

Correlations

An Expression for Ratio of Critical Temperature to Critical Pressure with the Heat Capacity for Low to Medium Molecular Weight Compounds

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In this paper, a new correlation for prediction of the ratio of critical temperature to critical pressure has been developed in terms of heat capacity at 298.15 K, which is readily available for many compounds. The correlation has been applied for more than 100 low to medium size compounds. The results of these estimations validate the generalization of this correlation. The comparison between predicted and available experimental data shows an absolute relative error of 4.69 %. The results show that the accuracy of the proposed correlation is similar to the methods of Constantinou and Gani,⁷ Ambrose,^{2,3} and Joback⁵ for various types of compounds.

Introduction

In the application of thermodynamic equations of state, one must have knowledge of critical temperature and critical pressure. The critical constants are key parameters in the prediction of thermodynamic and transfer properties via the principle of the corresponding state. They are also of importance in equation of state calculations and in the design of processes for supercritical fluid extraction. They are often used in composition-dependent mixing rules for the parameters to describe mixtures. Critical temperature and pressure are widely used in estimation of pure component constants. Many of the estimation methods are based on the group contribution concept and require knowledge of the boiling point and structure of the substance. Examples of such methods include those of Lydersen,¹ Ambrose,^{2,3} Fedors,⁴ Joback,⁵ Somayajulu,⁶ and Constantinou and Gani.⁷

One of the first successful group contribution methods to estimate critical properties was developed by Lydersen.¹ Joback⁵ suggested a modification of Lydersen's¹ method. This method depends on the group contribution method. Joback⁵ reevaluated Lydersen's¹ scheme, added several functional groups, and determined the new values of the group contributions. His proposed relations are

$$T_C = T_B \left[0.584 + 0.965 \sum \Delta_T - \left(\sum \Delta_T \right)^2 \right]^{-1} \quad (1)$$

$$P_C = \left(0.113 + 0.0032n_A - \sum \Delta_P \right)^{-2} \quad (2)$$

The units employed for T_C and P_C are, respectively, Kelvin and bar. n_A is the number of atoms in the molecule. The Δ quantities are evaluated by summing contributions for various atoms or groups of atoms.

Ambrose^{2,3} suggested another estimated method including a group contribution technique using the following correlations

$$T_C = T_B \left[1 + \left(1.242 + \sum \Delta_T \right)^{-1} \right] \quad (3)$$

$$P_C = M \left[0.339 + \sum \Delta_P \right]^{-2} \quad (4)$$

where T_C and P_C are, respectively, in Kelvin and bar. In employment of correlations, the normal boiling point T_B (at 1 atm) and molecular weight M are needed. The Joback⁵ and Ambrose^{2,3} methods perform well for low-to-medium molecular weight compounds. Their validity for high molecular weight and/or structurally complex compounds is not yet clear.⁸ The estimation of the critical properties with the methods of Lydersen,¹ Ambrose^{2,3} (see Reid et al.⁹), and Joback and Reid¹⁰ (and others, e.g., Klincewicz and Reid,¹¹ Somayajulu⁶) requires accurate values for the normal boiling point, which is usually not available for high molecular weight compounds. The recent group contribution method by Constantinou and Gani⁷ is more general in the sense that the critical temperature (and pressure) is estimated only from the structure of the compound.

Constantinou and Gani⁷ developed an advanced group contribution method based on the UNIFAC groups. It is more accurate than the methods of Klincewicz and Reid¹¹ and Lydersen.¹ They suggested the following correlations

$$\exp(T_C/181.128) = \sum_i N_i t_{ci} + \sum_j M_j t_{cj} \quad (5)$$

$$(P_C - 1.3705)^{-0.5} - 0.100220 = \sum_i N_i p_{ci} + \sum_j M_j p_{cj} \quad (6)$$

where T_C and P_C are, respectively, in Kelvin and bar. In these equations, N_i and M_j are number of occurrences of the type- i first-order group and the type- j second-order group in a compound, respectively. t_{ci} , t_{cj} and p_{ci} , p_{cj} are contributions of the type- i and type- j for estimation of the critical temperature and critical pressure, respectively. In the group contribution method proposed by Constantinou and Gani⁷—except from the classical UNIFAC main and subgroups which are called first-order groups—second-order groups have been incorporated for the differences of the physical properties among the isomers to be captured. Unlike the methods proposed by Joback and Reid¹⁰ and Ambrose^{2,3} (see Reid et al.⁹), Constantinou and Gani⁷ gave some emphasis on the proper extrapolation of the critical

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Table 1. Absolute Deviation between Experimental and Predicted Critical Temperature (K) and Critical Pressure (bar) by Various Group Contribution Methods

compound	ref	Constantinou and Gani		Ambrose		Joback	
		ΔT_C	ΔP_C	ΔT_C	ΔP_C	ΔT_C	ΔP_C
nC_{48}	12	0.00	^a	24	^a	349	^a

^a Lack of experimental data.

properties at high molecular weight; thus, their method may be more useful for high molecular weight compounds (see in Table 1). This point is not confirmed yet by literature evidence based on thorough evaluation/comparison of the above estimation methods for heavy/complex compounds.⁸

Elhassan et al.¹³ developed a correlation for *n*-alkanes which is based on the fact that the quantities of T_C/P_C are proportional to the molecular weight for each homologous series. The proposed relation is

$$\ln(T_C/P_C) = -3.70171 + 1.38315 \ln(M + 25.3538) \quad (7)$$

Kontogeorgis et al.⁸ suggested that the ratio $T_C:P_C$ can be expressed in terms of the van der Waals surface area that is estimated using the group increments given by Bondi¹⁴ and are readily available in all UNIFAC tables (e.g., Fredeslund et al.¹⁵) for any compounds. The method is suitable for medium to high molecular weight compounds. The proposed relation is

$$T_C/P_C = 9.0673 + 0.43309(Q_w^{1.3} + Q_w^{1.95}) \quad (8)$$

where T_C is in K; P_C is in bar; and Q_w is the van der Waals surface area.

