Excess Molar Enthalpies of Binary Mixtures Containing Propylene Carbonate + 23 Alkanoates at 298.15 K

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Excess molar enthalpies, H_{m}^{E} , of binary mixtures containing propylene carbonate + 23 alkanoates as a function of the mole fraction of propylene carbonate have been determined at 298.15 using a flow microcalorimeter. H_{m}^{E} values are positive for all mixtures, increasing as the chain length of the alkanoate is increased with a maximum at a mole fraction of ≈ 0.5 . Maximum values range from 26 J·mol¹ for methyl acetate to 960 J·mol⁻¹ for ethyl octanoate. Binary mixtures containing propylene carbonate + each one of the structural isomers have been considered. Results have been correlated using the Redlich–Kister equation and have been qualitatively explained.

Introduction

Several recent chemical and electrochemical studies have focused on propylene carbonate, an aprotic solvent with a high potential for industrial uses such as in lithium batteries (Gabano, 1983; Tobishima et al., 1988; Pistoia, 1994) because it does not react with lithium to evolve hydrogen.

Following our systematic studies on the physical properties of binary organic liquid mixtures with one or both components as dipolar-aprotic solvents, we report in this paper the excess molar enthalpies, $H_{\rm m}^{\rm E}$, of binary mixtures containing propylene carbonate + 23 alkanoates at 298.15 K.

We have not considered mixtures containing alkanoates with a number of carbon atoms n > 10 as they are only partially miscible in propylene carbonate.

To our knowledge, no literature results are available for the mixtures studied in this paper.

Experimental Section

Chemicals. Chemicals were purchased from Aldrich Chemical Co. with the exception of methyl and ethyl acetate and butyl butyrate, which were Fluka products.

Liquids were used without further purification after gas chromatography failed to show any significant impurities.

Purities of components were also checked by comparing their densities, ρ , at (293.15 or 298.15) K with those reported in the literature. Both ours and literature values are listed in Table 1.

Before measurements, liquids were kept in dark bottles, dried over molecular sieves (Union Carbide, type 4A, $^{1}/_{16}$ in. pellets), and degassed by ultrasound (Ultrasonic bath, Hellma, type 460, Milan, Italy).

Apparatus and Procedure. Densities, ρ , of pure components were determined using an Anton Paar vibrating-tube digital densimeter (DMA 60) equipped with a measuring cell (type 602). Procedural details have been described elsewere (Fermeglia and Lapasin, 1988). The

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Table 1.	Mole Pe	rcent Puri	ities of	Pure	Components	and
Densities	s, ρ, Com	pared with	h Litera	ature	Values	

component		$ ho / {f g} {f \cdot} {f cm}^{-3}$				
(purity mol %)	<i>T</i> /K	this paper	lit.			
propylene carbonate (99.7)	298.15	1.199 45	1.199 5 ^a			
methyl acetate (>99)	298.15	0.926 63	$0.927 \ 0^{b}$			
ethyl acetate (99.5)	298.15	0.894 38	0.894 55 ^c			
vinyl acetate (>99)	298.15	0.925 77	$0.925 5^d$			
propyl acetate (99)	298.15	0.883 33	0.883 03 ^c			
butyl acetate (99.7)	298.15	0.876 19	0.876 34 ^c			
pentyl acetate (99)	298.15	0.872 58	0.871 9 ^c			
hexyl acetate (99)	298.15	0.868 55	$0.868 \ 42^{e}$			
methyl propanoate (99)	293.15	0.914 89	0.915 0 ^f			
ethyl propanoate (99)	298.15	0.883 33	0.883 1 ^c			
propyl propanoate (99)	293.15	0.881 11	0.880 9 ^f			
butyl propanoate (99)	293.15	0.875 43	$0.875 \ 4^{f}$			
methyl butyrate (99)	293.15	0.898 50	0.898 4 ^f			
ethyl butyrate (99)	298.15	0.873 56	0.873 94 ^c			
propyl butyrate (99)	293.15	0.872 93	0.873 0 ^f			
butyl butyrate (>99)	293.15	0.869 60	0.870 0 ^f			
ethyl pentanoate (99)	298.15	0.869 38	0.869 0 ^f			
ethyl hexanoate (>99)	293.15	0.873 01	0.873 0 ^f			
ethyl heptanoate (99)	293.15	0.881 51	0.881 5 ^f			
ethyl octanoate (99)	298.15	0.862 32	$0.862 \ 4^{f}$			
<i>tert</i> -butyl acetate (>99)	293.15	0.866 30	0.866 5 ^f			
ethyl isobutyrate (99)	293.15	0.868 31	0.868 0 ^f			
isobutyl acetate (99)	293.15	0.871 5	$0.871 \ 2^{f}$			
methyl pentanoate (99)	298.15	0.884 85	0.884 50 ^g			

