

Equilibrium of Hydrogen + Cyclopentane and Carbon Dioxide + Cyclopentane Binary Hydrates[†]

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Cyclopentane (CP) forms sII hydrates, in which CP only occupies the large cavities. Small gas molecules such as hydrogen and carbon dioxide can be engaged in the small cavities. However, there are no reported data on the equilibrium conditions of CP + H₂ and CP + CO₂ binary hydrates, which are essential to developing CO₂ capturing or H₂ enriching processes. In this study, the dissociation temperature of CP + H₂ hydrate pressures ranging from (2.7 to 11.1) MPa and CP + CO₂ hydrates at pressures of (0.89 to 3.51) MPa was measured by using a high-pressure MicroDSC.

Introduction

Gas hydrates are crystalline compounds in which small molecules such as methane, nitrogen, carbon dioxide, hydrogen, etc. stabilize the cavities formed by hydrogen-bonded water molecules.^{1,2} The equilibrium condition of gas hydrates is predominately determined by the nature of hydrate formers; e.g., the dissociation pressure is 300 MPa for H₂ hydrates³ and 2.91 MPa for CO₂ hydrates¹ at 280 K, indicating that CO₂ preferably occupies the water cavities at the lower pressure. Therefore, it is possible to remove CO₂ from the H₂ + CO₂ mixture by hydrate formation.

The concentration of CO₂ in the precombustion stream after gasification is around (20 to 40) v/v % with a typical total pressure of (2.5 to 5) MPa.⁴ Having a large enough driving force for CO₂ removal in the hydrate form is related to reducing the equilibrium pressure of CO₂ hydrates. To reduce the equilibrium pressure of CO₂ hydrates, one approach is to reduce the crystallization temperature, but it increases the operating cost due to further cooling. Another option is to add a small amount of organic compounds such as tetrahydrofuran (THF),⁵ tetrabutylammonium bromide (TBAB),⁶ and cyclopentane (CP).

Cyclopentane (CP) is known to form sII hydrates with a melting point higher than that of THF hydrates at atmospheric pressure.^{7,8} Many studies have reported the dissociation conditions of binary hydrates of THF with different gases, such as H₂,^{9,10} CO₂,⁵ CH₄,¹¹ etc. However, there were a few studies on the equilibrium data of binary hydrates of CP with a gas,^{12–14} and no equilibrium data are available for the binary hydrates of CP with hydrogen and CO₂. The equilibrium condition of these binary hydrates is important in designing the CO₂ capturing processes of precombustion. In this work, the dissociation temperatures of CP + H₂ hydrates in a pressure range of (2.7 to 11.1) MPa and those of CP + CO₂ hydrates in a pressure range of (0.89 to 3.51) MPa are presented.

Experimental Section

Materials. Cyclopentane with a certified purity of > 95 % was purchased from Sigma-Aldrich. H₂ was supplied by

Labelmaster with a purity of 99 %, and CO₂ was obtained from T. W. Smith with a minimum purity of 99 %. All chemicals were used as received without further purification. Deionized water was produced in our laboratory with a resistivity of 17 mΩ·cm⁻¹.

Apparatus. Figure 1 shows the schematic diagram of the experimental setup to measure the dissociation temperatures of hydrates using a high-pressure MicroDSCVII (SETARAM). The principle of this technology was described in detail by Le Parlouër et al.¹⁵ This high-pressure differential scanning calorimetry is less time-consuming compared to the classical PVT technique. Several studies have indicated that this technique is accurate enough to determine the equilibrium conditions of gas hydrates.^{15–17}

Dalmazzone et al.¹⁷ compared the dissociation temperature of methane hydrates by using a classical thermodynamic method (PVT) and a calorimetric method (DSC), and they concluded that PVT and DSC results are in good agreement with data available in the literature.

The high-pressure cells with a volume of 0.33 cm³ are made of hastelloy, and they can be operated up to 40 MPa and at temperatures between (233.2 and 393.2) K. The uncertainty of temperature measurement stated by the manufacturer is ± 0.02 K. The MicroDSC was calibrated with *n*-decane (274.51 K), water (273.15 K), and naphthalene (353.38 K). The pressure of the sample cell is measured by using an ITS-5 M pressure transducer (ONEhalf20, (0 to 34.47) MPa) with the uncertainty of ± 0.05 MPa. The temperature, heat flow, and pressure of the sample cell are sampled by the SETSOFT interface. The onset temperature of the endothermic peak is taken as the dissociation temperature or the melting point.

