Vaporization Studies of Dysprosium Trichloride, Tribromide, and Triiodide

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The vapor pressures of DyCl₃, DyBr₃, and DyI₃ were measured by the torsion method, and the following selected equations were derived in the covered temperature ranges. DyCl₃: log(p/kPa) = 9.31 ± 0.30 - (12523 ± 300)(K/T), (924–1214 K). DyBr₃: log(p/kPa) = 11.47 ± 0.30 - (14344 ± 300)(K/T), (878–1151 K). DyI₃: log(p/kPa) = 11.34 ± 0.20 - (13800 ± 200)(K/T), (889–1157 K). Treating by second- and third-law methods the obtained results, the standard sublimation enthalpies, $\Delta_{sub}H^{\circ}$ (298 K) = 283 ± 5, 289 ± 6, and 282 ± 4 kJ mol⁻¹ for DyCl₃, DyBr₃, and DyI₃, respectively, were determined.

Introduction

Apparently, the early study on the vaporization of DyCl₃ was carried out by Moriarty (1963) by the Knudsen method. At high temperatures, Dudchik et al. (1969) measured the vapor pressure above the molten compound by the "boiling point" method and evaluated its vaporization enthalpy, $\Delta_{vap}H^{\circ}(1472 \text{ K}) = 197 \text{ kJ mol}^{-1}$. Myers and Graves (1977), employing estimated thermodynamic data, calculated the standard sublimation enthalpy of this compound using the Moriarty's vapor pressure data (244 and 297 kJ mol⁻¹, second- and third-law enthalpy values, respectively) and the Dudchik's ones (288 and 319 ± 17 kJ mol⁻¹, secondand third-law enthalpy values, respectively). Myers and Hannay (1980) measured by the Knudsen method two vapor pressure sets from which derived the following second- and third-law standard sublimation enthalpies, $\Delta_{\text{sub}}H^{\circ}(298 \text{ K}) = 303 \text{ and } 313 \pm 12 \text{ kJ mol}^{-1}$, respectively. Incidentally, these values were taken by Pankratz (1984) as source for the compilation of the thermodynamic table for this compound. A vapor pressure set was also measured by Evseeva and Zenkevich (1980) by using the same method. Recently Kudin et al. (1997) and Kuznetsov et al. (1997) using a Knudsen source coupled to a mass spectrometer found that, in addition to monomeric molecules, dimeric and very small amount of trimeric and tetramic molecules were also present in the gaseous phase in the temperature range (850-1010 K). According to their calculations, the Dy₂Cl₆ molar fraction increased with increasing temperature. Employing new thermodynamic functions, the standard enthalpies of DyCl₃ associated to the sublimation in both gaseous forms were derived. It is interesting to note that the standard enthalpy associated with the sublimation process as monomer, $\Delta_{sub}H^{\circ}(298 \text{ K})$ = (272 \pm 5) kJ mol⁻¹, is decidedly lower than that found by Myers and Hannay (1980) and those reported by Pankratz (1984) for the other lanthanide trichlorides, ranging from 306 kJ mol⁻¹ (TbCl₃) to 339 kJ mol⁻¹ (LaCl₃), except for europium trichloride (278 kJ mol⁻¹).

As concerns $DyBr_3$, apparently not many studies on the vaporization of this compound were found in the literature. In particular, the only vapor pressure values were those measured at high temperatures (1220–1535 K) by boiling

points (Makhmadmurodov et al., 1975; Makhmadmurodov et al., 1989) and at lower temperatures (873–1053 K), over the solid phase, by a mass spectrometer (Hilpert et al., 1995). The derived standard enthalpies, $\Delta_{sub}H^{\circ}(298 \text{ K}) = 273 \pm 14 \text{ kJ mol}^{-1}$ (second-law, Makhmadmurodov et al., 1975) and 278.4 \pm 7.4 and 283.9 \pm 11.3 kJ mol⁻¹ (second-and third-law, respectively, Hilpert et al., 1995) are in agreement within their errors. In addition to the monomer, also the presence of a small amount of the dimer form was observed by Hilpert et al. (1995) so that the dissociation process of the dimer was also studied by these authors.

As concerns DyI₃, Hirayama and Castle (1973), from the slope of a mass spectrometric log I⁺T vs 1/T equation, derived a second-law sublimation enthalpy of this compound equal to 290 \pm 7 kJ mol⁻¹ in agreement with a previous value estimated by Feber (1965) (287 kJ mol⁻¹). Later on Hirayama et al. (1975) measured by the Knudsen method new vapor pressure values in the temperature range 895-1045 K from which they derived a standard sublimation enthalpy equal to $286 \pm 1.7 \text{ kJ mol}^{-1}$. A mass spectrometric vapor pressure set was measured by Kaposi et al. (1983). They found that also for dysprosium triiodide, in addition to DyI₃(g), also a small amount of dimer form was present in the vapor in the temperature range 970-1150 K. On the contrary, a mass spectrometric analysis of the vapor carried out by Popovic et al. (1989) showed that the monomer was practically the only gaseous species present in the vapor, but unfortunately in their paper is not reported the covered temperature range.

Considering that the vapor pressure data for dysprosium trichloride, tribromide, and triiodide are scarce, most of which derived by mass spectrometer technique with inevitable uncertainties associated with the method and in particular that the sublimation enthalpy for DyCl₃, recently proposed by Kudin et al. (1997), seems to be low compared to those for the other lanthanide trichlorides, we have studied again these halides and measured their total vapor pressures by the torsion method from which new sublimation enthalpies have been derived.

