# Thermodynamics of associated solutions. Prediction of ternary excess molar enthalpies of alcohol mixtures containing an active non-associating component

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### **Abstract**

Ternary excess molar enthalpies of 1-propanol + triethylamine +  $n$ -heptane, 1propanol + 1-hexanol + 3-pentanone and I-propanol + 1-heptanol + 3-pentanone have been predicted using the **UNIQUAC** associated-solution model with binary parameters alone. For  $1$ -propanol + triethylamine +  $n$ -heptane, the **UNIQUAC** associated-solution model gives better predicted results than those obtained from the **ERAS** model of Heintz and the **NRTL** equation. For the two other ternary systems, the **UNIQUAC** associatedsolution model is superior to the group-contribution model of Nitta-Chao.

LIST OF SYMBOLS

1-propanol, triethylamine or 1-hexanol or 1-heptanol, and $n$ -heptane or 3-pentanone
binary energy parameter
imer of 1-propanol and jmer of 1-hexanol or 1-heptanol
complex containing $i$ molecules of 1-propanol and one molecule of triethylamine
complex containing $i$ molecules of 1-propanol and $j$ molecules of 1-hexanol or 1-heptanol
complex containing $i$ molecules of 1-propanol, $j$ molecules of 1-hexanol or 1-heptanol and one molecule of 3- pentanone

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*Greek letters* 



*Subscripts* 



# *Superscripts*



## **INTRODUCTION**

It has been found that the **UNIQUAC** associated-solution model is useful in predicting ternary excess molar enthalpies, not only for alcohol mixtures composed of completely miscible binary mixtures, but also for ternary alcohol mixtures which contain binary mixtures with partial miscibility [l-7]. Furthermore, the model has been successfully applied for tenary aniline + alcohol + benzene mixtures  $[8-11]$ . The number of ternary alcohol mixtures previously studied is not huge. The workability of the model needs to be examined using new experimental results on ternary alcohol mixtures, including one or two strongly polar non-associating components. Recently, Bender et al. [12] reported the excess molar enthalpies  $H^E$  of 1-propanol + triethylamine + n-heptane mixtures and its three binary mixtures, and compared their experimental ternary  $H<sup>E</sup>$  results with those calculated from the **ERAS** (extended real associated solution) model of Heintz [13] and the **NRTL** equation [14]. López and co-workers [15, 16] reported two sets of ternary experimental  $H^E$  data for 1-propanol + 1hexanol or 1-heptanol  $+3$ -pentanone and their component binaries, and presented a comparison of experimental results and theoretical calculations derived from the group-contribution Nitta-Chao model [17] for the two ternary systems. These three sets of ternary  $H^E$  data provide a good means of checking the prediction ability of the **UNIQUAC** associated-solution model.

### **THE UNIQUAC ASSOCIATED-SOLUTION MODEL**

One of the three ternary systems to be studied here contains only one alcohol, and the two others include two alcohols. We must use two different expressions of excess molar enthalpy for these systems.

## *1 -Propanol+ triethylamine+n-heptane system*

We assume that 1-propanol (A) self-associates to produce linear imers by chain reactions  $(A_i + A_1 = A_{i+1})$ , and the resultant *imers* of 1-propanol form chemical complexes with triethylamine (B) according to the reaction  $A_i + B = A_iB$ . *n*-Heptane does not form any chemical complexes with 1-propanol and triethylamine, as expected from its chemical nature. The two equilibrium constants  $K_A$  and  $K_{AB}$  for these two reactions are independent of the degree of association and depend on temperature

$$
K_{A} = \frac{\Phi_{A_{i+1}}}{\Phi_{A_i}\Phi_{A_1}i + 1}
$$
  
=  $K_A^* \exp\left(-\frac{h_A}{R}\left(\frac{1}{T} - \frac{1}{T^*}\right)\right)$  (1)

$$
K_{AB} = \frac{\Phi_{A_i B}}{\Phi_{A_i} \Phi_{B_i}} \frac{i}{ir_A + r_B}
$$
  
=  $K_{AB}^* \exp\left(-\frac{h_{AB}}{R} \left(\frac{1}{T} - \frac{1}{T^*}\right)\right)$  (2)

where  $\Phi_{A_{i+1}}, \Phi_{A_i}, \Phi_{A_i}, \Phi_{A_i}$  and  $\Phi_{B_i}$  are the segment fractions of the chemical species  $A_{i+1}$ ,  $A_i$ ,  $A_j$ ,  $A_j$  and  $B_j$ ,  $h_A$  and  $h_{AB}$  are the molar enthalpies of hydrogen bond and complex formation,  $r_A$  and  $r_B$  are the pure-component molecular size parameters, *R* is the gas constant, and the superscript  $*$  indicates the reference state (here taken as  $50^{\circ}$ C). The final expression of the ternary excess molar enthalpy is given by

