

# Compilation, Evaluation, and Selection of Physical-Chemical Property Data for $\alpha$ -, $\beta$ -, and $\gamma$ -Hexachlorocyclohexane

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A complete set of temperature-dependent physical-chemical property data (aqueous solubility ( $S_w$ ), octanol–water partition coefficient ( $K_{ow}$ ), vapor pressure ( $P$ ), Henry's law constant ( $H$ ), octanol–air partition coefficient ( $K_{oa}$ ), and octanol solubility ( $S_o$ )) for  $\alpha$ -,  $\beta$ -, and  $\gamma$ -hexachlorocyclohexane (HCH) is derived by evaluating, averaging, and regressing all experimentally obtained values reported in the literature. Properties for each isomer are adjusted slightly to ensure thermodynamic consistency. That adjustment is sized according to, and is smaller than, the uncertainty apparent from the range of reported experimental values. The data analysis confirms that an unusually high  $K_{oa}$  and an unusually low  $H$  reported for  $\beta$ -HCH are in agreement with the measured  $S_w$  and  $P$  values when these are converted to the liquid state. Linear solvation energy relationships fail to predict the observed differences in the partitioning behaviors of the three isomers.

## Introduction

The environmental fate of an organic chemical is strongly influenced by its distribution between various phases or compartments. Simple empirical relationships with an organic chemical's aqueous solubility ( $S_w$ ), vapor pressure ( $P$ ), octanol–water partition coefficient ( $K_{ow}$ ), Henry's law constant ( $H$ ), octanol–air partition coefficient ( $K_{oa}$ ), and solubility in octanol ( $S_o$ ) are traditionally used to characterize phase distribution in the environment. Models of organic pollutant fate thus usually require these physical-chemical properties as input parameters. Knowledge of the temperature dependence of the physical-chemical properties is necessary to quantify phase distribution at temperatures other than (20 or 25) °C. Over the relatively small environmentally relevant temperature range, this can be conveniently expressed through the respective internal energies of phase transfer ( $\Delta U$ ).

It is a considerable experimental challenge to reliably measure very low concentrations of organic chemicals in the gas and aqueous phases. As a result, for many sparingly soluble or semivolatile organic chemicals, the reported values for a property from independent measurements can show large discrepancies. Pontolillo and Eganhouse<sup>1</sup> illustrated that it is impossible to derive the true  $S_w$  and  $K_{ow}$  values for  $p,p'$ -dichlorodiphenyltrichloromethylmethane ( $p,p'$ -DDT) and  $p,p'$ -dichlorodiphenyldichloroethylene ( $p,p'$ -DDE) on the basis of the available studies because reporting errors, multilevel referencing, a common lack of precision information, and other problems lead to a multitude of property data with an intimidating degree of inconsistency.

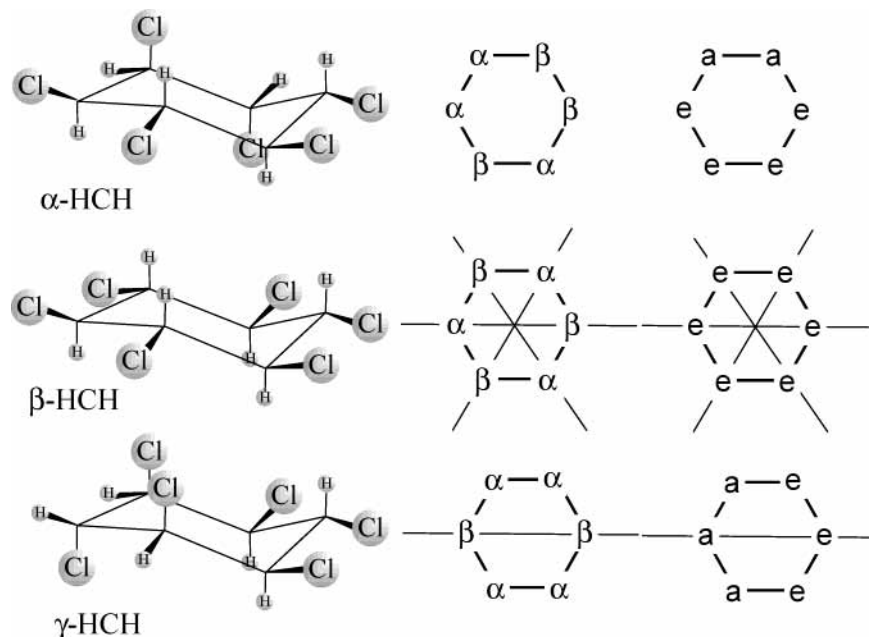
Recently, Beyer and co-workers<sup>2</sup> presented an adjustment technique to derive internally consistent sets of property data for one chemical, and they applied it to several organic substances. This algorithm is based on the thermodynamic relationships between the various physical-chemical properties. Li et al.<sup>3</sup> further complemented that approach by developing a rigorous and transparent procedure

for compiling and evaluating measured data from the literature, selecting literature-derived values through averaging or linear regression, and making estimates of the uncertainty of these values. These uncertainty estimates determine the extent of relative adjustment applied in the adjustment algorithm. The procedure was applied to 16 PCB congeners, and the resulting set of data shows consistency not only among the various partitioning properties for one congener but also for one property across various congeners.<sup>3</sup>

Technical hexachlorocyclohexane (HCH), which contains 60 to 70%  $\alpha$ -HCH, 5 to 12%  $\beta$ -HCH, 10 to 12%  $\gamma$ -HCH, 6 to 10%  $\delta$ -HCH, and 3 to 4%  $\epsilon$ -HCH, has been widely used as a pesticide on the global scale since the 1940s. As prominent organochlorinated contaminants, HCH isomers have been detected around the world.<sup>4</sup> Whereas, for the longest period of time, attention has been directed to quantifying and understanding the environmental behavior of the active insecticidal ingredient,  $\gamma$ -HCH, and the major constituent of the technical product,  $\alpha$ -HCH, recent investigations indicate surprisingly divergent environmental behavior for the  $\beta$ -HCH isomer (Figure 1). This includes a higher potential for bioaccumulation<sup>5</sup> and different transport pathways in the North Pacific.<sup>6</sup> Interpretation of such discrepancies requires a thorough grasp of the differences in the partitioning properties of the various isomers.

A large number of studies have reported physical-chemical properties for the  $\alpha$ - and  $\gamma$ -isomers. More recently, the partitioning properties for the  $\beta$ -HCH isomer have been measured, and some of them appear to suggest considerable deviations from those for  $\alpha$ - and  $\gamma$ -HCH. Such deviations may be due to the unusually high crystal energy of the  $\beta$ -isomer, which has a higher degree of symmetry than the other isomers (Figure 1). The objective of this work is to use the procedures described by Beyer et al.<sup>2</sup> and Li et al.<sup>3</sup> to derive a property data set for  $\alpha$ -,  $\beta$ -, and  $\gamma$ -HCH that makes use of all available measured data and is internally consistent. Partitioning property measurements for other HCH isomers are too rare to allow this procedure to be applied.

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**Figure 1.** Structures of the  $\alpha$ -,  $\beta$ -, and  $\gamma$ -isomers of hexachlorocyclohexane.  $\gamma$ -HCH has one plane of symmetry, and  $\beta$ -HCH has three planes of symmetry, whereas  $\alpha$ -HCH is a chiral molecule. The diagrams on the right indicate the chlorine substitutions in the axial (a) and equatorial (e) orientations.

## Methods

The principles and steps involved in the evaluation, selection, and adjustment procedure have been described previously<sup>2,3</sup> and will not be repeated here in detail. Briefly, the steps are as follows. Chemical Abstracts Service Source Index (CASSI) and other databases<sup>7</sup> are used to obtain and identify all the published literature on measured physical-chemical properties for the selected HCH isomers. Despite our efforts for comprehensiveness, it is likely that additional data sources exist that escaped our attention. To avoid multilevel referencing, only original data sources are considered; that is, no quoted values are included.<sup>1</sup> Values that refer to the same set of experiments, differ substantially from a cluster of other reported values, or are highly inconsistent with the other property values for the same chemical are eliminated from the data set. Values measured indirectly, such as those derived from chromatographic retention times, are only included if there is an insufficient number of directly measured values. Estimated values are excluded.