Experimental Section

The torsion apparatus employed in the present study was substantially the one described in detail in an our previous

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 Table 1. Instrument Constants of the Torsion Cells as

 Obtained in Different Experimental Runs

cell	materials	nominal diameter of the holes (mm)	$K^a imes 10^{-2}$ (kPa rad $^{-1}$)	$K^b imes 10^{-2}$ (kPa rad $^{-1}$)	$K imes 10^{-2}$ average (kPa rad $^{-1}$)
As	steel	1.8	0.394; 0.381;	0.382	0.38
Re	stool	1.0	1 22. 1 28	1 97	1 25
D3	steel	1.0	1.22, 1.20	1.67	1.2.5
Cs	steel	0.3	14.0;14.8; 14.1; 14.1	14.0; 15.1	14.5
Ac	graphite	1.3	0.311; 0.296	0.292	0.30
Bc	graphite	1.0	1.51: 1.60:	1.62: 1.65:	1.60
	0 1		1.56	1.59; 1.65	
Cc	graphite	0.6	3.00; 3.02		3.01
Dc	graphite	0.4	8.81; 8.91; 9.09	8.68; 8.90	8.90

 a Obtained using cadmium as standard. b Obtained using lead as standard.

paper (Piacente et al., 1994). Conventional torsion effusion cells, different for the materials from which were machined and for the nominal area of their effusion holes, were used. For each cell, the instrument constant necessary to convert the experimental torsion angles of the tungsten wire to which the cell is suspended in pressure data was evaluated vaporizing, in separate experiments, standards (cadmium and lead) having well-known vapor pressures (Hultgren et al., 1973). The instrument constants so determined and reported in Table 1 are reproducible within 15-20%, and this produces displacements in the $\log p$ values of about ± 0.1 . The calibration of the used Pt-(Pt-10% Rh) thermocouple was made following the procedure described in the previous work (Piacente et al., 1994) so that the uncertainty in the temperature measurements should not exceed ± 2 K. For torsion angles smaller than about 5°, errors ranging from 20% to 5% of their values were made; errors in the measurements of larger angles were decidedly negligible.

 $DyCl_3$ samples used in this work were supplied by Alfa-Johnson Matthey GmbH (Karlsruhe, Germany) 99.9% pure, $DyBr_3$ by Cerac Inc.(Milwaukee, WI), 99.9% pure, and DyI_3 by Aldrich Chem. Co., 99.99% pure, all percent purities as certified by the suppliers. To minimize oxidation and hydrolysis of the compounds, the cells were loaded in a drybox, rapidly introduced into the torsion apparatus filled with nitrogen, and then quickly evacuated.

Results

A. Dysprosium Trichloride. The total torsion vapor pressures above molten DyCl3 measured by the steel cells increasing and decreasing temperature are reported in Table 2 and Figure 1. Slopes and intercepts of the log *p* vs 1/T equations as obtained by least-squares treatment of the experimental data of each run are reported in Table 3. Some slopes of the log p vs 1/T equations obtained by the cell Cs (having the smallest effusion holes) are slightly higher than the slopes of the other equations obtained by the cells As and Bs. This is not thermodynamically justified (considering the negative value of the difference between the heat capacities of the vapor and liquid phase) but probably could be linked to small errors in temperature measurements when the sample was heated at high temperatures. Not evident temperature dependence of the slopes of the equations obtained using the cells As and Bs was observed. Considering the very good agreement between the absolute vapor pressure data measured by

Table 2. Torsion Total Vapor Pressure of DyCl₃ (in kPa)

	Cell As									
run /	As, 1	run /	run As, 2		run As, 3		run As, 4		run As, 5	
<i>T</i> /K	$-\log p_{ m tot}$	<i>T</i> /K	$-\log p_{\mathrm{tot}}$							
944	3.86	946	3.80	924	4.15	925	4.15	936	4.08	
958	3.66	962	3.58	942	3.89	944	3.85	958	3.75	
971	3.48	972	3.47	961	3.57	958	3.63	975	3.52	
981	3.35	977	3.37	986	3.23	970	3.50	990	3.32	
996	3.16	989	3.22	1003	3.04	983	3.33	1004	3.14	
1007	3.04	1003	3.05	1019	2.85	997	3.16	1023	2.90	
1016	2.92	1013	2.93	1032	2.70	1007	3.02	1043	2.69	
1029	2.78	1023	2.82	1040	2.61	1020	2.82			
1045	2.58	1027	2.77	1049	2.52	1040	2.66			
		1034	2.70	1058	2.46					

Cell B_s

run Bs, 1		run l	Bs, 2	run l	run Bs, 3		
	-log		-log		-log		
<i>T</i> /K	$p_{ m tot}$	<i>T</i> /K	$p_{ m tot}$	<i>T</i> /K	$p_{ m tot}$		
964	3.65	957	3.83	987	3.37		
978	3.47	969	3.65	1000	3.17		
998	3.24	977	3.53	1029	2.82		
1007	3.14	989	3.39	1052	2.53		
1022	2.99	1002	3.24	1063	2.46		
1032	2.81	1015	3.13	1073	2.33		
1038	2.78	1020	3.02	1083	2.24		
1048	2.64	1029	2.94	1091	2.15		
1050	2.64	1035	2.84	1101	2.04		
1064	2.46	1048	2.72	1109	1.97		
1068	2.44	1051	2.66				
1081	2.28	1066	2.50				
1082	2.28	1068	2.47				
1090	2.19	1084	2.28				
1098	2.10	1103	2.13				

