# ON A NEW KINETIC CLASSIFICATION OF THE SOLID-GAS THERMAL DECOMPOSITION REACTIONS WHICH OCCUR IN NON-ISOTHERMAL CONDITIONS

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## ABSTRACT

An analysis of the change in the non-isothermal reaction rate with heating rate presented in a previous paper allowed a classification criterion for the thermal decompositions which occur in non-isothermal conditions to be proposed and a kinetic classification of these reactions to be suggested. This paper attempts to explain the changes in the non-isothermal reaction rate with heating and, thus, to define the above-mentioned criterion and classification.

#### INTRODUCTION

The classical non-isothermal rate equation is [1]

$$\frac{\mathrm{d}\alpha}{\mathrm{d}T} = \frac{A}{\beta} f(\alpha) \,\mathrm{e}^{-E/RT} \tag{1}$$

the heating rate  $\beta$  being considered constant, with

$$A = \text{const.} \tag{2}$$

$$E = \text{const.}$$
 (3)

and

$$f(\alpha) = (1-\alpha)^n \alpha^m \left[ -\ln(1-\alpha) \right]^p \tag{4}$$

according to Šesták and Berggren [2] where  

$$n = \text{const.}; \quad m = \text{const.}; \quad p = \text{const.}$$
(5)

For variable kinetic parameters, the equation [1]

$$\frac{\mathrm{d}\alpha}{\mathrm{d}T} = \frac{A(\alpha)}{\beta} f^{\star}(\alpha) \,\mathrm{e}^{-E(\alpha)/RT} \tag{6}$$

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with

 $f^{\star}(\alpha) = f(\alpha, n(\alpha), m(\alpha), p(\alpha))$ <sup>(7)</sup>

should be used instead of eqn. (1)

In a previous paper [3], two types of change in the non-isothermal reaction rate with heating rate were demonstrated. For the dehydration of calcium oxalate with  $\alpha$  constant

$$\frac{\mathrm{d}\alpha}{\mathrm{d}T}(\beta)\downarrow \text{ as }\beta\uparrow \tag{8}$$

Correspondingly for the thermal decomposition of potassium permanganate with  $\alpha$  constant

$$\frac{\mathrm{d}\alpha}{\mathrm{d}T}(\beta)\uparrow \text{ as }\beta\uparrow \tag{9}$$

In the following we shall try to explain the differences in eqns. (8) and (9) using the classical equation, eqn. (1), as well as the non-classical equation, eqn. (6).

# CLASSICAL CASE

Integrating eqn. (1), one obtains

$$g(\alpha) = \frac{A}{\beta} \int_0^T e^{-E/RT} dT$$
(10)

or by solving approximately the integral from the right side of eqn. (10)

$$g(\alpha) = \frac{A}{\beta} \frac{RT^2}{E} e^{-E/RT} Q\left(\frac{E}{RT}\right)$$
(11)

where

$$Q\left(\frac{E}{RT}\right) < 1 \tag{12}$$

Let  $\alpha$  be constant and let

$$\frac{\mathrm{d}\alpha}{\mathrm{d}T}(\beta) = \alpha^{\star}(\beta) \tag{13}$$

Taking the derivative of eqn. (1) with respect to  $\beta$  for  $\alpha$  being constant

$$\frac{\mathrm{d}\alpha^{\star}(\beta)}{\mathrm{d}\beta} = \frac{A}{\beta}f(\alpha) \ \mathrm{e}^{-E/RT} \left[ -\frac{1}{\beta} + \frac{E}{RT^2} \frac{\mathrm{d}T}{\mathrm{d}\beta} \right]$$
(14)

where, for simplicity's sake, T is written for  $T(\beta)$ .

From eqn. (10), taking the derivative with respect to  $\beta$  we get [4]

$$g(\alpha) = A \ e^{-E/RT} \frac{\mathrm{d}T}{\mathrm{d}\beta}$$
(15)

Equation (14) with  $dT/d\beta$  given by eqn. (15) becomes

$$\frac{\mathrm{d}\alpha^{\star}(\beta)}{\mathrm{d}\beta} = \alpha^{\star}(\beta) \left[ -\frac{1}{\beta} + \frac{E}{RT^2} \,\mathrm{e}^{E/RT} \frac{g(\alpha)}{A} \right] \tag{16}$$

Substituting the pre-exponential factor A from eqn. (11) into eqn. (16)

$$\frac{\mathrm{d}\alpha^{\star}(\beta)}{\mathrm{d}\beta} = \frac{\alpha^{\star}(\beta)}{\beta} \left[ Q\left(\frac{E}{RT}\right) - 1 \right]$$
(17)

As  $\alpha^{\star}(\beta)/\beta > 0$ , taking into account relationship (12)

$$\frac{\mathrm{d}\alpha^{\star}(\beta)}{\mathrm{d}\beta} < 0 \tag{18}$$

According to inequality (18), the function  $\alpha^{\star}(\beta)$  decreases when the heating rate  $\beta$  increases, thus

$$\frac{\mathrm{d}\alpha}{\mathrm{d}T}(\beta)\downarrow \text{ as }\beta\uparrow \tag{19}$$

This result shows that a description of the decomposition in classical terms leads only to a decrease in the non-isothermal reaction rate with the heating rate (for  $\alpha$  constant), as was demonstrated experimentally in the dehydration of calcium oxalate.

