Relative Permittivities, Speeds of Sound, Viscosities, and Densities of Cyclohexanone + *cis*-Decalin and Cyclohexanone + *trans*-Decalin Mixtures at 283.15, 293.15, and 303.15 K

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Relative permittivities, speeds of sound, viscosities, and densities for the binary mixtures of cyclohexanone + *cis*-decalin and cyclohexanone + *trans*-decalin have been measured over the whole composition range at (283.15, 293.15, and 303.15) K. The excess volumes and the deviations in viscosity, speed of sound, isentropic compressibility, and molar polarization were calculated. The results were fitted to a Redlich–Kister type polynomial equation, and the corresponding parameters have been derived. The Kirkwood correlation factor was also calculated.

Introduction

Studies on excess functions of binary mixtures are of considerable importance in understanding the nature of molecular interactions. Continuing our work for the study of thermodynamic properties of binary organic solutions,^{1,2} we report in this paper the relative permittivities, speeds of sound, viscosities, and densities for the binary mixtures of cyclohexanone + *cis*-decalin and cyclohexanone + *trans*-decalin at (283.15, 293.15, and 303.15) K. From these results the excess volumes and the deviations in viscosity, speed of sound, isentropic compressibility, and molar polarization have been derived. The Kirkwood correlation factor was also calculated using relative permittivity data. All materials used in this work are of industrial interest.

Cyclohexanone is a polar cyclic ketone having relative permittivity $\epsilon = 16.3$ (293.15 K) and dipole moment $\mu = 3.01$ D, and it is used as a solvent for vinyl resins, crude rubber, waxes, fats, and shellac. It also is used for the production of adipic acid and resins. *cis*-Decalin and *trans*-decalin are diastereomer cycloalkanes with zero dipole moment and almost identical relative permittivities, $\epsilon_{cis} = 2.5$ and $\epsilon_{trans} = 2.4$ (293.15 K). Decalin is used as a solvent for naphthalene, fats, resins, oils, and waxes and is often a replacement for turpentine in lacquers, shoe polishes, and floor waxes and also for motor fuel and lubricants. The aim of this work is to test whether the presence of polar molecules of cyclohexanone induces dipoles in the decalin molecules.

Thermodynamic properties of cyclohexanone with alkanes³ and aromatic hydrocarbons⁴ have been reported in the literature. A survey in the literature showed that mixtures of cyclohexanone + *cis*-decalin and cyclohexanone + *trans*-decalin have not been studied.

Experimental Section

Materials. Cyclohexanone (Riedel-de Häen, >99.8%), *cis*-decalin (Merck, >98.0%), and *trans*-decalin (Merck,

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Table 1. Comparison of Experimental Densities (ρ) and Refractive Indices (n_D) of the Pure Liquids with Literature Values at 293.15 K

liquid	$ ho_{(exp)}/g\cdot cm^{-3}$	$ ho_{(ref)}/g\cdot cm^{-3}$	n _{D(exp)}	n _{D(ref)}
cyclohexanone	0.940 20 ^a	0.937 4 ^{a-c}	1.446 1 ^a	1.446 3 ^{a-c}
<i>cis</i> -decalin	0.896 71	$0.896\ 60^d$	1.481 3	1.481 1 ^d
<i>trans</i> -decalin	0.870 01	$0.896 \ 71^{\circ}$ $0.869 \ 00^{d}$	1.469 5	1.480 98 ^c 1.469 3 ^d
		0.869 71 ^e		1.469 32 ^e

 a Values at 303.15 K. b Aralaguppi et al., 1999 (ref 3). c Aralaguppi et al., 1999 (ref 4). d Korosi and Kovats, 1981 (ref 5). e Camin and Rossini, 1955 (ref 6).

> 98.0%) were used without purification. The purity of the liquids was assessed by comparing the experimental densities and refractive indices with the literature values (Table 1).