^{*a*} Moumouzias et al. (1991). ^{*b*} Martin et al. (1994). ^{*c*} Riddick et al. (1986). ^{*d*} Benito et al. (1994). ^{*e*} El-Banna (1997). ^{*f*} Beilstein Handbook. ^{*g*} Ortega et al. (1991).

temperature measurements were precise to ± 0.01 K, and the accuracy of density was better than $\pm 1 \times 10^{-5}$ g·cm^-3.

The flow microcalorimeter (LKB Produkter, model 2107, Bromma, Sweden) used for the H_m^E measurements and the experimental procedure have been described previously (Monk and Wadso, 1968; Francesconi and Comelli, 1986).

Chemicals were pumped into the mixing cell of the calorimeter by means of two automatic burets (ABU 80, Radiometer, Copenhagen, Denmark), and the calorimeter cell was thermostated at (298.15 \pm 0.01) K and controlled by calibrated thermoresistors inside the apparatus.

Mole fractions, x_1 , of propylene carbonate (component 1) have been determined from calibrated flow rates that were

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Table 2 Experimental Excess Molar Enthalpies $H^{\mathbb{C}}$ for Propylene Carbonate (1) + Alkanoate (2) Mixtures at	298 15 K

<i>X</i> 1	$\overline{H_{\mathrm{m}}^{\mathrm{E}}}/\mathrm{J}\boldsymbol{\cdot}\mathrm{mol}^{-1}$	<i>X</i> 1	$\overline{H_{\mathrm{m}}^{\mathrm{E}}}/\mathrm{J}\boldsymbol{\cdot}\mathrm{mol}^{-1}$	X1	$H_{\rm m}^{\rm E}/{\rm J}{\cdot}{ m mol}^{-1}$	Xı	$H_{\rm m}^{\rm E}/{ m J}\cdot{ m mol}^{-1}$	<i>x</i> ₁	$\overline{H_{\mathrm{m}}^{\mathrm{E}}}/\mathrm{J}\boldsymbol{\cdot}\mathrm{mol}^{-1}$	<i>X</i> 1	$\overline{H_{\mathrm{m}}^{\mathrm{E}}}/\mathrm{J}\boldsymbol{\cdot}\mathrm{mol}^{-1}$
0 0376	Q	0 1353	19	Propyle	ene Carbona 24	ate + Methy 0 5849	l Acetate 26	0 7898	20	0 9185	8
0.0726	14	0.1902	23	0.3851	25	0.6526	2.5	0.8493	16	0.9575	5
0.1051	18	0.2384	24	0.4843	25	0.7381	23	0.8826	10	0.0070	0
				Propyl	ene Carbor	nate + Ethyl	Acetate				
0.0460	38	0.1617	104	0.3666	164	0.6345	168	0.8224	108	0.9328	43
0.0879	68 87	0.2244	129	0.4355	175	0.6983	156	0.8741	79	0.9653	22
0.1264	87	0.2787	143	0.5365	1/8	0.7764	129	0.9025	60		
0.0526	64	0 1946	100	Propyle	ene Carbon	ate + Propy	I Acetate	0.8446	196	0 0499	76
0.0530	04 114	0.1640	241	0.4045	308	0.0708	265	0.8440	131	0.9422	40
0.1452	157	0.3117	275	0.5760	323	0.8030	220	0.9157	104	0.0702	40
				Propyl	ene Carbor	nate + Vinvl	Acetate				
0.0435	65	0.1540	184	0.3533	249	0.6211	214	0.8138	124	0.9291	41
0.0834	119	0.2145	220	0.4214	252	0.6860	190	0.8677	86	0.9633	19
0.1202	155	0.2670	238	0.5221	242	0.7662	151	0.8973	65		
				Propyl	ene Carbor	nate + Butyl	Acetate				
0.0609	118	0.2060	322	0.4378	475	0.7002	428	0.8617	269	0.9492	116
0.1148	210	0.2802	399	0.5090	488	0.7570	391	0.9033	205	0.9739	62
0.1629	273	0.3417	432	0.6090	473	0.8105	330	0.9257	162		
0.0000	104	0.0001	400	Propyle	ene Carbon	ate + Penty	I Acetate	0.0750	0.07	0.0540	100