Procedures. About 0.01 cm³ DI water and 0.015 cm³ CP were charged to the sample cell, followed by purging the gas phase with the test gas (H₂ or CO₂) twice. For the CP + water system, the dissociation conditions were measured at 0.1 MPa air. The sample cell was then pressurized with the test gas to a desired pressure. The cells were cooled down to 242.6 K and then heated up to 274.3 K for CP + water and CP + H₂ + water systems and 281.3 K for the CP + CO₂ + water system. The CP + water and CP + H₂ + water systems were held at 274.3 K for 2 h and then heated up to 293.2 K. The CP + CO₂ + water system was kept at 281.3 K for 0.5 h and then heated

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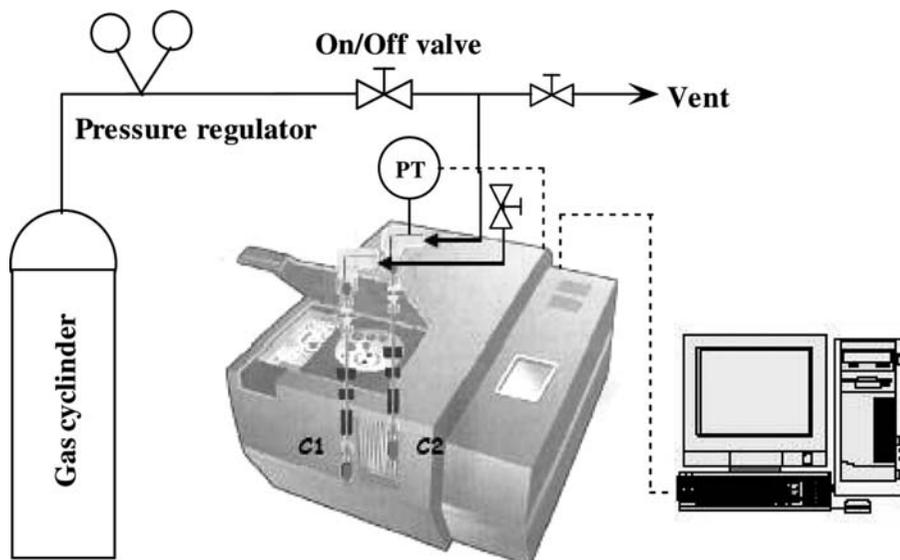


Figure 1. Schematic diagram of the experimental setup (modified from Parlouër¹⁵).

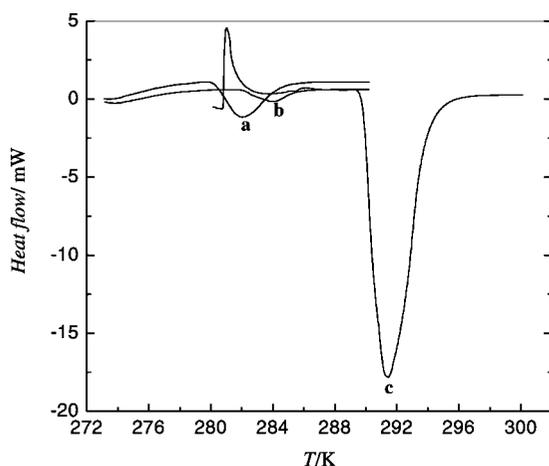


Figure 2. Thermograph of CP + water, CP + water + H₂, and CP + water + CO₂ hydrates: a, CP + water; b, CP + water + H₂, $P = 4.94$ MPa; c, CP + water + CO₂, $P = 1.84$ MPa.

Table 1. Dissociation Temperatures of CP + H₂ at Different Pressures

T/K	P/MPa (± 0.05 MPa)
280.68 ± 0.01	2.70
281.56 ± 0.01	4.94
282.36 ± 0.02	7.00
283.07 ± 0.01	9.04
283.72 ± 0.02	11.09

up to 303.2 K. The measurement at each data point was repeated three times, and the average value with the precision of measurement was reported in this work.

Results and Discussions

A typical DSC thermograph of the CP + water + gas (H₂ or CO₂) system is given in Figure 2 where the heating curves for three different hydrates are presented. Curve a is the heating curve for the CP hydrate, while curves b and c are representing the heating curves for the CP + H₂ and CP + CO₂ hydrates. In curve c, there is an exothermic peak, which indicates the formation of hydrates from the unconverted water before the dissociation of the CP + CO₂ hydrates.

