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# EXTERNAL TRANSVERSE MAGNETIC FIELD EFFECT ON ELECTROLYTE DIFFUSION IN CsCI-H<sub>2</sub>O SOLUTION

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#### ABSTRACT

Experiments using modified fritted glass diaphragm-cell method show that an externally applied magnetic field of  $5 \text{ kG}$  strength influences the integral diffusion coefficient of CsCI (measured at 25°C and at ambient pressure) in 0.04; 0.08; 0.17, 0.4 and 0.8 N CsCl- $H<sub>2</sub>O$  solution.

#### **INTRODUCTION**

By means of modified fritted glass diaphragm cell method  $1-9$ , it has been found that an applied transverse external magnetic field of 5 kG influences the integral diffusion coefficient values of CsCl in 0.04; 0.09; 0.17; 0.4 and 0.8 N CsCl-H<sub>2</sub>O solution at  $25^{\circ}$ C and at the ambient pressure (Table 1, Figs.  $1-3$ ).

The presented integral diffusion coefficient values (Table 1, Figs. 1-3) for CsCl were obtained using the standard dilute electrolyte solution diffusion coefficient calculation methods, for both the no applied field<sup> $1-5$ </sup> and the externally applied magnetic field states<sup>6-11</sup>. As in the case of KCI-, NaCI-, HCI- and LiCI-integral diffusion coefficient calculation<sup>6-9</sup> when the electrolyte solution is subjected to an applied magnetic field, it was assumed that the applied transverse magnetic field does not in any way influence or alter the physico-chemical properties (density, viscosity and electric resistance) of water\* and the used salt<sup>12-14</sup>. The obtained experimental results (Table 1, Figs.  $1-3$ ) strengthen the theoretical (Lielmezs and Musbally<sup>10</sup> and Dumarque, Humeau and Penot<sup>11</sup>) observations and the recent findings of Lielmezs and his coworkers<sup>6-9</sup> that an externally applied magnetic field influences the diffusion process of eIectroIytes in solution.

**<sup>&</sup>quot;Lielmas, Aleman and F5sh 1 5 have shown that rrailsvcrsally applied magaetic fieid of 5** kG strength **at 25°C increases the distiited water viscosity by 0.056%. In this work. however, this observed viscosity change effect was neglected, first. being too small in magnitude; and secondly, for the given behavior of eIeetroIyte diffusion in solution under the infiuenm of the applied magnetic fidd; this change effectively can be considered as constant background.** 

#### **TABLE I**

#### SUMMARY OF RESULTS<sup>\*</sup>



<sup>3</sup> All results listed are at 25±0.06 °C temperature. <sup>b</sup> Arithmetic mean average obtained for all measurements in any test run series (applied field or no applied field) for the given  $\tilde{C}'_{m}$  of CsCl in H<sub>2</sub>O.

<sup>2</sup> For definition of  $\overline{C}_{\text{m}}'$  see refs. 1–9. Then  $\overline{C}_{\text{m}}' = \frac{1}{N} \sum_{i}^{N} C_{\text{m}}'_{i}$ ; where  $i = 1 ... N$  for the specific test run

series.  $4$  Subscript " $H$ " refers to the applied transverse magnetic field condition, this work.  $5$  The no applied field condition means that these measurements were performed in the presence of the ambient

$$
\sum_{i}^{N} (X_i - \bar{X})^2
$$

earth magnetic field.  $\mathbf f$  Standard deviation,  $\sigma =$ where  $X_i$  is the value of the *i*th measure- $N-1$ 

ment;  $\hat{X}$  is the arithmetic mean average for N measurements and N is the total number of diffusion cells for the chosen concentration in the given test run series.

## **EXPERIMENTAL**

Lielmezs et al.<sup>6</sup> describe in detail the apparatus and methods used for the determination of the integral diffusion coefficient of KCl in the KCl-H<sub>2</sub>O solution. Similar techniques were also used by Lielmezs and Aleman<sup> $7-9$ </sup> in the determination of NaCl-, HCl- and LiCl-integral diffusion coefficient values for NaCl-, HCl- and  $LiCl-H<sub>2</sub>O$  solutions.