0.0680	164	0.2261	436	0.4071	604 622	0.7245	534 197	0.0122	325	0.9546	136
0.1274	366	0.3688	559	0.5369	602	0.8402	407 399	0.9132	243 194	0.9708	75
0.1707	000	0.0000	000	Dropyl	ono Carbon	$0.010 \pm$	Acotato	0.0001	101		
0 0752	216	0 2453	547	0 4938	ene Carbon 723	1210 + Hexy 0 7453	638	0 8864	419	0 9590	177
0.1398	371	0.2433	636	0.4558	725	0.7455	579	0.8804	298	0.9390	97
0.1960	477	0.3940	684	0.6611	704	0.8541	480	0.9398	249	0.0701	01
				Propylen	e Carbonato	e + Methvl i	Propanoate				
0.0450	38	0.1585	106	0.3611	174	0.6293	173	0.8716	80	0.9314	41
0.0861	68	0.2204	135	0.4298	181	0.6935	158	0.9005	57	0.9645	21
0.1238	89	0.2737	150	0.5309	183	0.7724	129				
				Propyler	ne Carbonat	te + Ethyl F	ropanoate				
0.0535	90	0.1844	236	$0.40\dot{4}\ddot{2}$	363	0.6706	340	0.8906	145	0.9421	76
0.1016	154	0.2533	290	0.4749	376	0.7307	307	0.9156	110	0.9702	39
0.1450	199	0.3114	325	0.5757	374	0.8028	248				
				Propylen	e Carbonat	e + Propyl I	Propanoate				
0.0606	137	0.2052	360	0.4364	527	0.6991	474	0.9029	199	0.9489	104
0.1143	237	0.2791	431	0.5080	545 532	0.7560	420	0.9253	149	0.9738	55
0.1022	505	0.3403	405	0.0077			551				
0.0678	183	0 2255	467	Propyler	ie Carbonat	te + Butyl F 0 7239	ropanoate 592	0 9129	252	0 9545	137
0.0078	310	0.2233	561	0.5381	684	0.7235	523	0.9129	196	0.9767	71
0.1792	396	0.3680	624	0.6361	652	0.8398	412	010002	100	010101	
				Propyle	ne Carbona	te + Methv	Butvrate				
0.0527	79	0.1820	212	0.4004	320	0.6670	299	0.8891	136	0.9413	71
0.1001	137	0.2503	258	0.4710	333	0.7276	272	0.9144	101	0.9697	37
0.1430	177	0.3080	288	0.5718	329	0.8003	221				
				Propyle	ene Carbon	ate + Ethyl	Butyrate				
0.0611	141	0.2066	364	0.4386	536	0.7010	476	0.9036	198	0.9494	109
0.1152	242	0.2809	438	0.5102	541	0.7576	427	0.9259	153	0.9740	56
0.1034	308	0.3424	480	0.0098	529	0.8242	330				
0.0000	100	0 0000	405	Propyle	ne Carbona	ate + Propyl	Butyrate	0.0100	950	0.0540	1 / 1
0.0680	188	0.2260	485	0.4670	692 602	0.7244	591 599	0.9132	258	U.9546 0 0760	141
0.1274	319 415	0.3687	638	0.5368	663	0.7780	520 416	0.9334	193	0.9708	74
5.1101	115	2.0001	000	Duant	no Corbert	1010%	Buturoto				
0.0751	234	0.2451	610	0.4935	ne Carbona 826	ate + Dutyl 0.7451	685	0.9212	315	0.9590	175
0.1397	402	0.3276	712	0.5650	816	0.7958	607	0.9397	237	0.9791	94
0.1959	524	0.3937	773	0.6608	769	0.8539	493				
				Propyler	ne Carbonat	te + Ethvl P	entanoate				
0.0683	189	0.2267	493	0.4680	683	0.7252	586	0.9135	269	0.9548	147
0.1278	323	0.3055	585	0.5398	687	0.7787	526	0.9337	208	0.9769	78
0.1803	416	0.3697	635	0.6376	665	0.8407	422				
				Propyler	ne Carbona	te + Ethyl I	Hexanoate				
0.0753	237	0.2451	606	0.4944	810	0.7458	683	0.9215	307	0.9591	176
0.1401	404	0.3283	710	0.5659	811	0.7964	608	0.9399	243	0.9791	94
0.1964	523	0.3946	175	0.6617	/6/	0.8544	493				

