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Solubilities of Phenylphosphinic Acid, Methylphenylphosphinic Acid, Hexachlorocyclotriphosphazene, and Hexaphenoxycyclotriphosphazene in Selected Solvents

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Supporting Information

ABSTRACT: Phenylphosphinic acid (PPA), methylphenylphosphinic acid (MPPA), hexachlorocyclotriphosphazene (HCCP), and hexaphenoxycyclotriphosphazene (HPCCP) were prepared and characterized by elemental analysis, nuclear magnetic resonance, differential scanning calorimetry, and thermogravimetric analysis. Using a static analytical method, the solubilities of PPA, MPPA, HCCP, and HPCCP were measured in ten solvents and correlated with an empirical equation. The calculated results showed good agreement with the experimental data. Furthermore, using the Scatchard—Hildebrand model, activity coefficients have also been calculated and compared with the experimental values. The partial molar excess enthalpies at infinite dilution were also predicted.

INTRODUCTION

Elemental phosphorus and its various compounds have been used to flame retard a wide variety of polymer-based materials for several decades. Environmental considerations have paved the way in recent years for the increased use of phosphorusbased flame retardants as alternatives to the halogen-containing compounds.

Phenylphosphinic acid (hereafter abbreviated as PPA; its formula is shown in Figure 1) (CAS RN 1779-48-2) has been widely used in a variety of fields.¹⁻³ Organic titanate containing phenyl phosphinic acid catalyzed polyester exhibits low aldehyde formation during melt processing steps as well as excellent color, and the solid state polymerization rates of polyester are increased.⁴ Moreover, it is also used as a modifying agent for use in polyamides, an improver of polysiloxane resins, an antioxidant, and a free radical promoter in emulsion polymerization.⁵ Methylphenylphosphinic acid (hereafter abbreviated as MPPA; its formula is shown in Figure 1) (CAS RN 4271-13-0) has been usually used as polymer's additive. Compositions based on branched polyamides including MPPA exhibit good fire resistance, mechanical properties, and heat resistance.⁶ Polyimides and polyquinoxalines were modified by MPPA and molded to give self-lubricating antifriction materials with good hardness, flexibility, and reduced wear at elevated temperature.⁷ Besides, it is also used for coatings⁸ and as bifunctional catalysis for organic reactions of arylamine.9

Cyclic phosphazene is a kind of inorganic—organic compound with a backbone of alternating phosphorus and nitrogen atom single and double bonds. Hexachlorocyclotriphosphazene (hereafter abbreviated as HCCP; its formula is shown in Figure 1) (CAS RN 940-71-6) was the first phosphazene compound obtained and the main raw materials for the production of cyclic phosphazene and polyphosphazene. The chloride atoms on the phosphorus atoms of hexachlorocyclotriphosphazene are extremely reactive and can be substituted with many nucleophilic reagents for synthesis of various functional organic cyclic phosphazenes. The cyclic phosphazene compound is very suitable for flame-retardant materials because of



Figure 1. Structures of compounds related in this work: (a) phenylphosphinic acid (PPA), (b) methylphenylphosphinic acid (MPPA), (c) hexachlorocyclotriphosphazene (HCCP), (d) hexaphenoxycyclotriphosphazene (HPCCP).

its high oxygen index, low smoke emissions, low corrosiveness, and low toxicity of the combustion gases.¹⁰ In addition, it can improve physical and mechanical properties of epoxy resin^{11,12} and can also be used as drugs for the treatment of inflammatory diseases, e.g., autoimmune diseases.¹³

Hexaphenoxycyclotriphosphazene (hereafter abbreviated as HPCCP; its formula is shown in Figure 1) (CAS RN 1184-10-7), which belongs to the derivatives of HCCP, can be prepared from phenol in a reaction with HCCP and has been widely used as flame-retardant additives of various resin compositions for improving their properties such as thermoplastic resin composition,¹⁴ polyamide,¹⁵ and epoxy resin.¹⁶

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Table 1. Characterization Data of Melting Point and Elemental Analysis for PPA, MPPA, HCCP, and HPCCP and Comparison with the Literature Values

| | melting point/K | | |
|-------------------------------|--------------------|--|--|
| compd | exp. ^a | lit. | elemental analysis (%, cal) |
| PPA | 356.00 | 353.15 to 356.15; ²⁴ 357.15; ²⁵ 353.15 ²⁶ | C, 51.31 % (50.72 %); H, 5.01 % (4.97 %) |
| MPPA | 409.35 | 409.15 to 409.65 ²⁷ | C, 53.12 % (53.85 %); H, 5.25 % (5.81 %) |
| HCCP | 385.86 | 385.15 to 386.15; ²⁸ 384.15 to 386.15 ²⁹ | N, 11.98 % (12.09 %) |
| HPCCP | 387.11 | 384.15 to 385.15 ²² | C, 62.08 % (62.34 %); H, 4.36 % (4.36 %); N, 6.03 % (6.06 %) |
| ^a The uncertaity o | of the melting poi | nt measurement is 0.26 K. | |

Table 2. Characterization Data of ¹H NMR and ³¹P NMR for PPA, MPPA, HCCP, and HPCCP and Comparison with Literature Values

| | 1 H NMR (δ , ppm) | | | ³¹ P NMR (δ , ppm) | |
|---------------|--|---|----------------|--|--|
| compd | exp. | lit. | exp. | lit. | |
| PPA MPPA | 6.14 (d, 1H), 7.47 to 7.79 (m, 5H), 12.64 (d, 1H) 1.51 to 1.62 (m, 3H), 7.26 to 7.75 (m, 5H), 10.53 (d, 1H) | 6.16 (d, 1H), 7.44 to 7.80 (m, 5H), 11.28 (d, 1H) 23 | 22.09 44.45 | 21.52 ²³ | |
| НССР НРССР | 6.92 to 7.18 (m, 5H) | 6.85 to 7.18 (m, 5H) | 19.44 9.37 | 20.30, ²⁸ 20.44 ²⁹ 8.45 ²² | |



Figure 2. Schematic diagram of the experimental apparatus: 1, thermocouple; 2, sample gauge; 3, rubber plug; 4, jacket; 5, equilibrium cell; 6, magnetic stirrer; 7, water circulator bath.

The thermal processing of polymers is under high temperature, and the flame-retardant additives for polymer should have good thermal stability and high purity. PPA can be prepared according to a U.S. patent.¹⁷ MPPA was obtained by the hydrolysis of methyl methylphenylphosphinate and recrystallized from ethanol.¹⁸

To prepare HPCCP, a solution of sodium phenoxide in an anhydrous solvent is added to a solution of HCCP. A variety of organic solvents have been used for substitution reaction of this tape.¹⁹ Knowledge of solubilities of these compounds in different solvents is very important for their preparation and purification. However, to the best of our knowledge, few data are found in the literature.²⁰ The solubilities of PPA, MPPA, HCCP, and HPCCP in selected organic solvents have not been reported in the literature. In this study, the solubilities of the four organic phosphorus compounds in ten solvents were systematically measured.

EXPERIMENTAL SECTION

Materials. PPA was provided by Shandong Wan Zhao Co., Ltd. MPPA was provided by Yunnan Jin Shan Co., Ltd. HCCP was purchased from Zhangjiagang Xinyi Chemical Co., Ltd. and recrystallized from heptanes before use. All the solvents were analytical grade reagents, which were purchased from Beijing Chemical Factory. Their mass fraction purities were all higher

Table 3. Results of Differential Scanning Calorimeter (DSC)Measurement of PPA, MPPA, HCCP, and HPCCP

| substance | enthalpy of fusion/kJ·mol $^{-1}$ | relative uncertainty/% |
|-----------|-----------------------------------|------------------------|
| PPA | 12.80 | 0.42 |
| MPPA | 25.45 | 0.25 |
| HCCP | 19.61 | 0.67 |
| HPCCP | 51.07 | 0.52 |

than 0.99. They were used without further purification. The water is double distilled before use.

Apparatus and Procedure. The melting points and enthalpy of fusion were determined with a DSC Q600 differential scanning calorimeter (DSC) in flowing nitrogen at a heating rate of $10 \text{ K} \cdot \text{min}^{-1}$. The elemental analysis was performed on an Elementar Vario EL element analyzer. ¹H NMR and ³¹P NMR spectra were obtainned with a BrukerARX-400 and JEOL ECA-600, respectively. Thermogravimetric analysis (TGA) was carried out with an SDT Q600 thermogravimetric analyzer at a heating rate of $10 \text{ K} \cdot \text{min}^{-1}$ under nitrogen from (298.15 to 1073.15) K.