The binary mixtures were prepared by mass using an electronic balance (Mettler A210P, ± 0.01 mg). The mole fractions were known from ± 0.0001 to ± 0.0005 in all cases.

Measurements. Densities were measured with an Anton Paar (DMA 58) microcomputer controlled precision densimeter with a built-in solid state thermostat. The estimated uncertainty of the measured densities was $\pm 0.000 \ 01$ g·cm⁻³. The DMA cell was calibrated with dry air and doubly distilled water at atmospheric pressure. The sample thermostat was controlled to ± 0.01 K.

Flow times of the solvent mixtures were measured with a viscosity measuring unit (Schott Geräte AVS 310), equipped with an Übbelohde capillary viscometer. The time measurement tolerance was $\pm 0.005\%$, and the display accuracy was ± 0.01 s. The temperature was maintained constant within ± 0.03 K. The viscosities were averaged from four readings. The uncertainty in the viscosity values was ± 0.001 mPa·s.

Relative permittivities were measured by a Hewlett-Packard impedance analyzer (HP 4291A RF). The frequency range was 1 MHz to 1.8 GHz, and the precision in the relative permittivity values was 1%. The calibration

Table 2. Experimental Densities (ρ), Viscosities (η), Speeds of Sound (u), Isentropic Compressibilities (k_s), Relative Permittivities (ϵ), and Kirkwood Correlation Factors (g) of Cyclohexanone (1) + Decalin (2) Mixtures at 283.15, 293.15, and 303.15 K