Cell Cs

run	Cs, 1	run	Cs, 2	run	Cs, 3	run	Cs, 4	run (Cs, 5
	-log								
<i>T</i> /K	$p_{\rm tot}$	<i>T</i> /K	p_{tot}						
1072	2.50	1086	2.23	1067	2.48	1044	2.80	1054	2.70
1086	2.28	1092	2.16	1096	2.22	1061	2.58	1064	2.58
1090	2.28	1095	2.11	1101	2.14	1083	2.38	1087	2.28
1102	2.08	1106	2.01	1101	2.18	1090	2.32	1107	2.10
1118	1.94	1113	1.97	1120	1.97	1103	2.13	1147	1.69
1126	1.86	1120	1.93	1123	1.95	1123	1.94	1177	1.42
1136	1.75	1128	1.81	1133	1.78	1125	1.90	1204	1.21
1139	1.72	1141	1.71	1134	1.82	1143	1.72	1212	1.14
1148	1.62	1142	1.67	1144	1.72	1158	1.55		
1155	1.56	1152	1.59	1147	1.65	1173	1.44		
1166	1.43	1160	1.53	1153	1.62	1190	1.24		
1168	1.45	1162	1.50	1161	1.52				
1176	1.34	1172	1.41	1165	1.50				
1184	1.28	1178	1.35	1176	1.39				
1192	1.22	1183	1.29	1176	1.40				
1193	1.19	1189	1.25	1185	1.31				
1201	1.14	1194	1.19	1190	1.26				
1205	1.11	1199	1.16	1198	1.20				
				1198	1.20				
				1209	1.14				
				1214	1 07				

different cells, the following equation, representative of the total vapor pressure above liquid $DyCl_3$, was selected weighting proportional to the number points each slope and intercept of the equations reported in Table 3 and giving double weight to the equations obtained by the cells As and Bs:

 $\log(p/kPa) = 9.31 \pm 0.30 - (12523 \pm 300)(K/T)$ (1)

where the overall associated errors were estimated. This equation was compared in Table 4 and Figure 2 with those



Figure 1. Torsion total vapor pressures of DyCl₃.

Table 3. Temperature Dependence of the Total Vapor Pressure of DyX_3 (X = Cl, Br, I)

		no. of		log(<i>p</i> /kPa) =	= A - B/(T/K)
compound	run	points	ΔT (K)	A ^a	B ^a
DyCl ₃ (liq)	As, 1	9	944-1045	9.26 ± 0.08	12376 ± 81
	As, 2	10	946-1034	9.24 ± 0.13	12337 ± 130
	As, 3	10	924 - 1058	9.37 ± 0.22	12460 ± 216
	As, 4	9	925-1040	9.43 ± 0.25	12539 ± 242
	As, 5	7	936-1043	9.60 ± 0.12	12795 ± 122
	Bs, 1	15	964-1098	9.04 ± 0.12	12248 ± 122
	Bs, 2	15	957-1103	$\textbf{8.99} \pm \textbf{0.12}$	12258 ± 119
	Bs, 3	10	987-1109	9.18 ± 0.16	12353 ± 167
	Cs, 1	18	1072 - 1205	9.95 ± 0.14	13304 ± 161
	Cs, 2	18	1086 - 1199	9.07 ± 0.13	12276 ± 153
	Cs, 3	21	1067 - 1214	$\textbf{9.49} \pm \textbf{0.14}$	12815 ± 160
	Cs, 4	11	1044 - 1190	9.83 ± 0.17	13201 ± 194
	Cs, 5	8	1054 - 1212	9.20 ± 0.17	12518 ± 190
DyBr ₃ (sol)	Ac, 1	7	936-1043	11.56 ± 0.13	14308 ± 125
	Ac, 2	11	878-1038	11.14 ± 0.14	13922 ± 138
	Ac, 3	8	919-1038	11.43 ± 0.07	14223 ± 67
	Bc, 1	9	950 - 1040	11.22 ± 0.11	14729 ± 107
	Bc, 2	10	917-1039	11.23 ± 0.10	13951 ± 103
	Cc, 1	9	965 - 1043	12.01 ± 0.09	14651 ± 87
	Cc, 2	10	954 - 1060	11.44 ± 0.31	14207 ± 312
	Cc, 3	10	965 - 1062	11.75 ± 0.31	14546 ± 310
	Cc, 4	8	956 - 1036	11.64 ± 0.21	14403 ± 206
	Dc, 1	9	1030 - 1151	11.34 ± 0.13	14307 ± 138
	Dc, 2	8	1037 - 1145	11.60 ± 0.26	14692 ± 282
DyI ₃ (sol)	Ac, 1	14	889-1015	11.18 ± 0.08	13648 ± 79
	Ac, 2	11	898-1000	11.15 ± 0.14	13664 ± 130
	Ac, 3	15	936-1023	11.30 ± 0.05	13795 ± 45
	Bc, 1	12	940 - 1027	11.29 ± 0.19	13871 ± 184
	Bc, 2	8	987-1060	11.78 ± 0.22	14086 ± 223
	Cc, 1	9	1002 - 1078	11.34 ± 0.10	13713 ± 108
	Cc, 2	12	982 - 1089	11.30 ± 0.16	13832 ± 173
	Cc, 3	10	996 - 1081	11.41 ± 0.20	13995 ± 210
	Cc, 4	11	981-1086	11.35 ± 0.16	13960 ± 168
	Dc, 1	15	1026 - 1157	11.28 ± 0.12	13517 ± 130
	Dc, 2	8	1013-1123	11.67 ± 0.18	13998 ± 187

^a The quoted errors are standard deviations.

reported in the literature. Our pressure data are in better agreement with those reported by Dudchik et al. (1969) and by Evseeva and Zenkevich (1980).