The setup for the solubility measurement was the same as that described in the literature.²¹ Figure 2 shows the schematic diagram of the experimental apparatus. A jacketed equilibrium cell was used for the solubility measurement with a working volume of 120 mL and a magnetic stirrer, and a circulating water bath was used with a thermostat (type 50 L, made from Shanghai Laboratory Instrument Works Co., Ltd.), which is capable of maintaining the temperature within \pm 0.05 K. An analytical balance (type TG328B, Shanghai Balance Instrument Works Co.) with an uncertainty of \pm 0.1 mg was used during the mass measurements.

Synthesis of HPCCP. HPCCP was prepared according to the literature.²² Hexachlorocyclotriphosphazene (8.6 g, 0.025 mol), phenol (14.0 g, 0.15 mol), anhydrous potassium phosphate (60.0 g, 0.28 mol), and 500 mL of acetonitrile were placed in a 1000 mL flask connected with a drying tube. The mixture was refluxed for 3 h and then cooled to room temperature. The solid was filtered and washed twice with 50 mL of acetonitrile. The filtrate and the washings were combined, and the solvent was distilled under reduced pressure. The

Table 4. Mole Fraction Solubilities (x) and Activity Coefficients (γ) of PPA in the Selected Solvents

Table 4. Continued

| solvent | T/K | x | γ | $(x - x^{\text{calcd}})/x$ |
|-----------------|------------------|--------|-------|----------------------------|
| methanol | 293.55 | 0.1726 | 2.311 | -0.0024 |
| | 298.15 | 0.2154 | 2.051 | -0.0246 |
| | 303.75 | 0.2795 | 1.652 | 0.0257 |
| | 308.35 | 0.3437 | 1.471 | 0.0104 |
| | 313.45 | 0.4292 | 1.276 | 0.0112 |
| | 318.25 | 0.5256 | 1.152 | -0.0160 |
| | 323.65 | 0.6554 | 0.991 | -0.0053 |
| ethanol | 283.25 | 0.0889 | 3 707 | 0.0085 |
| centurior | 288.65 | 0.1124 | 3 296 | -0.0082 |
| | 200.05 | 0.1357 | 2 968 | -0.0114 |
| | 298.35 | 0.1675 | 2.561 | 0.0114 |
| | 303.45 | 0.2046 | 2.301 | -0.0126 |
| | 308.25 | 0.2040 | 2.547 | 0.0120 |
| | 212.45 | 0.2434 | 1.870 | 0.0009 |
| | 219 55 | 0.2909 | 1.6/9 | -0.0008 |
| | 222.25 | 0.3337 | 1.091 | -0.0017 |
| -411 4 - 4 - | 525.55 202.45 | 0.0144 | 1.540 | -0.0017 |
| etnyi acetate | 293.45 | 0.0144 | 27.08 | -0.0075 |
| | 298.15 | 0.0185 | 23.39 | -0.054/ |
| | 303.25 | 0.02/5 | 17.16 | 0.0305 |
| | 313.45 | 0.0494 | 11.27 | 0.0228 |
| | 318.25 | 0.0661 | 9.062 | 0.04// |
| | 328.35 | 0.1073 | 6.477 | -0.0014 |
| | 333.25 | 0.1356 | 5.491 | -0.0151 |
| | 338.55 | 0.1739 | 4.602 | -0.0264 |
| dichloromethane | 288.15 | 0.0292 | 12.38 | 0.0148 |
| | 293.35 | 0.0386 | 10.29 | -0.0196 |
| | 296.25 | 0.0458 | 9.126 | -0.0183 |
| | 298.15 | 0.0528 | 8.182 | 0.0144 |
| | 303.45 | 0.0709 | 6.676 | 0.0093 |
| | 308.25 | 0.0910 | 5.625 | -0.0022 |
| acetone | 293.35 | 0.0305 | 13.02 | -0.0006 |
| | 298.15 | 0.0448 | 9.648 | 0.0182 |
| | 303.55 | 0.0671 | 7.060 | 0.0246 |
| | 308.25 | 0.0879 | 5.823 | -0.0408 |
| | 313.45 | 0.1243 | 4.475 | -0.0539 |
| | 318.25 | 0.1862 | 3.217 | 0.0304 |
| | 323.35 | 0.2559 | 2.526 | 0.0186 |
| chloroform | 293.15 | 0.1336 | 2.965 | 0.0116 |
| | 298.45 | 0.1573 | 2.763 | -0.0179 |
| | 303.25 | 0.1861 | 2.534 | -0.0189 |
| | 308.25 | 0.2284 | 2.242 | 0.0154 |
| | 313.15 | 0.2691 | 2.057 | 0.0175 |
| | 318.35 | 0.3150 | 1.904 | 0.0090 |
| | 323.25 | 0.3568 | 1.809 | -0.0185 |
| 2-ethoxyethanol | 288.15 | 0.1238 | 2.921 | 0.0267 |
| | 293.85 | 0.1359 | 2.951 | -0.0048 |
| | 298.25 | 0.1480 | 2.927 | -0.0129 |
| | 303.45 | 0.1647 | 2.873 | -0.0126 |
| | 313.15 | 0.2053 | 2.697 | 0.0174 |
| | 318.25 | 0.2265 | 2.645 | 0.0204 |
| | 323.65 | 0.2395 | 2.711 | -0.0211 |
| | 328.25 | 0.2593 | 2.676 | -0.0223 |
| | 333.45 | 0.2834 | 2.634 | -0.0218 |