Due to deficiencies and problems of available group contribution estimation methods for the critical properties, we suggest a correlation that tackles the problem of estimating the critical properties in a different and simpler way. We observed that, unlike the critical properties alone, the ratio $T_C:P_C$ follows a regular trend with the ratio of heat capacity at 298.15 K to the universal gas constant for low-to-medium molecular weight compounds.

The rest of the paper is organized as follows. The correlation of $T_C:P_C$ with the heat capacity of real gas at 298.15 K is presented, and an application of proposed correlation and comparison with other methods is given. We end with discussion of our results and the conclusions.

New Correlation

According to the above correlations, the critical temperature and pressure are dependent on the molecular structure of components. To propose a more general and simple correlation, a term that corresponds to the molecular structure can be used. The heat capacity could be related to the structure of the compounds.^{16–21} Joback⁵ suggested a group contribution method for the polynomial coefficient of heat capacity of ideal gases as follows

$$C_p(T) = \left(\sum_j n_j \Delta_a - 37.93 \right) + \left(\sum_j n_j \Delta_b + 0.210 \right) T + \left(\sum_j n_j \Delta_c - 3.91 \cdot 10^{-4} \right) T^2 + \left(\sum_j n_j \Delta_d + 2.06 \cdot 10^{-7} \right) T^3 \quad (9)$$

where n_j is the number of groups of the *j*th type and the Δ contributions are for the *j*th atomic or molecules group. The temperature T is in Kelvin, and C_p is in $J \cdot mol^{-1} \cdot K^{-1}$. Yoneda⁹ modified a group contribution technique for ideal heat capacity that was originally proposed by Anderson et al.^{9,16} In this method, one begins with a base molecule and sequentially

Table 2. Variety of Number of Data Points Used in This Study

compound type	no. of data points
hydrocarbons	79
oxygenated hydrocarbons	61
nitrogenated hydrocarbons	11
hydrocarbon sulfide and mercaptanes	7
halogenated hydrocarbons	8
inorganic	12
total	178

modifies the structure by substituting other groups to arrive at the final structure. Each substitution has a group contribution value, and values are summed to arrive at the final value of the heat capacity.

$$C_p(T) = \sum_j n_j \Delta_a + \left(\sum_j n_j \Delta_b \right) \left(\frac{T}{1000} \right) + \left(\sum_j n_j \Delta_c \right) \left(\frac{T}{1000} \right)^2 \quad (10)$$

Δ is the contribution, and n_j is the number of times the contribution is required. T is in Kelvin, and C_p is in $J \cdot mol^{-1} \cdot K^{-1}$.

A group contribution method for estimating the ideal gas heat capacity just for hydrocarbons is employed by Thinh et al.^{17,18} as the following equation

$$C_p(T) = \sum_j n_j \left[A + B_1 \exp\left(\frac{-C_1}{T^{n_1}} \right) - B_2 \exp\left(\frac{-C_2}{T^{n_2}} \right) \right] \quad (11)$$

where T is in Kelvin; C_p is in $J \cdot mol^{-1} \cdot K^{-1}$; and A , B_1 , B_2 , C_1 , C_2 , n_1 , and n_2 are constants for all hydrocarbon groups. This equation is a modified form suggested earlier by Yuan and Mok.¹⁹ It is sometimes inconvenient to use because it can not be integrated analytically, and numerical techniques must be employed. For the estimation of ideal gas heat capacity, an accurate group contribution method was developed by Benson^{20,21} and his colleagues. Contributions are given only for atoms with valences greater than unity. For each group, the key atom is given but followed by a notation specifying other atoms bonded to the key atom. The heat capacity is obtained by summing the necessary group contributions at the system temperature.

Using the aforementioned subjects, the heat capacity (C_p) is dependent on the molecular structure of each compound. Also, since the $T_C:P_C$ ratio is dependent on the molecular structure, one can relate the $T_C:P_C$ ratio to the heat capacity. An appropriate correlation for the ratio of the critical temperature to the critical pressure can be introduced in the form of

$$T_C/P_C = \varepsilon C_p/R \quad (12)$$

In this correlation, T_C is the critical temperature in Kelvin; P_C is the critical pressure in atm; R is the universal gas constant; C_p is the heat capacity of real gases at 298.15 K; and ε is the equation coefficient in $K \cdot atm^{-1}$. Note that the ratio of the heat capacity to the universal gas constant is dimensionless.