Table 2	. (Continued	l)									
<i>X</i> 1	$H_{\rm m}^{\rm E}/{ m J}{ m \cdot mol^{-1}}$	<i>x</i> ₁	$H_{\rm m}^{\rm E}/{ m J}{ m \cdot mol^{-1}}$	<i>X</i> 1	$H_{\rm m}^{\rm E}/{ m J}{ m \cdot mol^{-1}}$	<i>X</i> ₁	$H_{\rm m}^{\rm E}/{ m J}{ m \cdot mol^{-1}}$	<i>X</i> 1	$H_{\rm m}^{\rm E}/{ m J}{ m \cdot}{ m mol}^{-1}$	<i>x</i> ₁	$H_{\rm m}^{\rm E}/{ m J}{ m \cdot mol^{-1}}$
				Propyle	ene Carbonate	e + Ethyl	Heptanoate				
0.0822	275	0.2639	709	0.5182	898	0.7634	753	0.9281	356	0.9627	204
0.1520	477	0.3497	830	0.5891	889	0.8114	669	0.9451	293	0.9810	110
0.2119	618	0.4176	871	0.6826	849	0.8658	555				
				Propy	lene Carbonat	e + Ethy	l Octanoate				
0.0891	335	0.2812	845	0.5399	957	0.7789	777	0.9337	385	0.9657	228
0.1636	582	0.3698	941	0.6101	920	0.8244	699	0.9494	319	0.9826	121
0.2268	743	0.4389	954	0.7013	854	0.8756	601				
				Propyle	ene Carbonate	e + tert-B	utyl Acetate				
0.0610	141	0.2090	403	0.4423	588	0.7040	513	0.8638	300	0.9501	123
0.1167	255	0.2839	485	0.5139	607	0.7603	454	0.9049	225	0.9744	66
0.1654	339	0.3458	544	0.6133	576	0.8236	368	0.9269	175		
				Propyle	ene Carbonato	e + Ethyl	Isobutyrate				
0.0615	131	0.2076	351	0.4401	531	0.7022	495	0.9041	207	0.9497	109
0.1158	224	0.2821	428	0.5117	554	0.7585	434	0.9263	158	0.9742	56
0.1642	290	0.3438	483	0.6112	535	0.8250	340				
				Propy	lene Carbonat	e + Isobi	ıtyl Acetate				
0.0616	124	0.2081	336	0.4408	480	0.7029	429	0.9044	198	0.9498	110
0.1161	218	0.2828	408	0.5125	493	0.7593	384	0.9266	150	0.9743	61
0.1646	286	0.3445	443	0.6119	474	0.8255	311				
				Propyle	ne Carbonate	+ Methy	l Pentanoate				
0.0604	119	0.2045	328	0.4354	490	0.6982	438	0.9025	187	0.9487	111
0.1139	206	0.2783	403	0.5096	500	0.7552	396	0.9140	175	0.9737	58
0.1616	272	0.3395	447	0.6067	486	0.8223	315				

Table 3. Adjustable Parameters, a_k , Eq 1, and Standard Deviations, $\sigma(H_m^E)$, of Binary Mixtures of Propylene Carbonate + 23 Alkanoates at 298.15 K

mixture	a_0	a_1	a_2	a_3	a_4	$\sigma(H_{\rm m}^{\rm E})/{ m J}{ m \cdot mol^{-1}}$
propylene carbonate						
+ methyl acetate	101.5	12.1	88.7	-83.9		0.4
+ ethyl acetate	713.9	67.6	77.5	-217.4		1.1
+ vinyl acetate	973.2	-307.5	377.3	-316.1	-280.6	1.4
+ propyl acetate	1315.5	92.0				2.8
+ butyl acetate	1939.5	144.0	380.6			3.1
+ pentyl acetate	2462.6	307.6	548.9			4.0
+ hexyl acetate	2889.1	323.9	1144.8	472.5		4.8
+ methyl propanoate	741.8	12.2	25.9	-186.9		1.8
+ ethyl propanoate	1517.4	112.6	94.1	-376.5		2.2
+ propyl propanoate	2176.2	240.8	188.7	-495.1		2.6
+ butyl propanoate	2718.1	374.7	410.6	-269.2		3.9
+ methyl butyrate	1335.4	57.8	142.6	-254.5		2.2
+ ethyl butyrate	2179.9	210.6	244.0	-411.4		3.0
+ propyl butyrate	2776.1	269.7	416.7	-150.7		3.6
+ butyl butyrate	3272.3	248.9	741.6	363.6		4.7
+ ethyl pentanoate	2751.8	225.5	561.8			3.1
+ ethyl hexanoate	3247.5	261.3	801.0	339.0		2.2
+ ethyl heptanoate	3596.1	158.7	1204.0	1117.4		5.4
+ ethyl octanoate	3837.6	-455.0	1751.9	2280.8		6.2
+ <i>tert</i> -butyl acetate	2405.5	74.1	184.5			2.8
+ ethyl isobutyrate	2204.7	341.1	117.6	-386.4		3.7
+ isobutyl acetate	1962.3	72.5	363.7			2.5
+ methyl pentanoate	2006.4	105.2	191.5			2.8