| 338.35 0.3084 2.588 0.0181 343.25 0.3435 2.480 0.0112 348.25 0.3719 2.442 0.0128 353.25 0.3970 2.435 0.0028 358.55 0.4340 2.376 0.0137 363.15 0.0187 21.18 -0.0582 298.35 0.0282 15.38 0.0199 303.45 0.0389 12.16 0.0233 313.25 0.0652 8.510 -0.0426 318.15 0.0934 6.402 0.0446 323.35 0.1247 5.182 0.0446 328.15 0.1615 4.290 0.0479 333.55 0.1985 3.767 -0.0234 343.15 0.3158 2.694 -0.0320 343.15 0.3158 2.694 -0.0321 348.35 0.4130 2.202 -0.0084 343.15 0.3540 8.147 0.0198 313.25 0.1454 3.812 -0.037 | solvent | T/K | x | γ | $(x - x^{\text{calcd}})/x$ |
|--|---------|--------|--------|-------|----------------------------|
| 343.25 0.3435 2.480 0.0112 348.25 0.3719 2.442 0.0128 353.25 0.3970 2.435 0.0028 358.55 0.4340 2.376 0.0117 363.15 0.0590 2.372 0.0041 100000 293.15 0.0187 21.18 -0.0582 298.35 0.0282 15.38 0.0199 303.45 0.0389 12.16 0.0233 313.25 0.0652 8.510 -0.0426 318.15 0.0934 6.402 0.0406 323.35 0.1247 5.182 0.0446 328.15 0.1615 4.290 0.0479 333.55 0.1985 3.767 -0.0234 388.45 0.2545 3.141 -0.0193 343.15 0.3158 2.694 -0.0320 348.35 0.4130 2.202 -0.084 benzene 299.15 0.0540 8.147 0.0198 303.65 0.1108< | | 338.35 | 0.3084 | 2.588 | -0.0181 |
| 348.25 0.3719 2.442 0.0128 353.25 0.3970 2.435 0.0028 358.55 0.4340 2.376 0.0137 363.15 0.4590 2.372 0.0041 293.15 0.0187 21.18 -0.0582 298.35 0.0282 15.38 0.0199 303.45 0.0389 12.16 0.0233 313.25 0.0652 8.510 -0.0426 318.15 0.0934 6.402 0.0446 328.15 0.1615 4.290 0.0479 333.55 0.1985 3.767 -0.0234 338.45 0.2545 3.141 -0.0193 343.15 0.3158 2.694 -0.0320 348.35 0.4130 2.202 -0.084 benzene 299.15 0.0540 8.147 0.0198 303.65 0.1108 4.645 0.0293 313.25 0.1454 3.812 -0.0370 318.45 0.2254 2.665< | | 343.25 | 0.3435 | 2.480 | 0.0112 |
| 353.25 0.3970 2.435 0.0028 358.55 0.4340 2.376 0.0137 363.15 0.4590 2.372 0.0041 293.15 0.0187 21.18 -0.0582 298.35 0.0282 15.38 0.0199 303.45 0.0389 12.16 0.0233 313.25 0.0652 8.510 -0.0426 318.15 0.0934 6.402 0.0466 323.35 0.1247 5.182 0.0446 328.15 0.1615 4.290 0.0479 333.55 0.1985 3.767 -0.0234 338.45 0.2545 3.141 -0.0193 343.15 0.3158 2.694 -0.0320 348.35 0.4130 2.202 -0.0084 benzene 299.15 0.0540 8.147 0.0198 303.65 0.1108 4.645 0.0293 313.25 0.1454 3.812 -0.0370 318.45 0.2254 2.665 | | 348.25 | 0.3719 | 2.442 | 0.0128 |
| 358.55 0.4340 2.376 0.0137 363.15 0.4590 2.372 0.0041 293.15 0.0187 21.18 -0.0582 298.35 0.0282 15.38 0.0199 303.45 0.0389 12.16 0.0233 313.25 0.0652 8.510 -0.0426 318.15 0.0934 6.402 0.0406 323.35 0.1247 5.182 0.0446 328.15 0.1615 4.290 0.0479 333.55 0.1985 3.767 -0.0234 338.45 0.2545 3.141 -0.0193 343.15 0.3158 2.694 -0.0320 348.35 0.4130 2.202 -0.0084 benzene 299.15 0.0540 8.147 0.0198 303.65 0.1108 4.645 0.0293 313.25 0.1454 3.812 -0.0370 313.25 0.1454 3.812 -0.0312 323.15 0.5544 1.34 | | 353.25 | 0.3970 | 2.435 | 0.0028 |
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| 323.35 0.1247 5.182 0.0446 328.15 0.1615 4.290 0.0479 333.55 0.1985 3.767 -0.0234 338.45 0.2545 3.141 -0.0193 343.15 0.3158 2.694 -0.0320 348.35 0.4130 2.202 -0.0084 benzene 299.15 0.0540 8.147 0.0198 303.65 0.0709 6.695 -0.0337 308.55 0.1108 4.645 0.0293 313.25 0.1454 3.812 -0.0370 318.45 0.2254 2.665 0.0382 323.15 0.3085 2.089 0.0342 328.35 0.4152 1.674 -0.0094 333.15 0.5544 1.341 -0.0259 water 297.79 0.0095 45.42 0.0312 302.40 0.0129 35.93 -0.0161 305.22 0.0159 30.59 -0.0238 309.93 0.0 | | 318.15 | 0.0934 | 6.402 | 0.0406 |
| 328.15 0.1615 4.290 0.0479 333.55 0.1985 3.767 -0.0234 338.45 0.2545 3.141 -0.0193 343.15 0.3158 2.694 -0.0320 348.35 0.4130 2.202 -0.0084 benzene 299.15 0.0540 8.147 0.0198 303.65 0.0709 6.695 -0.0337 308.55 0.1108 4.645 0.0293 313.25 0.1454 3.812 -0.0370 318.45 0.2254 2.665 0.0382 323.15 0.3085 2.089 0.0342 328.35 0.4152 1.674 -0.0094 333.15 0.5544 1.341 -0.0259 water 297.79 0.0095 45.42 0.0312 300.25 0.0111 40.42 -0.0033 302.40 0.0129 35.93 -0.0161 305.22 0.0159 30.59 -0.0238 309.93 0. | | 323.35 | 0.1247 | 5.182 | 0.0446 |
| 333.55 0.1985 3.767 -0.0234 338.45 0.2545 3.141 -0.0193 343.15 0.3158 2.694 -0.0320 348.35 0.4130 2.202 -0.0084 benzene 299.15 0.0540 8.147 0.0198 303.65 0.0709 6.695 -0.0370 308.55 0.1108 4.645 0.0293 313.25 0.1454 3.812 -0.0370 318.45 0.2254 2.665 0.0382 323.15 0.3085 2.089 0.0342 328.35 0.4152 1.674 -0.0094 333.15 0.5544 1.341 -0.0259 water 297.79 0.0095 45.42 0.0312 300.25 0.0111 40.42 -0.0033 302.40 0.0129 35.93 -0.0161 305.22 0.0159 30.59 -0.0238 309.93 0.0218 24.17 -0.0643 312.84 0 | | 328.15 | 0.1615 | 4.290 | 0.0479 |
| $\benzene \benzene \$ | | 333.55 | 0.1985 | 3.767 | -0.0234 |
| 343.15 0.3158 2.694 -0.0320 348.35 0.4130 2.202 -0.0084 299.15 0.0540 8.147 0.0198 303.65 0.0709 6.695 -0.0537 308.55 0.1108 4.645 0.0293 313.25 0.1454 3.812 -0.0370 318.45 0.2254 2.665 0.0382 323.15 0.3085 2.089 0.0342 328.35 0.4152 1.674 -0.0094 333.15 0.5544 1.341 -0.0259 water 297.79 0.0095 45.42 0.0312 300.25 0.0111 40.42 -0.0033 302.40 0.0129 35.93 -0.0161 305.22 0.0159 30.59 -0.0238 309.93 0.0218 24.17 -0.0643 312.84 0.0305 18.08 0.0604 318.15 0.0433 13.81 0.0368 323.35 0.0572 11.2 | | 338.45 | 0.2545 | 3.141 | -0.0193 |
| 348.35 0.4130 2.202 -0.0084 299.15 0.0540 8.147 0.0198 303.65 0.0709 6.695 -0.0537 308.55 0.1108 4.645 0.0293 313.25 0.1454 3.812 -0.0370 318.45 0.2254 2.665 0.0382 323.15 0.3085 2.089 0.0342 328.35 0.4152 1.674 -0.0094 333.15 0.5544 1.341 -0.0259 water 297.79 0.0095 45.42 0.0312 300.25 0.0111 40.42 -0.0033 302.40 0.0129 35.93 -0.0161 305.22 0.0159 30.59 -0.0238 309.93 0.0218 24.17 -0.0643 312.84 0.0305 18.08 0.0604 318.15 0.0433 13.81 0.0368 323.35 0.0572 11.29 -0.0406 328.15 0.0850 8.15 | | 343.15 | 0.3158 | 2.694 | -0.0320 |
| benzene 299.15 0.0540 8.147 0.0198 303.65 0.0709 6.695 -0.0537 308.55 0.1108 4.645 0.0293 313.25 0.1454 3.812 -0.0370 318.45 0.2254 2.665 0.0382 323.15 0.3085 2.089 0.0342 328.35 0.4152 1.674 -0.0094 333.15 0.5544 1.341 -0.0259 water 297.79 0.0095 45.42 0.0312 300.25 0.0111 40.42 -0.0033 302.40 0.0129 35.93 -0.0161 305.22 0.0159 30.59 -0.0238 309.93 0.0218 24.17 -0.0643 312.84 0.0305 18.08 0.0604 318.15 0.0433 13.81 0.0368 323.35 0.0572 11.29 -0.0406 333.45 0.1102 6.774 -0.0461 338.25 0.1 | | 348.35 | 0.4130 | 2.202 | -0.0084 |
| $\begin{array}{cccccccccccccccccccccccccccccccccccc$ | benzene | 299.15 | 0.0540 | 8.147 | 0.0198 |
| $\begin{array}{cccccccccccccccccccccccccccccccccccc$ | | 303.65 | 0.0709 | 6.695 | -0.0537 |
| $\begin{array}{cccccccccccccccccccccccccccccccccccc$ | | 308.55 | 0.1108 | 4.645 | 0.0293 |
| $\begin{array}{cccccccccccccccccccccccccccccccccccc$ | | 313.25 | 0.1454 | 3.812 | -0.0370 |
| $\begin{array}{cccccccccccccccccccccccccccccccccccc$ | | 318.45 | 0.2254 | 2.665 | 0.0382 |
| $\begin{array}{cccccccccccccccccccccccccccccccccccc$ | | 323.15 | 0.3085 | 2.089 | 0.0342 |
| 333.15 0.5544 1.341 -0.0259 water 297.79 0.0095 45.42 0.0312 300.25 0.0111 40.42 -0.0033 302.40 0.0129 35.93 -0.0161 305.22 0.0159 30.59 -0.0238 309.93 0.0218 24.17 -0.0643 312.84 0.0305 18.08 0.0604 318.15 0.0433 13.81 0.0368 323.35 0.0572 11.29 -0.0406 333.45 0.1102 6.774 -0.0461 338.25 0.1606 4.965 0.0305 343.15 0.2076 4.097 -0.0096 | | 328.35 | 0.4152 | 1.674 | -0.0094 |
| water 297.79 0.0095 45.42 0.0312 300.25 0.0111 40.42 -0.0033 302.40 0.0129 35.93 -0.0161 305.22 0.0159 30.59 -0.0238 309.93 0.0218 24.17 -0.0643 312.84 0.0305 18.08 0.0604 318.15 0.0433 13.81 0.0368 323.35 0.0572 11.29 -0.0406 333.45 0.1102 6.774 -0.0461 338.25 0.1606 4.965 0.0305 343.15 0.2076 4.097 -0.0096 | | 333.15 | 0.5544 | 1.341 | -0.0259 |
| $\begin{array}{cccccccccccccccccccccccccccccccccccc$ | water | 297.79 | 0.0095 | 45.42 | 0.0312 |
| $\begin{array}{cccccccccccccccccccccccccccccccccccc$ | | 300.25 | 0.0111 | 40.42 | -0.0033 |
| $\begin{array}{cccccccccccccccccccccccccccccccccccc$ | | 302.40 | 0.0129 | 35.93 | -0.0161 |
| $\begin{array}{cccccccc} 309.93 & 0.0218 & 24.17 & -0.0643 \\ 312.84 & 0.0305 & 18.08 & 0.0604 \\ 318.15 & 0.0433 & 13.81 & 0.0368 \\ 323.35 & 0.0572 & 11.29 & -0.0406 \\ 328.15 & 0.0850 & 8.152 & 0.0361 \\ 333.45 & 0.1102 & 6.774 & -0.0461 \\ 338.25 & 0.1606 & 4.965 & 0.0305 \\ 343.15 & 0.2076 & 4.097 & -0.0096 \\ \end{array}$ | | 305.22 | 0.0159 | 30.59 | -0.0238 |
| $\begin{array}{cccccccccccccccccccccccccccccccccccc$ | | 309.93 | 0.0218 | 24.17 | -0.0643 |
| 318.150.043313.810.0368323.350.057211.29-0.0406328.150.08508.1520.0361333.450.11026.774-0.0461338.250.16064.9650.0305343.150.20764.097-0.0096 | | 312.84 | 0.0305 | 18.08 | 0.0604 |
| $\begin{array}{rrrrrrrrrrrrrrrrrrrrrrrrrrrrrrrrrrrr$ | | 318.15 | 0.0433 | 13.81 | 0.0368 |
| 328.150.08508.1520.0361333.450.11026.774-0.0461338.250.16064.9650.0305343.150.20764.097-0.0096 | | 323.35 | 0.0572 | 11.29 | -0.0406 |
| 333.450.11026.774-0.0461338.250.16064.9650.0305343.150.20764.097-0.0096 | | 328.15 | 0.0850 | 8.152 | 0.0361 |
| 338.250.16064.9650.0305343.150.20764.097-0.0096 | | 333.45 | 0.1102 | 6.774 | -0.0461 |
| 343.15 0.2076 4.097 -0.0096 | | 338.25 | 0.1606 | 4.965 | 0.0305 |
| | | 343.15 | 0.2076 | 4.097 | -0.0096 |