\mathbf{x}_1	$ ho/{ m g}{ m \cdot}{ m cm}^{-3}$	η /mPa·s	$u/m \cdot s^{-1}$	$k_{\rm s}/{\rm TPa^{-1}}$	ϵ	g	\mathbf{x}_1	$ ho/{ m g}{ m \cdot}{ m cm}^{-3}$	$\eta/mPa\cdot s$	$u/m \cdot s^{-1}$	$k_{\rm s}/{\rm TPa^{-1}}$	ϵ	g
Cyclohexanone (1) + <i>cis</i> -Decalin (2) 283.15 K							Cyclohexanone (1) + <i>trans</i> -Decalin (2) 283.15 K						
0.0000	0.904 40	4.092	1499.4	492	2.4		0.0000	0.877 39	2.578	1439.0	550	2.4	
0.0500	0.905 89	3.971	1495.6	494	2.6	0.520	0.0500	0.879 76	2.562	1438.0	550	2.6	0.534
0.1446	0.908 46	3.788	1488.6	497	3.4	0.803	0.1500	0.884 46	2.540	1435.3	549	3.3	0.721
0.2281	0.911 34	3.643	1483.7	498	4.0	0.767	0.2415	0.889 59	2.534	1435.0	546	4.1	0.780
0.3500	0.916 18	3.458	1477.1	500	5.1	0.774	0.3447	0.896 02	2.543	1435.3	542	5.1	0.803
0.4482	0.920 81	3.332	1473.7	500	6.3	0.814	0.4511	0.903 37	2.570	1436.7	536	6.0	0.767
0.5559	0.926 34	3.218	1470.5	499	8.3	0.919	0.5088	0.907 71	2.592	1438.1	533	6.7	0.781
0.6271	0.930 42	3.156	1469.0	498	9.5	0.939	0.6731	0.921 80	2.686	1444.7	520	8.8	0.790
0.7252	0.936 61	3.089	1468.1	495	11.0	0.932	0.6779	0.922 25	2.689	1444.9	519	9.3	0.843
0.8051	0.942 12	3.050	1468.3	492	12.3	0.925	0.7761	0.932 00	2.769	1452.1	509	10.8	0.842
0.8571	0.946 02	3.033	1469.0	490	13.5	0.944	0.8609	0.941 14	2.852	1458.7	499	12.6	0.873
0.9322	0.952 11	3.019	1470.7	486	15.0	0.945	0.9315	0.949 50	2.932	1466.3	490	13.5	0.843
1.0000	0.957 99	3.018	1473.1	481	16.5		1.0000	0.957 99	3.018	1473.3	481	16.5	
		293	3.15 K						293	3.15 K			
0.0000	0.896 71	3.361	1456.1	526	2.5		0.0000	0.870 01	2.118	1397.1	589	2.4	
0.0500	0.898 08	3.262	1452.3	528	2.7	0.544	0.0500	0.872 29	2.114	1396.1	588	2.6	0.561
0.1446	0.900 51	3.118	1445.3	532	3.4	0.763	0.1500	0.876 76	2.103	1393.3	588	3.2	0.681
0.2281	0.903 33	3.006	1440.4	534	4.0	0.759	0.2415	0.881 85	2.105	1392.8	585	4.0	0.777
0.3500	0.907 98	2.863	1433.8	536	5.0	0.761	0.3447	0.888 12	2.119	1393.0	580	4.9	0.789
0.4482	0.912 49	2.767	1430.6	536	6.2	0.820	0.4511	0.895 32	2.147	1394.4	574	5.9	0.787
0.5559	0.917 90	2.680	1427.3	535	8.1	0.926	0.5088	0.899 60	2.168	1395.7	571	6.5	0.787
0.6271	0.921 90	2.634	1425.9	534	9.3	0.955	0.6731	0.913 42	2.253	1402.0	557	8.5	0.797
0.7252	0.927~92	2.586	1424.9	531	10.5	0.923	0.6779	0.913 78	2.256	1402.5	556	9.1	0.864
0.8051	0.933 33	2.560	1425.2	528	12.2	0.961	0.7761	0.923 40	2.326	1408.4	546	10.5	0.858
0.8571	0.937 20	2.549	1425.9	525	13.3	0.975	0.8609	0.932 39	2.397	1415.6	535	12.1	0.878
0.9322	0.943 12	2.543	1427.7	520	14.8	0.979	0.9315	0.940 61	2.466	1422.7	525	13.0	0.851
1.0000	0.949 11	2.546	1430.2	515	16.3		1.0000	0.949 11	2.546	1430.6	515	16.3	
303.15 K								303	3.15 K				
0.0000	0.889 11	2.641	1412.8	563	2.5		0.0000	0.862 51	1.767	1356.6	630	2.4	
0.0500	0.890 32	2.558	1409.1	566	2.7	0.572	0.0500	0.864 63	1.758	1355.3	630	2.6	0.590
0.1446	0.892 69	2.471	1402.1	570	3.4	0.801	0.1500	0.868 96	1.744	1352.5	629	3.2	0.716
0.2281	0.895 41	2.399	1397.2	572	3.9	0.751	0.2415	0.873 92	1.737	1351.8	626	3.9	0.771
0.3500	0.899 88	2.302	1390.5	575	4.9	0.772	0.3447	0.880 13	1.737	1351.9	622	4.8	0.800
0.4482	0.904 31	2.231	1387.4	574	6.1	0.841	0.4511	0.887 21	1.744	1353.2	616	5.8	0.806
0.5559	0.909 59	2.159	1384.2	574	7.9	0.943	0.5088	0.891 42	1.750	1354.5	611	6.4	0.810
0.62/1	0.913 50	2.115	1382.8	5/3	9.0	0.964	0.6731	0.904 90	1.784	1360.4	597	8.3	0.814
0.7252	0.91941	2.060	1381.9	570	10.4	0.961	0.6779	0.905 33	1.785	1360.7	597	8.9	0.885
0.8051	0.924 /0	2.019	1382.0	566	12.0	0.993	0.7761	0.914 /0	1.815	1366.7	585	10.2	0.8/3
0.85/1	0.928 50	1.995	1383.8	562	13.0	1.000	0.8609	0.923 59	1.848	13/3.4	5/4	11.6	0.881
0.9322	0.934 26	1.904	1385.6	337 559	14.4	1.000	0.9315	0.931 /1	1.880	1380.3	503	12.7	0.873
1.0000	0.940 20	1.915	1388.1	55Z	16.0		1.0000	0.940 20	1.915	1388.3	55Z	16.0	

was carried out by capacitors of standard values (0 S, 0 Ω , and 50 Ω) supplied by the manufacturer.