In this study, to obtain the equation coefficient (ε), an extensive database of critical temperature and pressure data together with heat capacities of real gases for low-to-medium molecular weight compounds is used.^{22,23} Table 2 represents the variety of number of compounds used in this study. Values of $RT_C/P_C C_p$ have been determined for the data training set which consist of 178 compounds (see Table 3). The data training set includes hydrocarbons (i.e., alkane, alkene, alkyne, and cyclo compounds), halogenated hydrocarbons, oxygenated hydrocarbons (i.e., ether, ketone, ester, alcohol, aldehyde, and carboxylic acid), nitrogenated hydrocarbons, hydrocarbon sulfide, mercaptanes, and inorganic compounds. As one can see in this table,

Table 3 Continued

compd no.	chemical special	chemical formula	$(RT_C/P_C C_P)$		$(T_C/P_C)/K \cdot \text{atm}^{-1}$				100 RE
			K · atm ⁻¹	predicted by eq 13	Joback ⁵	Cons. & Gani ⁷	Ambrose ^{2,3}	Kontogeorgis et al. ⁸	
167	Air		1.0153 ^b	3.4487	3.4487	3.4487	3.4487	2.6066	
168	Oxygen	O ₂	0.8840	3.4988	3.4988	3.4988	3.4988	12.136	Kontogeorgis et al. ⁸
169	Nitrogen	N ₂	1.0765	3.4682	3.4682	3.4682	3.4682	8.0538	
170	Ammonia	NH ₃	0.8504	4.3792	4.3792	4.3792	4.3792	20.393	
171	Nitrous oxide	N ₂ O	0.9263	4.3087	4.3087	4.3087	4.3087	11.645	
172	Cyanogen	C ₂ N ₂	0.9937 ^b	7.2499	7.2499	7.2499	7.2499	6.2131	
173	Carbon monoxide	CO	1.1010	3.4696	3.4696	3.4696	3.4696	10.093	
174	Carbon dioxide	CO ₂	0.9311	4.6133	4.6133	4.6133	4.6133	10.601	
175	Hydrogen chloride	HCl	1.1224	3.4703	3.4703	3.4703	3.4703	11.804	
176	Hydrogen sulfide	H ₂ S	1.0225	4.2053	4.2053	4.2053	4.2053	0.4193	
177	Sulfur dioxide	SO ₂	1.1569	2.5529	2.5529	2.5529	2.5529	26.518	
178	Sulfur trioxide	SO ₃	0.9959	6.0727	6.0727	6.0727	6.0727	5.7617	

^a Estimated by the second-order group contribution method. ^b In column 4, is obtained from ref 22 and other values from ref 23.

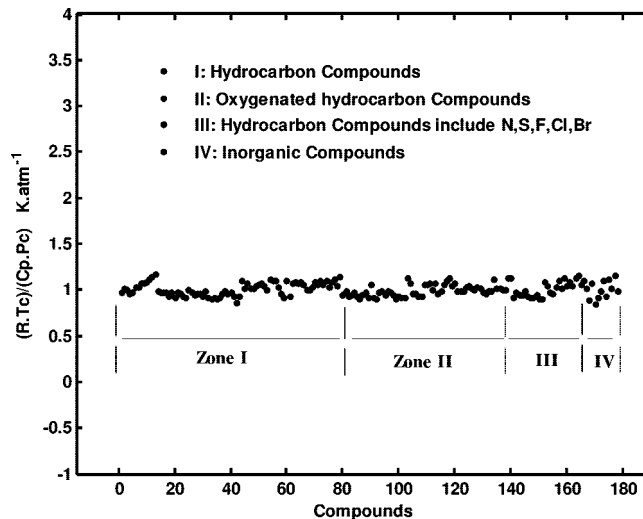
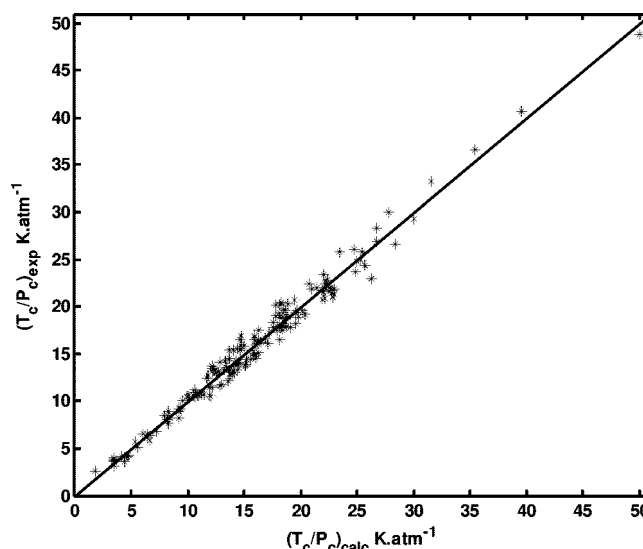
Figure 1. Correlation of $RT_C/P_C C_P$ for 178 compoundsFigure 2. Correlation of experimental T_C/P_C versus T_C/P_C calculated from eq 13 for the training data set.

Table 4. Variety of Number of Test Data Used in This Study

compound type	no. of data points
hydrocarbons	23
oxygenated hydrocarbons	18
nitrogenated hydrocarbons	3
hydrocarbon sulfide and mercaptanes	2
halogenated hydrocarbons	3
total	49

the values of $RT_C/P_C C_P$ for all of the compounds used are nearly close to one. The mean absolute relative error between values of $RT_C/P_C C_P$ and one is less than 5.89 %. Therefore, the equation coefficient (ϵ) in eq 12 is considered equal to one.