residue was dissolved in ethyl acetate and washed with 10 % NaOH solution three times and then with water and dried over anhydrous sodium sulfate. After filtration and evaporation, the product was purified by recrystallization from ethyl acetate and dried to get HPCCP (14.23 g). The yield was 82 %.

Characterization of Compounds. Characterization data of NMR, EA, and melting point for PPA, MPPA, HCCP, and HPCCP with the corresponding literature values²³⁻²⁹ are listed in Tables 1 and 2. The results obtained are in good agreement with those listed in the literature. On the basis of the above analysis, the mass fraction purity of PPA, MPPA, HCCP, and HPCCP used in this work was higher than 95 %.

Solubility Measurement. The solubilities were measured by a gravimetric method.³⁰ For each measurement, an excess mass of PPA, MPPA, HCCP, and HPCCP was added to a known mass of solvent. Then the equilibrium cell was heated to a constant temperature with continuous stirring. After at least 2 h (the temperature of

Table 5. Mole Fraction Solubilities (x) and Activity Coefficients (γ) of MPPA in the Selected Solvents

| solvent | T/K | x | γ | $(x - x^{\text{calcd}})/x$ |
|-----------------|--------|--------|-------|----------------------------|
| ethanol | 293.25 | 0.2055 | 0.317 | -0.0134 |
| | 298.15 | 0.2658 | 0.287 | 0.0222 |
| | 303.35 | 0.3325 | 0.270 | 0.0191 |
| | 308.25 | 0.3901 | 0.266 | -0.0282 |
| | 313.55 | 0.4861 | 0.250 | -0.0248 |
| | 318.45 | 0.6142 | 0.227 | 0.0154 |
| | 323.15 | 0.7336 | 0.216 | 0.0127 |
| | 328.25 | 0.8716 | 0.208 | -0.0047 |
| ethyl acetate | 288.35 | 0.0484 | 1.142 | -0.0114 |
| , | 293.15 | 0.0621 | 1.044 | 0.0145 |
| | 298.25 | 0.0750 | 1.020 | -0.0270 |
| | 303.45 | 0.0941 | 0.955 | -0.0263 |
| | 313.35 | 0.1516 | 0.796 | 0.0398 |
| | 318.15 | 0.1818 | 0.760 | 0.0318 |
| | 328.15 | 0.2654 | 0.683 | 0.0324 |
| | 333.35 | 0.3042 | 0.681 | -0.0182 |
| | 338.15 | 0.3593 | 0.651 | -0.0198 |
| | 343.25 | 0.4277 | 0.619 | -0.0188 |
| dichloromethane | 288 55 | 0.0465 | 1 196 | 0.0111 |
| diemoromethane | 200.55 | 0.0697 | 0.946 | -0.0289 |
| | 296.15 | 0.0904 | 0.791 | 0.0192 |
| | 290.15 | 0.1045 | 0.734 | -0.0200 |
| | 303.25 | 0.1640 | 0.545 | 0.0306 |
| | 308.35 | 0.2347 | 0.444 | -0.0135 |
| methanol | 208.35 | 0.2577 | 0.242 | -0.0010 |
| methanoi | 202.15 | 0.3172 | 0.242 | -0.0024 |
| | 209.15 | 0.3719 | 0.200 | -0.0027 |
| | 212.25 | 0.3718 | 0.2/9 | 0.0032 |
| | 210.25 | 0.4202 | 0.290 | 0.0049 |
| | 222.15 | 0.4592 | 0.317 | 0.00053 |
| | 228.15 | 0.4708 | 0.357 | -0.0000 |
| ahlanafama | 202.15 | 0.1117 | 0.504 | -0.0099 |
| chloroform | 293.15 | 0.1217 | 0.581 | 0.0054 |
| | 296.25 | 0.1559 | 0.581 | -0.0078 |
| | 208.25 | 0.1992 | 0.572 | -0.0030 |
| | 212.15 | 0.1665 | 0.554 | 0.0147 |
| | 210.45 | 0.2142 | 0.500 | -0.0082 |
| | 318.45 | 0.2552 | 0.540 | 0.0050 |
| | 229.15 | 0.2002 | 0.530 | -0.0129 |
| taluana | 202.25 | 0.3396 | 0.555 | -0.0048 |
| toluelle | 295.25 | 0.1470 | 0.542 | -0.0048 |
| | 298.35 | 0.1470 | 0.522 | 0.0178 |
| | 303.25 | 0.10/5 | 0.534 | -0.0180 |
| | 308.35 | 0.2043 | 0.510 | 0.0128 |
| | 313.15 | 0.2292 | 0.524 | -0.0255 |
| | 323.25 | 0.32/1 | 0.486 | 0.0231 |
| | 328.35 | 0.3/68 | 0.484 | 0.0168 |
| | 333.25 | 0.4182 | 0.494 | -0.0167 |
| | 338.15 | 0.4792 | 0.488 | -0.0145 |
| | 343.45 | 0.5643 | 0.471 | 0.0086 |
| 2-ethoxyethanol | 298.15 | 0.2522 | 0.302 | -0.0035 |
| | 303.15 | 0.2889 | 0.308 | 0.0170 |
| | 313.25 | 0.3479 | 0.346 | -0.0185 |
| | 318.15 | 0.3972 | 0.348 | 0.0117 |