Experimental details of measurements of density, viscosity, and relative permittivity are the same as those described previously.^{1.2.7}

The speeds of sound were measured with an Anton Paar (DSA 48) sound analyzer. The temperature was maintained constant within ± 0.01 K. The sound analyzer was calibrated with distilled water and air at the experimental temperatures. The uncertainty of the measured speeds of sound was $\pm 1 \text{ m} \cdot \text{s}^{-1}$. The isentropic compressibility (k_s) was calculated from density (ρ) and speed of sound (u) data, as $k_s = 1/(u^2\rho)$.

Results and Discussion

The values of density (ρ) , viscosity (η) , speed of sound (u), isentropic compressibility (k_s) , and relative permittivity (ϵ) are given in Table 2. The calculations of excess molar volumes (V^{E}) and the deviations in viscosity $(\Delta \eta)$, speeds of sound (Δu) , isentropic compressibilities (Δk_s) , and molar polarizations (ΔP) were carried out from the general equation

$$\Delta Y = Y_{\rm m} - \sum c_i Y_i \tag{1}$$

where ΔY refers to $V^{\text{E}/\text{cm}^3 \cdot \text{mol}^{-1}}$, $\Delta \eta/\text{mPa} \cdot \text{s}$, $\Delta k_s/\text{TPa}^{-1}$, $\Delta u/\text{m} \cdot \text{s}^{-1}$, and $\Delta P/\text{cm}^3 \cdot \text{mol}^{-1}$; Y_{m} and Y_i refer to the mixture property and to the respective property of the *i*th pure component; and the term c_i is the mixture composition expressed in mole fraction (x_i) for the calculation of V^{E} , $\Delta \eta$, Δu , and ΔP and in volume fraction (φ_i) for the calculation of Δk_{s} .

The molar polarizations of the mixture (P_m) and of the *i*th pure component (P_i) were calculated using the Clausius–Mossotti equation:⁸

$$P_{\rm m} = \frac{(\epsilon - 1)}{(\epsilon + 2)} \frac{\sum x_i M_i}{\rho}$$
(2)

$$P_i = \frac{(\epsilon_i - 1)}{(\epsilon_i + 2)} \frac{M_i}{\rho_i} \tag{3}$$

where M_i is the molar mass of the *i*th pure component.

The values of V^{E} , $\Delta \eta$, Δu , ΔP , and Δk_{s} were fitted to the Redlich–Kister⁹ equation:

$$\Delta Y = c_1 c_2 \sum_{k=0}^{n} A_k (2c_1 - 1)^k \tag{4}$$

where A_k represent the parameters.



Figure 1. Excess molar volume (V^{E}) versus the mole fraction (x_1) for cyclohexanone (1) + *cis*-decalin (2) mixtures at the following temperatures: \Box , 283.15 K; \bigcirc , 293.15 K; \triangle , 303.15 K.

