# Volumetric and Speed of Sound of Ionic Liquid, 1-Butyl-3-methylimidazolium Hexafluorophosphate with Acetonitrile and Methanol at $T=(298.15$ to 318.15) $K$ 

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#### Abstract

We report the density ( $\rho$ ) and speed of sound ( $u$ ) data for 1-butyl-3-methylimidazolium hexafluorophosphate $\left([\mathrm{BMIM}]\left[\mathrm{PF}_{6}\right]\right)+$ methanol and $\left([\mathrm{BMIM}]\left[\mathrm{PF}_{6}\right]\right)+$ acetonitrile binary mixtures over the entire range of their compositions at $T=(298.15$ to 318.15$) \mathrm{K}$. From these data, excess molar volume and isentropic compressibility deviation values have been calculated and fitted to the fourth-order Redlich-Kister equation. The excess molar volume values ( $V^{\mathrm{E}}$ ) for acetonitrile mixtures are more negative than methanol mixtures. Isentropic compressibility deviation values ( $\Delta \kappa_{\mathrm{s}}$ ) in methanol mixtures are more than acetonitrile mixtures. The results have been interpreted in terms of ion-dipole interactions and structural factors of the ionic liquid and these organic solvents.


## Introduction

Room-temperature ionic liquids (RTILs) are a class of organic salts that are liquids at or near room temperature in their pure state. They exhibit many interesting properties such as negligible vapor pressure, low melting point ( $<373 \mathrm{~K}$ ), a wide liquid range, suitable viscosity, stability up to high temperature, and high solubility for both polar and nonpolar organic and inorganic substances. ${ }^{1-3}$ Due to their nonvolatile nature and favorable solvation properties, RTILs have been suggested as green and benign replacements for traditional volatile organic solvents. These ionic liquids have been recently used as solvents in catalysis, chemical processing, liquid-liquid separations, vaporliquid equilibria, batteries, and fuel cells investigations. ${ }^{4-7}$ Despite their importance and interest, detailed knowledge on the thermodynamic behavior of the mixtures of ionic liquids with organic molecular solvents, which is important for the design of any technological processes, is very limited. The 1-butyl-3-methylimidazolium hexafluorophosphate ( $\left.[\mathrm{BMIM}]\left[\mathrm{PF}_{6}\right]\right)$ is historically the most important and the most commonly investigated ionic liquid. Thermodynamic functions such as heat capacities, enthalpy changes, and densities for $[B M I M]\left[\mathrm{PF}_{6}\right]$ have been reported at different temperatures. ${ }^{8,9}$ Solid-liquid and liquid-liquid equilibria of this ionic liquid in water and 1-butanol have been studied. ${ }^{10-12}$ Its solubilities in aromatic hydrocarbons and alkanes have been performed by dynamic method. ${ }^{13}$ Computational method such as Monte Carlo simulation for investigation of this ionic liquid has been performed, and volumetric properties such as isothermal compressibility and volume expansibility values have been computed. ${ }^{14}$ The volume expansibility and isothermal compressibility properties of this ionic liquid in pure state have also been obtained. ${ }^{15}$ However, there are no reports on the volumetric properties of this ionic liquid in nonaqueous ordinary solvents. There are reports on the volumetric properties of other ionic liquids in aqueous and nonaqueous solvents. Heintz et al. ${ }^{16}$ determined the excess molar volumes and viscosities for mixtures of methanol with 4-methyl- $N$ -

[^0]butylpyridinium tetrafluoroborate at different temperatures. Wang et al. ${ }^{17}$ have determined densities and viscosities for mixtures of 1-butyl-3-methylimidazolium tetrafluoroborate ionic liquid with acetonitrile, dichloromethane, 2 -butanone, and $N, N$-dimethylformamide. Recently, experimental data of densities and viscosities have been presented for 1-ethyl-3-methylimidazolium tetrafluoroborate $+\mathrm{H}_{2} \mathrm{O}$ binary systems over the entire range of compositions at different temperatures by Zhang et al. ${ }^{18}$ Also, Rebelo et al. ${ }^{19}$ reported the excess molar volumes for 1-butyl-3-methylimidazolium tetrafluoroborate $+\mathrm{H}_{2} \mathrm{O}$. Aki et al. ${ }^{20}$ reported that the solvent strength and polarity of [BMIM] $\left[\mathrm{PF}_{6}\right]$, as measured using two different fluorescent probes, is more polar than MeCN and less polar than MeOH .