B. Dysprosium Tribromide. In Table 5 and Figure 3 are reported the total vapor pressure values measured above solid $DyBr_3$ by graphite cells. In Table 3 are reported log(p) vs 1/T equations obtained in each experimental run. Contrary to trichloride, all the slopes of the equations determined by different torsion cells in different temperature ranges were found comparable enough within their standard deviations. The pressures measured by the cell Dc are slightly lower than those measured by other cells. In the overall temperature range covered in our experiments (878 to 1151 K), the total vapor pressure of tribro-

mide can be expressed by the following equation evaluated as for DyCl₃:

$$\log(p/kPa) = 11.47 \pm 0.30 - (14344 \pm 300)(K/T) \quad (2)$$

where the associated errors were estimated. This equation was compared in Table 4 and Figure 4 with those reported in the literature. Taking into account the contribution of the heat of fusion, our data seem to be in better agreement with the results reported by Makhmadmurodov et al. (1975).

C. Dysprosium Triiodide. Despite the certified purity, the vaporization of about 4-5% of the original weight of the sample due to the vaporization of unidentified impurities was observed at about 500 K; of course, this vaporization step was neglected in the subsequent runs. On increasing the temperature, the vapor pressure falls below the instrument sensitivity so that the pressures measured at higher temperatures were considered representative of the vapor pressures above practically pure DyI₃. In Tables 3 and 6 and in Figure 5 were reported the obtained results. The log p vs 1/T equations so determined are in agreement between themselves even though, contrary to that observed in the measurements above DyBr₃, the pressures measured by the cell Dc are slightly higher than those measured by the other cells. From these equations, the following one, representative of the total vapor pressure of DyI₃ in the temperature range 889 to 1157 K, was selected:

$$\log(p/kPa) = 11.34 \pm 0.20 - (13800 \pm 200)(K/T) \quad (3)$$

where the associated errors were estimated. This equation and those found in the literature were reported in Table 4 and in Figure 6 for comparison. Even though the absolute pressure data are decidedly in agreement with those found in the previous works [Hirayama et al. (1975) and Kaposi et al. (1983)], the slope of our selected eq 3 seems to be slightly lower.

Discussion

A. Dysprosium Trichloride. Considering that a small dimer amount is present in the vapor in the temperature range covered in our experiments, the partial pressures of the monomer were calculated at 50 K intervals in the temperature range 1000-1200 K from the total vapor pressures derived from eq 1 and the dimer percents evaluated from the mass spectrometric results reported by Kuznetsov (1997). These pressures are in Table 7. The second-law vaporization enthalpy of this compound in monomer form, $\Delta_{vap}H^{\circ}(1069 \text{ K}) = 238 \pm 6 \text{ kJ mol}^{-1}$, was derived from the slope of the equation, $log(\bar{p}DyCl_3/kPa) =$ $9.19 \pm 0.30 - (12425 \pm 300)(K/T)$, obtained treating the DyCl₃ partial pressures by least squares. The errors were considered equal to those associated to the selected eq 1. The enthalpic value was reported to 298 K, $\Delta_{sub}H^{\circ}(298 \text{ K})$ = 287 ± 6 kJ mol⁻¹, by 9 kJ mol⁻¹ (needed to convert $\Delta_{vap}H^{o}$ from 1069 K to melting point 924 K), by the heat of fusion equal to 25.5 kJ mol⁻¹ [value calorimetrically obtained by Dworkin and Bredig, 1971 (25.5 kJ mol⁻¹), and from the second-law sublimation and vaporization enthalpies reported by Kudin et al., 1997, both corrected at 924 K (25.4 \pm 6 kJ mol⁻¹)] and by 14.6 kJ mol⁻¹ [difference of the enthalpic increments for solid and gaseous compound from the melting point to 298 K, Pankratz, 1984]. The standard sublimation enthalpy of DyCl₃ was also calculated by the third-law method using two sets of free energy function, $\Delta \{ [G^{\circ}(T) - H^{\circ}(298 \text{ K})]/T \} = \Delta \text{fef, those reported in}$ Pankratz's tables and those derived from the Kudin's

Table 4.	Temperature D	ependence of	f the Total V	Vapor Pressure	e of DyX ₃	$(\mathbf{X} = 0)$	C l , Br ,	I)
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compound	method	$\Delta T/K$	total vapor pressure
DyCl ₃	Knudsen	1023-1123	$\log(p/kPa)^a = 8.56 - 11025(K/T)$
	boiling point	1325 - 1620	$\log(p/kPa)^b = 29.873 - 15066(K/T) - 6.0 \log(T/K)$
	Knudsen	924-1031	$\log(p/kPa)^{c} = 10.06 - 13459(K/T)$
	Knudsen	973-1073	$\log(p/kPa)^d = 7.65 - 10668(K/T)$
	mass spectrom.	850-924	$\log(p/kPa)^{e,1} = 10.84 - 13458(K/T)$
	mass spectrom.	924-1010	$\log(p/kPa)^{e,2} = 9.18 - 11922(K/T)$
	this work	924-1214	$\log(p/kPa) = 9.31 \pm 0.30 - (12523 \pm 300)(K/T)$
$DyBr_3$	boiling point	1220 - 1535	$\log(p/kPa)^{f} = 26.02 \pm 0.11 - (13349 \pm 72)(K/T) - 5 \log(T/K)$
	mass spectrom.	803-1053	$\log(p/kPa)^g = 11.54 - 13942(K/T)$
	this work	878-1151	$\log(p/kPa) = 11.47 \pm 0.30 - (14344 \pm 300)(K/T)$
DyI_3	Knudsen	843-1060	$\log(p/kPa)^h = 11.80 \pm 0.14 - (14085 \pm 133)(K/T)$
Ū I	mass spectrom.	970-1150	$\log(p/kPa)^{i} = 12.704 - 15023(K/T)$
	this work	889-1157	$\log(p/kPa) = 11.34 \pm 0.20 - (13800 \pm 200)(K/T)$

