

Solubility of Behenic Acid in Supercritical CO₂ with *n*-Pentane or *n*-Octane Cosolvents

Bing Guan, Zhimin Liu, Buxing Han,* and Haike Yan

Institute of Chemistry, Chinese Academy of Sciences, Beijing 100080, People's Republic of China

Solubilities of behenic acid in supercritical (SC) CO₂ with *n*-pentane or *n*-octane cosolvents were measured at 308.15 K, 318.15 K, and 328.15 K in the pressure range from 9.0 MPa to 16.0 MPa and cosolvent concentration range from 0 mol % to 7.5 mol %. The effects of cosolvent concentration, pressure, and temperature on solubility were investigated.

Introduction

Supercritical fluids (SCFs) possess extraordinary properties including high diffusivity, low viscosity, and high compressibility, which make them attractive solvents for many industrial processes. Supercritical (SC) CO₂ is the most popular among SCFs because it is nontoxic, nonflammable, and easy to obtain and has a near-ambient critical temperature. However, the solubility of some strongly polar substances in SC CO₂ is very low, which has become an obstacle for its utilization.

Many researchers have studied the effects of polar cosolvents on the solubilities of polar organic compounds in SC CO₂ (Guan et al., 1998a,b, 1999; Zhong et al., 1997; Koga et al., 1996; Johannsen and Brunner, 1995; Foster et al., 1993; Gurdial et al., 1993; Lemert and Johnston, 1991; Walsh et al., 1987). The mechanism of the effect of a cosolvent on the solubility is very complicated and is not well-understood. However, it is known that a polar cosolvent may interact with a polar solute through hydrogen bonding, dispersion forces, dipole–dipole forces, etc. Studies of the effect of nonpolar cosolvents on the solubility are scarce.

Behenic acid (CH₃(CH₂)₂₀COOH) has a large alkyl chain and a polar head. The solubility of behenic acid in pure SC CO₂ is very low (Chrastil, 1982; Yoon et al., 1998); however it can be enhanced by an ethanol cosolvent (Guan et al., 1999). No reports about the effect of nonpolar cosolvents on the solubility of behenic acid in SC CO₂ were found in the literature. It is expected that dispersion forces play a major role in the effect of a nonpolar cosolvent on its solubility. In this work, we studied the solubility of behenic acid in SC CO₂ with *n*-pentane or *n*-octane cosolvents.

Experimental Section

Apparatus and Procedures. The apparatus and experimental procedures for measuring the solubility were described in detail previously (Ke et al., 1996). The apparatus consisted mainly of an optical cell, a gas cylinder, a syringe pump, a digital pressure gauge, a solenoid-operated pump, a vapor sample bomb, a constant-temperature bath, and valves and fittings of various kinds.

The reliability of the apparatus and the procedures were verified by measuring the solubilities of salicylic acid and

Table 1. Solubility of Solute in the SC CO₂–Pentane Mixture and the Apparent Density of CO₂ at 318.15 K

$Y_3 \times 10^2$	$Y_2 \times 10^5$	$d_1/$ (mol·L ⁻¹)	$Y_3 \times 10^2$	$Y_2 \times 10^5$	$d_1/$ (mol·L ⁻¹)
9.0 MPa					
0.00	0.59	7.55	3.33	2.63	9.89
2.06	1.20	9.43	5.17	4.10	11.5
9.5 MPa					
0.00	1.05	9.53	4.05	3.98	12.1
2.94	2.24	11.6	5.03	4.22	12.4
10.0 MPa					
0.00	1.26	12.1	4.08	4.37	12.9
1.89	2.14	12.8	5.08	4.47	12.7
11.0 MPa					
0.00	1.82	13.5	3.81	4.57	13.7
2.92	3.24	14.0	5.64	7.76	13.6
13.5 MPa					
0.00	2.95	16.1	3.61	5.61	15.2
2.69	5.37	15.4	4.57	7.94	14.9
16.0 MPa					
0.00	3.55	17.3	3.36	8.51	16.1
2.68	6.46	16.3	4.87	11.2	16.0

stearic acid in SC CO₂ and then comparing these results with data reported by others. This was discussed in our previous papers (Ke et al., 1996; Guan et al., 1999). It is estimated that the accuracy of the data is better than ±5%.

Materials. CO₂ with a purity of 99.995% was supplied by Beijing Analytical Instrument Factory; *n*-pentane and *n*-octane were analytical reagent (A.R.) grade (99.7%) produced by Beijing Chemical Plant and were used without further purification. The behenic acid (A.R. grade) was supplied by Beijing Chemical Reagent Co. Before use, it was recrystallized, and the melting range of the purified chemical was determined to be from 353.0 K to 354.9 K.