The measured data are converted into appropriate and identical units and compiled in spreadsheets. If no exact experimental temperature is provided, a temperature of 23 °C is assumed to apply. If the data are reported as a linear equation, discrete values are calculated for four or five temperatures, which are either the experimental temperatures indicated in the reference or temperatures in the environmentally relevant range. The HCH isomers are solids at environmental temperatures. The reported solid-phase vapor pressure and solubility values ( $P_S$ ,  $S_{WS}$ ,  $S_{OS}$ ) are converted into the properties of the supercooled liquid ( $P_L$ ,  $S_{WL}$ ,  $S_{OL}$ ) using compound specific entropy of fusion values ( $\Delta_{fus}S$ ) and melting point temperatures ( $T_M$ ) in eq 1:

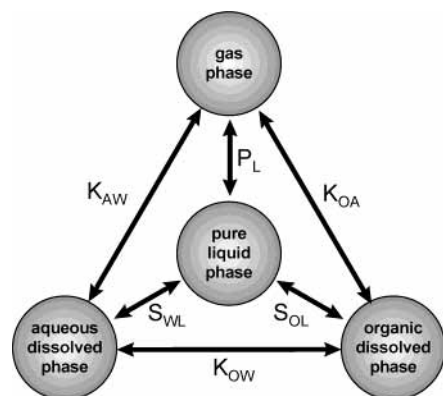
$$S_{WS}/S_{WL} = S_{OS}/S_{OL} = P_S/P_L = \exp(-\Delta_{fus}S((T_M/T) - 1)/R) \quad (1)$$

$R$  is the ideal gas constant, and  $T$  is the experimental temperature in kelvin. If a compound-specific  $\Delta_{fus}S$  is not available, a generic default value of  $56 \text{ J}\cdot\text{K}^{-1}\cdot\text{mol}^{-1}$  is used.

If measured values for a property exist at several temperatures, a linear regression equation between the logarithm of all noneliminated data and reciprocal absolute temperature is derived. The value for 25 °C obtained from the regression line and the product of the slope of the regression line and  $R$  are chosen as literature-derived values (LDVs) for the property and the corresponding internal energy of phase transfer, respectively. If measurements had only been performed within the fairly small temperature range (20 to 25) °C, the values are adjusted to 25 °C by using an estimated energy of phase transfer. In such cases the LDV is the logarithmic mean of the noneliminated values. The arithmetic mean would give undue weight to higher values. Temperature-dependent  $S_{OL}$ <sup>8</sup> and  $K_{OA}$ <sup>9</sup> for the HCHs had only been measured by a single study, respectively. The LDVs for  $\Delta U_O$  and  $\Delta U_{OA}$  were taken directly from the relevant studies.

For each LDV, an uncertainty estimate ( $u_X$ ) between 1 and 5 was assigned on the basis of the size of the database, the deviations between different measurements, and the general reliability of data reported by a particular research group. For example, a large  $u_X$ , indicating high uncertainty, was assigned to properties for which few or no directly measured data exist (e.g.  $K_{OA}$  for all the isomers) or for which several reported values are highly divergent (e.g.  $S_{WL}$  of  $\beta$ -HCH), whereas properties that had been measured directly several times with accepted techniques yielding comparable values would deserve a low  $u_X$  (e.g.  $K_{OW}$  for  $\gamma$ -HCH). It is not feasible to use strictly numerical criteria in the assignment of uncertainty, rendering the assessment somewhat subjective. The uncertainty parameters are used to achieve consistency among the properties for one chemical. Therefore, the relative size of  $u_X$  for the properties of one HCH isomer is more important than the relative size for one property of different isomers.

The LDVs were adjusted using the algorithm by Beyer et al.<sup>2</sup> This technique adjusts a set of physical-chemical property values in such a way that they conform to thermodynamic constraints (Figure 2) yet deviate as little as possible from the original values. For example, on the basis of a thermodynamic triangle,  $\log K_{OA}$  should equal



**Figure 2.** Illustration of the relationship between the six investigated partitioning properties. Any three properties forming one of the four triangles in this figure need to be consistent with each other.

$\log S_{OL} - \log P_L/RT$ . The LDVs of the three properties generally do not satisfy this condition, and thus, they need to be adjusted so that they do. If LDVs exist for all six partitioning properties, four such thermodynamic triangles exist. The extent of the adjustment to each property is scaled according to the uncertainty factor ( $u_x$ ) assigned to it. The adjusted values are referred to as final adjusted values (FAVs). Missing property values (such as the  $S_{OL}$  for  $\beta$ -HCH) are calculated at the same time. Because the HCHs are not very hydrophobic ( $\log K_{OW} < 4$ ), we ignore the effect of the mutual solubility of octanol and water on the partitioning of the HCH isomers between octanol and water, and we assume that  $K_{OW}$  equals  $S_{OL}/S_{WL}$ . For a detailed account of the thermodynamic basis of the adjustment procedure and the equations on which it is based, see ref 2. A computer program with the algorithm is available from [www.usf.uos.de/projects/elpos/download/adjust.en.html](http://www.usf.uos.de/projects/elpos/download/adjust.en.html).

## Results

The physical-chemical properties for  $\alpha$ -,  $\beta$ -, and  $\gamma$ -HCH are compiled in Tables 1–3. At the top of each section of the table are the data that are included in the derivation of the LDVs, including the experimental temperature, the method used, and the reference. For comparison and completeness, the data that are not included in the derivation of the LDVs are listed toward the bottom of each section of the table, together with the reason for exclusion. The LDVs and the FAVs at 25 °C for each property are also included in Tables 1–3. A summary of the LDVs at 25 °C is presented in Table 4 along with the uncertainty estimates ( $u_x$ ) assigned to each property. Such LDVs could be derived for all properties, except for the solubility of  $\beta$ -HCH in octanol, for which no measured data are available. The corresponding FAVs and percentage adjustment are listed in Table 5. The internal energies of phase transfer ( $\Delta U$ ), their origins, and their uncertainty estimates are presented in Table 6. Lack of measured data prevented the derivation of LDVs for  $\Delta U_W$  of  $\alpha$ - and  $\beta$ -HCH and for  $\Delta U_O$  of  $\beta$ -HCH. The FAVs for  $\Delta U$  and the required percentage of adjustment are presented in Table 7. Plots of the logarithm of a property, which include the measured data, LDVs, and FAVs, versus reciprocal absolute temperature are shown in Figures 3–8.

## Discussion

**Property Values at 25 °C.** The literature-derived values for the three HCH isomers are reasonably consistent. The maximum required adjustment to the LDVs at 25 °C is

34%. In general, however, much smaller adjustments on the order of 10% were sufficient to obtain consistency. This is an indication of both the accuracy of the measurements and the success of the procedure used in deriving the LDVs. The variability in the entries for a property in Tables 1–3 gives an approximate indication of the uncertainty of the measured values. The required adjustments are normally well within this uncertainty and further confirm that the procedures applied in the selection of the LDVs eliminated at least some of the experimental error.

Melting point temperatures well above 50 °C imply that the HCH congeners are solids at environmentally relevant temperatures. The conversion of the experimentally accessible properties of the solid to those of the subcooled liquid depends on the knowledge of the entropy or enthalpy of fusion. Uncertain entropies of fusion ( $\Delta_{fus}S$ ) or the use of a default value can lead to significant errors in the calculated liquid property, especially for substances with a high melting point temperature. However, no experimentally determined  $\Delta_{fus}S$  for  $\beta$ -HCH, the isomer with by far the highest melting point, could be obtained, making it necessary to use a default value. It is encouraging to see nevertheless good consistency between the five LDVs for this isomer, which points to accurate measurements and suggests that the real entropy of fusion is likely close to the default value.

A comparison of the FAVs for the three isomers reveals that the  $\beta$ -HCH partitions more strongly from the gas phase into water and octanol than the other two isomers. It had previously been noted that the Henry's law constant of the  $\beta$ -isomer is 1 order of magnitude lower<sup>10</sup> and its  $K_{OA}$  value 1 order of magnitude higher than those of  $\alpha$ - and  $\gamma$ -HCH.<sup>9</sup> The fact that the LDVs for water solubility, vapor pressure, and  $K_{OW}$  for  $\beta$ -HCH are consistent with both the low  $K_{AW}$  and the high  $K_{OA}$  lends further credibility to these values. According to the FAVs, this divergent behavior of the  $\beta$ -HCH is not due to an unusually low volatility (the vapor pressure of the  $\beta$ -isomer is only marginally lower than that of  $\gamma$ -HCH) but is caused by a higher solubility in water and octanol.