# NON-CLASSICAL CASE

For  $\alpha$  constant, the derivative of eqn. (6) with respect to  $\beta$  gives

$$\frac{\mathrm{d}\alpha^{\star}(\beta)}{\mathrm{d}\beta} = \alpha^{\star}(\beta) \left[ -\frac{1}{\beta} + \frac{E(\alpha)}{RT^2} \frac{\mathrm{d}T}{\mathrm{d}\beta} \right]$$
(20)

In this case,  $dT/d\beta$  cannot be evaluated as a function of the kinetic parameters.

Nevertheless, taking into account that for  $\alpha$  constant [5]

$$\frac{1}{T} = a + b \ln \beta \qquad (a = \text{const.}, b = \text{const.})$$
(21)

and

$$\frac{\mathrm{d}T}{\mathrm{d}\beta} = -T^2 \frac{b}{\beta} \tag{22}$$

Taking into account this result, eqn. (2) becomes

$$\frac{\mathrm{d}\alpha^{\star}(\beta)}{\mathrm{d}\beta} = \frac{\alpha^{\star}(\beta)}{\beta} \left[ -1 - \frac{E(\alpha)b}{R} \right]$$
(23)

The sign of this expression cannot be predicted for the general case as the dependences of b on the kinetic parameters are unknown. Assessing the dependences of b on  $A(\alpha)$ ,  $f^{\star}(\alpha)$  and  $E(\alpha)$  is a future project. For the time

being, b and  $E(\alpha)$  will be determined from experimental data. The two following examples make use of experimental data given elsewhere [3].

First example: the decomposition of potassium permanganate

 $\alpha = 0.45$   $E(\alpha = 0.45) = 33.87 \text{ kcal mol}^{-1}$  $\beta_1 = 1.5 \text{ K min}^{-1} \text{ and } \beta_2 = 3 \text{ K min}^{-1}$ 

The system

$$\frac{1}{514.0} = a + b \ln 1.5$$

$$\frac{1}{529.5} = a + b \ln 3$$
(24)

leads to the following value for b

$$b = -8.2163 \times 10^{-5} \text{ K}^{-1} \tag{25}$$

For the expression  $d\alpha^{\star}(\beta)/d\beta$ , obviously

$$\frac{\mathrm{d}\alpha^{\star}(\beta)}{\mathrm{d}\beta} = 0.4004 \frac{\alpha^{\star}(\beta)}{\beta} > 0$$
(26)

Thus for the decomposition of potassium permanganate

$$\frac{\mathrm{d}\alpha}{\mathrm{d}T} = \alpha^{\star}(\beta) \uparrow \text{ as } \beta \uparrow$$
(27)

in qualitative agreement with the experimental data.

Second example: the dehydration of calcium oxalate

$$\alpha = 0.50$$

$$E = (\alpha = 0.50) = \frac{E(\alpha = 0.4583) + E(\alpha = 0.5417)}{2} = 23.03 \text{ kcal mol}^{-1}$$

$$\beta_1 = 1 \text{ K min}^{-1} \text{ and } \beta_2 = 5 \text{ K min}^{-1}$$
From the system
$$\frac{1}{429.2} = a + b \ln 1$$

$$\frac{1}{449.2} = a + b \ln 5$$
(28)

it follows that

$$b = -6.4455 \times 10^{-5} \,\mathrm{K}^{-1} \tag{29}$$

and

$$\frac{\mathrm{d}\alpha^{\star}(\beta)}{\mathrm{d}\beta} = -0.2530 \frac{\alpha^{\star}(\beta)}{\beta} < 0$$
(30)

Thus, in this case

$$\frac{\mathrm{d}\alpha}{\mathrm{d}T}(\beta) = \alpha^{\star}(\beta) \downarrow \text{ as } \beta \uparrow$$
(31)

in qualitative agreement with the experimental data.

# CONCLUSIONS

(1) For the change in  $d\alpha/dT(\beta)$  with the heating rate,  $\beta$ , at  $\alpha$  constant, the classical model predicts only the case  $d\alpha/dT(\beta) \downarrow$  as  $\beta \uparrow$ .

(2) The non-classical model with variable kinetic parameters predicts the previous case as well as the case  $[d\alpha/dT](\beta)\uparrow$  as  $\beta\uparrow$ .

(3) The decompositions in solid-gas systems which occur in non-isothermal conditions can be classified according to the changes in the non-isothermal reaction rate with the heating rate at  $\alpha$  constant.

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