Results and Discussion

The solubility of behenic acid in SC CO₂ with *n*-pentane or *n*-octane as cosolvent was measured at 308.15 K, 318.15 K, and 328.15 K in the pressure range from 9.0 MPa to 16.0 MPa and the cosolvent concentration range from 0 mol % to 7.5 mol %. There is only one fluid phase under our experimental conditions, which was seen clearly in the optical cell of the experimental apparatus. The results are listed in Tables 1–4, where Y_2 and Y_3 are the mole fractions of the solute and the cosolvents in the fluid phase, respectively; d_1 is the apparent density of CO₂, expressed as moles of CO₂ per liter of the mixture.

* To whom the correspondence should be addressed. Fax: (010)-62569564. E-mail: hanbx@pplas.icas.ac.cn.

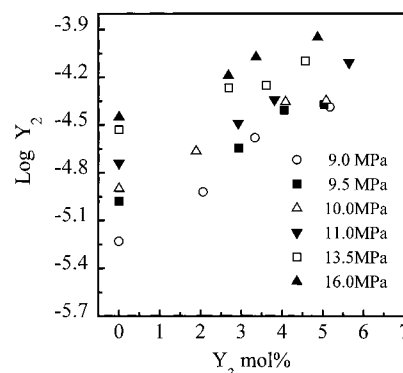
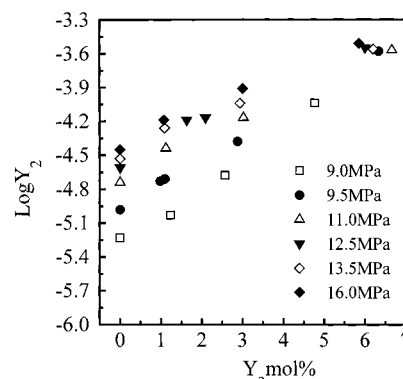
Table 2. Solubility of Solute in the SC CO₂-Pentane Mixture and the Apparent Density of CO₂ at 328.15 K

$Y_3 \times 10^2$	$Y_2 \times 10^5$	$d_l/$ (mol·L ⁻¹)	$Y_3 \times 10^2$	$Y_2 \times 10^5$	$d_l/$ (mol·L ⁻¹)
9.0 MPa					
0.00	0.32	6.82	5.36	2.14	7.90
4.07	1.05	7.05	7.50	6.03	6.89
9.5 MPa					
0.00	0.63	7.64	6.07	4.33	7.16
3.08	1.95	8.02	7.16	6.31	7.15
10.0 MPa					
0.00	1.02	7.69	5.17	6.31	8.94
4.34	3.55	8.40	6.15	8.13	9.82
4.66	3.89	8.48			
11.0 MPa					
0.00	1.63	9.96	5.19	10.4	11.1
3.74	6.87	10.4	5.54	13.8	11.5
13.5 MPa					
0.00	6.17	14.2	4.73	25.1	13.6
3.77	23.1	13.5	5.59	27.5	13.1
16.0 MPa					
0.00	11.2	15.8	4.13	35.5	14.6
3.53	25.1	14.4	5.59	39.8	14.2

Table 3. Solubility of Behenic Acid in the SC CO₂-*n*-Octane Mixture and the Apparent Density of CO₂ at 308.15 K

$Y_3 \times 10^2$	$Y_2 \times 10^5$	$d_l/$ (mol L ⁻¹)	$Y_3 \times 10^2$	$Y_2 \times 10^5$	$d_l/$ (mol L ⁻¹)
8.0 MPa					
0.00	0.68	11.5	2.14	1.32	14.5
1.03	0.79	13.7	3.04	1.82	14.6
8.5 MPa					
0.00	0.91	13.9	2.08	1.66	15.3
1.04	1.12	14.9	2.85	2.09	15.2
1.94	1.26	15.4			
9.5 MPa					
0.00	1.07	15.7	3.06	2.51	15.7
1.03	1.35	15.8	3.24	2.63	15.7
2.06	1.91	16.0			
11.0 MPa					
0.00	1.23	16.9	2.16	2.19	16.5
1.11	1.58	16.7	3.01	3.16	16.3
13.5 MPa					
0.00	1.32	18.0	2.89	3.47	17.0
1.15	1.82	17.6	3.06	3.49	16.9
2.05	2.40	17.4			
16.0 MPa					
0.00	1.38	18.8	1.98	2.51	17.9
0.96	2.09	18.5	2.75	4.07	17.6