| solvent | T/K | x | γ | $(x - x^{\text{calcd}})/$ |
|---------|--------|--------|-------|---------------------------|
| | 323.35 | 0.4406 | 0 362 | 0.0102 |
| | 323.33 | 0.4716 | 0.302 | -0.0102 |
| | 333.15 | 0.5193 | 0.303 | -0.0152 |
| | 338.45 | 0.5175 | 0.402 | 0.0190 |
| | 343 35 | 0.6392 | 0.415 | 0.0071 |
| | 348.35 | 0.6965 | 0.429 | 0.0058 |
| | 353.15 | 0.7509 | 0.444 | -0.0002 |
| benzene | 293.25 | 0.0386 | 1.686 | 0.0093 |
| | 298.15 | 0.0541 | 1.409 | -0.0209 |
| | 303.15 | 0.0809 | 1.102 | 0.0186 |
| | 308.35 | 0.1126 | 0.926 | -0.0153 |
| | 313.25 | 0.1625 | 0.741 | 0.0181 |
| | 318.15 | 0.2183 | 0.633 | -0.0093 |
| | 323.25 | 0.3012 | 0.528 | -0.0130 |
| | 328.15 | 0.4194 | 0.432 | 0.0150 |
| | 333.35 | 0.5628 | 0.368 | -0.0029 |
| acetone | 293.15 | 0.0473 | 1.370 | -0.0096 |
| | 298.15 | 0.0609 | 1.251 | -0.0161 |
| | 303.25 | 0.0816 | 1.095 | 0.02053 |
| | 308.15 | 0.0995 | 1.042 | -0.0190 |
| | 313.35 | 0.1268 | 0.952 | -0.0206 |
| | 318.15 | 0.1649 | 0.838 | 0.0239 |
| | 323.25 | 0.2041 | 0.779 | 0.0124 |
| water | 298.15 | 0.0154 | 4.948 | -0.0093 |
| | 303.35 | 0.0204 | 4.401 | 0.0286 |
| | 310.45 | 0.0270 | 4.109 | -0.0055 |
| | 314.25 | 0.0320 | 3.876 | -0.0005 |
| | 320.45 | 0.0414 | 3.563 | -0.0005 |
| | 324.15 | 0.0477 | 3.416 | -0.0073 |
| | 329.25 | 0.0579 | 3.221 | -0.0137 |
| | 333.65 | 0.0679 | 3.076 | -0.0229 |
| | 338.75 | 0.0865 | 2.744 | 0.0295 |
| | 343.45 | 0.0968 | 2.747 | -0.0267 |
| | 348.25 | 0.1197 | 2.489 | 0.0172 |

the water bath approached a constant value, then the actual value of the temperature was recorded), the stirring was stopped, and the solution was kept still until it was clear. A preheated on—off injector with a cotton filter withdrew 2 mL of the clear upper portion of the solution to another previously weighed measuring vial (m_0) . The vial was quickly and tightly closed and weighed (m_1) to determine the mass of the sample $(m_1 - m_0)$. Then the vial was uncovered with a piece of filter paper to prevent dust contamination. After the solvent in the vial had completely evaporated, the vial was dried and reweighed (m_2) to determine the mass of the constant residue solid $(m_2 - m_0)$. Thus, the solid concentration of the sample solution in mole fraction, x, could be determined from eq 1³¹

$$x = \frac{(m_2 - m_0)/M_1}{(m_2 - m_0)/M_1 + (m_1 - m_2)/M_2}$$
(1)

Different dissolution times were tested to determine a suitable equilibrium time. It was found that 2 h was enough for PPA, MPPA, HCCP, and HPCCP in solvent to reach equilibrium. During our experiments, three parallel measurements were performed at the same composition of solvent for each temperature, and an average

Table 6. Mole Fraction Solubilities (x) and Activity Coefficients (γ) of HCCP in the Selected Solvents

$(x - x^{\text{calcd}})/x$ solvent T/Kγ х ethanol 298.45 0.0106 16.24 0.0312 -0.0503303.25 0.0164 10.96 308.45 0.0295 7.262 -0.0074313.35 0.0487 4.988 $-4 \cdot 10^{-6}$ 319.85 0.0938 3.085 0.0217 0.0420 324.35 0.1464 2.237 328.15 0.1943 1.717-0.02300.3163 1.192 -0.0174333.55 $5.8 \cdot 10^{-5}$ ethyl acetate 298.55 0.0701 2.387 0.0829 -0.0017 303.35 2.283 0.0027 308.35 0.0988 2.183 313.45 0.1160 2.089 -0.00570.0044 319.95 0.1442 1.978 324.15 0.1635 1.912 0.0006 328.05 0.1848 1.854 0.0063 333.65 0.2149 1.776 -0.0066diethyl ether 0.0023 293.25 0.0944 1.541 296.15 0.1035 1.513 -0.0028299.05 0.1140 1.486 -0.0016301.15 0.1225 1.467 0.0027 303.25 0.1303 1.449 -0.00210.1388 0.0014 305.15 1.432 THF 0.1772 0.820 0.0015 293.25 299.15 0.1991 0.853 -0.0012303.15 0.2150 0.875 -0.0025308.35 0.2381 0.905 0.0010 0.0034 312.85 0.2592 0.930 318.95 0.2867 0.964 -0.0040323.15 0.987 0.0021 0.3100 328.35 0.3374 1.016 -0.00020.0296 -0.0040293.15 4.875 acetone 300.45 0.0426 4.177 0.0110 303.25 0.0478 3.945 -0.0042308.25 0.0600 3.570 -0.0023313.25 0.0743 3.242 -0.0065318.35 0.0937 2.947 0.0090 322.95 0.11170 2.712 -0.0038dichloromethane 0.1142 -0.0018293.15 1.265 0.0019 298.05 0.1331 1.243 300.55 0.1435 1.232 0.0026 303.35 0.1554 1.221 0.0001 305.65 -0.0045 0.1653 1.211 0.0018 308.35 0.1795 1.200 acetonitrile 293.15 0.0018 83.49 0.0067 299.85 0.0025 68.65 0.0035 303.25 0.0030 62.36 -0.0009308.45 0.0040 54.07 0.0062 -0.0209313.05 0.0049 47.84 0.0066 41.53 -0.0022318.55 323.25 0.0082 36.93 -0.01130.0009 328.25 0.0105 32.72 0.0211 332.35 0.0128 29.72 0.0162 -0.0028338.25 25.97

| solvent | T/K | x | γ | $(x - x^{\text{calcd}})/x$ |
|-----------------|--------|--------|-------|----------------------------|
| 2-ethoxyethanol | 299.95 | 0.0322 | 5.572 | 0.0321 |
| | 303.35 | 0.0365 | 4.984 | -0.0426 |
| | 308.35 | 0.0532 | 4.250 | 0.0474 |
| | 313.15 | 0.0635 | 3.664 | -0.0393 |
| | 318.65 | 0.0862 | 3.108 | -0.0287 |
| | 323.35 | 0.1158 | 2.712 | 0.0229 |
| | 328.05 | 0.1473 | 2.376 | 0.0272 |
| | 332.45 | 0.1715 | 2.107 | -0.0369 |
| | 338.25 | 0.2303 | 1.806 | -0.0167 |
| | 343.15 | 0.2988 | 1.593 | 0.0178 |
| | 348.35 | 0.3734 | 1.399 | 0.0086 |
| | 353.15 | 0.4568 | 1.245 | 0.0017 |
| oluene | 298.15 | 0.0585 | 2.822 | -0.0037 |
| | 301.55 | 0.0645 | 2.798 | -0.0032 |
| | 303.25 | 0.0677 | 2.787 | -0.0030 |
| | 308.45 | 0.0782 | 2.752 | -0.0024 |
| | 312.85 | 0.0880 | 2.724 | -0.0018 |
| | 318.25 | 0.1013 | 2.692 | -0.0012 |
| | 322.85 | 0.1138 | 2.665 | -0.0006 |
| | 328.25 | 0.1298 | 2.634 | $-4.8 \cdot 10^{-5}$ |
| n-heptane | 293.15 | 0.0046 | 31.27 | -0.0053 |
| | 298.25 | 0.0069 | 24.73 | 0.0226 |
| | 303.35 | 0.0094 | 19.71 | -0.0276 |
| | 308.45 | 0.0139 | 15.83 | 0.0168 |
| | 313.45 | 0.0182 | 12.86 | -0.0385 |
| | 318.35 | 0.0266 | 10.55 | 0.0267 |
| | 323.05 | 0.0356 | 8.779 | 0.0242 |
| | 328.15 | 0.0462 | 7.234 | -0.0214 |

Table 6. Continued

value is given. The maximum standard deviation of each triplicate data is 0.24 %, and the minimum is 0.16 %. The estimated relative uncertainty of the solubility values based on error analysis and repeated observations was within 0.02.

RESULTS AND DISCUSSION

The results of DSC measurements are summarized in Table 3. An analysis report for the uncertaity of DSC measurement is provided in the Supporting Information. The TGA results show that there is a single-step decomposition, and no or very little residues remain for MPPA, HCCP, and HPCCP.

The mole fraction solubilities x of PPA, MPPA, HCCP, and HPCCP in selected solvents measured in this work are summarized in Tables 4 to 7 and plotted as $\ln x$ vs 1/T in Figures 3 to 7. From these figures, it can be seen that a trend of increasing solubility with temperature is observed.