Again, in this work we have used the same apparatus set-up: the Varian Associates 9-in. electromagnet system and the diffusion cell assembly (consult ref. 6). On the other hand, following the HCl- and LiCi- $H_2O$  solution diffusion coefficient measurement methods<sup>8,9</sup>, for this work we used the dual-diffusion cell measuring system; that is, we at the same time performed two diffusion coefficient measurements: one diffusion cell was placed in the applied magnetic field, while the other was kept at the ambient earth field. Upon completing the measurement, the order of cells (field-no field) was alternated. This arrangement for the same thermodynamic conditions (ambient temperature, pressure and the same initial electrolyte concen-

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tration in the water) permitted to consider the salt diffusion process as a difference between two possibly similar, simultaneously occurring diffusion processes observed at two separate, distinct external magnetic states: one found at the applied transverse external magnetic field (first diffusion cell); the second subject to the ambient earth magnetic field (second diffusion cell, the no-field condition).

For both of the simultaneously operated diffusion cells (cell I and cell II), the CsCI-H,O solutions were prepared, the cell compartments filled, the solutions removed at the end of the experiment and final CsCl concentrations determined using methods and techniques as described previously<sup>6-9</sup>. The diffusion cell compartment and diaphragm pore volumes were determined following previously established procedures<sup>6-9</sup>. Table 2 presents the determined and used physical constants of both diaphragm diffusion cells\_

**TABLE 2** 

**PHYSICAL PROPERTIES OF THE DIAPXRAGM CELLS** 

Cell	$V_1$ (cm <sup>3</sup> )	$V_{2}$ (cm <sup>3</sup> )	$V_3$ (cm <sup>3</sup> )		
1	30.11	29.80	0.407	0.2248	
п	26.65	27.20	0.375	0.2325	

**RESULTS XFD DISCUSSION** 

The diaphragm cell integral diffusion coefficient<sup>1-5</sup>,  $\overline{D}$ , for CsCl electrolyte diffusion in water, was obtained following the previously used calculation methods<sup>6-9</sup>. The results of this work are summarized in Tables I- 2 and Figs. 1-3.

Table 1 gives for all considered arithmetic mean average  $\overline{C}'_m \left( \overline{C}'_m = \frac{1}{N} \sum_{k=1}^N C'_{m,k} \right)$  $\mathcal{N}$  :

where  $i = 1...N$  measurements  $\overline{\prime}$ ccncentrations of CsCl– $H_2O$  solution; the arithmetic

mean average diffusion coefficient  $\langle \bar{D}_{H}^{\circ} \rangle$  and  $\langle \bar{D}^{\circ} \rangle$ , with field and with no applied field conditions\*, and the corresponding arithmetic mean average fractional integral diffusion coefficient,  $(\langle \overline{D}_H^{\circ} \rangle - \langle \overline{D}^{\circ} \rangle)/\langle \overline{D}^{\circ} \rangle \times 100$ , at 25 °C, values.

Figure 1 shows a comparative plot of the arithmetic means average fractional integral diffusion coefficient at 25 °C plotted against the CsCl concentration,  $\bar{C}_{\text{m}}$ , in water. Figure 2 on the other hand represents a comparison, when plotted against the

<sup>\*</sup>In expressions  $\langle \bar{D}_{B}^{\circ} \rangle$ ,  $\langle \bar{D}^{\circ} \rangle$  and  $(\langle \bar{D}_{B}^{\circ} \rangle - \langle \bar{D}^{\circ} \rangle)/\langle \bar{D}^{\circ} \rangle \times 100$ ; superscript "0" denotes the no applied **magnetic field (except for the presence of the earth magnetic field) condition; while subscript "W"**  represents the transversally applied magnetic field of  $H = 5$  kG state. Hence, the expression  $\langle \bar{D}_R^{\circ} \rangle$ **could be read: the arithmetic mean average integral diffusion coefficient at applied magnetic field nf H = 5 kG, taken with respect to the earth magnetic field at the standard magnetic reference state.** 



Fig. 1. The arithmetic mean average fractional integral diffusion coefficient and concentration plot at  $25 \pm 0.06$  °C for CsCl-H<sub>2</sub>O solution.



Fig. 2. The arithmetic mean average integral diffusion coefficient and concentration plot at 25±0.06°C for CsCl-H<sub>2</sub>O solution. Literature data for CsCl-diffusion coefficient values may be found in refs. 28 and 29. Solid line represents no-field; dashed line represents applied magnetic field conditions.