In the present work, we report the density and speed of sound measurements on mixtures of $[\mathrm{BMIM}]\left[\mathrm{PF}_{6}\right]$ with methanol ( MeOH ) and acetonitrile ( MeCN ) over the entire composition range at $T=$ (298.15 to 318.15 ) K , from which the excess molar volume ( $V^{\mathrm{E}}$ ) and isentropic compressibility deviation $\left(\Delta \kappa_{\mathrm{s}}\right)$ values have been calculated. The chosen solvents MeOH and MeCN are versatile compounds, especially in their wide range of applicability as solvents in chemical and technological processes. These solvents are also the most commonly used for background electrolytes in nonaqueuos capillary electrophoresis. ${ }^{21}$ These solvents are inexpensive and easily available at high purity. The calculated quantities can be used in a qualitatively or quantitatively way to provide information about molecular structure and nature of intermolecular forces in these kind of liquid mixtures. ${ }^{22,23}$

## Experimental Section

Materials. $[\mathrm{BMIM}]\left[\mathrm{PF}_{6}\right]$ was obtained from Solvent Innovation Co. (Köln, Germany) with mass fraction of $>0.98$, and it was used after being vacuum desiccated for at least 4 h to remove trace amounts of water. MeOH and MeCN were supplied from Merck, with purity gradient grade (mass fraction $>0.999$ ), and were used without further purification. During the course of the experiments, the purity of the solvents was monitored by density measurements.

Table 1. Physical Properties of Pure Components at $T=$ 298.15 K: Density ( $\rho$ ) and Speed of Sound ( $u$ ) Data

|  | $\rho / \mathrm{g} \cdot \mathrm{cm}^{-3}$ |  |  |  | $u / \mathrm{m} \cdot \mathrm{s}^{-1}$ |  |
| :--- | :---: | :---: | :---: | :---: | :---: | :---: |
| component | exp. | lit. | exp. | lit. |  |  |
| MeOH | 0.786531 | $0.78656,{ }^{32} 0.78654^{30}$ |  | 1102.68 | $1101.9^{32}$ |  |
| MeCN | 0.776533 | $0.776532,,^{33}$ | $0.776588^{34}$ |  | 1278.62 |  |
| $1280.8^{35}$ |  |  |  |  |  |  |
| $[\mathrm{BMIM}]\left[\mathrm{PF}_{6}\right]$ | 1.366657 | $1.36603,{ }^{34} 1.3603^{14,15}$ |  | 1442.41 |  |  |

Apparatus and Procedure. Density and speed of sound data were continuously measured using a commercial density and speed of sound measurement apparatus (Anton Paar DSA 5000 densimeter and speed of sound analyzer). Details of the experimental setup and measuring procedure have been given elsewhere. ${ }^{24}$ The temperature was automatically kept constant within uncertainty $\pm 0.001 \mathrm{~K}$. In each measurement, the uncertainty of density and speed of sound were $\pm 3.0 \cdot 10^{-6} \mathrm{~g} \cdot \mathrm{~cm}^{-3}$ and $\pm 0.1 \mathrm{~m} \cdot \mathrm{~s}^{-1}$, respectively. Density and speed of sound values of the pure components are given in Table 1 at 298.15 K and compared with the literature values.

## Results and Discussion

The experimental density ( $\rho$ ) and speed of sound ( $u$ ) data for the MeCN (1) $+[\mathrm{BMIM}]\left[\mathrm{PF}_{6}\right]$ (2) and MeOH (1) + $[\mathrm{BMIM}]\left[\mathrm{PF}_{6}\right]$ (2) mixtures, as a function of $[\mathrm{BMIM}]\left[\mathrm{PF}_{6}\right]$ mole fraction ( $x_{2}$ ) at the temperature range from $T=$ (298.15 to 318.15) K are presented respectively in Tables 2 and 3.