**Comparison with Linear Solvation Energy Relationship (LSER) Predictions.** Recently, Abraham et al.<sup>11</sup> derived solvation descriptors for the HCH isomers from data on chromatographic retention times and partitioning properties. In contrast to the FAVs, the solute descriptors for  $\beta$ -HCH did not deviate substantially from those of the  $\alpha$ - and  $\gamma$ -isomers. The solute excess molar refractivity ( $E$ ), the McGowan characteristic volume ( $V$ ), and the summation hydrogen bond acidity ( $A$ ) are identical, whereas the solute dipolarity/polarizability ( $S$ ), the summation hydrogen bond basicity ( $B$ ), and the gas–hexadecane partition coefficient ( $L$ ) are very similar for the three isomers.<sup>11</sup> Accordingly, partitioning properties predicted for  $\beta$ -HCH using LSERs are comparable to those of  $\alpha$ - and  $\gamma$ -HCH; that is, the predicted  $K_{AW}$  and  $K_{OA}$  values for the three isomers are within 0.3 log units of each other. This in turn implies large deviations between the FAVs and the LSER predicted partition coefficients for  $\beta$ -HCH of almost 1 order of magnitude (Figure 9). Abraham et al.<sup>11</sup> had noted that the descriptors for  $\beta$ -HCH are not “very different from those of the other isomers, although some physicochemical properties of  $\beta$ -HCH are considerably different, for example, mp [i.e., melting point], water solubility, and vapor pressure. However, these properties are functions of the crystal energy that cancels out when transfers between solvents are considered.” Our data analysis suggests that the latter statement is not correct. Although the subcooled

**Table 1. Reported and Selected Physical-Chemical Properties for  $\alpha$ -HCH<sup>a</sup>**

registry no.	319-84-6		melting point/ $^{\circ}\text{C}$		158	
name	(1 $\alpha$ ,2 $\alpha$ ,3 $\beta$ ,4 $\alpha$ ,5 $\beta$ ,6 $\beta$ )-1,2,3,4,5,6-hexachlorocyclohexane		$\Delta_{\text{fus}}S/\text{J}\cdot\text{K}^{-1}\cdot\text{mol}^{-1}$		71.92 (ref 14)	
molar mass/ $\text{g}\cdot\text{mol}^{-1}$	290.85					
Aqueous Solubility						
$t/^{\circ}\text{C}$	$S_{\text{WS}}/\text{mol}\cdot\text{m}^{-3}$	$S_{\text{WL}}/\text{mol}\cdot\text{m}^{-3}$	$\log(S_{\text{WL}}/\text{mol}\cdot\text{m}^{-3})$	method	ref	note
28	0.00698	0.291	-0.54	slow stirring-GC	15	
25	0.00688	0.325	-0.49	generator column-GC	16	
25	0.00560	0.264	-0.58	shake flask-GC	17	
20	0.0344	2.01	0.30		18	not used, outlier
LDV at 25 $^{\circ}\text{C}$		0.293		log mean		
FAV at 25 $^{\circ}\text{C}$		0.333				$\log(S_{\text{WL}}/\text{mol}\cdot\text{m}^{-3}) = -398.5/(T/\text{K}) + 0.859$ Figure 3
Octanol-Water Partition Coefficient						
$t/^{\circ}\text{C}$			$\log K_{\text{OW}}$	method	ref	note
25			3.81	shake flask-GC (RI)	15	
28			3.82	shake flask-GC	19	
25			3.78	slow stirring-GC/HPLC	20	
5			3.92	slow stirring-SPME-GC	21	
25			3.79			
45			3.75			
LDV at 25 $^{\circ}\text{C}$			3.81	linear regression		$\log K_{\text{OW}} = 374.5/(T/\text{K}) + 2.55$ $r^2 = 0.8385$ Figure 4
FAV at 25 $^{\circ}\text{C}$			3.94			$\log K_{\text{OW}} = 266.2/(T/\text{K}) + 3.04$ Figure 4
Vapor Pressure						
$t/^{\circ}\text{C}$	$P_{\text{S}}/\text{Pa}$	$P_{\text{L}}/\text{Pa}$	$\log(P_{\text{L}}/\text{Pa})$	method	ref	note
0	0.000200	0.73	-1.54	effusion manometer	22	
10	0.000867	1.21	-1.11			
20	0.00333	3.31	-0.72			
30	0.0119	4.38	-0.35			
40	0.0387	6.75	-0.01			
50	0.116	9.77	0.31			
60	0.327	19.8	0.61			
70	0.867	0.84	0.89			
0		1.47	-1.75	GC-retention time	23	calc from a linear equation
10		2.00	-1.29			
20		2.95	-0.86			
30		4.12	-0.45			
40		5.69	-0.08			
20	0.002	8.03	-0.95	relative loss rate	24	
LDV at 25 $^{\circ}\text{C}$			-0.61	linear regression		$\log(P_{\text{L}}/\text{Pa}) = -3434/(T/\text{K}) + 10.91$ $r^2 = 0.991$ Figure 5
FAV at 25 $^{\circ}\text{C}$			-0.61			$\log(P_{\text{L}}/\text{Pa}) = -3497/(T/\text{K}) + 11.12$ Figure 5
Henry's Law Constant						
$t/^{\circ}\text{C}$	$H/\text{Pa}\cdot\text{m}^{-3}\cdot\text{mol}^{-1}$		$\log(H/\text{Pa}\cdot\text{m}^{-3}\cdot\text{mol}^{-1})$	method	ref	note
0.5	0.104		-0.98		25	
10	0.225		-0.65			
23	0.677		-0.17			
35	1.34		0.13			
45	3.27		0.51			
25	1.239		0.09		26	
10	0.17		-0.77		27	
20	0.43		-0.37			
30	0.92		-0.04			
35	1.52		0.18			
40	2.21		0.34			
5	0.094		-1.03	dynamic headspace method	10	
10	0.15		-0.82			
20	0.38		-0.42			
30	0.79		-0.10			
35	1.32		0.12			
5	0.098		-1.01	bubble stripping method	10	
10	0.13		-0.89			
20	0.42		-0.38			
30	0.92		-0.04			
35	1.24		0.09			
23	2.36		0.37		28	outlier
LDV at 25 $^{\circ}\text{C}$			-0.19	linear regression		$\log(H/\text{Pa}\cdot\text{m}^{-3}\cdot\text{mol}^{-1}) = -3171/(T/\text{K}) + 10.45$ $r^2 = 0.962$ Figure 6
FAV at 25 $^{\circ}\text{C}$			-0.13			$\log(H/\text{Pa}\cdot\text{m}^{-3}\cdot\text{mol}^{-1}) = -3099/(T/\text{K}) + 10.26$ Figure 6



Table 1 (Continued)

Octanol–Air Partition Coefficient						
$t/^\circ\text{C}$	$\log K_{\text{OA}}$	method	ref	note		
5	8.39	generator column-GC	9	reported as a linear regression equation		
10	8.18					
15	7.98					
20	7.79					
25	7.61					
LDV at 25 °C	7.61	directly taken		$\log K_{\text{OA}} =$ $3231/(TK) - 3.23$		Figure 7
FAV at 25 °C	7.464			$\log K_{\text{OA}} =$ $3235/(TK) - 3.39$		Figure 7
Octanol Solubility						
$t/^\circ\text{C}$	$S_{\text{OS}}/\text{mol}\cdot\text{m}^{-3}$	$S_{\text{OL}}/\text{mol}\cdot\text{m}^{-3}$	$\log(S_{\text{OL}}/\text{mol}\cdot\text{m}^{-3})$	method	ref	note
4	21.9	2663	3.43	shake flask	8	
12	32.4	2701	3.43			
20	51.3	2996	3.48			
LDV at 25 °C		3050		linear regression		$\log(S_{\text{OL}}/\text{mol}\cdot\text{m}^{-3}) =$ $-257.8/(TK) + 4.35$ $r^2 = 0.826$ Figure 8
FAV at 25 °C		2872				$\log(S_{\text{OL}}/\text{mol}\cdot\text{m}^{-3}) =$ $-132.2/(TK) + 3.90$ Figure 8

<sup>a</sup> The subscripts O and W refer to octanol and water, whereas the subscripts S and L refer to the solid and liquid states. *H* designates the Henry's law constant between air and water. LDV stands for literature-derived value and FAV for final adjusted value.