 Table 3. Parameters of the Redlich-Kister Equation and

 Standard Deviations (d) of Excess Functions of

 Cyclohexanone + cis-Decalin and Cyclohexanone +

 trans-Decalin Mixtures at 283.15, 293.15, and 303.15 K

function	A_0	A_1	A_2	A_3	d
	Cyclohe	exanone +	<i>cis</i> -Decalir	ı	
	5	283.15 H	K		
V ^E /cm ³ ⋅mol ⁻¹	1.4035	-0.4908	0.0442	0.2209	0.0133
∆η/mPa∙s	-1.1192	-0.0071	-0.1116	0.1510	0.0026
$\Delta u/m \cdot s^{-1}$	-57.488	-4.849	-4.672	-2.551	0.1721
$\Delta k_{\rm s}/{\rm TPa^{-1}}$	48.520	-14.188	5.753	-2.887	0.1506
ΔP /cm ³ ·mol ⁻¹	75.911	-1.683	-10.171	-13.168	1.0301
		293.15 H	ζ		
V ^E /cm ³ ⋅mol ⁻¹	1.5420	-0.5036	0.1987	0.2916	0.0115
$\Delta \eta$ /mPa·s	-0.9191	-0.0045	-0.1107	0.1459	0.0026
$\Delta u/m \cdot s^{-1}$	-58.028	-5.043	-6.098	-3.769	0.1902
$\Delta k_{\rm s}/{\rm TPa^{-1}}$	54.296	-15.125	7.845	-2.750	0.1766
$\Delta P / \text{cm}^3 \cdot \text{mol}^{-1}$	69.122	3.533	-11.728	-12.194	0.8885
		303 15 F	ζ		
V ^E /cm ³ ⋅mol ⁻¹	1.6605	-0.5435	0.3393	0.3399	0.0089
$\Lambda n/mPa\cdots$	-0.3275	0.0427	-0.0900	0.4702	0.0051
$\Delta u/m \cdot s^{-1}$	-60.153	-8.158	-4.170	1.110	0.3711
Δk /TPa ⁻¹	61.945	-14.853	6.028	-7.724	0.3122
$\Lambda P/cm^3 \cdot mol^{-1}$	67.002	8.262	-10.177	-20.065	0.8435
	Cyclobox	$anono \pm t$	rane Docal	in	
	Cyclollex	283 15 F	<i>ans</i> -Decar (111	
V ^E /cm ³ ⋅mol ⁻¹	1.2063	-0.4771	-0.1508	-0.0930	0.0115
$\Lambda n/mPa\cdots$	-0.8391	-0.0468	-0.0097	0.0058	0.0004
$\Delta u/m \cdot s^{-1}$	-73.648	-16.063	1.826	14.747	0.3318
$\Delta k_{\rm s}/{\rm TPa}^{-1}$	39.397	-16.295	-0.733	-9.492	0.2597
$\Delta P/cm^3 \cdot mol^{-1}$	69.755	-24.954	-11.975	22.705	0.9728
		203 15 I	7		
$I E/cm^3 mol^{-1}$	1 3159	-0.4716	0.0/19	-0 1024	0.0144
$\Lambda n/mPa \cdot s$	-0 6699	-0.0508	-0.0125	-0.0951	0.0144
$\Delta u/m \cdot s^{-1}$	-73 692	-15883	-6.0120	3 011	0.0011
$\Delta k/TPa^{-1}$	44 922	-15,000	5 112	-7 954	0.2378
$\Lambda P/cm^3 \cdot mol^{-1}$	66 942	-18880	-19672	15 891	0.2070
	00.012	10.000	, 10.012	10.001	0.0402
TÆ/31−1	1 4105	303.15 P	\	0 0000	0.0100
V ^L /cm ³ ·mol ⁻¹	1.4185	-0.4563	0.3376	-0.2293	0.0126
$\Delta \eta$ /mPa·s	-0.3669	-0.0252	-0.0012	0.0016	0.0003
$\Delta u/m \cdot s^{-1}$	-/2.862	-15.048	-8.8/3	2.213	0.1941
$\Delta K_{\rm s}/1Pa^{-1}$	50.257	-15.699	9.245	-11.144	0.218/
$\Delta P/\text{cm}^{3}\cdot\text{mol}^{-1}$	65.150	-14.827	-21.701	5.364	0.8081

A nonlinear least-squares method was used to estimate the parameters A_k . The optimum number of the parameters was obtained through examination of the standard deviation (*d*). The values of A_k and *d* are presented in Table 3.

The $V^{\mathbb{E}}$ values are positive (Figures 1 and 2), the $\Delta \eta$ values are negative (Figures 3 and 4), and both increase with increasing temperature. The positive $V^{\mathbb{E}}$ values indi-



Figure 2. Excess molar volume (V^{E}) versus the mole fraction (x_1) for cyclohexanone (1) + *trans*-decalin (2) mixtures at the following temperatures: **I**, 283.15 K; **O**, 293.15 K; **A**, 303.15 K.