The solubilities were correlated as a function of temperature by

$$\ln x = A + B/(T/K) \tag{2}$$

The parameters A and B for each solvent are provided in the Supporting Information. The relative standard deviations (RSD) are also presented in the Supporting Information. The smoothed data calculated from eq 2 are compared with the experimental data, and the results are listed in Tables 4 to 7. The results show that eq 2 can be used to correlate the solubility data. Within the temperature range of the measurements, the solubilities of PPA, MPPA, HCCP,

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Table 7. Mole Fraction Solubilities (x) and Activity Coefficients (γ) of HPCCP in the Selected Solvents

Table 7. Continued

| solvent | T/K | x | γ | $(x - x^{\text{calcd}})/x$ |
|-----------------|--------|--------|-------|----------------------------|
| ethanol | 298.25 | 0.0096 | 0.926 | 0.0075 |
| | 300.95 | 0.0099 | 1.076 | -0.0006 |
| | 303.25 | 0.0102 | 1.215 | -0.0030 |
| | 308.15 | 0.0110 | 1.564 | -0.0072 |
| | 313.45 | 0.0119 | 2.012 | $-7 \cdot 10^{-5}$ |
| | 318.75 | 0.0129 | 2.578 | 0.0029 |
| | 323.05 | 0.0136 | 3.150 | -0.0002 |
| | 328.35 | 0.0147 | 3.981 | 0.0018 |
| ethyl acetate | 298.15 | 0.0592 | 0.148 | 0.0079 |
| | 300.95 | 0.0655 | 0.162 | 0.0085 |
| | 303.25 | 0.0699 | 0.178 | -0.0082 |
| | 308.25 | 0.0829 | 0.208 | -0.0098 |
| | 313.25 | 0.0983 | 0.241 | -0.0067 |
| | 310.05 | 0.1104 | 0.241 | 0.0005 |
| | 222.15 | 0.1264 | 0.207 | 0.0005 |
| | 220.15 | 0.1509 | 0.317 | 0.0030 |
| diathral ath on | 202.15 | 0.1300 | 0.500 | 0.0030 |
| diethyl ether | 295.15 | 0.0101 | 0.612 | 0.0010 |
| | 290.25 | 0.0122 | 0.033 | 0.0046 |
| | 299.05 | 0.0140 | 0.662 | -0.0125 |
| | 300.35 | 0.0154 | 0.005 | 0.0078 |
| | 303.15 | 0.0178 | 0.694 | -0.0076 |
| | 306.05 | 0.0211 | 0.708 | 0.0057 |
| THF | 293.25 | 0.1510 | 0.041 | -0.0052 |
| | 298.15 | 0.1746 | 0.050 | 0.0115 |
| | 304.35 | 0.2001 | 0.067 | -0.0086 |
| | 308.25 | 0.2225 | 0.078 | 0.0022 |
| | 314.25 | 0.2526 | 0.100 | -0.0125 |
| | 318.45 | 0.2852 | 0.114 | 0.0125 |
| | 323.15 | 0.3151 | 0.137 | 0.0079 |
| | 328.25 | 0.3461 | 0.168 | -0.0084 |
| acetone | 293.15 | 0.0295 | 0.209 | 0.0032 |
| | 296.45 | 0.0349 | 0.224 | 0.0076 |
| | 300.25 | 0.0423 | 0.240 | 0.0168 |
| | 304.35 | 0.0496 | 0.269 | -0.0160 |
| | 308.25 | 0.0588 | 0.293 | -0.0239 |
| | 314.25 | 0.0782 | 0.323 | -0.0040 |
| | 318.35 | 0.0930 | 0.349 | -0.0057 |
| | 323.15 | 0.1166 | 0.371 | 0.0209 |
| dichloromethane | 293.35 | 0.0990 | 0.063 | 0.0064 |
| | 295.95 | 0.1108 | 0.068 | -0.0096 |
| | 300.35 | 0.1385 | 0.074 | 0.0023 |
| | 303.15 | 0.1583 | 0.078 | 0.0044 |
| | 306.05 | 0.1790 | 0.083 | -0.0066 |
| | 310.35 | 0.2194 | 0.090 | 0.0030 |
| acetonitrile | 298.25 | 0.0040 | 2.227 | 0.0042 |
| | 303.55 | 0.0060 | 2.100 | 0.0164 |
| | 308.25 | 0.0082 | 2.100 | -0.0241 |
| | 313.35 | 0.0122 | 1.960 | 0.0029 |
| | 318.35 | 0.0170 | 1.913 | -0.0129 |
| | 323.45 | 0.0243 | 1.809 | 0.0038 |
| | 328.15 | 0.0332 | 1.741 | 0.0069 |
| | 333.25 | 0.0457 | 1.685 | 0.0021 |
| 2-ethoxyethanol | 298.15 | 0.0065 | 1.350 | -0.0023 |
| , | | | | |

| solvent | T/K | x | γ | $(x - x^{\text{calcd}})/$ |
|-------------------|--------|--------|-------|---------------------------|
| | 300.95 | 0.0074 | 1.433 | 0.0100 |
| | 303.25 | 0.0081 | 1.531 | 0.0019 |
| | 310.15 | 0.0106 | 1.842 | -0.0142 |
| | 314.55 | 0.0126 | 2.036 | -0.0104 |
| | 318.75 | 0.0148 | 2.240 | -0.0093 |
| | 323.65 | 0.0182 | 2.454 | 0.0086 |
| | 328.05 | 0.0212 | 2.713 | 0.0036 |
| | 333.15 | 0.0259 | 2.951 | 0.0267 |
| | 343.25 | 0.0352 | 3.743 | -0.0075 |
| | 348.35 | 0.0420 | 4.077 | 0.0052 |
| | 353.15 | 0.0478 | 4.545 | -0.0136 |
| toluene | 298.05 | 0.0572 | 0.153 | 0.0028 |
| | 300.95 | 0.0650 | 0.164 | 0.0132 |
| | 303.35 | 0.0717 | 0.174 | 0.0151 |
| | 310.25 | 0.0904 | 0.217 | -0.0196 |
| | 314.45 | 0.1063 | 0.240 | -0.0145 |
| | 318.65 | 0.1233 | 0.268 | -0.0187 |
| | 323.55 | 0.1499 | 0.295 | 0.0033 |
| | 327.95 | 0.1734 | 0.330 | -0.0023 |
| | 333.15 | 0.2089 | 0.366 | 0.0108 |
| | 338.25 | 0.2461 | 0.411 | 0.0097 |
| <i>n</i> -heptane | 298.15 | 0.0035 | 2.516 | 0.0049 |
| | 303.45 | 0.0039 | 3.206 | -0.0069 |
| | 308.35 | 0.0044 | 3.929 | -0.0040 |
| | 313.05 | 0.0049 | 4.742 | -0.0003 |
| | 318.25 | 0.0056 | 5.779 | 0.0074 |
| | 323.35 | 0.0062 | 7.076 | $5.9 \cdot 10^{-5}$ |
| | 328.25 | 0.0069 | 8.453 | 0.0041 |
| | 333.15 | 0.0075 | 10.18 | -0.0058 |



Figure 3. Mole fraction solubilities of phenylphosphinic acid in selected solvents. Experimental data: \oplus , methanol; \bigcirc , ethanol; \blacksquare , chloroform; \Box , benzene; \blacktriangledown , acetone; \bigtriangledown , toluene; \blacktriangle , ethyl acetate; \triangle , water; -, solubility curve calculated from eq 2.

and HPCCP in all of the investigated solvents increased with increasing temperature.

PPA is a most soluble substance in all selected solvents, especially at a relatively higher temperature. In polar solvents,



Figure 4. Mole fraction solubilities of methylphenylphosphinic acid in selected solvents. Experimental data: \blacksquare , ethanol; \Box , methanol; \blacklozenge , toluene; \bigcirc , chloroform; \blacktriangle , ethyl acetate; Δ , acetone; \blacktriangledown , water; -, solubility curve calculated from eq 2.



Figure 5. Mole fraction solubilities of phenylphosphinic acid (PPA) and methylphenylphosphinic acid (MPPA) in selected solvents. Experimental data: ●, PPA in 2-ethoxyethanol; ◆, PPA in dichloromethane; ■, MPPA in 2-ethoxyethanol; ▼, MPPA in dichloromethane; ▲, MPPA in benzene; −, solubility curve calculated from eq 2.

PPA shows good solubility because of intermolecular hydrogen bonds between the hydrogen atom in PPA and the hydroxyl group in the solvent molecule such as water,²⁰ ethanol, methanol, and 2-ethoxyethanol. In addition, it was found that PPA has higher solubility in toluene and benzene which was related to the theory of similarity and compatibility.^{32–34} Thus, the investigated solvents could be recommended as the better solvent for the purification of PPA, especially polar solvents. Compared with PPA, due to the similar structure, MPPA shows similar soluble behavior. However, the molecular volume of MPPA is bigger than PPA because of the introduction of a methyl group, so the solubilities of MPPA are smaller than PPA.