Results and Discussion

Figure 1 shows the value of $RT_C/P_C C_P$ for 178 compounds. It can be seen that the proposed correlation works well for the light and medium organic compounds, but there are considerable errors for some organic and inorganic compounds. Although high molecular weight compounds have a high error, this error is not necessarily for high molecular weight compounds. The value of $RT_C/P_C C_P$ for some of the light compounds deviates from unity similar to the high molecular weight compounds. It

Table 5. Value of $RT_C/P_C C_P$ and Comparison of the Estimated Ratio T_C/P_C by Equation 13 with the Experimental Data and Various Group Contribution Methods, Together with Values for Relative Errors RE = $((T_C/P_C)_{\text{exp}} - (T_C/P_C)_{\text{calc}})/((T_C/P_C)_{\text{exp}})$ for 49 Compounds (Test Data Set)

compd no.	chemical special	chemical formula	$(RT_C/P_C C_P)$				$(T_C/P_C)/K \cdot \text{atm}^{-1}$				100 RE			
			exp.	predicted by eq 13	Joback ⁵	Cons. & Gani ⁷	Ambrose ^{2,3}	Kontogeorgis et al. ⁸	predicted by eq 13	Joback ⁵	Cons. & Gani ⁷	Ambrose ^{2,3}	Kontogeorgis et al. ⁸	
1	<i>n</i> -Hexane	C ₆ H ₁₄	0.9914	16.918	16.552	16.658	17.128	17.823	2.1633	1.5368	1.2412	5.3400		
2	<i>n</i> -Heptane	C ₇ H ₁₆	1.0174	20.123	19.568	19.749 ^a	20.186	20.070	2.8708	3.1426	0.3112	0.2628		
3	2,2-Dimethylpropane	C ₅ H ₁₂	0.9331	13.735	12.933	12.386	12.243	16.080	8.3089	9.8201	10.859	17.075		
4	3-Methylpentane	C ₆ H ₁₄	0.9593	16.376	16.243	16.171	16.619	18.400	0.8152	1.2525	1.4808	12.359		
5	3-Methylheptane	C ₈ H ₁₈	0.9889	22.389	22.159	22.335	22.858	22.530	1.0274	0.6524	2.0957	0.6325		
6	3,4-Dimethylhexane	C ₈ H ₁₈	0.9641	21.419	21.742	22.126	22.791	22.511	1.6174	3.3015	6.4039	5.0967		
7	3-Ethyl-3-methylpentane	C ₈ H ₁₈	0.9099	20.843	22.423	21.733	22.544	24.052	7.5829	4.2719	15.395	16.088		
8	2,2,3,3-Tetramethylpentane	C ₈ H ₂₀	0.8787	22.463	25.174	25.924 ^a	25.254	26.077	11.765	15.408	12.427	16.088		
9	2,2,5-Trimethylheptane	C ₁₀ H ₂₂	0.9697	27.081	27.855	28.207	27.892	28.633	4.5149	4.1576	2.9954	5.7324		
10	Propylene	C ₃ H ₆	1.0279	8.0003	8.2040	7.9079	7.9834	12.020	2.5456	1.546	0.2109	50.190		
11	1-Hexene	C ₆ H ₁₂	1.0347	16.264	15.714	16.302 ^a	16.340	17.006	3.3791	2.2372	0.4637	4.5815		
12	2-Methyl-1-butene	C ₆ H ₁₂	1.0318	13.656	13.458	14.172	12.949	15.499	1.4470	3.7744	5.1799	13.492		
13	1-Dodecene	C ₁₂ H ₂₄	1.0284	33.411	33.728	30.087	34.757	33.020	0.9487	9.9478	4.0297	1.1600		
14	<i>n</i> -Tetradecane	C ₁₄ H ₃₀	1.1482	44.725	44.412	45.505	42.995	42.335	0.6992	1.7444	3.8672	5.3420		
15	Methylacetylene	C ₃ H ₄	0.9940	7.2548	7.5041	7.6520	7.7615	11.814	6.1586	0.1942	5.4474	62.851		
16	Dimethylacetylene	C ₄ H ₆	1.0497	9.8654	10.291	10.124	10.398	13.195	0.3736	4.1914	5.4029	33.758		
17	1-Heptyne	C ₇ H ₁₂	0.9937 ^b	18.096	17.973	17.391	17.799	18.792	0.6768	9.1014	1.6412	3.8481		
18	1-Octyne	C ₈ H ₁₄	1.0040 ^b	21.019	20.506	20.573	19.890	21.145	2.4368	5.7378	3.3728	6.000		
19	Cyclobutane	C ₄ H ₈	1.0861	9.3381	9.0324	9.3160	9.5546	12.348	3.2732	0.2364	5.0573	32.236		
20	Cyclohexane	C ₆ H ₁₂	1.0622	13.680	13.131	14.530	13.648	15.554	5.9215	9.8359	0.2309	13.693		