Table 2. Reported and Selected Physical-Chemical Properties for  $\beta$ -HCH<sup>a</sup>

registry no.	319-85-7			melting point/ $^\circ\text{C}$	315	
name	(1 $\alpha$ ,2 $\beta$ ,3 $\alpha$ ,4 $\beta$ ,5 $\alpha$ ,6 $\beta$ )-1,2,3,4,5,6-hexachlorocyclohexane			$\Delta_{\text{fus}}S/J\cdot\text{K}^{-1}\cdot\text{mol}^{-1}$	56.0 (default value)	
molar mass/ $\text{g}\cdot\text{mol}^{-1}$	290.85					
Aqueous Solubility						
$t/^\circ\text{C}$	$S_{\text{WS}}/\text{mol}\cdot\text{m}^{-3}$	$S_{\text{WL}}/\text{mol}\cdot\text{m}^{-3}$	$\log(S_{\text{WL}}/\text{mol}\cdot\text{m}^{-3})$	method	ref	note
28	0.000688	0.42	-0.38	slow stirring-GC	15	not at 25 °C, used anyhow, because <i>T</i> dependence judged minor compared to variability in measurements
25	0.000825	0.58	-0.24	generator column-GC	16	
25	0.00241	1.68	0.23	shake flask-GC	17	
20	0.00550	4.81	0.68		29, 30	not at 25 °C, used anyhow, because <i>T</i> dependence judged minor compared to variability in measurements
20	0.0172	15.0	1.18		18	not at 25 °C, and outlier
LDV at 25 °C		1.18		log mean		
FAV at 25 °C		1.44				$\log(S_{\text{WL}}/\text{mol}\cdot\text{m}^{-3}) =$ $110.1/(TK) - 0.211$ Figure 3
Octanol–Water Partition Coefficient						
$t/^\circ\text{C}$	$\log K_{\text{OW}}$	method	ref	note		
25	3.80	shake flask-GC	15			
28	3.80	shake flask-GC	19			
25	3.84	slow stirring-GC/HPLC	20			
5	3.99	slow stirring-SPME-GC	21			
25	3.88					
45	3.87					
LDV at 25 °C	3.84	log mean at 25 °C				
FAV at 25 °C	3.92			$\log K_{\text{OW}} =$ $847.5/(TK) + 1.07$		Figure 4
Vapor Pressure						
$t/^\circ\text{C}$	$P_{\text{S}}/\text{Pa}$	$P_{\text{L}}/\text{Pa}$	$\log(P_{\text{L}}/\text{Pa})$	method	ref	note
0	0.00000173	0.00408	-2.39	effusion manometer	22	
10	0.00000840	0.0118	-1.93			
20	0.0000373	0.0327	-1.49			
30	0.000153	0.0859	-1.07			
40	0.000560	0.207	-0.68			
50	0.00191	0.476	-0.32			
60	0.00600	1.04	0.02			
70	0.0176	2.15	0.33			
80	0.0493	4.35	0.64			
90	0.129	8.37	0.92			

**Table 2 (Continued)**

Vapor Pressure (Continued)						
$t/^\circ\text{C}$	$P_S/\text{Pa}$	$P_L/\text{Pa}$	$\log(P_L/\text{Pa})$	method	ref	note
80	0.0493	4.35	0.64			
90	0.129	8.37	0.92			
100	0.320	15.5	1.19			
110	0.765	28.0	1.45			
20	0.0000290	0.0254	-1.60		24	
5		0.0117	-1.93	GC retention time	Bidleman, unpublished	calc from a linear regression
15		0.0317	-1.50			
25		0.0803	-1.10			
35		0.192	-0.72			
45		0.433	-0.36			
LDV at 25 °C			-1.21	linear regression		$\log(P_L/\text{Pa}) = -3563/(T/\text{K}) + 10.74$ $r^2 = 0.994$ Figure 5
FAV at 25 °C			-1.28			$\log(P_L/\text{Pa}) = -3563/(T/\text{K}) + 10.67$ Figure 5
Henry's Law Constant						
$t/^\circ\text{C}$	$H/\text{Pa}\cdot\text{m}^{-3}\cdot\text{mol}^{-1}$	$\log(H/\text{Pa}\cdot\text{m}^{-3}\cdot\text{mol}^{-1})$	method	ref	note	
25	0.045	-1.35	equilibrium	26		
5	0.0054	-2.27	concentration ratio bubble stripping method	10		
10	0.0092	-2.04				
20	0.022	-1.66				
30	0.053	-1.28				
35	0.088	-1.06				
LDV at 25 °C		-1.43	linear regression			$\log(H/\text{Pa}\cdot\text{m}^{-3}\cdot\text{mol}^{-1}) = -3454/(T/\text{K}) + 10.16$ $r^2 = 0.992$ Figure 6
FAV at 25 °C		-1.43				$\log(H/\text{Pa}\cdot\text{m}^{-3}\cdot\text{mol}^{-1}) = -3673/(T/\text{K}) + 10.89$ Figure 6
Octanol–Air Partition Coefficient						
$t/^\circ\text{C}$	$\log K_{OA}$	method	ref	note		
5	10.06	generator column-GC	9	reported as a linear regression equation		
15	9.44					
25	8.87					
35	8.33					
45	7.83					
LDV at 25 °C	8.87	directly taken			$\log K_{OA} = 4937/(T/\text{K}) - 7.69$	Figure 7
FAV at 25 °C	8.74				$\log K_{OA} = 4391/(T/\text{K}) - 5.98$	Figure 7
Octanol Solubility						
	$S_{OL}/\text{mol}\cdot\text{m}^{-3}$	$\log(S_{OL}/\text{mol}\cdot\text{m}^{-3})$	method	ref	note	
FAV at 25 °C	11 816	4.07			$\log(S_{OL}/\text{mol}\cdot\text{m}^{-3}) = 957.6/(T/\text{K}) + 0.861$	Figure 8

<sup>a</sup> The subscripts O and W refer to octanol and water, whereas the subscripts S and L refer to the solid and liquid states.  $H$  designates the Henry's law constant between air and water. LDV stands for literature-derived value and FAV for final adjusted value.

**Table 3. Reported and Selected Physical-Chemical Properties for  $\gamma$ -HCH (Lindane)<sup>a</sup>**

registry no.	58-89-9	$\Delta_{\text{fus}}S/\text{J}\cdot\text{K}^{-1}\cdot\text{mol}^{-1}$	67.11 (DTA, ref 32)			
name	(1 $\alpha$ ,2 $\alpha$ ,3 $\beta$ ,4 $\alpha$ ,5 $\alpha$ ,6 $\beta$ )-1,2,3,4,5,6-hexachlorocyclohexane		62.79 (phase equilibrium, ref 33)			
molar mass/g·mol <sup>-1</sup>	290.85		58 (Rordorf, unpublished work)			
melting point/°C	114		40.88 (DSC method, outlier, ref 14)			
$\Delta_{\text{fus}}S/\text{J}\cdot\text{K}^{-1}\cdot\text{mol}^{-1}$	61.10 (DSC, ref 23)		61.23 (avg of refs 23, 31, 32, and 33 and Rordorf, unpublished work)			
	57.16 (DSC, ref 31)					
Aqueous Solubility						
$t/^\circ\text{C}$	$S_{WS}/\text{mol}\cdot\text{m}^{-3}$	$S_{WL}/\text{mol}\cdot\text{m}^{-3}$	$\log(S_{WL}/\text{mol}\cdot\text{m}^{-3})$	method	ref	note
25	0.030	0.269	-0.57	shake flask-colorimetric	34	
25	0.025	0.225	-0.65	slow stirring-polarography	35	
35	0.041	0.272	-0.57			
45	0.048	0.237	-0.63			
25	0.026	0.232	-0.63	shake flask-GC	36	
28	0.025	0.208	-0.68	slow stirring-GC (RI)	15	
25	0.027	0.241	-0.62	generator column-GC	16	
15	0.0074	0.0925	-1.03	slow stirring (sonicator stirring)-GC	37	
25	0.023	0.210	-0.68			
35	0.039	0.258	-0.59			
45	0.052	0.257	-0.59			

Table 3 (Continued)

