 74	1.3669	-0.697	-0.030
0.0527	0.4679	0.761 27	1.3667	-0.768	-0.033
0.0565	0.5019	0.763 56	1.3665	-0.779	-0.033
0.0635	0.5640	0.767 97	1.3662	-0.782	-0.033
0.0727	0.6453	0.774 21	1.3655	-0.753	-0.031
0.0813	0.7221	0.780 68	1.3646	-0.688	-0.027
0.0905	0.8041	0.788 33	1.3632	-0.575	-0.022
0.1012	0.8988	0.798 31	1.3608	-0.385	-0.014
0.0208	0.0868	0.740 54	1.3667	-0.280	-0.013
0.0388	0.1617	0.745 13	1.3669	-0.481	-0.022
0.0594	0.2478	0.750 84	1.3671	-0.671	-0.029
0.0774	0.3227	0.756 28	1.3672	-0.800	-0.034
0.0974	0.4059	0.762 96	1.3671	-0.903	-0.038
0.1073	0.4472	0.766 56	1.3670	-0.938	-0.038
0.1160	0.4833	0.769 90	1.3669	-0.960	-0.039
0.1345	0.5604	0.777 63	1.3664	-0.973	-0.037
0.1544	0.6433	0.787 09	1.3656	-0.935	-0.034
0.1728	0.7201	0.797 14	1.3642	-0.844	-0.029
0.1935	0.8065	0.810 35	1.3618	-0.665	-0.021
0.0329	0.0745	0.741 21	1.3669	-0.350	-0.009
0.0660	0.1494	0.747 23	1.3674	-0.626	-0.015
0.0871	0.1970	0.751 33	1.3677	-0.769	-0.018
0.1317	0.2979	0.761 00	1.3680	-0.999	-0.022
0.1587	0.3590	0.767 71	1.3680	-1.094	-0.023
0.1772	0.4010	0.772 80	1.3679	-1.140	-0.023
0.1901	0.4302	0.776 59	1.3678	-1.162	-0.024
0.2158	0.4883	0.784 92	1.3674	-1.181	-0.024
0.2437	0.5514	0.795 31	1.3666	-1.157	-0.024
0.2739	0.6197	0.808 60	1.3649	-1.070	-0.025
0.3065	0.6935	0.826 07	1.3618	-0.889	-0.027
0.0386	0.0595	0.741 01	1.3669	-0.347	-0.016
0.0813	0.1254	0.747 40	1.3674	-0.649	-0.027
0.1201	0.1852	0.753 76	1.3678	-0.866	-0.033
0.1698	0.2619	0.763 06	1.3681	-1.082	-0.040
0.2069	0.3192	0.771 15	1.3682	-1.202	-0.044
0.2233	0.3445	0.775 09	1.3682	-1.243	-0.045
0.2396	0.3696	0.779 29	1.3682	-1.275	-0.047
0.2814	0.4340	0.791 49	1.3678	-1.317	-0.049
0.3126	0.4822	0.802 24	1.3672	-1.302	-0.048
0.3517	0.5425	0.818 20	1.3658	-1.209	-0.043
0.3933	0.6067	0.839 24	1.3629	-0.993	-0.029
0.0518	0.0506	0.741 84	1.3670	-0.412	-0.018
0.0966	0.0943	0.747 56	1.3675	-0.692	-0.031
0.1467	0.1433	0.754 53	1.3680	-0.941	-0.043
0.1928	0.1883	0.761 69	1.3683	-1.122	-0.050
0.2562	0.2503	0.773 22	1.3685	-1.308	-0.056
0.2786	0.2721	0.777 88	1.3686	-1.356	-0.057
0.3120	0.3047	0.785 57	1.3686	-1.410	-0.057
0.3569	0.3486	0.797 59	1.3684	-1.443	-0.055
0.4016	0.3922	0.811 94	1.3678	-1.423	-0.051
0.4512	0.4407	0.831 74	1.3664	-1.318	-0.043
0.5059	0.4941	0.860 34	1.3628	-1.073	-0.030
0.5942	0.4058	0.878 95	1.3620	-1.097	-0.029
0.5317	0.3632	0.844 15	1.3659	-1.368	-0.050
0.4910	0.3354	0.826 86	1.3673	-1.462	-0.057
0.4543	0.3103	0.813 65	1.3680	-1.493	-0.060
0.4197	0.2867	0.803 36	1.3686	-1.520	-0.060
0.3954	0.2701	0.796 65	1.3687	-1.503	-0.059
0.7447	0.2553	0.917 40	1.3585	-0.992	-0.025
0.7135	0.2446	0.894 56	1.3615	-1.171	-0.043
0.6795	0.2329	0.873 75	1.3637	-1.314	-0.057
0.6559	0.2248	0.860 86	1.3647	-1.367	-0.063