21	Methylcyclohexane	C ₇ H ₁₄	1.0249	16.660	16.199	16.729	16.936	16.936	2.7652	6.2133	1.6592	5.1056		
22	Cyclopentene	C ₅ H ₈	1.0962	10.680	10.166	10.773	11.531 ^a	13.215	4.8117	0.8814	9.7939	0.3652		
23	<i>o</i> -Xylene	C ₈ H ₁₀	1.0719	17.077	15.906	17.324	17.834	16.604	6.8523	4.3007	4.3630	1.4505		
24	Ethanol	C ₂ H ₆ O	1.0861	8.5087	9.1288	7.9023 ^a	8.3536	13.500	2.9649	7.3000	1.8218	58.669		
25	1-Propanol	C ₃ H ₈ O	1.0334	10.622	10.685	11.130	10.540	15.175	0.6014	4.7744	0.7721	42.859		
26	1-Butanol	C ₄ H ₁₀ O	1.0128	13.145	13.223	13.493	12.825	17.097	0.5935	4.4428	2.6472	30.062		
27	Cyclohexanol	C ₆ H ₁₂ O	1.0118	15.496	15.349	14.137	14.692 ^a	18.925	0.9426	8.7642	5.1922	22.124		
28	<i>o</i> -Cresol	C ₇ H ₈ O	0.9123	13.968	15.345	14.248	14.316	15.581	9.8642	1.2192	2.0072	11.551		
29	1-Nonanol	C ₉ H ₂₀ O	0.9559	23.033	23.626	25.757	24.525	25.628	11.827	6.4781	11.973	11.268		
30	Methyl <i>n</i> -butyl ether	C ₆ H ₁₄ O	0.9809 ^b	15.612	15.892	15.426	15.756	16.678	1.2158	0.6003	0.9248	6.8321		
31	Methyl <i>tert</i> -butyl ether	C ₆ H ₁₄ O	0.9603 ^b	14.770	15.409	14.835	15.089	16.961	0.4381	0.7867	2.6677	14.830		
32	1-Butanal	C ₄ H ₈ O	1.0146	12.600	12.705	12.283	11.623	14.363	0.8399	2.6101	1.2392	13.993		
33	1-Hexanal	C ₆ H ₁₂ O	0.9686	17.307	17.661	17.078	17.478	18.221	2.0456	1.3223	7.7537	5.2810		
34	2-Hexanone	C ₆ H ₁₂ O	1.0073	17.970	17.635	18.439	18.441	18.221	1.8627	2.6086	2.6187	1.3950		
35	3-Pentanone	C ₅ H ₁₀ O	0.9842	15.361	15.614	16.546	15.365	16.170	0.4886	7.7122	0.0314	5.2630		
36	Pentaonic acid	C ₅ H ₁₀ O ₂	1.0742 ^b	18.194	16.816	17.057	18.562	17.047	7.5733	6.2501	14.209	2.0227		
37	Ethyl formate	C ₃ H ₆ O ₂	1.0162	10.937	11.149	10.645	10.872	13.466	1.9469	8.4562	6.703	23.125		
38	Ethyl acetate	C ₄ H ₈ O ₂	1.0074	13.772	13.857	12.786	12.845	15.135	0.6181	7.8140	5.4896	9.9010		
39	Ethyl propanoate	C ₅ H ₁₀ O ₂	0.9614	20.770	21.147	20.322	21.661	21.602	1.8157	4.3319	4.2938	4.0066		
40	Propyl 2-methylpropanoate	C ₇ H ₁₄ O ₂	1.0250	21.855	20.876	21.362	21.104	21.583	4.4795	5.0502	2.2576	1.2440		
41	3-Methylbutyl ethanoate	C ₇ H ₁₄ O ₂	1.0214	21.593	20.702	21.066	21.448	21.583	4.1241	9.3837	2.4426	0.0469		
42	Dimethyl amine	C ₂ H ₇ N	0.9889 ^b	8.4219	8.9505	9.1774	7.6932	8.6329	6.2769	8.3416	2.5055	44.670		
43	Aniline	C ₆ H ₇ N	0.9920	13.238	13.558	14.358	13.998	14.177	2.4241	7.9056	5.7377	7.0930		
44	Butyl amine	C ₄ H ₁₁ N	0.9518	13.209	14.046	14.283	12.992	15.292	6.3368	8.1313	1.6388	15.771		
45	<i>n</i> -Propyl mercaptan	C ₃ H ₇ S	1.0291 ^b	11.743	11.764	11.409	12.632	13.995	0.1828	0.8187	2.8439	19.177		
46	Isopentyl mercaptan	C ₅ H ₁₂ S	1.0082	17.481	17.180	15.906	16.074	20.808	1.7216	9.0109	8.0477	1.3901		
47	Bromomethane	CH ₃ Br	1.1570 ^b	5.9148	5.3331	7.1621	6.3936	5.6813	9.8338	21.087	8.0954	90.296		
48	Fluoroethane	C ₂ H ₅ F	1.0658	7.5905	7.5165	7.8913	8.1090	11.255	0.9748	3.9475	6.8317	7.996		
49	2-Chlorobutane	C ₄ H ₉ Cl	1.0658	14.314	13.637	14.148	13.327	15.373	4.7281	1.1577	1.9893	7.3996		

^a Estimated by the second-order group contribution method. ^b In column 4: obtained from ref 22 and other values from ref 23.