^{*a*} Evaluated by us from four points reported by Moriarty (1963). ^{*b*} Dudchik et al. (1969). ^{*c*} Evaluated by us from the vapor pressure data reported by Myers and Hannay (1980). ^{*d*} Evseeva and Zenkevich (1980). ^{*e*}. ^{*i*,*e*,2} Calculated by us from the slopes and intercepts of the temperature-partial pressure equations for DyCl₃(g) and Dy₂Cl₆(g) reported by Kudin et al. (1997) and Kuznetsov et al. (1997) over the solid (e,1) and molten DyCl₃ (e,2), respectively. ^{*f*}Makhmadmurodov et al. (1975). ^{*g*} Calculated by us from slopes and intercepts of the temperature-partial pressure equations for DyBr₃(g) and Dy₂Br₆(g) reported by Hilpert et al. (1995). ^{*h*} Hirayama et al. (1975). ^{*i*} Calculated by us from the vapor pressure values reported by Kaposi et al. (1983).



Figure 2. Comparison of the total vapor pressures of $DyCl_3$ with the literature data.



Figure 3. Torsion total vapor pressures of DyBr₃.

thermodynamic data. The obtained results are in Table 7. The third-law sublimation enthalpies obtained using Kudin's free energy functions do not present an appreciable temperature trend and their average value, $\Delta_{vap}H^{*}(298 \text{ K}) = 281 \text{ kJ mol}^{-1}$, agrees within the uncertainties with the second-law one. Giving more weight to the third-law results, we propose as the standard sublimation enthalpy of DyCl₃ the value 283 kJ mol⁻¹ with an estimated error that could not exceeded $\pm 5 \text{ kJ mol}^{-1}$. This selected value is slightly higher than the Kudin's results (270 \pm 4 and 272 \pm 6 kJ mol⁻¹ second- and third-law values, respectively) and then the standard enthalpy values obtained



Figure 4. Comparison of the total vapor pressures of $\rm DyBr_3$ with the literature data.

treating the previous vapor pressure data reported in the literature by Kudin's thermodynamic functions [272 \pm 10 kJ mol⁻¹ (second-law), Moriarty (1963); 278 \pm 9 and 277 \pm 10 kJ mol⁻¹ (second- and third law, respectively), Dudchik et al. (1969); 250 \pm 7 and 275 \pm 10 kJ mol⁻¹ (second- and third-law, respectively), Evseeva and Zenkevich (1980)].

B. Dysprosium Tribromide. Also, the monomer partial pressures of this compound were calculated from selected eq 2 and the dimer amount present in the vapor was evaluated from the data reported by Hilpert (1995). The DyBr₃ pressures so calculated at 100 K intervals in the temperature range 800-1100 K are in Table 8. These values fit well on the linear equation: $\log(\bar{p}DyBr_3/kPa) =$ $11.29 \pm 0.30 - (14200 \pm 300)(K/T)$. The associated errors are those in eq 2. From the slope of this equation, the second-law sublimation enthalpies of DyBr₃, $\Delta_{sub}H^{\circ}(1015)$ K) = 272 \pm 6 kJ mol^{-1} and $\Delta_{sub} H^{*}(298\ \text{K})$ = 289 \pm 6 kJ mol^{-1} , were obtained. The enthalpic increment value, $\Delta[H^{\circ}(1015 \text{ K}) - H^{\circ}(298 \text{ K})](\text{gas} - \text{cr}) \text{ equal to } -17 \text{ kJ mol}^{-1},$ was evaluated as the difference of the enthalpic increment reported by Pankratz (1984) for the gaseous compound, and the enthalpy increment for the solid compound obtained by the heat capacities, $C_p/(\text{J mol}^{-1} \text{ K}^{-1}) = 95.02 \pm 0.11 +$ (17.5 ± 0.2) 10⁻³*T*, calorimetrically measured by Elsam and Preston (1992). The standard enthalpy so obtained is within the error comparable with that selected by Hilpert et al. (1995) $[\Delta_{sub}H^{\circ}(298 \text{ K}) = 281.1 \pm 6.2 \text{ kJ mol}^{-1}]$. It is interesting to note that previously Myers and Graves

Table 6. Torsion Total Vapor Pressure of DyI₃ (in kPa)