Aqueous Solubility (Continued)						
$t/^\circ\text{C}$	$S_{\text{WS}}/\text{mol}\cdot\text{m}^{-3}$	$S_{\text{WL}}/\text{mol}\cdot\text{m}^{-3}$	$\log(S_{\text{WL}}/\text{mol}\cdot\text{m}^{-3})$	method	ref	note
24	0.027	0.251	-0.60	shake flask-GC	38	
25	0.025	0.222	-0.65	generator column-SPME-GC	39	
LDV at 25 °C		0.233		log mean of values at 25 °C		$\log(S_{\text{WL}}/\text{mol}\cdot\text{m}^{-3}) = -749.8/(T/\text{K}) + 1.83$ $r^2 = 0.337$ Figure 3
FAV at 25 °C		0.247				$\log(S_{\text{WL}}/\text{mol}\cdot\text{m}^{-3}) = -788.4/(T/\text{K}) + 2.04$ Figure 3
Octanol–Water Partition Coefficient						
$t/^\circ\text{C}$			$\log K_{\text{OW}}$	method	ref	note
25			3.72	shake flask-GC (RI)	15	
28			3.72	shake flask-GC	19	
25			3.69	slow stirring-GC/HPLC	20	
25			3.69	slow stirring-SPME-GC	39	
5			3.85	slow stirring-SPME-GC	21	
25			3.72			
45			3.73			
23			3.30	shake flask-GC	40	room temp, assumed to be 23 °C; not used, outlier
25			3.51	shake flask-GC	41	not used, outlier
20			3.57	shake flask-HPLC	42	not used, outlier
LDV at 25 °C			3.70	log mean		$\log K_{\text{OW}} = 282.2/(T/\text{K}) + 2.78$ $r^2 = 0.455$ Figure 4
FAV at 25 °C			3.83			$\log K_{\text{OW}} = 533.2/(T/\text{K}) + 2.04$ Figure 4
Vapor Pressure						
$t/^\circ\text{C}$	$P_{\text{S}}/\text{Pa}$	$P_{\text{L}}/\text{Pa}$	$\log(P_{\text{L}}/\text{Pa})$	method	ref	note
0	0.0000387	0.00083	-3.08	effusion manometer	22	
10	0.000240	0.0036	-2.45			
20	0.00125	0.013	-1.88			
30	0.00600	0.046	-1.34			
40	0.0257	0.146	-0.84			
50	0.103	0.440	-0.36			
60	0.371	1.22	0.09			
70	1.23	3.16	0.50			
80	3.85	7.80	0.89			
90	11.5	18.6	1.27			
20	0.00435	0.046	-1.34	gas saturation-GC	43	
30	0.0171	0.13	-0.88			
40	0.0608	0.35	-0.46			
30	0.0167	0.13	-0.89			
30	0.0173	0.13	-0.88			
20	0.0233	0.25	-0.61	evaporation rate	44	
40	0.340	1.93	0.29			
60	3.46	11.4	1.06			
20	0.00260	0.0275	-1.56	relative loss rate	24	
30	0.0419	0.321	-0.49	gas saturation-GC	45	
20	0.00940	0.0993	-1.00			
10	0.00221	0.0329	-1.48			
0	0.000449	0.00967	-2.01			
-10	0.0000844	0.00270	-2.57			
-20	0.00000735	0.000361	-3.44			
-30	0.00000170	0.000133	-3.88			
19.63	0.00374	0.0400	-1.40	Knudsen-diffusion	46	
24.95	0.00737	0.0663	-1.18			
28.42	0.0116	0.0934	-1.03			
33.58	0.0225	0.155	-0.81			
37.82	0.0381	0.231	-0.64			
37.86	0.0396	0.239	-0.62			
43.32	0.0718	0.371	-0.43			
48.06	0.123	0.556	-0.26			
53.07	0.217	0.856	-0.07			
37.35	0.0562	0.345	-0.46	Knudsen-effusion	47	
39.35	0.0776	0.449	-0.35			
44.35	0.102	0.513	-0.29			
44.85	0.117	0.581	-0.24			
48.35	0.162	0.727	-0.14			
49.35	0.200	0.870	-0.06			
53.35	0.295	1.16	0.06			
54.85	0.331	1.25	0.10			
55.35	0.363	1.35	0.13			
56.35	0.398	1.44	0.16			
62.85	0.832	2.54	0.41			
63.35	0.813	2.45	0.39			
65.35	0.977	2.81	0.45			
66.35	1.05	2.93	0.47			

Table 3 (Continued)

Vapor Pressure (Continued)						
$t/^\circ\text{C}$	$P_S/\text{Pa}$	$P_L/\text{Pa}$	$\log(P_L/\text{Pa})$	method	ref	note
69.85	1.58	4.08	0.61			
71.35	1.91	4.73	0.67			
71.85	1.78	4.36	0.64			
73.35	2.24	5.29	0.72			
74.35	2.40	5.54	0.74			
74.85	3.09	7.05	0.85			
80.35	4.07	8.19	0.91			
80.85	4.27	8.48	0.93			
83.85	7.08	13.1	1.12			
87.35	7.08	12.2	1.09			
88.85	9.33	15.5	1.19			
93.85	12.3	18.4	1.26			
99.35	23.4	31.2	1.49			
25	0.00670	0.0601	-1.22		Rordorf, unpublished	
50	0.150	0.643	-0.19			
75	2.00	4.55	0.66			
100	20.0	26.3	1.42			
125	150	122	2.09			
0		0.00476	-2.32	GC-retention time	23	calc from a linear regression
10		0.0142	-1.85			
20		0.0395	-1.40			
30		0.103	-0.99			
40		0.250	-0.60			
LDV at 25 °C			-1.11	linear regression		$\log(P_L/\text{Pa}) =$ $-3890/(TK) + 11.94$ $r^2 = 0.959$ Figure 5
FAV at 25 °C			-1.12			$\log(P_L/\text{Pa}) =$ $-3905/(TK) + 11.98$ Figure 5
Henry's Law Constant						
$t/^\circ\text{C}$	$H/\text{Pa}\cdot\text{m}^{-3}\cdot\text{mol}^{-1}$	$\log(H/\text{Pa}\cdot\text{m}^{-3}\cdot\text{mol}^{-1})$	method	ref	note	
23	0.202	-0.70	wetted-wall column	48		
0.5	0.0721	-1.14	gas purging	25		
10	0.126	-0.90				
23	0.339	-0.47				
35	0.624	-0.21				
45	1.17	0.068				
25	0.521	-0.28	wetted-wall column	26		
10	0.0730	-1.14		27		
20	0.180	-0.75				
30	0.390	-0.41				
35	0.580	-0.24				
40	0.800	-0.097				
5	0.0390	-1.41	dynamic headspace method	10		
10	0.0620	-1.21				
20	0.140	-0.85				
30	0.330	-0.48				
35	0.600	-0.22				
5	0.0440	-1.36	bubble stripping method	10		
10	0.0540	-1.27				
20	0.150	-0.82				
30	0.340	-0.47				
35	0.550	-0.26				
LDV at 25 °C		-0.57	linear regression		$\log(H/\text{Pa}\cdot\text{m}^{-3}\cdot\text{mol}^{-1}) =$ $-2940/(TK) + 9.29$ $r^2 = 0.917$ Figure 6	
FAV at 25 °C		-0.51			$\log(H/\text{Pa}\cdot\text{m}^{-3}\cdot\text{mol}^{-1}) =$ $-3117/(TK) + 9.94$ Figure 6	
Octanol-Air Partition Coefficient						
$t/^\circ\text{C}$	$\log K_{OA}$	method	ref	note		
5	8.67	generator column-GC	9	reported as a linear regression equation		
10	8.45					
15	8.24					
20	8.04					
25	7.84					
LDV at 25 °C	7.84	directly taken		$\log K_{OA} =$ $3415/(TK) - 3.61$ Figure 7		
FAV at 25 °C	7.74			$\log K_{OA} =$ $3521/(TK) - 4.07$ Figure 7		



Table 3 (Continued)

$t/^\circ\text{C}$	Octanol Solubility					
	$S_{\text{OS}}/\text{mol}\cdot\text{m}^{-3}$	$S_{\text{OL}}/\text{mol}\cdot\text{m}^{-3}$	$\log(S_{\text{OL}}/\text{mol}\cdot\text{m}^{-3})$	method	ref	note
4	100	1852	3.27	shake flask	8	
12	141	1961	3.29			
20	182	1923	3.28			
LDV at 25 °C	1969			linear regression		$\log(S_{\text{OL}}/\text{mol}\cdot\text{m}^{-3}) = -84.1/(TK) + 3.58$ $r^2 = 0.435$ Figure 8
FAV at 25 °C	1679					$\log(S_{\text{OL}}/\text{mol}\cdot\text{m}^{-3}) = -255.0/(TK) + 4.08$ Figure 8

<sup>a</sup> The subscripts O and W refer to octanol and water, whereas the subscripts S and L refer to the solid and liquid states. *H* designates the Henry's law constant between air and water. LDV stands for literature-derived value and FAV for final adjusted value.

Table 4. Literature-Derived Values (LDVs) and Assigned Uncertainty Estimates (*u*) for the Physical-Chemical Properties of  $\alpha$ -,  $\beta$ -, and  $\gamma$ -HCH at 25 °C<sup>a</sup>

compd	$S_{\text{WL}}/\text{mol}\cdot\text{m}^{-3}$		$K_{\text{OW}}$		$P/\text{Pa}$		$H/\text{Pa}\cdot\text{m}^3\cdot\text{mol}^{-1}$		$K_{\text{OA}}$		$S_{\text{OL}}/\text{mol}\cdot\text{m}^{-3}$	
	LDV	$u_{\text{W}}$	LDV	$u_{\text{OW}}$	LDV	$u_{\text{A}}$	LDV	$u_{\text{AW}}$	LDV	$u_{\text{OA}}$	LDV	$u_{\text{O}}$
$\alpha$ -HCH	0.293	3	$6.47 \times 10^3$	2	0.248	2	0.652	2	$4.05 \times 10^7$	5	3050	5
$\beta$ -HCH	1.18	4	$6.91 \times 10^3$	3	0.0613	3	0.0374	3	$7.39 \times 10^8$	5		
$\gamma$ -HCH	0.233	1	$5.05 \times 10^3$	1	0.0772	1	0.272	2	$6.98 \times 10^7$	4	1969	5

<sup>a</sup> Water solubility ( $S_{\text{WL}}$ ), octanol solubility ( $S_{\text{OL}}$ ), and vapor pressure ( $P_{\text{L}}$ ) refer to the liquid state. *H* designates the Henry's law constant between air and water.