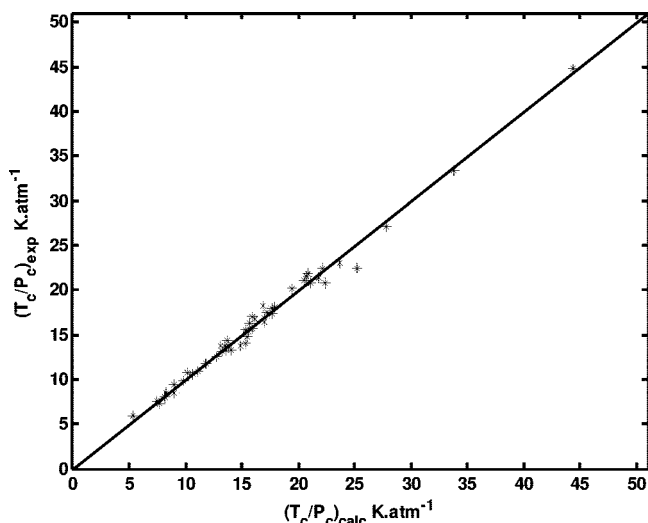


Figure 3. Correlation of experimental T_C/P_C versus of T_C/P_C calculated from eq 13 for the test data set.

can be described that the characterizations and properties of the compounds are extremely dependent on the structure of the compounds. For example, the compounds which have double or triple bonds will deviate more from unity because these bonds affect the properties of compounds. In addition, some of the groups such as O, N, and Cl will influence the electronegativity of compounds and so change the compounds' properties. Therefore, not only deviation from unity for some compounds is dependent on the molecular weight but also it is affected by the molecular structure. Consequently, to improve the accuracy of the previous correlation (eq 12), a cubic polynomial function is considered as follows

$$\frac{T_C}{P_C} = a \left(\frac{C_P}{R} \right)^3 + b \left(\frac{C_P}{R} \right)^2 + c \left(\frac{C_P}{R} \right) + d \quad (13)$$

By optimizing the relative error between experimental data and predicted values, it is found that the optimal constants of this equation are: $a = 0.0006314$, $b = -0.03017$, $c = 1.384$, $d = -1.038$. The linear regression, R -value, and RMSE between the desired and the predicted values from the correlation (13) are 0.9818 and 0.9852, respectively. The predicted values for T_C/P_C given by this new correlation, together with the values for various group contribution methods and relative errors (RE) for 178 components, are given in Table 3.

Figure 2 shows the closeness of the correlation between the predicted results from eq 13 and the experimental training data set. A perfect fit (experimental equal to predicted data) is indicated by the solid line. The close proximity of the best linear fit to the perfect fit, as observed in Figure 2, shows a good correlation among predictions and experimental data.

Also, the performance of the proposed correlation was tested using another set of 49 experimental data (Table 5) that were not previously used for training of the correlation. Table 4 provides information on the type and number of different compounds that comprised the test data set used in this study. The results indicate that the mean relative error (MRE) of the proposed correlation is less than 3.33 % for the test data set.

Figure 3 indicates there is good correlation between predicted and experimental test data of the T_C/P_C ratio. In this figure, the correlation outputs are plotted versus the experimental data as stars. A perfect fit (experimental equal to predicted data) is indicated by the solid line. The slope and the y -intercept of the best linear regression relating experimental to predicted data

are, respectively, 0.9661 and 0.4614 which nearly overlaps the perfect linear fit. The correlation coefficient (R -value) between the predictions and the experimental test data is 0.9896. This shows a very good correlation among the training and test data.

The results obtained using the proposed simple new correlation (eq 13) were compared with the experimental T_C/P_C test data and the values predicted using the methods of Joback,⁵ Ambrose,^{2,3} Constantinou and Gani,⁷ and also Kontogeorgis⁸ in Table 5. Also, in this table, results for the 49 compounds including the values of $RT_C/P_C C_P$ and relative errors (RE) are shown. The mean relative error between values of $RT_C/P_C C_P$ and one is less than 4.24 %. Also, the mean relative errors (MRE) between all the predictive methods and experimental data for this data set are: proposed correlation 3.33 %; Ambrose^{2,3} method 4.15 %; Constantinou and Gani⁷ method 4.78 %; Joback⁵ method 4.99 %; and Kontogeorgis⁸ method 16.37 %. The results show a good agreement between the proposed correlation and the experimental data. Also, the MRE of the proposed correlation is less than the previous methods for the test data set.

One of the advantages of the proposed correlation is in its ability to predict the T_C/P_C ratio for organic and inorganic compounds. It should be noted (as can be seen at the end of Table 3) that the proposed correlation is the only applicable method to predict the T_C/P_C ratio for inorganic compounds. The other methods are unable to predict the T_C/P_C ratio for inorganic compounds since there are not enough group contributions for these compounds. This limitation could be considered as a weakness for the other methods.

According to Table 3, one of the disadvantages of the Constantinou and Gani⁷ and Kontogeorgis⁸ methods appears when these are used to evaluate the T_C/P_C ratio for isomers of compounds such as octane. Critical temperature and pressure estimation by these methods is independent of any properties of the compounds such as boiling point temperature, molecular weight, or atom numbers in the molecule, so the estimation of T_C and P_C is only dependent on group contributions. Since isomers of one compound have the same group contributions, then the methods developed based on group contribution are not able to accurately predict values for T_C and P_C .

Tables 3 and 5 show the Kontogeorgis⁸ method strongly depends on the molecular weight of the compounds. The evaluated T_C/P_C ratio by the Kontogeorgis⁸ method would be more accurate for high molecular weight compounds. So, it could be better to use this method only for medium-to-high molecular weight compounds.