The order of mole fraction solubility of HCCP in the select solvent at constant temperature is THF > dichloromethane > diethyl ether > ethyl acetate > toluene > acetone >2-ethoxyethanol > ethanol > *n*-heptane > acetonitrile. The solubility of HCCP in THF shows the highest value and in acetonitrile shows the lowest values. Compared with HCCP, HPCCP shows also good



0.0032

lnx

0.0028

Figure 6. Mole fraction solubilities of hexachlorocyclotriphosphazene in selected solvents. Experimental data: \blacksquare , THF; \Box , dichloromethane; \bullet , diethyl ether; \bigcirc , ethyl acetate; \blacktriangle , toluene; \triangle , acetone; \blacktriangledown , 2-ethoxyethanol; \bigtriangledown , ethanol; \blacklozenge , *n*-heptane; \diamondsuit , acetonitrile; -, solubility curve calculated from eq 2.

K/T

0.0030



Figure 7. Mole fraction solubilities of hexaphenoxycyclotriphosphazene in selected solvents. Experimental data: \blacksquare , THF; \Box , dichloromethane; \bullet , toluene; \bigcirc , ethyl acetate; \blacktriangle , acetone; Δ , diethyl ether; \blacktriangledown , ethanol; \bigtriangledown , 2-ethoxyethanol; \blacklozenge , acetonitrile; \diamondsuit , *n*-heptane; -, solubility curve calculated from eq 2.

solubility in THF, dichloromethane, ethyl acetate, and toluene. When the chloride atom on the phosphorus atom of HCCP is substituted by a phenoxy group, the solubility of HPCCP in toluene is increased to some extent. This is due to the introduction of the benzene ring and the theory of similarity and compatibility.

To obtain the activity coefficients of PPA, MPPA, HCCP, and HPCCP in the solvents from the experimental data, the following equilibrium equation for solute was derived as a fair approximation³⁵

$$\ln \frac{1}{x_1 \gamma_1} = \frac{\Delta_{\text{fus}} H}{RT_{\text{m}}} \left(\frac{T_{\text{m}}}{T} - 1 \right)$$
(3)

where $\Delta_{\text{fus}}H$ refers to the enthalpy of fusion; T_{m} is the melting temperature; R is the gas constant; and x_1 and γ_1 refer to the mole fraction and activity coefficient of solute in the solution, respectively. With the experimental x_1 , T, $\Delta_{\text{fus}}H$, and T_{m} values known, the activity coefficients of PPA, MPPA, HCCP, and HPCCP in different

0.0034

Table 8. Solubility Parameter and Liquid Molar Volume of Selected Solvents³⁶ and PPA, MPPA, HCCP, and HPCCP

| substance | $\delta_i/(\mathbf{J}\cdot\mathbf{cm}^{-3})^{1/2}$ | $10^6 V_i/\mathrm{m}^3 \cdot \mathrm{mol}^{-1}$ |
|-----------------|--|---|
| methanol | 29.52 | 40.70 |
| ethanol | 26.42 | 58.52 |
| 2-ethoxyethanol | 21.54 | 97.46 |
| toluene | 18.35 | 106.6 |
| acetone | 19.77 | 73.93 |
| ethyl acetate | 18.35 | 98.59 |
| dichloromethane | 20.38 | 64.43 |
| chloroform | 19.03 | 80.66 |
| benzene | 18.71 | 89.48 |
| THF | 19.13 | 81.94 |
| acetonitrile | 24.09 | 52.68 |
| n-heptane | 15.21 | 147.0 |
| diethyl ether | 15.53 | 104.7 |
| PPA | 25.40 | 119.0 |
| MPPA | 24.10 | 129.8 |
| НССР | 23.20 | 135.3 |
| НРССР | 22.70 | 525.5 |

solvents were obtained from eq 3. The results are listed in Tables 4 to 7. The experimental data show that the higher the temperature, the greater the solubility, and the smaller the activity coefficient in all selected solvents. For example, the solubility of PPA in methanol shows the largest value and in water shows the lowest value, while its activity coefficient in methanol is the lowest and in water is the largest at the same temperature. Compared with the activity coefficients of PPA and HCCP, the variation range of the activity coefficients for MPPA and HPCCP is relatively small. Generally, a relatively small solubility and a large activity coefficient result from the deviation from ideal behavior, which illustrated that the interaction between the solutes and the solvents is weak and that the polar or specific chemical force between the molecules of the solid is strong.

Correlation. The Scatchard—Hildebrand activity coefficient model for regular solution, ^{35,36} eq 4, will be used to correlate the activity coefficients listed in Tables 4 to 7. On the basis of this model and a further simplification, the activity coefficient model used for the correlation in this paper can be expressed as

$$RT \ln \gamma_1 = V_1 x_2^2 (\delta_1 - \delta_2)^2$$
 (4)

where γ_1 is the activity coefficient of solute; V_1 is the molar volume of the subcooled liquid of pure solid solute; δ_1 and δ_2 are the solubility parameters of the solute and solvent; R is the gas constant; T is temperature in Kelvin; and x_2 refers to the mole fraction of the solvent. The density of the PPA + ethanol binary solution at 298.15 K related in this work was measured according to ref 37. At a specific composition and with the density of ethanol known,³⁸ the value of molar volume of the subcooled liquid for solid solute PPA can be obtained, and the results are listed in Table 8. However, these values of MPPA, HCCP, and HPCCP cannot be determined with the same method because of relatively lower solubility. They were estimated using advanced chemistry development (ACD/Laboratories) Software V11.02, and the results are listed in Table 8. On the basis of eq 4 and with the solubility parameter δ_2 of the solvents obtained from the literature,³⁸ the solubility parameter of the solute δ_1 can be determined. The results are also listed in Table 8.

Table 9. Parameters of Equation 7 and AAD of MeasuredActivity Coefficients with the Calculated Results fromEquations 6 and 5 for Solutes in Selected Solvents

| solvent | а | Ь | С | AAD % | |
|-----------------|---------|---|--|-------|--|
| | | DDA | | | |
| | 0.00/1 | PPA 2.00 10 ⁻⁴ | 0 | 1.04 | |
| methanoi | 0.0964 | $-3.09 \cdot 10$ | 0 2.72 10^{-6} | 1.94 | |
| ethanol | 0.3783 | $-2.31 \cdot 10$ -6.10, 10 ⁻³ | $3./2 \cdot 10$ | 1.18 | |
| dight acetate | 0.1524 | $-6.19 \cdot 10$ $-4.22 \cdot 10^{-4}$ | 9.12.10 | 1.41 | |
| achioromethane | 0.1524 | $-4.53 \cdot 10$ $-4.07 \cdot 10^{-3}$ | $0 7.08 \cdot 10^{-6}$ | 2.41 | |
| aterone | 1.5047 | $-0.82 \cdot 10^{-3}$ | $1.50 \cdot 10^{-5}$ | 2.09 | |
| 2 othorrotorin | 1.5047 | $-9.82 \cdot 10$ -4.56 $\cdot 10^{-3}$ | $1.39 \cdot 10$ 7 81 · 10 ⁻⁶ | 2.08 | |
| 2-euroxyeuranor | 1 4799 | $-8.08 \cdot 10^{-3}$ | $1.26 \cdot 10^{-5}$ | 3.97 | |
| hongono | 1.4/00 | $-0.78 \cdot 10^{-3}$ | $1.30 \cdot 10$ $1.47 \cdot 10^{-5}$ | 2.27 | |
| Delizene | 0.2020 | $-2.70 \cdot 10^{-3}$ | $1.4/10^{-6}$ | 2.99 | |
| water | 0.2929 | 2.70*10 | 5.80*10 | 3.24 | |
| | | MPPA | | | |
| ethyl acetate | -1.1233 | $7.52 \cdot 10^{-3}$ | $-1.30 \cdot 10^{-5}$ | 3.12 | |
| dichloromethane | -2.9893 | $2.15 \cdot 10^{-2}$ | $-3.87 \cdot 10^{-5}$ | 1.79 | |
| methanol | -0.5503 | $3.72 \cdot 10^{-3}$ | $-6.97 \cdot 10^{-6}$ | 1.15 | |
| chloroform | -1.0599 | $7.03 \cdot 10^{-3}$ | $-1.21 \cdot 10^{-5}$ | 3.01 | |
| toluene | -3.9452 | $2.57 \cdot 10^{-2}$ | $-4.25 \cdot 10^{-5}$ | 4.77 | |
| acetone | -0.5514 | $3.96 \cdot 10^{-3}$ | $-7.24 \cdot 10^{-6}$ | 1.58 | |
| water | -0.1354 | $-5.60 \cdot 10^{-4}$ | $8.10 \cdot 10^{-7}$ | 1.14 | |
| НССР | | | | | |
| ethanol | 0.3317 | $-9.97 \cdot 10^{-4}$ | 0 | 2.26 | |
| ethyl acetate | 0.1984 | $-1.32 \cdot 10^{-3}$ | $2.12 \cdot 10^{-6}$ | 2.30 | |
| diethyl ether | -0.0545 | $-4.75 \cdot 10^{-5}$ | 0 | 0.05 | |
| THF | -0.0810 | $1.91 \cdot 10^{-4}$ | 0 | 0.58 | |
| acetone | 0.0756 | $-1.90 \cdot 10^{-4}$ | 0 | 0.62 | |
| dichloromethane | 0.0027 | $-1.85 \cdot 10^{-5}$ | 0 | 0.03 | |
| acetonitrile | 0.1292 | $-2.00 \cdot 10^{-4}$ | 0 | 0.68 | |
| 2-ethoxyethanol | 0.1259 | $-3.18 \cdot 10^{-4}$ | 0 | 1.44 | |
| toluene | -0.0528 | $1.68 \cdot 10^{-4}$ | 0 | 0.54 | |
| n-heptane | 0.2200 | $-7.58 \cdot 10^{-4}$ | 0 | 1.10 | |
| HPCCP | | | | | |
| ethanol | -0.0757 | $2.14 \cdot 10^{-4}$ | 0 | 1.13 | |
| ethyl acetate | -0.1260 | $4.84 \cdot 10^{-4}$ | $-5.98 \cdot 10^{-7}$ | 0.57 | |
| diethyl ether | -0.0950 | $6.43 \cdot 10^{-5}$ | 0 | 0.45 | |
| THF | -0.2191 | $1.20 \cdot 10^{-3}$ | $-2.01 \cdot 10^{-6}$ | 2.05 | |
| acetone | -0.1472 | $7.94 \cdot 10^{-4}$ | $-1.21 \cdot 10^{-6}$ | 1.26 | |
| dichloromethane | -0.8222 | $5.52 \cdot 10^{-3}$ | $-9.52 \cdot 10^{-6}$ | 0.96 | |
| acetonitrile | 0.0081 | $-2.15 \cdot 10^{-5}$ | 0 | 0.87 | |
| 2-ethoxyethanol | -0.0431 | $1.45 \cdot 10^{-4}$ | 0 | 2.99 | |
| toluene | -0.2004 | $1.00 \cdot 10^{-3}$ | $-1.50 \cdot 10^{-6}$ | 3.99 | |
| n-heptane | -0.1734 | $3.30 \cdot 10^{-4}$ | 0 | 1.59 | |
| | | | | | |