Table 5. Internally Consistent Physical-Chemical Properties of  $\alpha$ -,  $\beta$ -, and  $\gamma$ -HCH at 25 °C after Adjustment (FAV: Final Adjusted Value)<sup>a</sup>

compd	$S_{\text{WL}}/\text{mol}\cdot\text{m}^{-3}$		$K_{\text{OW}}$		$P_{\text{L}}/\text{Pa}$		$H/\text{Pa}\cdot\text{m}^3\cdot\text{mol}^{-1}$		$K_{\text{OA}}$		$S_{\text{OL}}/\text{mol}\cdot\text{m}^{-3}$	
	FAV	adj	FAV	adj	FAV	adj	FAV	adj	FAV	adj	FAV	adj
$\alpha$ -HCH	0.333	14%	$8.63 \times 10^3$	33%	0.245	-1%	0.735	13%	$2.91 \times 10^7$	-28%	2870	-6%
$\beta$ -HCH	1.44	22%	$8.22 \times 10^3$	19%	0.0529	-14%	0.037	-2%	$5.54 \times 10^8$	-25%	11800 <sup>b</sup>	
$\gamma$ -HCH	0.247	6%	$6.79 \times 10^3$	34%	0.0757	-2%	0.306	12%	$5.50 \times 10^7$	-21%	1680	-15%

<sup>a</sup> The required percentage of adjustment to achieve consistency is also given. Water solubility ( $S_{\text{WL}}$ ), octanol solubility ( $S_{\text{OL}}$ ), and vapor pressure ( $P_{\text{L}}$ ) refer to the liquid state. *H* designates the Henry's law constant between air and water. <sup>b</sup> No literature-derived value exists, and the final adjusted value is calculated from the other properties.

Table 6. Literature-Derived Values ( $\Delta U$ ) and Assigned Uncertainty Estimates (*u*) for the Internal Energies of Phase Transfer of  $\alpha$ -,  $\beta$ -, and  $\gamma$ -HCH in  $\text{kJ}\cdot\text{mol}^{-1}$ 

compd	$\Delta U_{\text{W}}$	$u_{\text{W}}$	$\Delta U_{\text{OW}}$	$u_{\text{OW}}$	$\Delta U_{\text{A}}$	$u_{\text{A}}$	$\Delta U_{\text{AW}}$	$u_{\text{AW}}$	$\Delta U_{\text{OA}}$	$u_{\text{OA}}$	$\Delta U_{\text{O}}$	$u_{\text{O}}$
$\alpha$ -HCH			-7.2 <sup>b</sup>	3 <sup>b</sup>	63.3 <sup>e</sup>	2 <sup>e</sup>	58.2 <sup>h</sup>	2 <sup>h</sup>	-61.9 <sup>k</sup>	5 <sup>k</sup>	4.9 <sup>l</sup>	4 <sup>l</sup>
$\beta$ -HCH			-5.8 <sup>c</sup>	5 <sup>c</sup>	65.7 <sup>f</sup>	3 <sup>f</sup>	63.7 <sup>i</sup>	2 <sup>i</sup>	-94.5 <sup>k</sup>	5 <sup>k</sup>		
$\gamma$ -HCH	14.4 <sup>a</sup>	4 <sup>a</sup>	-10.4 <sup>d</sup>	4 <sup>d</sup>	72.0 <sup>g</sup>	1 <sup>g</sup>	53.8 <sup>j</sup>	2 <sup>j</sup>	-58.0 <sup>k</sup>	5 <sup>k</sup>	1.6 <sup>l</sup>	5 <sup>l</sup>

<sup>a</sup> Regression of  $\log S_{\text{WL}}$  versus  $1/(TK)$  using data from refs 15, 16, 34, 35, 36, 37, 38, and 39. <sup>b</sup> Regression of  $\log K_{\text{OW}}$  versus  $1/(TK)$  using data from refs 15, 19, 20, and 21. <sup>c</sup> Regression of  $\log K_{\text{OW}}$  versus  $1/(TK)$  using data from refs 15, 19, 20, and 21. <sup>d</sup> Regression of  $\log K_{\text{OW}}$  versus  $1/(TK)$  using data from ref 21. <sup>e</sup> Regression of  $\log P_{\text{L}}$  versus  $1/T$  using data from refs 22, 23, and 24. <sup>f</sup> Regression of  $\log P_{\text{L}}$  versus  $1/T$  using data from refs 22 and 24 and Bidleman et al., unpublished work. <sup>g</sup> Regression of  $\log P_{\text{L}}$  versus  $1/(TK)$  using data from refs 22, 23, 24, 43, 44, 45, 46, and 47 and Rordorf, unpublished work. <sup>h</sup> Regression of  $\log K_{\text{AW}}$  versus  $1/(TK)$  using data from refs 10, 25, 26, and 27. <sup>i</sup> Regression of  $\log K_{\text{AW}}$  versus  $1/(TK)$  using data from refs 10 and 26. <sup>j</sup> Regression of  $\log K_{\text{AW}}$  versus  $1/(TK)$  using data from refs 10, 25, 26, 27, and 48. <sup>k</sup> Derived from data given in ref 9. <sup>l</sup> Regression of  $\log S_{\text{OL}}$  versus  $1/(TK)$  using data from ref 8.

liquid vapor pressure of  $\beta$ -HCH is indeed comparable to those of the other isomers, the subcooled liquid water solubility,  $K_{\text{AW}}$ , and  $K_{\text{OA}}$  are not.

The solvation descriptors for  $\beta$ -HCH were largely derived from gas-liquid chromatographic retention times.<sup>11</sup> The retention behaviors of the three HCH isomers on gas chromatographic columns are indeed very similar; that is, they elute generally close to each other. The failure of the LSERs to identify the divergent partitioning behavior of the  $\beta$ -isomer may thus indicate that partitioning into liquid chromatographic stationary phases is not always a good surrogate for partitioning into bulk phases such as octanol. This also highlights the limitations of property estimation methods based on gas chromatographic retention times,<sup>12</sup>

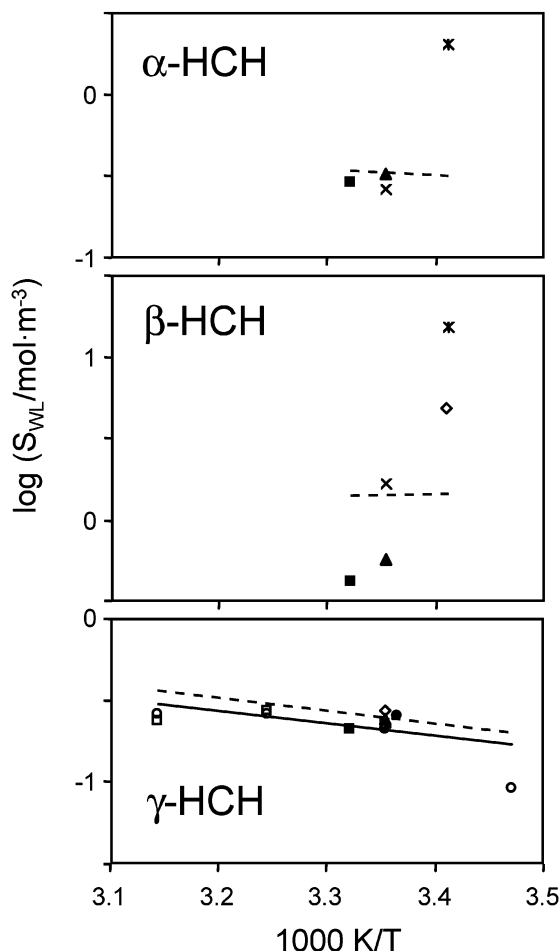
in particular their limitations in discriminating among the partitioning properties of chemicals with similar structures but large differences in melting points.

**Energies of Phase Transfer.** The measured temperature dependences of the properties for  $\alpha$ - and  $\gamma$ -HCH are in excellent agreement. The required adjustment to the  $\Delta U$  values is usually less than 30%. Only the measured temperature dependence of the octanol solubilities ( $\Delta U_{\text{O}}$ ) had to be adjusted by a higher percentage, which can be explained by the relatively small size and large uncertainty of the  $\Delta U_{\text{O}}$  values. Also for  $\beta$ -HCH, the need for adjusting the LDVs for the  $\Delta U$  values is usually minor—the maximum adjustment, needed for  $\Delta U_{\text{OW}}$ , is only about 10  $\text{kJ}\cdot\text{mol}^{-1}$ .