Although these methods have some disadvantages, it should be mentioned that the Constantinou and Gani⁷ method requires no compound properties to be measured but only the structural formula of a compound. This shows the generality of this method. A major benefit of using the Ambrose,^{2,3} Constantinou and Gani,⁷ and Joback⁵ methods is the ability of these methods to predict both critical temperature and critical pressure while the proposed correlation can be used to estimate one of the two critical properties whenever only the other one is available.

It is considerable that these methods are relatively complex because they need to be familiar with the molecular structure which in some cases is really time consuming, but the proposed correlation is simple and just needs the heat capacity to predict the T_C/P_C ratio. In addition, the calculation of critical temperature and pressure by these methods may be impossible because the group contributions of some compounds such as methane, ethylene, and acetylene are not available.

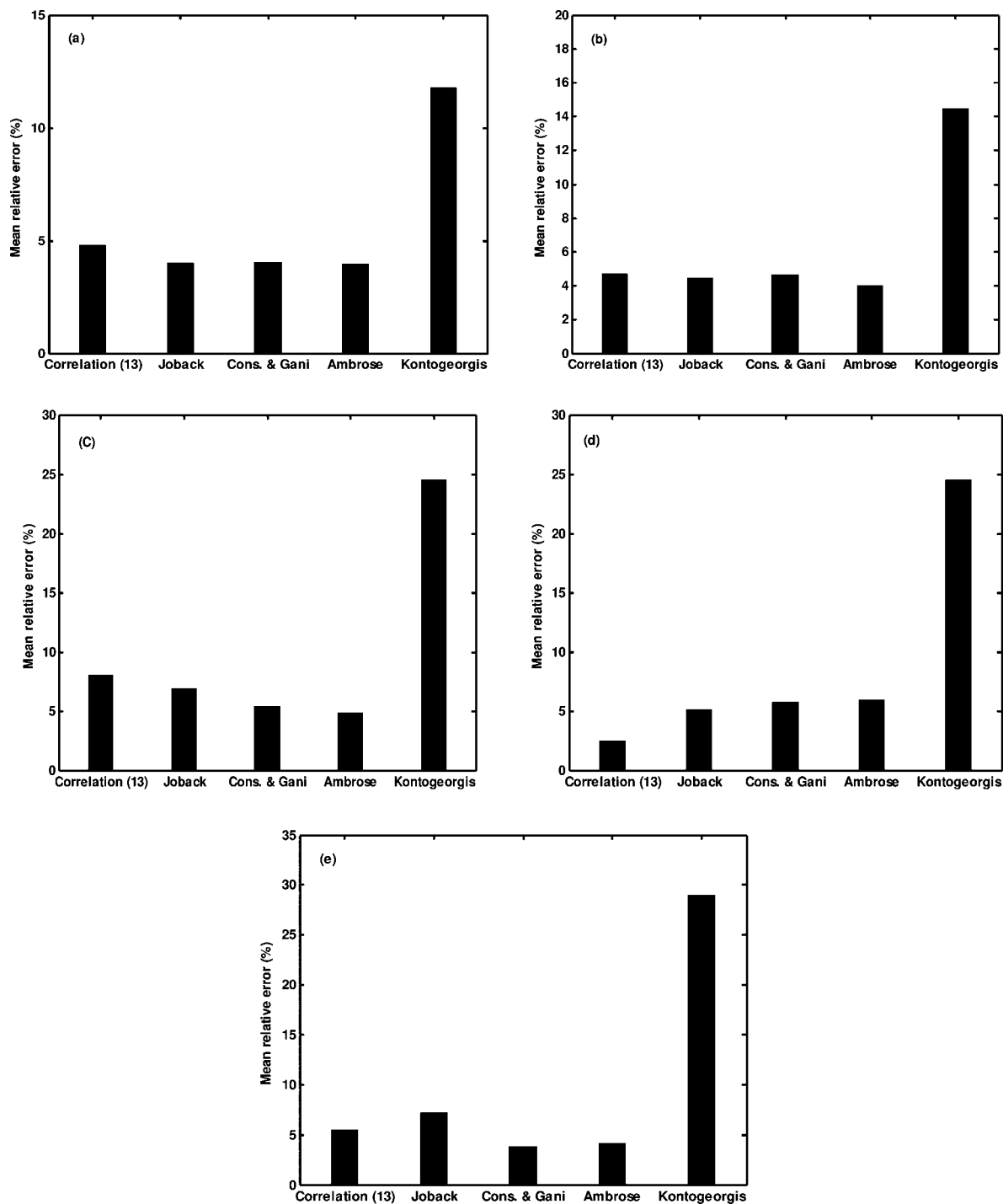


Figure 4. Mean relative errors of proposed correlation and various methods used in prediction of T_C/P_C for all types of compounds. (a) Hydrocarbons. (b) Oxygenated hydrocarbons. (c) Nitrogenated hydrocarbons. (d) Hydrocarbon sulfide and mercaptanes. (e) Halogenated hydrocarbons.