Figure 1 shows the effect of *n*-pentane concentration on the solubility of behenic acid in the CO₂-*n*-pentane system at 318.15 K, which indicates that the solubility increases with cosolvent concentration under the same pressure. *n*-Octane has a similar effect on solubility, as shown in Figure 2. However, *n*-octane enhances the solubility more significantly than *n*-pentane at the same molar concentration, which can be observed from Figures 1 and 2. This can be interpreted qualitatively. The interaction between behenic acid and the cosolvent molecules is mainly due to dispersion forces. The interaction between *n*-octane and behenic acid molecules is stronger because the size of *n*-octane is larger than that of *n*-pentane, which enhances its solubility. On the other hand, SC CO₂ can aggregate with the cosolvent and solute molecules, which causes larger local density around the cosolvent and solute molecules. The aggregation between the solvent and cosolvent molecules reduces the interaction between the cosolvent and solute. The interaction between CO₂ and

**Figure 1.** Solubility of behenic acid in the SC CO₂-*n*-pentane mixture at 318.15 K.**Figure 2.** Solubility of behenic acid in the SC CO₂-*n*-octane mixture at 318.15 K.**Table 4. Solubility of Solute in the SC CO₂-*n*-Octane Mixture and the Apparent Density of CO₂ at 318.15 K**

$Y_3 \times 10^2$	$Y_2 \times 10^5$	$d_l/$ (mol L ⁻¹)	$Y_3 \times 10^2$	$Y_2 \times 10^5$	$d_l/$ (mol L ⁻¹)
9.0 MPa					
0.00	0.58	8.65	2.57	2.08	10.3
1.24	0.94	9.28	4.77	9.11	11.3
9.5 MPa					
0.00	1.05	10.5	2.88	4.17	12.7
0.98	1.86	11.3	6.34	26.3	13.3
1.10	1.95	11.5			
11.0 MPa					
0.00	1.84	14.4	3.02	6.90	14.3
1.12	3.59	14.3	6.66	27.1	14.0
12.5 MPa					
0.00	2.44	15.6	2.09	6.70	14.8
1.63	6.47	15.2	6.00	28.2	14.6
13.5 MPa					
0.00	2.92	16.4	2.93	9.20	15.6
1.09	5.45	15.8	6.20	27.8	14.8
16.0 MPa					
0.00	3.51	17.3	3.00	12.2	15.9
1.07	6.51	16.9	5.85	30.7	15.2

n-octane is stronger than that between CO₂ and *n*-pentane, which is not favorable to enhancing the solubility of behenic acid. The overall effect depends on which of these two factors is dominant. The solubility measurements show that the first factor is dominant; thus *n*-octane affects solubility more significantly.

Figures 3 and 4 show the dependence of the solubility on pressure. The figures demonstrate that at lower pressures or lower cosolvent concentrations, the solubility is a strong function of pressure. At higher pressures and higher cosolvent concentrations the effect is relatively weak because the effect of pressure on the density of the fluid

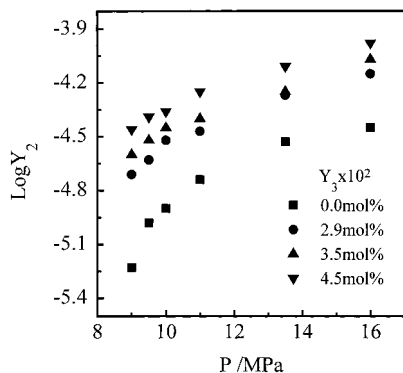


Figure 3. Effect of pressure on the solubility of behenic acid in the SC CO₂-*n*-pentane mixture at 318.15 K.

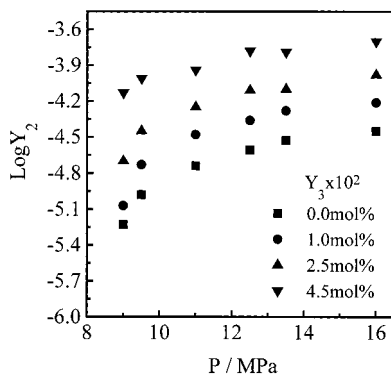


Figure 4. Effect of pressure on the solubility of behenic acid in the SC CO₂-*n*-octane mixture at 318.15 K.

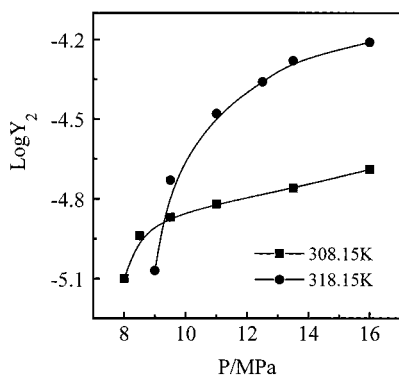


Figure 5. Effect of temperature on the solubility of behenic acid at an *n*-octane concentration of 1.0 mol %.

phase is very limited at these conditions, as shown by the measurements in Tables 1 and 4.

