Correction

Phase Equilibria of Chlorofluorocarbon Alternative Refrigerant Mixtures.

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J. Chem. Eng. Data **1999**, *44*, 190−192.

1. Equation 7 was incorrectly typeset: The correct equation is

$$b_{12} = (b_1^{1/3} + b_2^{1/3})^3/8$$

2. In Table 3 at $T = 323.15$ K, the pressure of 20.60 bar is incorrect. The correct value should be 28.21 bar.

We thank Dr. R. Stryjek and Dr. K. Malanowski of the Polish Academy of Science for pointing out these errors.

JE000494F

10.1021/je000494f
Published on Web 08/24/2000

New Apparatus for the Fast Determination of High-Pressure Vapor−Liquid Equilibria of Mixtures and of Accurate Critical Pressures.

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J. Chem. Eng. Data **2000**, *45* (2), 265−271.

(1) Equation 15 is incorrect. The correct eq 15 is

$$D = \sum_i \frac{x_i a_i}{RT}\left(\frac{2}{3b_i + c_i}\right) - \frac{G_\gamma^{ex}}{RT} \qquad (15)$$

(2) The optimized parameters for the PT-EoS with the NRTL mixing rule at 313.15 K for the system CO_2 (1) + ethanol (2),

$$\alpha_{ij} = 0.401, \quad \tau_{12}\,(\text{J/mol}) = 112.8251, \quad \tau_{21}\,(\text{J/mol}) = 0.81219, \quad \text{and} \quad k_{12} = 0.4188$$

are incorrect. The correct optimized parameters are

$$\alpha_{ij} = 0.401, \quad \tau_{12}\,(\text{J/mol}) = 1932.33, \quad \tau_{21}\,(\text{J/mol}) = 13.9101, \quad \text{and} \quad k_{12} = 0.4188$$

(3) The supplier for the isobutane is MG Industries (Malvern, PA).

(4) The optimized parameters for the system carbon dioxide + 2-propanol,

$$\alpha_{ij} = 0.350, \quad \tau_{12}\,(\text{J/mol}) = 121.3830, \quad \tau_{21}\,(\text{J/mol}) = 65.2578, \quad \text{and} \quad k_{12} = 0.5153$$

are incorrect. The correct optimized parameters are

$$\alpha_{ij} = 0.350, \quad \tau_{12}\,(\text{J/mol}) = 2074.7158, \quad \tau_{21}\,(\text{J/mol}) = 1124.8813, \quad \text{and} \quad k_{12} = 0.5153$$

JE000498K

10.1021/je000498k
Published on Web 09/29/2000