	Cell Ac						
run Ac, 1			run Ac, 2			run A	c, 3
<i>T</i> /K	-log	$p_{\rm tot}$	<i>T</i> /K	$-\log p_t$	tot T/	T/K –log p _{tot}	
936	3.7	3	878	4.75	91	19	4.05
942	3.6	3	901	4.45	93	36	3.75
977	3.0	/ 3	920 940	4.05	96	50 74	3.37
1002	2.5	3 7	954 954	3.47	98	89	2.95
1026	2.4	0	968	3.27	100)5	2.72
1043	2.1	5	981	3.07	102	25	2.44
			994	2.88	103	38	2.26
			1007	2.69			
			1020	2.26			
			Cel	l Bc			
	run I	Bc, 1			run	Bc, 2	
T	ľΚ	-log	$g p_{ m tot}$	T	K	-log	g $p_{ m tot}$
9	50	3.	69	9	17	3.	99
9	163	3.	4/ 39	9	129 154	3.	30
g	83	3.	32 17	9	67	3.	21
9	93	2.	99	9	80	3.	01
10	04	2.	85	9	91	2.	85
10	20	2.	62	10	04	2.	68
10	131	2.	47 37	10	15 97	2. 2	37
10	10	2.	01	10	39	2.	18
			Cal				
run	Cc. 1	run	Cc. 2	run	Сс. 3	run	n Cc. 4
<i>T</i> /K	$-\log p_{tot}$	<i>T</i> /K	$-\log p_{tot}$	<i>T</i> /K	$-\log p_{tot}$	<i>T</i> /K	$-\log p_{tot}$
965	3.17	954	3.45	965	3.37	956	3.45
977	2.99	981	3.03	977	3.15	968	3.25
988	2.81	993	2.87	989	2.94	976	3.11
998	2.66	1005	2.70	980	3.11	989	2.92
1016	2.33	1017	2.30	1000	2.67	1014	2.75
1024	2.30	1036	2.30	1018	2.52	1027	2.40
1034	2.16	1044	2.20	1028	2.38	1036	2.27
1043	2.03	1052	2.07	1036	2.26		
		1000	1.90 Cel	1002	2.00		
	run	Dc, 1		I Dt	run	Dc, 2	
T	γĸ	-log	$g p_{tot}$	T	ΪK	-log	$g p_{tot}$
10	30	2.	57	10	37	2.5	567
10	41	2.	39	10	58	2.2	266
10	153	2.	27	10	070 101	2.1	169
10	175	1.3	97 83	10	98	1.3	905 754
11	.02	1.	64	11	12	1.0	613
11	18	1.	45	11	28	1.421	
11	.33	1.	29	11	45	1.2	235
11	51	1.	11				
(1077) using t	ho pro	seuro-to	mnora	turo ogu	ation 1	conortod
hv Ma), using t akhmadn	nurodo	vetal ((1975) a	and esti	mated	thermo-
dynar	nic funct	ions. d	lerived t	wo sta	ndard si	ublima	tion en-
thalp	v values.	$\Lambda_{aub}H$	°(298 K)	= 278	k.J mol-	1 and 2	294 + 17
k.J mo	ol^{-1} (seco	nd- an	d third-l	aw. res	spectivel	v) also	compa-
rable	with ou	r resu	lt. Trea	ting by	v third-	law pr	ocedure
$\Delta_{\rm sub}H$	°(298 K)	deter	mined i	n the	present	work	and the
DyBr	3 partial	pressu	res, the	free en	ergy fun	nction o	hanges,
∆fef =	$= \Delta \{ [G^{\circ}($	(T) - H	₽°(298 K	$]/T$ {g	as – cr)	, assoc	iated to
the su	ıblimatio	on reac	tion wer	e calcu	ılated. K	nowin	g the fef
select	ed by Ba	arin (1	993) for	DyBr ₃	(g), the	fef va	lues for
solid	DyBr ₃ w	ere so	evaluat	ed at t	he temp	oeratur	re range
800-	1100 K a	and rep	ported in	n Table	e 8. It is	intere	sting to
note t	note that a rough extrapolation at 1400 K of Δ fef, gave a						

			Cel	l Ac				
run Ac, 1			run Ac, 2			run A	c, 3	
<i>T</i> /K	-log	p_{tot}	<i>T</i> /K	$-\log p$	tot T/H	ζ -	-log p _{tot}	
889	9 4.1	7	898	4.06	93	6	3.44	
900) 3.9	8	906	3.90	94	6	3.29	
912	2 3.7	'9	9 917		95	2	3.20	
924	4 3.5	6	932	3.53	95	6	3.13	
93	7 3.3	9	940	3.41	96	3	3.02	
94	5 3.2	6	946	3.31	96	8	2.95	
954	4 3.1	4	949	3.23	97	3	2.89	
962	2 3.0	1	958	3.10 97		9	2.79	
97	1 2.8	9	977	2.85	98	6	2.70	
980) 2.7	5	991	2.63	99	1	2.62	
989	9 2.6	3	1000	2.51	99	7	2.54	
99	7 2.5	0			100	4	2.45	
100	3 2.3	8			100	9	2.37	
101	5 2.2	5			101	6	2.27	
					102	3	2.19	
			Cel	l Bc				
run Bc, 1					run	Bc, 2		
	[/K	-log	$g p_{tot}$	7	7K	-lo	g p_{tot}	
	940	3	49	ç	987	2	47	
	952	3	27	ç	999	2	35	
	958	3	19	1010		2	17	
	966	3	09	1019		2.05		
	973	2	97	1029		1.91		
	980	2	2.37		1020		1.01	
	987	2 75		1051		1.63		
	995	2.75		1060		1.50		
1	003	2	53			-		
1	010	2	49					
1	019	2.	34					
1	027	2.	22					
			Cel	l Cc				
ru	n Cc, 1	run	Cc, 2	rur	n Cc, 3	rur	n Cc, 4	
<i>T</i> /K	$-\log p_{tot}$	<i>T</i> /K	$-\log p_{tot}$	<i>T</i> /K	-log p _{tot}	<i>T</i> /K	$-\log p_{tot}$	
1002	2.31	982	2.77	996	2.57	981	2.91	
1015	2.16	995	2.61	1007	2.46	992	2.71	
1028	2.01	1006	2.46	1020	2.27	1001	2.61	
1038	1.88	1016	2.31	1030	2.16	1010	2.46	
1045	1.79	1028	2.16	1040	2.01	1021	2.31	