Figure 3. Deviations in viscosity $(\Delta \eta)$ versus the mole fraction (x_1) for cyclohexanone (1) + cis-decalin (2) mixtures at the following temperatures: \Box , 283.15 K; \bigcirc , 293.15 K; \triangle , 303.15 K.



Figure 4. Deviations in viscosity $(\Delta \eta)$ versus the mole fraction (x_1) for cyclohexanone (1) + *trans*-decalin (2) mixtures at the following temperatures: **I**, 283.15 K; **O**, 293.15 K; **A**, 303.15 K. cate that the interactions between like molecules are stronger than the interactions between unlike molecules. The fact that the $\Delta \eta$ values are negative shows that dispersion forces are dominating.

The Δk_s values, presented in Figure 5, are positive and increase with increasing temperature, indicating that the elasticity of the solution is diminished.



Figure 5. Deviations in isentropic compressibility (Δk_s) versus the volume fraction (φ_1) for cyclohexanone (1) + cis-decalin (2) mixtures at the following temperatures: \Box , 283.15 K; \bigcirc , 293.15 K; \triangle , 303.15 K.



Figure 6. Molar polarization (*P*) versus the mole fraction (x_1) for cyclohexanone (1) + *cis*-decalin (2) mixtures at the following temperatures: \Box , 283.15 K; \bigcirc , 293.15 K; \triangle , 303.15 K.

The ΔP values are positive and are approximately independent of temperature. The molecular polarization values *P* increase with the cyclohexanone concentration, as is expected (Figure 6).Figures 5 and 6 refer to cyclohexanone + *cis*-decalin mixtures. The corresponding figures for *trans*-decalin mixtures are not displayed, as they are very similar. It is observed that the values af all properties are lower for mixtures containing *trans*-decalin.This fact can be attributed to the different geometries of the *trans*and *cis*-decalin molecules.

The relative permittivity results were used for the calculation of the Kirkwood¹⁰ correlation factor (g) according to the equation

$$g = \frac{9k_{\rm B}T}{4\pi N\mu^2 x_1} \frac{(2\epsilon + \epsilon_{\infty})^2}{(\epsilon_{\infty} + 2)^2 (2\epsilon + 1)} \left[V \frac{(\epsilon - 1)}{\epsilon} - \frac{3x_2 V_2(\epsilon_2 - 1)}{(2\epsilon + \epsilon_2)} - \frac{3x_1 V_1(\epsilon_{\infty} - 1)}{(2\epsilon + \epsilon_{\infty})} \right]$$
(5)

where μ is the dipole moment of cyclohexanone; V, V_1 , and V_2 are the molar volumes of the mixture, cyclohexanone, and decalin, respectively; ϵ and ϵ_2 are the relative permittivities of the mixture and decalin, respectively; ϵ_{∞} is taken as the square of the refractive index of cyclohexanone; $k_{\rm B}$ is the Boltzmann constant; N is Avogadro's number; and T is the temperature.

The Kirkwood parameter g is a measure of short-range orientational correlations and is expressed as the ratio μ^*/μ , where μ^* is the dipole moment of a sphere where the central molecule has a steady orientation while the other molecules are oriented in the sphere by structural factors, and μ is the dipole moment of the polar molecule in the liquid. The departure of g from unity is a measure of the degree of hindered molecular orientation. Positive deviations from unity indicate parallel alignment of the dipoles of the neighboring molecules, and negative deviations, that antiparallel orientation is favored.^{11,12}

In this work is observed a monotonic increase of the correlation factors with the increase of cyclohexanone molar fraction. The values tend to unity for pure cyclohexanone (Table 2), indicating that the decalin molecules exhibit a structure breaking behavior to the cyclohexanone multimers.

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