Values of the excess molar volume ( $V^{\mathrm{E}}$ ) were calculated using the relation:

$$
\begin{equation*}
V^{\mathrm{E}}=\sum_{j=1}^{2} x_{j} M_{j}\left(\rho^{-1}-\rho_{j}^{-1}\right) \tag{1}
\end{equation*}
$$

where $M_{j}, x_{j}, \rho_{j}$, and $\rho$ are molar mass of the components, mole fractions, densities of pure liquids, and densities of mixtures, respectively, and subscript $j=1$ is for the MeCN or MeOH and $j=2$ is for the $[\mathrm{BMIM}]\left[\mathrm{PF}_{6}\right]$.

The $V^{\mathrm{E}}$ values have been fitted to the Redlich-Kister equation ${ }^{25}$ :

$$
\begin{equation*}
V^{\mathrm{E}} / \mathrm{m}^{3} \cdot \mathrm{~mol}^{-1}=x_{2}\left(1-x_{2}\right) \sum_{i} A_{i}\left(1-2 x_{2}\right)^{i} \tag{2}
\end{equation*}
$$

It was found that the fourth-order Redlich-Kister equation represents satisfactorily the experimental excess molar volumes for the studied systems. The polynomial coefficients $\left(A_{i}\right)$ of eq 2 for the studied systems along with the corresponding standard deviations $\left(\sigma\left(\mathrm{V}^{\mathrm{E}}\right)\right.$ ) are collected in Table 4.

Speed of sound measurements in solutions furnishes knowledge about ion-ion and ion-solvent interactions. ${ }^{22,23,26}$ Using the speed of sound and density data, the isentropic compressibilities ( $\kappa_{\mathrm{s}}$ ) were calculated from the LaplaceNewton's equation:

$$
\begin{equation*}
\kappa_{\mathrm{s}}=\frac{1}{\rho u^{2}} \tag{3}
\end{equation*}
$$

where $u$ is the speed of sound for the investigated mixtures. The experimental isentropic compressibility deviations ( $\Delta \kappa_{\mathrm{s}}$ ) are obtained using the relation:

$$
\begin{equation*}
\Delta \kappa_{\mathrm{s}}=\kappa_{\mathrm{s}}-\left(\sum_{j}^{2} x_{j} \kappa_{\mathrm{s} j}\right) \tag{4}
\end{equation*}
$$

where $\kappa_{\mathrm{s} j}$ is the value of isentropic compressibility of pure
Table 2. Experimental Density ( $\rho$ ) and Speed of Sound (u) Data for the MeCN (1) $+[$ BMIM $]\left[\mathrm{PF}_{6}\right]$ (2) System
Table 3. Experimental Density ( $\rho$ ) and Speed of Sound (u) Data for the MeOH (1) $+\left[\mathrm{BMIM}^{2}\right]\left[\mathrm{PF}_{6}\right]$ (2) System