Melting Point of Ice and CP Hydrates. The melting point of ice is (273.69, 273.46, and 273.01) K at a heating rate of

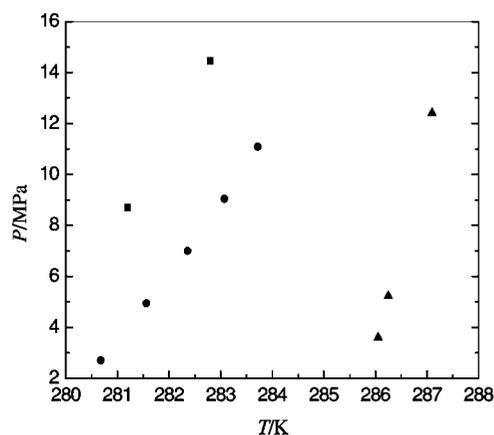


Figure 3. Dissociation conditions for H₂ binary hydrates: ■, THF + H₂, weight fraction of THF = 0.1907;⁹ ●, CP + H₂; ▲, TBAB + H₂, weight fraction of TBAB = 0.43.⁶

Table 2. Dissociation Temperatures of CP + CO₂ at Different Pressures

T/K	P/MPa (± 0.05 MPa)
286.65 ± 0.16	0.89
289.00 ± 0.01	1.50
289.86 ± 0.10	1.84
291.42 ± 0.10	2.23
292.19 ± 0.04	2.72
292.40 ± 0.09	3.11
292.61 ± 0.13	3.51

0.25 K·min⁻¹, 0.5 K·min⁻¹, and 1 K·min⁻¹, respectively. The heating rate of 1 K·min⁻¹ was used in this work to determine the dissociation temperature of hydrates since the ice melting point at this rate is the closest to 273.15 K. The difference between the melting point reported here and the literature value is due to the systematic or gross error. The small difference may be noted with the real temperature due to the thermal gradient and the time for the heat to cross the cell wall and the detector, although the measurement is carried out in the sample.

Figure 2 shows that the melting point of CP hydrates is (280.17 \pm 0.16) K at atmospheric pressure. Werezak⁸ reported the melting point of CP hydrates is 280.85 K, which is 0.63 K higher than the quadruple point temperature (280.22 K) of the CP + water system.¹⁸ This quadruple point temperature determined by PVT measurements can be more reliable than

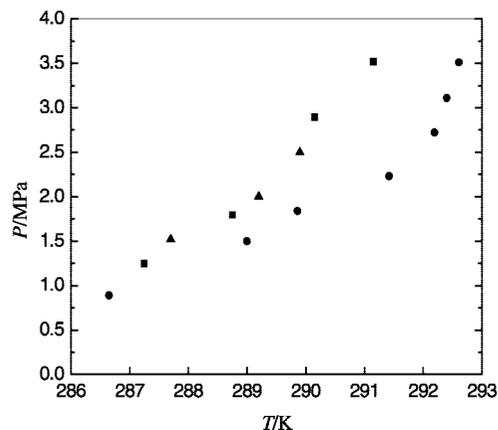


Figure 4. Dissociation conditions for CO₂ binary hydrates: ■, THF + CO₂, weight fraction of THF = 0.1097;⁵ ●, CP + H₂; ▲, TBAB + CO₂, weight fraction of TBAB = 0.427.⁶

the reported melting point because no detail of apparatuses and procedures was presented by Werezak.⁸ The quadruple point temperature is almost identical to the melting point, like a very small difference between the ice melting point and the triple point of water. The melting point of CP hydrates (280.17 K) presented here is very close to the reported quadruple point temperature (280.22 K), suggesting that the heating rate of 1 K·min⁻¹ is sufficient for determining the dissociation temperature of hydrates in our MicroDSC.

CP + H₂ Hydrates. The dissociation temperature of CP + H₂ hydrates at pressures between (2.7 and 11.1) MPa is summarized in Table 1, and the results are also plotted in Figure 3. The dissociation temperature of CP + H₂ hydrates is lower than that of TBAB + H₂ hydrates⁶ but higher than that of THF + H₂ hydrates.⁹ This trend coincides with the melting point of THF hydrates, CP hydrates, and TBAB semiclathrate hydrates.

CP + CO₂ Hydrates. The dissociation temperature of CP + CO₂ at pressures of (0.89 to 3.51) MPa is listed in Table 2, and the results are also plotted in Figure 4. The dissociation temperature of CP + CO₂ is a little higher than that of TBAB + CO₂ and THF + CO₂ hydrates^{5,6} at the same pressures, while the dissociation temperature of TBAB + CO₂ is close to that of THF + CO₂ hydrates. The effect of THF, CP, and TBAB on the equilibrium conditions of CO₂ binary hydrates does not follow the order of the melting point of THF hydrates, CP hydrates, and TBAB semiclathrate hydrates. One possible explanation is that the high concentration of dissolved CO₂ in aqueous phase has a significant effect on the activity of THF and TBAB.

Conclusion

The dissociation temperatures of CP + H₂ hydrates in a pressure range of (2.7 to 11.1) MPa and those of CP + CO₂ hydrates at pressures of (0.89 to 3.51) MPa were determined by using a high-pressure MicroDSC. The dissociation temper-

atures of H₂ binary hydrates with other hydrate promoters are strongly dependent on the nature of the promoters. However, the dissociation temperature of CO₂ binary hydrates is less affected by the property of the other hydrate promoters.