1.4	1	
	Cell	Dc

1047

1054

1063

1072

1081

1.91

1.83

1.71

1.60

1.48

1029

1038

1050

1061

1071

1086

2.23

2.10

1.97

1.82

1.68

1.50

1.70

1.60

1.48

1.38

1053

1060

1070

1078

_

1039

1046

1056

1064

1073

1081

1089

2.01

1.93

1.79

1.68

1.63

1.46

	een	20				
r	un Dc, 1	run Dc, 2				
<i>T</i> /K	$-\log p_{\rm tot}$	<i>T</i> /K	$-\log p_{tot}$			
1026	1.87	1013	2.15			
1039	1.72	1028	1.97			
1050	1.60	1043	1.75			
1053	1.56	1058	1.56			
1062	1.44	1072	1.37			
1073	1.34	1085	1.22			
1085	1.20	1102	1.03			
1096	1.08	1123	0.82			
1103	0.99					
1115	0.85					
1123	0.76					
1132	0.64					
1141	0.55					
1149	0.49					
1157	0.39					

value (–185 \pm 2 J K^{-1} mol^{-1}) equal to that estimated by Myers and Graves (1977) $(-186 \text{ J K}^{-1} \text{ mol}^{-1})$. From the fef

Table 7. Third-Law Partial Standard Sublimation Enthalpy of DyCl₃ in Monomeric Form

<i>T</i> (K)	p _{tot} ^a (kPa)	<i>x</i> Dy ₂ Cl ₆ ^b	₽DyCl₃ (kPa)	Δ fef (Kudin) (J K ⁻¹ mol ⁻¹)	∆ _{sub} <i>H</i> ° (298 K) (kJ mol ^{−1})	Δ fef (Pankratz) (J K ⁻¹ mol ⁻¹)	$\Delta_{sub}H^{\circ}$ (298 K) (kJ mol ⁻¹)
1000 1050 1100 1150 1200	$\begin{array}{c} 6.1\times10^{-4}\\ 2.4\times10^{-3}\\ 8.4\times10^{-3}\\ 2.6\times10^{-2}\\ 7.5\times10^{-2} \end{array}$	4.7 5.5 6.4 7.3 8.2	$\begin{array}{c} 5.8\times10^{-4}\\ 2.3\times10^{-3}\\ 7.9\times10^{-3}\\ 2.4\times10^{-2}\\ 6.9\times10^{-2} \end{array}$	-180.7 -178.8 -176.9 -175.1 -173.3	281.0 281.1 281.1 281.0 280.7	$\begin{array}{r} -209.15 \\ -206.95 \\ -204.82 \\ -202.74 \\ -200.74 \end{array}$	309.4 310.7 311.8 312.8 313.7

^a As calculated from eq 1. ^b Dy₂Cl₆ % from Kuznetsov partial pressure data (1997).

Table 8. Thermodynamic Functions, fef = $[G^{\circ}(T) - H^{\circ}(298 \text{ K})]/T$ and $S^{\circ}(298 \text{ K})$ for Solid DyBr₃ from Third-Law Treatment of Its Vapor Pressures $[\Delta_{sub}H^{\circ}(298 \text{ K}) = (289 \pm 6) \text{ J K}^{-1} \text{ mol}^{-1}]$

<i>T</i> (K)	$p_{tot}{}^a$ (kPa)	<i>x</i> Dy ₂ Br ₆ ^b	<i>̄</i> pDyBr₃ (kPa)	Δfef (J K ⁻¹ mol ⁻¹)	fefDyBr ₃ (g) ^c (J K ⁻¹ mol ⁻¹)	fefDyBr ₃ (s) (J K ⁻¹ mol ⁻¹)	<i>S</i> °(298 K) (J K ⁻¹ mol ⁻¹)
800	$3.47 imes10^{-7}$	1.3	$3.42 imes 10^{-7}$	-199.1	-433.3	-234.19	197.2
900	$3.41 imes10^{-5}$	3.0	$3.30 imes10^{-5}$	-197.0	-439.6	-242.64	197.7
1000	$1.34 imes10^{-3}$	7.0	$1.24 imes10^{-3}$	-195.0	-445.6	-250.60	198.0
1100	$2.69 imes10^{-2}$	12.0	$2.37 imes10^{-2}$	-193.2	-451.2	-257.97	198.1

^a As calculated from eq 2. ^b Dy₂Cl₆ % from Kuznetsov partial pressure data (1997). ^c Selected by Barin (1993).



Figure 5. Torsion total vapor pressures of DyI₃.