| $x_{2}$ | T/K |  |  |  |  |  |  |  |  |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | 298.15 |  |  | 303.15 |  |  | 308.15 |  |  | 313.15 |  |  | 318.15 |  |  |
|  | $\rho$ | $u$ | $10^{6} V^{E}$ | $\rho$ | $u$ | $10^{6} V^{E}$ | $\rho$ | $u$ | $10^{6} V^{E}$ | $\rho$ | $u$ | $10^{6} V^{E}$ | $\rho$ | $u$ | $10^{6} V^{E}$ |
|  | $\mathrm{kg} \cdot \mathrm{m}^{-3}$ | $\mathrm{m} \cdot \mathrm{s}^{-1}$ | $\mathrm{m}^{3} \cdot \mathrm{~mol}^{-1}$ | $\mathrm{kg} \cdot \mathrm{m}^{-3}$ | $\mathrm{m} \cdot \mathrm{s}^{-1}$ | $\mathrm{m}^{3} \cdot \mathrm{~mol}^{-1}$ | $\mathrm{kg} \cdot \mathrm{m}^{-3}$ | $\mathrm{m} \cdot \mathrm{s}^{-1}$ | $\mathrm{m}^{3} \cdot \mathrm{~mol}^{-1}$ | $\mathrm{kg} \cdot \mathrm{m}^{-3}$ | $\mathrm{m} \cdot \mathrm{s}^{-1}$ | $\mathrm{m}^{3} \cdot \mathrm{~mol}^{-1}$ | $\mathrm{kg} \cdot \mathrm{m}^{-3}$ | $\mathrm{m} \cdot \mathrm{s}^{-1}$ | $\mathrm{m}^{3} \cdot \mathrm{~mol}^{-1}$ |
| 1 | 1366.657 | 1442.41 | 0 | 1362.401 | 1430.58 | 0 | 1358.304 | 1418.95 | 0 | 1354.195 | 1407.53 | 0 | 1350.081 | 1396.27 | 0 |
| 0.9208 | 1357.705 | 1435.22 | -0.095 | 1353.548 | 1423.47 | -0.115 | 1349.387 | 1411.94 | -0.112 | 1345.226 | 1400.58 | -0.111 | 1341.078 | 1389.38 | -0.113 |
| 0.7736 | 1337.498 | 1421.10 | -0.292 | 1333.239 | 1409.46 | -0.308 | 1328.992 | 1397.95 | -0.307 | 1324.76 | 1386.56 | -0.310 | 1320.543 | 1375.31 | -0.316 |
| 0.6222 | 1308.958 | 1400.51 | -0.439 | 1304.585 | 1388.86 | -0.453 | 1300.243 | 1377.38 | -0.455 | 1295.964 | 1365.94 | -0.467 | 1291.779 | 1354.65 | -0.491 |
| 0.4572 | 1263.599 | 1366.68 | -0.594 | 1259.044 | 1355.14 | -0.603 | 1254.805 | 1343.61 | -0.631 | 1250.504 | 1332.11 | -0.656 | 1246.033 | 1320.70 | -0.667 |
| 0.3573 | 1223.908 | 1340.69 | -0.691 | 1219.386 | 1329.07 | -0.711 | 1214.871 | 1317.49 | -0.724 | 1210.364 | 1305.95 | -0.741 | 1205.873 | 1294.50 | -0.760 |
| 0.2156 | 1136.500 | 1280.66 | -0.761 | 1131.894 | 1268.92 | -0.784 | 1127.297 | 1257.18 | -0.805 | 1122.699 | 1245.49 | -0.828 | 1118.121 | 1233.85 | -0.855 |
| 0.1869 | 1111.366 | 1261.62 | -0.754 | 1106.761 | 1249.80 | -0.779 | 1102.148 | 1237.97 | -0.800 | 1097.528 | 1226.13 | -0.824 | 1092.914 | 1214.27 | -0.851 |
| 0.0786 | 972.943 | 1180.74 | -0.578 | 968.272 | 1167.69 | -0.598 | 963.583 | 1154.62 | -0.618 | 958.877 | 1141.58 | -0.639 | 954.071 | 1128.58 | -0.656 |
| 0.0484 | 914.856 | 1155.52 | -0.467 | 910.156 | 1141.54 | -0.483 | 905.442 | 1127.55 | -0.498 | 900.703 | 1113.58 | -0.515 | 895.952 | 1099.67 | -0.533 |
| 0.0223 | 852.499 | 1132.08 | -0.285 | 847.778 | 1116.93 | -0.294 | 843.039 | 1101.80 | -0.303 | 838.277 | 1086.69 | -0.313 | 833.490 | 1071.68 | -0.324 |
| 0 | 786.531 | 1102.68 | 0 | 781.808 | 1086.37 | 0 | 777.066 | 1070.11 | 0 | 772.283 | 1053.96 | 0 | 767.474 | 1037.91 | 0 |

component $j$. The $\Delta \kappa_{\mathrm{s}}$ values were also correlated by the Redlich-Kister equation: ${ }^{25-27}$

$$
\begin{equation*}
\Delta \kappa_{\mathrm{s}} / \mathrm{Pa}^{-1}=x_{2}\left(1-x_{2}\right) \sum_{i} A_{\kappa i}\left(1-2 x_{2}\right)^{i} \tag{5}
\end{equation*}
$$

The fitting parameters $A_{\kappa i}$ were estimated by the leastsquares method, and the obtained values together with the related standard deviations $\left(\sigma\left(\Delta \kappa_{\mathrm{s}}\right)\right)$ are given in Table 5.