**Figure 3.** Composition dependence of the excess molar volume of water + ethanol + MTBE at 298.15 K and atmospheric pressure.**Figure 4.** Excess molar volume isolines for water + ethanol + MTBE at 298.15 K and atmospheric pressure.**Table 3. Coefficients and Standard Deviations (σ) for the Excess Volume–Composition and ΔR –Composition Curves Fitted to the Data for the Ethanol (1) + MTBE (2) System**

property	$A_0/(\text{cm}^3\cdot\text{mol}^{-1})$	$A_1/(\text{cm}^3\cdot\text{mol}^{-1})$	$A_2/(\text{cm}^3\cdot\text{mol}^{-1})$	$\sigma/(\text{cm}^3\cdot\text{mol}^{-1})$
V^E	-2.0902	0.1855	-0.3160	0.001
ΔR	-0.0820	0.0336		0.001

Kister polynomial (Redlich and Kister, 1948)

$$Q_{12} = x_1(1 - x_1) \sum_{k=0}^N A_k (2x_1 - 1)^k \quad k = 0, 1, 2, \dots, N \quad (1)$$

where Q_{12} is either V^E or ΔR , x_1 is the mole fraction of the first component, and N corresponds to the number of polynomial coefficients.

For the ternary system, the above properties were correlated using the polynomials of Redlich and Kister (1948)

$$Q_{123} = Q_{12} + Q_{23} + Q_{31} + x_1 x_2 x_3 (A + B(x_1 - x_2) + C(x_2 - x_3) + D(x_3 - x_1) + E(x_1 - x_2)^2 + \dots) \quad (2)$$

Cibulka (1982)

$$Q_{123} = Q_{12} + Q_{23} + Q_{31} + x_1 x_2 x_3 (A + Bx_1 + Cx_2) \quad (3)$$

and Singh *et al.* (1984)

$$Q_{123} = Q_{12} + Q_{23} + Q_{31} + x_1 x_2 x_3 (A + Bx_1(x_2 - x_3) + Cx_1^2(x_2 - x_3)^2) \quad (4)$$

all of which include terms Q_{ij} for each binary system involved (the term Q_{31} is considered to be zero here, since

Table 4. Coefficients and Standard Deviations (σ) for the Excess Volume–Composition and ΔR –Composition Surfaces Fitted to the Data for the Water + Ethanol + MTBE System

property	polynomial	A/(cm ³ ·mol ⁻¹)	B/(cm ³ ·mol ⁻¹)	C/(cm ³ ·mol ⁻¹)	D/(cm ³ ·mol ⁻¹)	E/(cm ³ ·mol ⁻¹)	F/(cm ³ ·mol ⁻¹)	G/(cm ³ ·mol ⁻¹)	σ /(cm ³ ·mol ⁻¹)
V^E	Redlich–Kister	-19.225	-19.217	17.028	2.189	-20.809	-28.472	-1.927	0.03
	Cibulka	-34.916	-0.039	41.525					0.05
	Singh <i>et al.</i>	-18.703	85.640	-609.77					0.07
ΔR	Redlich–Kister	-0.946	-1.095	0.648	0.447				0.006
	Cibulka	-1.148	-1.340	1.945					0.006
	Singh <i>et al.</i>	-0.810	1.171						0.008

it corresponds to the immiscible binary subsystem water + MTBE). These equations were fitted to the corresponding excess molar property–composition data by least-squares regression, applying Fischer's F-test to compare fits and thus minimize the number of coefficients, except in the case of the Cibulka polynomial. The coefficients and their mean standard deviations (σ) in cm³·mol⁻¹ for both excess properties have already been published for the water + ethanol system (Arce *et al.*, 1993) and are listed in Table 3 for the binary ethanol + MTBE system and in Table 4 for the ternary water + ethanol + MTBE system.

Conclusions

For the miscible ternary mixtures water + ethanol + MTBE at 298.15 K and atmospheric pressure, excess molar volumes were negative and quite large, reaching ca. -1.52 cm³·mol⁻¹. The V^E –composition values were best correlated using the Redlich–Kister polynomial, although it required a greater number of coefficients than the polynomials of Cibulka and Singh *et al.*

The deviations of R from the mole fraction average of the molar refractions of the pure components were also negative, but had smaller values which did not exceed ca. -0.06 cm³·mol⁻¹. The mean standard deviations (σ) were similar for the three polynomials: it is noteworthy that the very slightly higher value of σ obtained for the polynomial of Singh *et al.* was not improved by the inclusion of the second-order term and that, of the other two correlations, the Cibulka polynomial required the fewest coefficients.

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Received for review June 26, 1995. Accepted August 25, 1995.* This work was partly supported by the DGICYT (Spain) under Project PB94-0658.

JE950147J

* Abstract published in *Advance ACS Abstracts*, October 1, 1995.