Literature Cited

- (1) Mao, W. L.; Mao, H. K.; et al. Hydrogen clusters in clathrate hydrate. *Science* **2002**, *297*, 2247–2249.
- (2) Sloan, E. D.; Koh, C. A. *Clathrate Hydrate of Natural Gases*, 3rd ed.; CRC Press: Boca Raton, 2008.
- (3) Mao, W. L.; Mao, H. K. Hydrogen storage in molecular compounds. *Proc. Natl. Acad. Sci. U.S.A.* **2004**, *101*, 708–710.
- (4) Gupta, M.; Colye, I.; Thambimuthu, K. CO₂ capture technologies and opportunities in Canada. 1st Canadian CC&S Roadmap Workshop, Calgary, Canada, September 18–19, 2003. Available at <http://www.nrcan.gc.ca/es/etb/cetc/combustion/co2trm>.
- (5) Delahaye, A.; Fournaison, L.; Marinhas, S.; Chatti, I.; Petitet, J. P.; Dalmazzone, D.; Furst, W. Effect of THF on equilibrium pressure and dissociation enthalpy of CO₂ hydrates applied to secondary refrigeration. *Ind. Eng. Chem. Res.* **2006**, *45*, 391–397.
- (6) Arjmandi, M.; Chapoy, A.; Tohidi, B. Equilibrium data of hydrogen, methane, nitrogen, carbon dioxide, and natural gas in semi-clathrate hydrates of tetrabutyl ammonium bromide. *J. Chem. Eng. Data* **2007**, *52*, 2153–2158.
- (7) Zhang, Y.; Debenedetti, P. G.; Rud'homme, R. K.; Pethica, B. A. Differential scanning calorimetry studies of clathrate hydrate formation. *J. Phys. Chem. B* **2004**, *108*, 16717–16722.
- (8) Werezak, G. N. Aqueous solution concentration by a clathrate type of gas hydrate formation. *Chem. Eng. Prog. Symp. Ser.* **1969**, *65* (91), 6–18.
- (9) Anderson, R.; Chapoy, A.; Tohidi, B. Phase relationships and binary clathrate hydrate formation in system H₂-THF-H₂O system. *Langmuir* **2007**, *23*, 3440–3444.
- (10) Florusse, L. J.; Peters, C. J.; Schoonman, J.; Hester, K. C.; Koh, C. A.; Dec, S. F.; Marsh, K. N. Stable low-pressure hydrogen clusters stored in a binary clathrate hydrate. *Science* **2004**, *306*, 469–471.
- (11) de Deugd, R. M.; Jager, M. D.; Arons, J. D. Mixed hydrates of methane and water-soluble hydrocarbons modeling of empirical results. *AIChE J.* **2001**, *47*, 693–704.
- (12) Sun, Z. G.; Fan, S. S.; Guo, K. H.; Shi, L.; Guo, Y. K.; Wang, R. Z. Gas hydrate phase equilibrium data of cyclohexane and cyclopentane. *J. Chem. Eng. Data* **2002**, *47*, 313–315.
- (13) Tohidi, B.; Danesh, A.; Todd, A. C.; Burgass, R. W.; Ostergaard, K. K. Equilibrium data and thermodynamic modeling of cyclopentane and neopentane hydrate. *Fluid Phase Equilib.* **1997**, *138*, 241–250.
- (14) Takeya, S.; Ohmura, R. Phase equilibrium for structure II hydrates formed with krypton co-existing with cyclopentane, cyclopentene, or tetrahydropyran. *J. Chem. Eng. Data* **2006**, *51*, 1800–1883.
- (15) Le Parlouër, P.; Dalmazzone, C.; Herzhaft, B.; Rousseau, L.; Mathonat, C. Characterization of gas hydrates formation using a new high pressure micro-DSC. *J. Therm. Anal. Calorim.* **2004**, *78*, 165–172.
- (16) Dalmazzone, D.; Hamed, N.; Dalmazzone, C.; Rousseau, L. Application of high pressure DSC to the kinetics of formation of methane hydrate water-in-oil emulsion. *J. Therm. Anal. Calorim.* **2006**, *85*, 361–368.
- (17) Dalmazzone, D.; Kharrat, M.; Lachet, V.; Fouconnier, B.; Clausse, D. DSC and PVT measurements methane and trichlorofluoromethane hydrate dissociation equilibria. *J. Therm. Anal. Calorim.* **2002**, *70*, 493–505.
- (18) Fan, S. S.; Liang, D. Q.; Guo, K. H. Hydrate equilibrium conditions for cyclopentane and a quaternary cyclopentane-rich mixture. *J. Chem. Eng. Data* **2001**, *46*, 930–932.

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