The experimental $V^{\mathrm{E}}$ values for the investigated systems together with the curves obtained using eq 2 are represented in Figures 1 and 2. Similarly, the experimental $\Delta \kappa_{\mathrm{s}}$ and obtained curves using eq 5 are shown in Figures 3 and 4. For $V^{\mathrm{E}}$ and $\Delta \kappa_{\mathrm{s}}$, the Redlich-Kister fitting curves are asymmetric. Also, a minimum in $V^{\mathrm{E}}$ and $\Delta \kappa_{\mathrm{s}}$ are reached with mole fraction of this ionic liquid near to 0.3 and 0.2 for $\mathrm{MeCN}(1)+[\mathrm{BMIM}]\left[\mathrm{PF}_{6}\right](2)$ and $\mathrm{MeOH}(1)+[\mathrm{BMIM}]-$ [ $\left.\mathrm{PF}_{6}\right]$ (2) systems, respectively. Similar behavior has been observed for 1-butyl-3-methylimidazolium tetrafluoroborate in nonaqueous organic solvent such as MeCN , dichloromethane, 2-butanone and $\mathrm{N}, \mathrm{N}$-dimethylformamide. ${ }^{17}$ The magnitude and sign of $V^{\mathrm{E}}$ values are a reflection of the type of interactions taking place in the mixture, which are the result of different effects containing the breakdown of the MeCN dipolar interactions and MeOH self-associated molecules from each other (a positive volume), the breakdown of the ionic liquid ion-pair (a positive volume), and the negative contribution of volume due to the packing effect and ion-dipole interaction of MeCN or MeOH molecules with the ionic liquid. The molar volume for [BMIM] $\left[\mathrm{PF}_{6}\right]$ is $207.94 \cdot 10^{-6} \mathrm{~m}^{3} \cdot \mathrm{~mol}^{-1}$, which is greater than the molar volumes of $\mathrm{MeOH}\left(40.74 \cdot 10^{-6} \mathrm{~m}^{3} \cdot \mathrm{~mol}^{-1}\right)$ and $\mathrm{MeCN}\left(52.86 \cdot 10^{-6} \mathrm{~m}^{3} \cdot \mathrm{~mol}^{-1}\right)$ at $T=298.15 \mathrm{~K}$. The large difference between molar volumes of these solvents and $[\mathrm{BMIM}]\left[\mathrm{PF}_{6}\right]$ imply that the relatively small MeOH or MeCN molecules fit in the available free volume of ionic liquid upon mixing. Also, the negative values of $V^{\mathrm{E}}$ show that the effect due to the ion-dipole interactions between organic solvents ( MeOH or MeCN ) and $[\mathrm{BMIM}]\left[\mathrm{PF}_{6}\right]$ are dominating over the disruption of dipolar orders in MeCN or MeOH .

As can be seen from the Figures 1 and 2, the $V^{\mathrm{E}}$ values for MeCN mixtures are more negative than the MeOH mixtures. Similar behavior is observed for the other isotherms. Then, the larger negative $V^{\mathrm{E}}$ values for the $\mathrm{MeCN}(1)+[\mathrm{BMIM}]\left[\mathrm{PF}_{6}\right](2)$ than the $\mathrm{MeOH}(1)+[\mathrm{BMIM}]-$ [ $\mathrm{PF}_{6}$ ] (2) imply that in the MeCN solutions there are stronger ion-dipole interactions and packing effects than the MeOH solutions. The higher relative permittivity and dipole moment of MeCN as compared with the corresponding values for methanol ${ }^{28}$ and strong hydrogen bonding between MeOH molecules indicate the stronger ion-dipole interactions and packing effects of MeCN in ionic liquid solutions.