**Table 7. Internal Energies of Phase Transfer of  $\alpha$ -,  $\beta$ -, and  $\gamma$ -HCH after Adjustment (FAV: Final Adjusted Value)<sup>a</sup>**

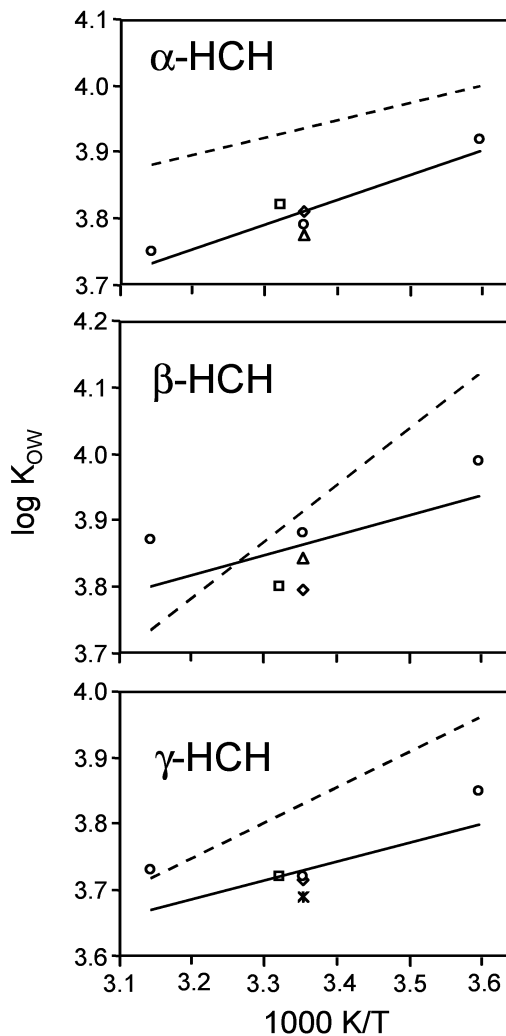
compd	$\Delta U_W/\text{kJ}\cdot\text{mol}^{-1}$		$\Delta U_{OW}/\text{kJ}\cdot\text{mol}^{-1}$		$\Delta U_A/\text{kJ}\cdot\text{mol}^{-1}$		$\Delta U_{AW}/\text{kJ}\cdot\text{mol}^{-1}$		$\Delta U_{OA}/\text{kJ}\cdot\text{mol}^{-1}$		$\Delta U_O/\text{kJ}\cdot\text{mol}^{-1}$	
	FAV	adj	FAV	adj	FAV	adj	FAV	adj	FAV	adj	FAV	adj
$\alpha$ -HCH	7.6		-5.1	-29%	64.5	1.9%	56.8	-2.4%	-61.9	0.1%	2.5	-49%
$\beta$ -HCH	-2.1		-16.2	181%	65.7	0%	67.8	6.6%	-84.1	-11%	-18.3	
$\gamma$ -HCH	15.1	5.1%	-10.2	-2%	72.3	0.4%	57.2	6.3%	-67.4	16%	4.9	203%

<sup>a</sup> The required percentage of adjustment to achieve consistency is also given. If no percentage of adjustment is given, no literature-derived value existed and the value was calculated from the other properties.



**Figure 3.** Relationships between the logarithm of the liquid solubility in water in moles per cubic meter ( $\log S_{WL}$ ) of  $\alpha$ -,  $\beta$ -, and  $\gamma$ -HCH and the reciprocal absolute temperature in kelvin ( $T$ ) based on data from Kurihara et al. ( $\blacksquare$ ),<sup>15</sup> Weil et al. ( $\blacktriangle$ ),<sup>16</sup> Kanazawa et al. ( $\times$ ),<sup>17</sup> Slade ( $*$ ),<sup>18</sup> Isnard and Lambert ( $\diamond$ ),<sup>29,30</sup> Lipke and Kearns (shaded triangle),<sup>34</sup> Richardson and Miller ( $-$ ),<sup>35</sup> Masterton and Lee ( $\Delta$ ),<sup>36</sup> Biggar and Riggs ( $\circ$ ),<sup>37</sup> Chiou et al. ( $\bullet$ ),<sup>38</sup> and Paschke et al. ( $\square$ ).<sup>39</sup> The solid line ( $-$ ) indicates the linear regression through the literature-derived values; the dashed line ( $- -$ ) represents the final adjusted values.

The FAVs suggest that the air–water and air–octanol partitioning equilibria of  $\beta$ -HCH are more strongly influenced by temperature than those of the other two investigated isomers. The FAVs further suggest that the  $\Delta U_O$  for  $\beta$ -HCH has a different sign from that of the other isomers, that is, displays an opposite temperature dependence. Because there are no measured data for the  $\Delta U_O$  and  $\Delta U_W$  of  $\beta$ -HCH,  $\Delta U_A$  is not being adjusted. A negative  $\Delta U_O$  value for  $\beta$ -HCH is needed to account for a significantly higher  $\Delta U_{OA}$  value reported for this isomer by Shoeib and Harner.<sup>9</sup> It is obviously possible that  $\Delta U_A$  for  $\beta$ -HCH is higher or  $\Delta U_{OA}$  should be lower. However, even though the  $\Delta U_{OA}$  values of all three isomers are assigned a high

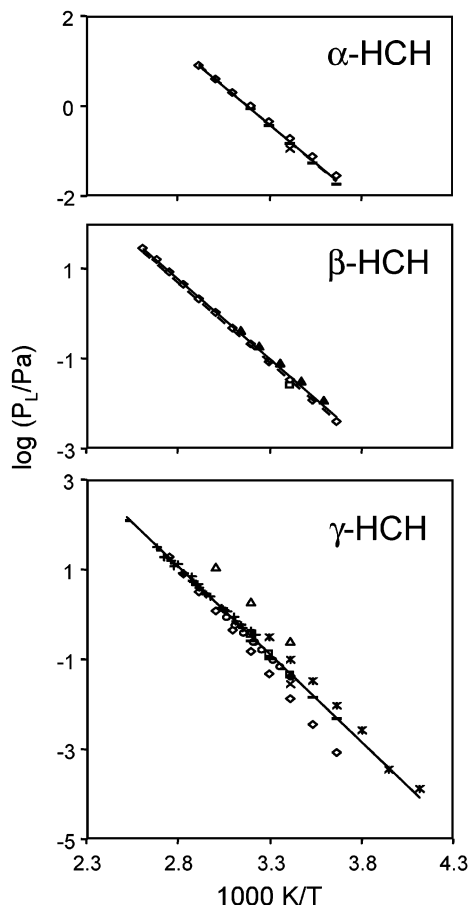


**Figure 4.** Relationships between the logarithm of the octanol–air partition coefficient ( $\log K_{OW}$ ) of  $\alpha$ -,  $\beta$ -, and  $\gamma$ -HCH and the reciprocal absolute temperature in kelvin ( $T$ ), based on data from Kurihara et al. ( $\diamond$ ),<sup>15</sup> Kurihara and Fujita ( $\square$ ),<sup>19</sup> De Bruijn et al. ( $\Delta$ ),<sup>20</sup> Paschke and Schüürmann ( $*$ ),<sup>21</sup> and Paschke et al. ( $\circ$ ).<sup>39</sup> The solid line ( $-$ ) indicates the linear regression through the literature-derived values; the dashed line ( $- -$ ) represents the final adjusted values.

uncertainty ( $u_{OA}$ ), the maximum adjustment to any of these values is only 16.3%.

### Conclusions

By using information for all partitioning properties simultaneously instead of one at a time, it is easier to constrain the range in which the true value for a property will lie. An internally consistent set of physical-chemical property data for three HCH isomers is derived on the basis of all experimentally obtained values reported for these isomers in the literature. The final adjusted data set should



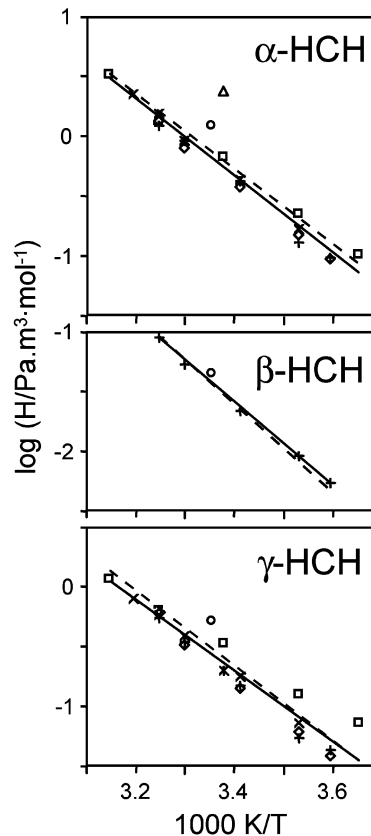
**Figure 5.** Relationships between the logarithm of the liquid vapor pressure in pascal ( $\log P_L$ ) of  $\alpha$ -,  $\beta$ -, and  $\gamma$ -HCH and the reciprocal absolute temperature in kelvin ( $T$ ), based on data from Balson ( $\diamond$ ),<sup>22</sup> Hinckley et al. ( $-$ ),<sup>23</sup> Dobbs and Cull ( $\times$ ),<sup>24</sup> Bidleman et al. ( $\blacktriangle$ ), Spencer and Cliath ( $\square$ ),<sup>43</sup> Gückel et al. ( $\triangle$ ),<sup>44</sup> Wania et al. ( $*$ ),<sup>45</sup> Boehncke et al. ( $\circ$ ),<sup>46</sup> Giustini et al. ( $+$ ),<sup>47</sup> and Rordorf, unpublished data ( $-$ ). The solid line ( $-$ ) indicates the linear regression through the literature-derived values; the dashed line ( $- -$ ) represents the final adjusted values.