Figure 6. Comparison of the total vapor pressures of DyI_3 with the literature data.

of solid DyBr₃ so determined and C_p measured by Elsam and Preston (1992), the absolute entropy at 298 K of this compound was derived (see Table 8). The average value, $S^{\circ}(298 \text{ K}) = 198 \text{ J} \text{ mol}^{-1} \text{ K}^{-1}$, was selected with an error of $\pm 10 \text{ J} \text{ mol}^{-1} \text{ K}^{-1}$ roughly estimated considering the uncertainties in the standard sublimation enthalpy value, in the fef for DyBr₃(g) and in the evaluation of DyBr₃(g) partial pressures (linked both to errors in our experimental total vapor pressures and in the evaluation of the monomer amount present in the vapor). This entropy value is comparable with those reported by Pankratz (1984) for

Table 9. Standard Sublimation Enthalpies of LanthanideTrihalides Derived from the Enthalpies of FormationReported by Pankratz (See Text)

$\Delta_{\rm sub} H^{\circ}(298 \text{ K})/\text{kJ mol}^{-1}$						
Ln	LnF ₃	LnCl ₃	LnBr ₃	LnI ₃		
La	435	338	303	279		
Ce	440	330	286	278		
Pr	431	325	297	275		
Nd	440	323	295	273		
Sm	428					
Eu	436	278				
Gd	452	312	297	277		
Tb	445	306		274		
Dy	446	313				
Ďy		287 ± 5^a	289 ± 6^a	282 ± 4^{a}		
Ho	455	323	292			
Er	449	320				
Tm	440					
Yb	444					
Lu	435					

^a This work.

tribromides of some lanthanides, values ranging from 178 J mol⁻¹ K⁻¹ (lanthanum) to 207 J mol⁻¹ K⁻¹ (cerium).

C. Dysprosium Triiodide. For this compound, the presence of dimer form in the vapor in the covered temperature range was considered negligible so that its second-law sublimation enthalpies, $\Delta_{sub} H^{\circ}(1023 \text{ K}) = 264$ \pm 4 kJ mol⁻¹ and $\Delta_{sub}H^{\circ}(298 \text{ K}) = 282 \pm 4 \text{ kJ mol}^{-1}$, were determined from the slope of the selected eq 3. ΔC_p equal to -24 J mol⁻¹ K⁻¹ (Kaposi et al., 1983) was used in the extrapolation of the sublimation enthalpy to 298 K. The enthalpy value selected in the present work is comparable with that estimated by Feber (1965) 287 kJ mol⁻¹ and with those measured by Hirayama and Castle (1973) (290.4 \pm 6.7 kJ mol^{-1}) Hirayama et al. (1975) (286.2 \pm 2.5 kJ mol}{-1}), and Kaposi et al. (1983) (292 \pm 12 kJ mol⁻¹). The value is comparable also with the standard sublimation enthalpies for triiodides of some lanthanides (see Table 9) as derived from the Pankratz's Tables.

Conclusion

The standard sublimation enthalpies of DyCl₃, DyBr₃, and DyI₃ determined in the present work, $\Delta_{sub}H^{\circ}(298 \text{ K})$ = 283 ± 5, 289 ± 6, and 282 ± 4 kJ mol⁻¹, respectively, are decidedly comparable. This is in contrast with the evident trend of the standard sublimation enthalpies for trihalides of some lanthanides (going from trifluorides to

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triiodides) evaluated as the difference between the heats of formation of solid and gaseous compounds reported by Pankratz (1984) (see Table 9). It is interesting to note that the standard sublimation enthalpy value of DyCl₃ is also lower than those for trichlorides of other lanthanides. Considering that the major difference with the Pankratz data was observed for DyCl₃, we have further studied this compound and carried out several vaporization runs. The obtained results (see Figure 1) are decidedly reproducible, and a critical analysis of the errors associated with the standard sublimation enthalpy values determined by second- and third-law treatment of the vapor pressure data shows that those are minor. In fact, as concerns the secondlaw $\Delta_{sub} H^{\circ}(298 \text{ K})$ value, taking into account the large number of the experimental points obtained by different cells and the negligible uncertainties in temperature and torsion angle measurements, the error associated with the vaporization enthalpy of liquid DyCl₃ is very small (decidedly smaller than that overestimated, $\pm 6 \text{ kJ mol}^{-1}$). Also minor could be the errors associated with the heat of fusion (considering the agreement of the data reported in the literature) and the enthalpic increment (comparable enough with those for other lanthanide trichlorides) used to report the vaporization enthalpy at 298 K. On this basis, we believe that an overall error of 10 kJ mol⁻¹ is decidedly the maximum uncertainty in the second-law enthalpy.

The third-law $\Delta_{sub} H^{\circ}(298 \text{ K})$ values evaluated employing Kudin's Δ fef could be decidedly more reliable than those obtained using Pankratz's ∆fef, considering their comparison with the second-law result and the evident temperature trend of Pankratz's enthalpies (see Table 7). This could be due to the use of erroneous Δ fef values, and it should cause the suspicion that also the sublimation enthalpies of other trichlorides derived from Pankratz's table may be in error primarily for erroneous Δ fef. Also, the corrections of the total pressure values for the presence in the vapor of different amounts of dimer in the evaluation of DyCl₃ partial pressures do not produce appreciable change of the final third-law enthalpy value. On this basis, we are persuaded that the error associated with the third-law sublimation enthalpy could be considered more minor than that overestimated for the second-law enthalpy.

This critical analysis of our results on DyCl₃ and the agreement of our final enthalpy value with those of other authors (see previous discussion) induce us to believe that the proposed sublimation enthalpy of DyCl₃, $\Delta_{sub}H^{\circ}(298 \text{ K}) = 283 \pm 5 \text{ kJ mol}^{-1}$, is reliable enough and that those of other trichlorides derived from Pankratz's table could be considered upper limits so that new measurements of sublimation enthalpies of these compounds are necessary.

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