Figure 5 shows that the $\kappa_{\mathrm{s}}$ values for MeCN mixtures are less than the MeOH mixtures at $T=298.15 \mathrm{~K}$, and similar behavior is observed for the other isotherms. It is obvious from Figure 5 that the solution of $[\mathrm{BMIM}]\left[\mathrm{PF}_{6}\right]$ in MeOH is more compressible than the solutions of [BMIM]$\left[\mathrm{PF}_{6}\right]$ in MeCN at a particular concentration and temperature. This indicates a different solvation process of [BMIM] $\left[\mathrm{PF}_{6}\right]$ in MeOH in comparison with the MeCN , because of its characteristic structure as compared with the MeCN. X-ray analysis on pure MeCN has revealed that the linear MeCN dipoles are arranged in antiparallel positions, ${ }^{21,29}$ leading to a smaller value for $\kappa_{\mathrm{s}}$ for MeCN than MeOH for which it was found that it is extensively self-associated through hydrogen bonding in the pure

Table 4. Coefficients of the Redlich-Kister Equation (eq 2) for Excess Molar Volumes ( $V^{\mathbf{E}}$ ) and the Standard Deviations $\left(\sigma\left(V^{\mathrm{E}}\right)\right)$ of the $\mathrm{MeCN}(1)+[B M I M]\left[\mathrm{PF}_{6}\right]$ (2) and MeOH (1) $+[\mathrm{BMIM}]\left[\mathrm{PF}_{6}\right]$ (2) Mixtures

| solvent | $T / \mathrm{K}$ | $10^{6} A_{0}$ | $10^{6} A_{1}$ | $10^{6} A_{2}$ | $10^{6} A_{3}$ | $10^{6} A_{4}$ | $10^{6} \sigma\left(V^{\mathrm{E}} / \mathrm{m}^{3} \cdot \mathrm{~mol}^{-1}\right)^{a}$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| MeCN | 298.15 | -4.8252 | -2.7242 | 1.4250 | -3.4221 | -6.2046 | 0.024 |
|  | 303.15 | -5.0024 | -2.5483 | 0.6903 | -4.3954 | -5.0195 | 0.029 |
|  | 308.15 | -5.2218 | -2.8504 | 0.5481 | -3.9914 | -4.5048 | 0.010 |
|  | 313.15 | -5.4397 | -2.8728 | 1.0872 | -4.6767 | -6.2037 | 0.027 |
|  | 318.15 | -5.6770 | -3.0345 | 1.0321 | -4.998 | -6.6254 | 0.029 |
| MeOH | 298.15 | -2.2895 | -1.4392 | -0.9797 | -3.6861 | -3.8364 | 0.021 |
|  | 303.15 | -2.3350 | -1.4879 | -1.1601 | -3.6384 | -4.0424 | 0.022 |
|  | 308.15 | -2.4076 | -1.5835 | -0.9273 | -3.7417 | -4.4814 | 0.022 |
|  | 313.15 | -2.4888 | -1.6311 | -0.7823 | -3.9311 | -4.8176 | 0.022 |
|  | 318.15 | -2.5558 | -1.6167 | -0.8983 | -4.2095 | -4.0886 | 0.022 |
|  | $\left[\sum_{i}\left(V_{\exp }^{\mathrm{E}}-V_{\mathrm{cal}}^{\mathrm{E}}\right)^{2}\right]$ |  |  |  |  |  |  |
| ${ }^{a} \sigma\left(V^{\mathrm{E}}\right)=$ |  | ; $n$ is number of the experimental data; the units of $A_{i}$ values are $\mathrm{m}^{3} \cdot \mathrm{~mol}^{-1}$. |  |  |  |  |  |