Fig. 3. Arithmetic mean fractional integral diffusion coefficient and concentration plot for CsCl-H<sub>2</sub>O solution at 25±0.06<sup>°</sup>C in semilogarithmic coordinates.

concentration  $\bar{C}'_m$ , between the two calculated arithmetic mean average integral diffusion coefficients: one obtained the infiuence of an applied magnetic field; the other, without the presence of an applied magnetic field (i.e., the ambient earth magnetic field) for the CsCl-electrolyte solution in water. Figure 3 represents the data as found in Fig. 1; only now represented in semi-logarithmic fashion. It appears that for smaller concentrations there exists a straight line relation.

In our previous work<sup>6-9</sup> we discussed the effect of titration and temperature fluctuations during the run on the calculated integral diffusion coefficient (applied and the no field conditions) in great detail. In this work, as in the previous work<sup>6-9</sup> we find that the experimental errors inherent in the titration process and in temperature variations around the  $25^{\circ}$ C isotherm do not affect meaningfully the observed fractional integral diffusion coefficient values (Table 1, Figs. 1-3).

Since in this work we have used the dual diffusion cell method (compare with refs. 8 and 9), the diffusion process behavior has been observed and evaluated nearly at the same error level using the arithmetic mean average values for the involved parameter,  $\langle \bar{D}_{H}^{\circ} \rangle$ ;  $\langle \bar{D}^{\circ} \rangle$  and  $\bar{C}_{m}$ . This has assured us that the observed fractional integral diffusion coefficient values (Table 1, Figs. l-3) are indeed due to the applied field, the only state parameter which has been kept different for each cell during the dual diffusion cell experiment.

Results (Table 1, Figs. 1–3) show that for  $0.04; 0.083; 0.17; 0.4; 0.8 N; CsCl-H<sub>2</sub>O$ solutions the arithmetic mean average integral diffusion coefficient at constant

temperature (in this work  $25 \div 0.06^{\circ}C$ ) and at constant, externally applied transverse to the sait diffusion path magnetic field of 5 kG; decreases as the salt concentration is increased. This decreaze reaches the largest value around a concentration of 0.2 moI CsCl per litre; then steadily becomes smaller as higher CsCl concentrations are approached. Previous work<sup>6-8</sup> shows that when the KCl-, NaCl- and HCl-H<sub>2</sub>O solutions were subjected to an externally applied magnetic field, the integral diffusion coefficient did increase; although similarly with CsCl behavior, these effects vanish at ligher salt concentrations. On the other hand, experiments with  $LiCl-H<sub>2</sub>O$  solution did show', that simiIarIy to CsCI-eIectroIyte behavior (this work); the LiCI-eIectroIyte integral diffusion coefficient value under the influence of an external magnetic field of 5 kG strength, did decrease as the salt concentration in water was increased. For LiCI this decrease reached the largest vaIue around a concentration of 0.8 mo1 LiCI per Iitre; then steadiIy vanished as higher LiCI concentrations in water were approached.

The exact cause for the observed applied external magnetic field influence on the behavior of the diffusion process of electrolyte solution through inert diaphra\_m (Figs. 1-3) cannot be decided with certainty at this time<sup>6-9</sup>. Most probably the reason for this electrolyte diffusion process behavior in water may be found in various solute-solvent-diaphragm interaction aspects<sup>16-25</sup> and the possible fluid structural and property changes<sup>16.25–27</sup> associated with the magnetic state change of electrolytewater solution. Indeed, if an idealized mechanism of icn passage through porous obstruction (diaphragm, membrane, plug) under the influence of an applied magnetic field in excess of the ambient earth magnetic field could be established; then it may be possible to propose<sup>26,27</sup> a molecular or kinetic theory to predict the electrolyte diffusion coefficient changes caused by this field. Lacking such a model, the use of the methods of thermodynamics of irreversible processes may present another even more general approach to this problem. \i'hether this could be achieved by generalizing the work of Lielmezs and Musbally<sup>10</sup> in which they introduced the Lorentz force as describing the interaction between the drift veIocity of an eIectrolyte in solution and the applied magnetic field; or the more complex work of Dumarque et al.<sup>11</sup>, is the subject matter of further study.

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