Figure 5 gives the solubility of behenic acid in the CO₂-*n*-octane system at 308.15 K and 318.15 K with an *n*-octane concentration of 1.0 mol %. It can be seen that there is a crossover point at about 9.3 MPa. At a pressure less than this value, the solute is more soluble at the lower temperature; at the higher pressures, the solute is more soluble at a higher temperature. Temperature affects the solubility in the following ways in opposition: the volatility of the

solute increases with temperature, which is favorable to increasing the solubility, but, the density of the fluid decreases with temperature, which is not favorable to increasing the solubility. As shown in Tables 3 and 4, the density of CO₂ at 318.15 K is much lower than that at 308.15 K at the lower pressures. Thus, the density effect is dominant, and the solubility decreases with temperature. At higher pressures, the density of CO₂ is not as sensitive to the pressure as that at lower pressures, and the volatility effect becomes dominant and the solubility increases with temperature.

Conclusion

The solubility of behenic acid in SC CO₂-*n*-pentane or in SC CO₂-*n*-octane mixtures increases with cosolvent concentration and pressure. Under similar experimental conditions, *n*-octane affects the solubility more significantly than *n*-pentane. The solubility is more sensitive to pressure at lower pressures.

Literature Cited

- Chrastil, J. Solubility of Solids and Liquids in Supercritical Gases. *J. Phys. Chem.* **1982**, *86*, 3016–3021.
- Foster, N. R.; Singh, H. S.; Yun, L. J.; Tomasko, D. L.; Macnaughton, S. J. Polar and Nonpolar Cosolvent Effects on the Solubility of Cholesterol in Supercritical Fluids. *Ind. Eng. Chem. Res.* **1993**, *32*, 2849–2853.
- Guan, B.; Han, B. X.; Yan, H. K. Effect of Acetic Acid + Acetonitrile and Ethanol + Acetonitrile Mixed Cosolvents on the Solubility of Stearic Acid in Supercritical CO₂. *Fluid Phase Equilib.* **1998a**, *149*, 277–286.
- Guan, B.; Han, B. X.; Yan, H. K. Solubility of Stearic Acid in Supercritical CO₂-Acetic Acid and CO₂-*n*-Octane Mixtures at 308.15 K. *J. Supercrit. Fluids* **1998b**, *11*, 123–128.
- Guan, B.; Liu, Z. M.; Han, B. X.; Yan, H. K. The Solubility of Behenic Acid in Supercritical CO₂ with Ethanol. *J. Supercrit. Fluids* **1999**, *14*, 213–218.
- Gurdial, G. S.; Macnaughton, S. J.; Tomasko, D. L.; Foster, N. R. Influence of Chemical Modifiers on the Solubility of *o*- and *m*-Hydroxybenzoic Acid in Supercritical CO₂. *Ind. Eng. Chem. Res.* **1993**, *32*, 1488–1497.
- Johannsen, M.; Brunner, G. Measurements of Solubilities of Xanthines in Supercritical Carbon Dioxide + Methanol. *J. Chem. Eng. Data* **1995**, *40*, 431–434.
- Ke, J.; Mao, C.; Zhong, M. H.; Han, B. X.; Yan, H. K. Solubilities of Salicylic Acid in Supercritical Carbon Dioxide with Ethanol Cosolvent. *J. Supercrit. Fluids* **1996**, *9*, 82–87.
- Koga, Y.; Iwai, Y.; Hata, Y.; Yamamoto, M.; Arai, Y. Influence of Cosolvent on Solubilities of Fatty Acids and Higher Alcohols in Supercritical Carbon Dioxide. *Fluid Phase Equilib.* **1996**, *125*, 115–128.
- Lemert, R. M.; Johnston, K. P. Chemical Complexing Agents for Enhanced Solubilities in Supercritical Fluid Carbon Dioxide. *Ind. Eng. Chem. Res.* **1991**, *30*, 1222–1231.
- Walsh, J. M.; Ikononou, G. D.; Donohue, M. D. Supercritical Phase Behavior: The Entrainer Effect. *Fluid Phase Equilib.* **1987**, *33*, 295–314.
- Yoon, S. H.; Nakaya, H.; Ito, O.; Miyawaki, O.; Park, K. H.; Nakamura, K. Effects of Substrate Solubility in Interesterification with Triolein by Immobilized Lipase in Supercritical Carbon Dioxide. *Biosci., Biotechnol., Biochem.* **1998**, *62*, 170–172.
- Zhong, M. H.; Han, B. X.; Yan, H. K. Solubility of Stearic Acid in Supercritical CO₂ with Cosolvents. *J. Supercrit. Fluids* **1997**, *10*, 113–118.

Received for review February 22, 1999. Accepted July 8, 1999. The authors are grateful to the National Natural Science Foundation of China for financial support (Grant No. 29633020, 29725308).

JE990058X