The prediction accuracy of the simplified Scatchard– Hildebrand regular solution model eq 4 can be further improved if a binary interaction parameter l_{12} is added to eq 4 as given by

$$T \ln \gamma_1 = V_1 x_2^2 [(\delta_1 - \delta_2)^2 + 2l_{12}\delta_1\delta_2]$$
 (5)

In this work, the parameter l_{12} was correlated as a function of temperature by

$$l_{12} = a + b(T/K) + c(T/K)^2$$
(6)

The parameters *a*, *b*, and *c* for each solvent obtained by regression from the experimental data are list in Table 9. The absolute average deviation (AAD) of the activity coefficients calculated by eq 5 is also listed in Table 9 where the AAD is defined as

$$AAD = \frac{1}{N} \sum_{i} \left| \frac{\gamma_1^{exp} - \gamma_2^{cal}}{\gamma_1^{exp}} \right|$$
(7)

where exp stands for experimental values; cal stands for calculated values, respectively, of the activity coefficients; and *N* is the number of data points.

Table 10. Coefficients of Equation 8 and Values of $H_1^{E,\infty}$ Derived from Equation 9 for Solutes in Selected Solvents

| solvent | a' | b'/K | $H_1^{\mathrm{E},\infty}/\mathrm{kJ}\cdot\mathrm{mol}^{-1}$ | | | |
|-------------------|---------|---------|---|--|--|--|
| РРА | | | | | | |
| methanol | -6.6332 | 2313.5 | 19.2 | | | |
| ethanol | -2.4624 | 1140.5 | 9.48 | | | |
| ethyl acetate | -8.1301 | 3386.9 | 28.2 | | | |
| dichloromethane | -6.4158 | 2619.6 | 21.8 | | | |
| acetone | -8.7139 | 3329.2 | 23.7 | | | |
| chloroform | -4.6966 | 1850.7 | 15.4 | | | |
| 2-ethoxyethanol | 13.162 | -3741.8 | -31.1 | | | |
| toluene | -7.9197 | 3230.1 | 26.9 | | | |
| benzene | -9.5844 | 3554.7 | 29.5 | | | |
| water | -9.3469 | 3931.7 | 32.7 | | | |
| MPPA | | | | | | |
| ethyl acetate | -13.834 | 4269.6 | 35.5 | | | |
| dichloromethane | -24.598 | 7184.5 | 59.7 | | | |
| methanol | -14.309 | 3393.1 | 28.2 | | | |
| chloroform | -9.8506 | 2795.4 | 23.2 | | | |
| toluene | -29.839 | 9102.2 | 75.7 | | | |
| acetone | -7.4307 | 2294.2 | 19.1 | | | |
| water | -1.7562 | 1010.0 | 8.40 | | | |
| НССР | | | | | | |
| ethanol | -19.891 | 6786.4 | 56.4 | | | |
| ethyl acetate | -0.3154 | 384.42 | 3.20 | | | |
| diethyl ether | -0.5571 | 317.80 | 2.64 | | | |
| THF | 2.7589 | -899.56 | -7.48 | | | |
| acetone | -2.8370 | 1320.6 | 11.0 | | | |
| dichloromethane | -0.2847 | 171.14 | 1.42 | | | |
| acetonitrile | -3.6387 | 2363.0 | 19.6 | | | |
| 2-ethoxyethanol | -5.1725 | 2092.3 | 17.4 | | | |
| toluene | 2.3273 | -348.01 | -2.89 | | | |
| n-heptane | -8.7046 | 3565.4 | 29.6 | | | |
| НРССР | | | | | | |
| ethanol | 16.222 | -4863.3 | -40.4 | | | |
| ethyl acetate | 5.7756 | -2361.0 | -19.6 | | | |
| diethyl ether | 2.8646 | -986.87 | -8.20 | | | |
| THF | -0.1086 | -1266.5 | -10.5 | | | |
| acetone | 3.4762 | -1505.8 | -12.5 | | | |
| dichloromethane | -17.344 | 4164.8 | 34.6 | | | |
| acetonitrile | -1.4862 | 684.11 | 5.69 | | | |
| 2-ethoxyethanol | 8.9613 | -2580.6 | -21.5 | | | |
| toluene | 4.1993 | -1868.2 | -15.5 | | | |
| <i>n</i> -heptane | 14.399 | -4020.0 | -33.4 | | | |

The activity coefficients at infinite dilution of solutes γ_1^{∞} are extrapolated based on eq 5 to satisfy the condition $x_2 \rightarrow 1$. The results of γ_1^{∞} were correlated with temperature by the following equation

$$\ln \gamma_1^{\infty} = a' + b'/(T/K) \tag{8}$$

According to the Gibbs—Helmholtz equation, the value for the partial molar excess enthalpy at infinite dilution $H_1^{E,\infty}$ can be directly obtained from the slope of a straight line derived from eq 8.³⁹

$$\frac{\partial \ln \gamma_1^{\infty}}{\partial (1/T)} = \frac{H_1^{E_1 \infty}}{R} \tag{9}$$

The coefficients a' and b' and the values of $H_1^{E,\infty}$ derived from eq 8 are listed in Table 10. These results are useful for the estimation of the heat of dissolution of the phosphorus-containing compounds in the selected solvents.

CONCLUSIONS

The solubilities of PPA, MPPA, HCCP, and HPCCP in the selected organic solvents and water were systematically measured. These data are important contributions to the fulfillment of the demand for purification process design in the organic phosphorus industry. They can be correlated as a linear function of inverse temperature. The solubility data calculated by the equation are in good agreement with the experimental values. Moreover, the activity coefficients of solutes have also been obtained, and the results are correlated with the Scatchard—Hildebrand activity coefficient model. The absolute average deviation of the modeling is less than 5 %. The partial molar excess enthalpies at infinite dilution were also predicted.

ASSOCIATED CONTENT

Supporting Information. The information of ¹H NMR and ³¹P NMR spectra and the DSC and TGA graphs of PPA, MPPA, HCCP, and HPCCP, an analysis report for the uncertainty of DSC measurement, and the parameters of eq 2. This material is available free of charge via the Internet at http://pubs. acs.org.

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