Table 5. Coefficients of the Redlich-Kister Equation (eq 5) for Isentropic Compressibility Deviations ( $\Delta \kappa_{s}$ ) and the Standard Deviations $\left(\sigma\left(\Delta \kappa_{5}\right)\right)$ of the MeCN (1) $+[B M I M]\left[\mathrm{PF}_{6}\right]$ (2) and MeOH (1) $+[B M I M]\left[\mathrm{PF}_{6}\right]$ (2) Mixtures

| solvent | T/K | $10^{10} A_{\kappa} 0$ | $10^{10} A_{\kappa} 1$ | $10^{10} A_{\kappa} 2$ | $10^{10} A_{\kappa} 3$ | $10^{10} A_{\kappa} 4$ | $10^{10} \sigma\left(\Delta \kappa_{\mathrm{s}} / \mathrm{Pa}^{-1}\right)^{a}$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| MeCN | 298.15 | -6.601 | -4.586 | -2.700 | -4.464 | -4.571 | 0.014 |
|  | 303.15 | -6.996 | -4.852 | -2.881 | -4.824 | -4.880 | 0.016 |
|  | 308.15 | -7.422 | -5.171 | -3.142 | -5.153 | -5.093 | 0.015 |
|  | 313.15 | -7.885 | -5.483 | -3.278 | -5.656 | -5.719 | 0.019 |
|  | 318.15 | -8.384 | -5.837 | -3.508 | -6.177 | -6.250 | 0.021 |
| MeOH | 298.15 | -11.652 | -8.009 | -3.457 | -12.712 | -14.917 | 0.062 |
|  | 303.15 | -12.231 | -8.392 | -3.559 | -13.687 | -16.160 | 0.066 |
|  | 308.15 | -12.844 | -8.796 | -3.650 | -14.727 | -17.498 | 0.070 |
|  | 313.15 | -13.487 | -9.223 | -3.754 | -15.827 | -18.903 | 0.075 |
|  | 318.15 | -14.167 | -9.668 | -3.862 | -17.001 | -20.400 | 0.080 |
|  | $\left[\sum_{i}\left(\Delta \kappa_{\mathrm{s}(\exp )}-\Delta \kappa_{\mathrm{s}(\mathrm{cal})}\right)^{2}\right]^{1 / 2}$ |  |  |  |  |  |  |
| ${ }^{a} \sigma\left(\Delta \kappa_{\mathrm{s}}\right)=$ | $n$ | - $]$ | of $A_{\kappa i}$ va | re $\mathrm{Pa}^{-1}$ |  |  |  |



Figure 1. Excess molar volume $\left(V^{\mathrm{E}}\right)$ vs mol fraction of [BMIM]$\left[\mathrm{PF}_{6}\right]$ for $\mathrm{MeCN}(1)+[\mathrm{BMIM}]\left[\mathrm{PF}_{6}\right]$ (2) mixture: $\square$, 298.15 K ; $\square$, $303.15 \mathrm{~K} ; \diamond, 308.15 \mathrm{~K} ; \bullet 313.15 \mathrm{~K} ; \mathbf{\Delta}, 318.15 \mathrm{~K}$; solid line, Redlich-Kister (eq 2).
state. ${ }^{29}$ The results obtained from the $\kappa_{\mathrm{s}}$ values for the studied mixtures are compatible with those obtained from the excess molar volumes. Recently, similar results have been obtained for tetraalkylammonium tetraphenylborate and tetraalkylammonium bromide in MeOH and MeCN


Figure 2. Excess molar volume $\left(V^{\mathrm{E}}\right)$ vs mol fraction of [BMIM]$\left[\mathrm{PF}_{6}\right]$ for $\mathrm{MeOH}(1)+[\mathrm{BMIM}]\left[\mathrm{PF}_{6}\right]$ (2) mixture: $\square, 298.15 \mathrm{~K}$; $\boldsymbol{\square}$, $303.15 \mathrm{~K} ; \diamond, 308.15 \mathrm{~K} ; \bullet, 313.15 \mathrm{~K} ; \mathbf{\Delta}, 318.15 \mathrm{~K}$; solid line, Redlich-Kister (eq 2).
solutions using the association constants determined from conductometric measurements. ${ }^{36}$ The association constants for the both studied organic salts in MeOH are higher than that of MeCN . This means that while ion-ion interactions


Figure 3. Variation of isentropic compressibility deviations ( $\Delta \kappa_{\mathrm{s}}$ ) vs mol fraction of [BMIM] [PF6] for MeOH (1) + [BMIM] [PF6] (2) mixture: $\square, 298.15 \mathrm{~K} ; ~ ■, 303.15 \mathrm{~K} ; \diamond, 308.15 \mathrm{~K} ; ~ \bullet 313.15 \mathrm{~K} ; ~ \Perp$, 318.15 K; solid line, Redlich-Kister (eq 5).