be useful when seeking to interpret the differential fate of HCH isomers in the environment.<sup>13</sup> They will also be indispensable in chemical fate modeling, especially when the intention is to evaluate the fate of individual isomers or understand changes in isomeric composition (e.g.  $\alpha/\gamma$ -ratios). Internally consistent values of the six partitioning properties at a particular temperature can be obtained by inserting the FAVs in Tables 5 and 7 in the following equation:

$$\log K(T) = \log K(25^\circ\text{C}) - \frac{(\Delta U_{XY} + R(298.15\text{ K}))}{(\ln(10) R)(1/T - 1/298.15\text{ K})} \quad (2)$$

where the  $K$  stands for the physical-chemical property and  $\Delta U_{XY}$  for the corresponding internal energy of phase transfer.  $T$  is temperature in kelvin. The subscripts  $X$  and  $Y$  describe different phases.

The final adjusted values indicate a partitioning behavior for the  $\beta$ -isomer which differs substantially from those of the other two investigated HCHs. In particular, it partitions much more strongly from the gas phase to the aqueous and octanol phases. This difference cannot be explained by the higher crystal energy of the  $\beta$ -HCH, and it is also not in accord with the retention behavior on gas chromatographic columns. Caution should thus be applied when estimating partitioning behavior of closely related

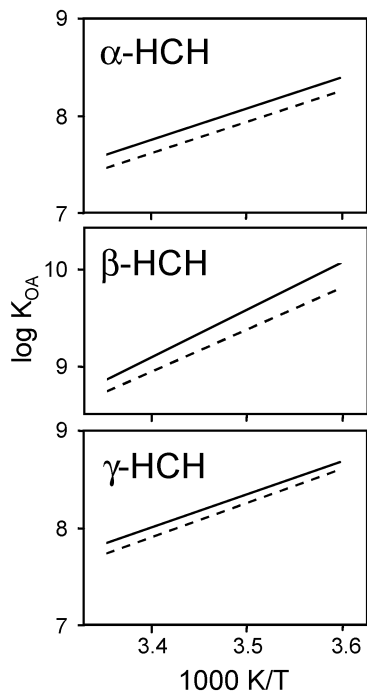


**Figure 6.** Relationships between the logarithm of the Henry's law constant in pascal cubic meters per mole ( $\log H$ ) of  $\alpha$ -,  $\beta$ -, and  $\gamma$ -HCH and the reciprocal absolute temperature in kelvin ( $T$ ), based on data from Sahuvar et al. (dynamic headspace method) ( $\diamond$ ),<sup>10</sup> Sahuvar et al. (bubble stripping method) ( $+$ ),<sup>10</sup> Kucklick et al. ( $\square$ ),<sup>25</sup> Altschuh et al. ( $\circ$ ),<sup>26</sup> Jantunen and Bidleman ( $\times$ ),<sup>27</sup> Atlas et al. ( $\triangle$ ),<sup>28</sup> and Fendinger and Glotfelty ( $*$ ).<sup>48</sup> The solid line ( $-$ ) indicates the linear regression through the literature-derived values; the dashed line ( $- -$ ) represents the final adjusted values.

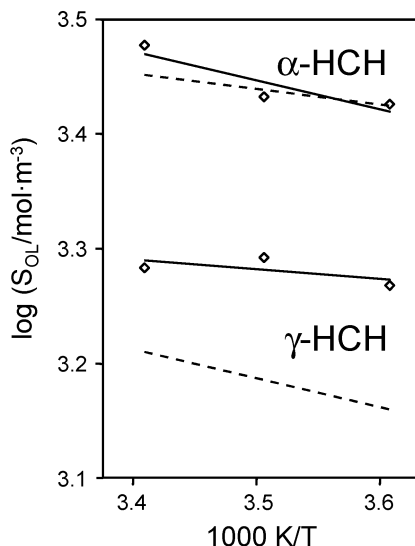
substances from gas chromatographic retention times or when using LSER equations with solvation descriptors which are solely derived from chromatographic data.

The divergent partitioning behavior of  $\beta$ -HCH may result in substantially different environmental pathways. Scavenging of organic vapor by rain becomes increasingly important at Henry's law constants below  $0.1\text{ Pa}\cdot\text{m}^3\cdot\text{mol}^{-1}$ , and it is likely that  $\beta$ -HCH is scavenged much more efficiently than  $\alpha$ - and  $\gamma$ -HCH. This will limit its atmospheric long-range transport potential relative to those of  $\alpha$ - and  $\gamma$ -HCH, and it could account for the different distribution patterns of HCHs in the Northern Pacific and the Arctic Ocean.<sup>6</sup> A higher  $K_{OA}$  value implies stronger retention of  $\beta$ -HCH in soils and plant foliage. In contrast to  $\alpha$ - and  $\gamma$ -HCH, the  $\beta$ -isomer may even sorb to atmospheric particles at very low ambient temperatures, such as occur in polar regions. The FAVs suggest that the  $\log K_{OW}$  for  $\beta$ -HCH is comparable to those of the  $\alpha$ - and  $\gamma$ -isomers. This implies that more efficient bioaccumulation observed for the  $\beta$ -HCH<sup>5</sup> is more likely due to higher resistance to metabolic conversion than to higher lipophilicity.

A data evaluation exercise as presented here can indicate what additional types of measurement would be most effective in further constraining the partitioning characteristics of an organic chemical. The study suggests that the reported data for  $\alpha$ - and  $\gamma$ -HCH are generally very consistent and their partitioning characteristics are thus

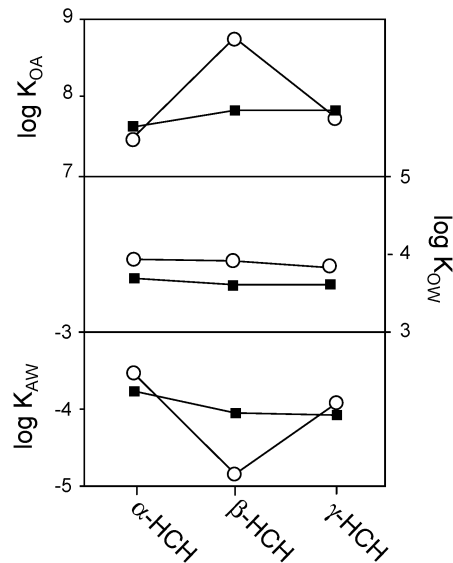


**Figure 7.** Relationships between the logarithm of the octanol–air partition coefficient ( $\log K_{OA}$ ) of  $\alpha$ -,  $\beta$ -, and  $\gamma$ -HCH and the reciprocal absolute temperature in kelvin ( $T$ ). The final adjusted values (dashed line, - - -) are somewhat lower than the measured data reported by Shoeib and Harner (solid line, —).<sup>9</sup>



**Figure 8.** Relationships between the logarithm of the liquid solubility in octanol ( $\log(S_{O/L}/\text{mol}\cdot\text{m}^{-3})$ ) of  $\alpha$ - and  $\gamma$ -HCH and the reciprocal absolute temperature in kelvin ( $T$ ), based on data from Niimi ( $\diamond$ ).<sup>8</sup> The solid line (—) indicates the linear regression for the values from Niimi;<sup>8</sup> the dashed line (- - -) represents the final adjusted values.

already better established than those of most other highly chlorinated organic substances. Although only few measurements of the properties of the  $\beta$ -isomer have been conducted, the reported data are encouragingly consistent. Most useful would be measured values of the entropy of fusion, as well as measurements of the water solubility as a function of temperature for that isomer. It would also be desirable to have independent validation of  $\beta$ -HCH's unusually high  $K_{OA}$  and low  $K_{AW}$ . Although the data availability for the remaining HCH isomers is poor, it may not be justified to expend great effort on the determination of



**Figure 9.** Comparison of the final adjusted values ( $\circ$ ) for the  $\log K_{OA}$ ,  $\log K_{OW}$ , and  $\log K_{AW}$  of  $\alpha$ -,  $\beta$ -, and  $\gamma$ -HCH with the values ( $\blacksquare$ ) predicted using the linear solvation energy relationships and solvation descriptors from Abraham et al.<sup>11</sup> Discrepancies are large for the  $\log K_{OA}$  and  $\log K_{AW}$  of  $\beta$ -HCH.

their properties, considering that they are generally not detected in the environment.

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