Figure 4 shows the mean relative errors corresponding to the proposed correlation and Joback,⁵ Constantinou and Gani,⁷ Ambrose,^{2,3} and Kontogeorgis⁸ methods for hydrocarbons, oxygenated hydrocarbons, nitrogenated hydrocarbons, hydrocarbon sulfide and mercaptanes, and halogenated hydrocarbons. This figure illustrates that the Kontogeorgis⁸ method is the least accurate method in prediction of the $T_C:P_C$ ratio for various types of compounds used with errors of 11.79 % for hydrocarbons, 13.30 % for oxygenated hydrocarbons, 24.51 % for nitrogenated hydrocarbons, 24.52 % for hydrocarbon sulfide and mercaptanes, and 29.04 % for halogenated hydrocarbons. According to Figure 4a, b, and c, almost all methods except the Kontogeorgis⁸ method result in similar errors when they are used for

hydrocarbons, oxygenated and nitrogenated hydrocarbons. Furthermore, it should be noted that the proposed correlation requires just one basic property (i.e., heat capacity), whereas in the Joback⁵ method, normal boiling point and number of atoms in the molecule, and in the Ambrose^{2,3} method, molecular weight and normal boiling point, in addition to group contributions are also required.

Figure 4d presents that the proposed correlation is the best accurate method in prediction of the $T_C:P_C$ ratio for hydrocarbon sulfide and mercaptanes with an error of 2.46 %, while the Ambrose^{2,3} method has an error of 5.91 %, Joback⁵ method 5.15 %, and Constantinou and Gani⁷ method 5.71 %. As can be seen in Figure 4e, it seems that the Constantinou and Gani⁷ and

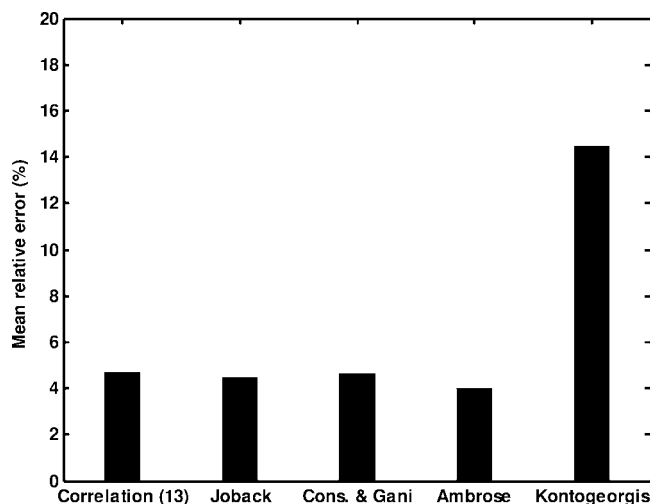


Figure 5. Overall performance of proposed correlation and various methods in the prediction of T_C/P_C for all types of compounds

Ambrose^{2,3} methods are the best for halogenated hydrocarbons with errors of 3.80 % and 4.19 %, respectively. The proposed correlation is the next most accurate approach with an error of 5.48 %.

Figure 5 shows the overall performance of proposed correlation and various methods in prediction of the $T_C:P_C$ ratio for all types of compounds. The correlation of Ambrose^{2,3} yields the best result, with a typical error less than 3.99 %. The overall performance of the Joback⁵ method is rather good with an error of around 4.45 %. The proposed correlation is equally good with respect to Constantinou and Gani,⁷ with an error of 4.69 %, but the proposed correlation is more general. The Kontogeorgis⁸ method is the least accurate method with an error less than 14.50 %. It seems that the accuracy of the proposed correlation is similar to the methods of Constantinou and Gani,⁷ Ambrose,^{2,3} and Joback,⁵ for various types of compounds.

However, the important point is that the proposed correlation is simple and general to predict critical temperature to critical pressure ratio for low to medium molecular weight compounds.

Conclusions

It was shown in this study that, unlike the critical properties alone, a simple correlation of the $T_C:P_C$ ratio with the heat capacity at 298.15 K can be developed for low to medium molecular weight compounds. The proposed correlation can be used to estimate one of the two critical properties whenever only the other one is available.

It is important to note that the proposed correlation just requires one basic property (i.e., heat capacity), whereas the other methods need two basic properties in addition to group contributions.

The proposed correlation is simple and general to predict critical temperature to critical pressure ratio for low to medium molecular weight compounds. This proposed correlation is applicable to predict the $T_C:P_C$ ratio for organic and inorganic compounds, while the other methods just predict this ratio for organic compounds.

Appendix

Nomenclature

C_p	Heat capacity
M	Molecular weight
M_j	Number of occurrences of the type- j second-order group in a compound

n_A	Number of atoms in the molecule
n_j	Number of groups of the j th type
N_i	Number of occurrences of the type- i first-order group in a compound
p_{c1i}	Contribution of the type- i first-order group for estimation of the critical pressure
p_{c2j}	Contribution of the type- j second-order group for estimation of the critical pressure
P_C	Critical pressure
Q_w	van der Waals surface area
R	Universal gas constant
t_{c1i}	Contribution of the type- i first-order group for estimation of the critical temperature
t_{c2j}	Contribution of the type- j second-order group for estimation of the critical temperature
T_B	Normal boiling point at 1 atm
T_C	Critical temperature
SG	Specific gravity of liquid hydrocarbons at 60 °F relative to water at the same temperature
Δ	Contributions for the j th atomic or molecules group
Δ_P	Group contribution for P_C
Δ_T	Group contribution for T_C

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