Figure 4. Variation of isentropic compressibility deviations ( $\Delta \kappa_{\mathrm{s}}$ ) vs mol fraction of [BMIM][PF6] for MeCN (1) + [BMIM][PF6] (2) + mixture: $\square$, $298.15 \mathrm{~K} ; \mathbf{■}, 303.15 \mathrm{~K} ; \diamond$, $308.15 \mathrm{~K} ; \bullet, 313.15 \mathrm{~K}$; ©, 318.15 K ; solid line, Redlich-Kister (eq 5).
are dominant in MeOH solutions, in the case of MeCN solutions ion-solvent interactions are dominant.

For the both systems the values of $\Delta \kappa_{\mathrm{s}}$ are negative over the entire composition range and at all the temperatures studied. Figures 3 and 4 show that for these systems, the behavior of $\Delta \kappa_{\mathrm{s}}$ versus ionic liquid mole fraction is very similar to those of excess molar volume at the all studied temperatures. The behavior of $\Delta \kappa_{\mathrm{s}}$ implies that these mixtures are less compressible than the ideal mixture. This is due to a closer approach of unlike molecules and stronger interaction between components of mixtures ${ }^{26,30}$ that lead to decreasing compressibility.


Figure 5. Variation of isentropic compressibility ( $\kappa_{\mathrm{s}}$ ) vs mol fraction of $[\mathrm{BMIM}]\left[\mathrm{PF}_{6}\right]: \mathrm{O}, \mathrm{MeOH}(1)+\left[\mathrm{BMIM}^{2}\right]\left[\mathrm{PF}_{6}\right]$ (2); $\mathrm{MeCN}(1)+[\mathrm{BMIM}]\left[\mathrm{PF}_{6}\right](2)$ mixtures at 298.15 K .

## Conclusions

Excess molar volume ( $V^{\mathrm{E}}$ ) and isentropic compressibility deviation $\left(\Delta \kappa_{\mathrm{s}}\right)$ values of $[\mathrm{BMIM}]\left[\mathrm{PF}_{6}\right]$ in MeOH and MeCN mixtures have been calculated from the measured density and speed of sound data at $T=(298.15$ to 318.15) K. For $V^{\mathrm{E}}$ and $\Delta \kappa_{\mathrm{s}}$, the Redlich-Kister fitting curves are asymmetric. Also, a minimum in $V^{\mathrm{E}}$ and $\Delta \kappa_{\mathrm{s}}$ are reached with a mole fraction of this ionic liquid near 0.3 and 0.2 for the $\mathrm{MeCN}(1)+[\mathrm{BMIM}]\left[\mathrm{PF}_{6}\right]$ (2) and $\mathrm{MeOH}(1)+[\mathrm{BMIM}]\left[\mathrm{PF}_{6}\right]$ (2) systems, respectively. The measured negative $V^{\mathrm{E}}$ values for these systems indicate that effect due to the ion-dipole interactions and packing between organic solvents (MeOH or MeCN ) and $[\mathrm{BMIM}]\left[\mathrm{PF}_{6}\right]$ are dominating over the disruption of dipolar orders in MeCN or MeOH .

The $V^{\mathrm{E}}$ values for MeCN mixtures are more negative than the MeOH mixtures, which imply that in the MeCN solutions there are stronger ion-dipole interactions and packing effects than the MeOH solutions. Similar results are obtained from comparison of the isentropic compressibility values for theses systems.

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Received for review April 30, 2005. Accepted June 27, 2005.
JE050165T


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