selected to cover the whole mole fraction range. In the extreme points, the measurements were carried out at a flow speed of 0.125 mL/min. The average uncertainty in $H_{\rm m}^{\rm E}$ was estimated to be 1%, and that in mole fraction was $\pm 1 \times 10^{-4}$. Two replicate measurements were made for each point.

Before measurements, the calorimeter was checked using the test mixture cyclohexane + hexane for which literature values are well-known (Gmehling, 1993), and the agreement between ours and literature data was better than 0.5% over the central range of mole fraction of cyclohexane.

Results and Discussion

The H_m^E data are given in Table 2, and their graphical representation is shown in Figure 1. H_m^E values were

fitted to the Redlich-Kister equation

$$H_{\rm m}^{\rm E}/{\rm J} \cdot {\rm mol}^{-1} = x_1 x_2 \sum_{k \ge 0} a_k (x_1 - x_2)^k \tag{1}$$

where a_k are the adjustable parameters obtained by unweighted least-squares regression and x_1 , x_2 are the molar fractions of propylene carbonate and alkanoates, respectively. The parameters a_k and the standard deviations, $\sigma(H_{\rm m}^{\rm E})$, are listed in Table 3.

Figure 1 reports all 23 mixtures. For sake of clarity, only the Redlich–Kister curves are represented and not the experimental points, which in many cases overlap within the limits of the experimental uncertainty.

Mixtures show endothermic mixing in all cases, and H_m^E values exhibit a maximum at a mole fraction close to



Figure 1. Excess molar enthalpies, H_{m}^{E} , of propylene carbonate + 23 alkanoates at 298.15 K, according to their increasing number of C-atoms. Solid lines, Redlich-Kister equation. (a) methyl acetate (3 C-atoms, C_3); (b) vinyl acetate (C_4); (c) propyl acetate, methyl butyrate (C₅); (d) ethyl propionate (C₅); (e) methyl pentanoate, isobutyl acetate, butyl acetate (C₆); (f) ethyl isobutyrate, propyl propanoate, ethyl butyrate (C₆); (g) *tert*-butyl acetate (C₆); (h) pentyl acetate (C₇); (i) butyl propanoate, ethyl pentanoate (C₇); (l) hexyl acetate (C₈); (m) ethyl hexanoate, butyl butyrate (C₈); (n) ethyl heptanoate (C_9); (o) ethyl octanoate (C_{10}).

0.5 increasing as the chain length of the alkanoates is increased. Maximum values range from 26 to 960 J·mol⁻¹.

Figure 1 shows also the grouping of 19 of the 23 mixtures into four sets of structural isomers with 5 to 8 C atoms, respectively. For example, curves c and d refer to the structural isomers with five atoms of carbon. Moreover, curve c refers to $H_{\rm m}^{\rm E}$ data of propylene carbonate + propyl acetate and + methyl butyrate, which overlap (see Table 2).

We see that (1) isoalkanoates show the same $H_{\rm m}^{\rm E}$ of the corresponding alkanoates; (2) within each set of isomers, alkyl acetates have the smallest values of $H_{\rm m}^{\rm E}$; (3) the $H_{\rm m}^{\rm E}$ values of vinyl acetate (four C atoms) follow the same trend of the other compounds as the number of C atoms is increased. However, the double bond leads to a significant increase of H_m^E in comparison to methyl acetate (three C atoms) in mixtures with propylene carbonate. Also asymmetry of the H_m^E vs x_1 curve is evident, in

contrast to the nearly symmetrical curves of saturated alkanoates.

It must be pointed out that vinyl acetate and methyl acetate, in mixtures with dimethyl carbonate, show a calorimetric behavior quite different from that in propylene carbonate (Comelli et al., 1997), with negative $H_{\rm m}^{\rm E}$'s for mixtures containing vinyl acetate and very low positive values for mixtures with methyl acetate.

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Received for review October 17, 1997. Accepted January 28, 1998. JE9702504