$$
H_{\rm m}^{\rm E} = h_{\rm A} K_{\rm A} X_{\rm A} (\Phi_{\rm A_1} - \Phi_{\rm A_1}^0) + h_{\rm AB} K_{\rm AB} \Phi_{\rm B_1} r_{\rm A} x_{\rm A} \frac{(1 - K_{\rm A} \Phi_{\rm A_1})}{(1 + r_{\rm A} K_{\rm AB} \Phi_{\rm B_1})}
$$

$$
- R \sum_{I}^{3} \frac{\sum_{j}^{3} \theta_{J} (\partial \tau_{JI} / \partial (1/T))}{\sum_{J}^{3} \theta_{J} \tau_{JI}} \tag{3}
$$

where  $q$  is the pure-component molecular area parameter; the segment fraction  $\Phi$ , the surface fraction  $\theta$  and the binary coefficient  $\tau_{II}$  are given by

$$
\Phi_I = x_I r_I \bigg/ \sum_{j=1}^{3} x_j r_j \tag{4}
$$

$$
\theta_l = x_l q_l / \sum_{j=1}^{3} x_j q_j \tag{5}
$$

$$
\tau_{II} = \exp(-a_{II}/T) \tag{6}
$$

The energy parameters are assumed to change linearly with temperature

$$
a_{II} = C_{II} + D_{II}(T - 273.15), \quad a_{II} = C_{II} + D_{II}(T - 273.15) \tag{7}
$$

The monomer segment fractions  $\Phi_{A_1}$  and  $\Phi_{B_1}$  are solved simultaneously from the mass balance equations

$$
\Phi_{A} = \frac{\Phi_{A_1}}{(1 - K_A \Phi_{A_1})^2} (1 + r_A K_{AB} \Phi_{B_1})
$$
\n(8)

$$
\Phi_{\mathbf{B}} = \Phi_{\mathbf{B}_1} \left( 1 + \frac{r_{\mathbf{B}} K_{\mathbf{A} \mathbf{B}} \Phi_{\mathbf{A}_1}}{(1 - K_{\mathbf{A}} \Phi_{\mathbf{A}_1})} \right)
$$
(9)

The monomer segment fraction of the pure alcohol is expressed by

$$
\Phi_{A_1}^0 = [2K_A + 1 - (1 + 4K_A)^{0.5}]/2K_A^2 \tag{10}
$$

## *1 -Propanol + 1 -hexanol or 1 -heptanol + 3-pentanone systems*

We assume that the multi-cross association between an imer of 1-propanol (A) and a jmer of 1-hexanol or 1-heptanol (B) yields  $(A_iB_j)_k$ ,<br>(B.A.),  $A_i(B_iA_j)_i$ , and  $B_i(A_iB_j)_i$ , according to the reaction  $(B_iA_j)_k$ ,  $A_i(B_jA_k)_l$  and  $B_i(A_iB_k)_l$  according  $A_iB_iA_i + B_i = A_iB_iA_kB_i$ , and that the equilibrium constant is independent of the degrees of the self-association and cross-association

$$
K_{AB} = \frac{\Phi_{A_iB_jA_kB_l}}{\Phi_{A_iB_jA_k}\Phi_{B_l}} \frac{r_{A_iB_jA_k}r_{B_l}}{r_{A_iB_jA_kB_l}r_Ar_B}
$$
(11)

The resultant alcohol polymers and copolymers and 3-pentanone (C) produce additional chemical complexes  $A_iC$ ,  $B_iC$ ,  $(A_iB_i)_kC$ ,  $(B_iA_i)_kC$ ,  $A_i(B_iA_k)_iC$  and  $B_i(A_iB_k)_iC$ . The equilibrium constants for these chemical complex-forming reactions are assumed to be independent of the degrees of the self-association and cross-association.

The ternary  $H_m^E$  is expressed by

$$
H_{\rm m}^{\rm E} = h_{\rm A}x_{\rm A} \left( \frac{\bar{U}_{\rm A}\Phi_{\rm A}}{\Phi_{\rm A}} - \bar{U}_{\rm A}^{\rm 0}\Phi_{\rm A}^{\rm 0} \right) + h_{\rm B}x_{\rm B} \left( \frac{\bar{U}_{\rm B}\Phi_{\rm B}}{\Phi_{\rm B}} - U_{\rm A}^{\rm 0}\Phi_{\rm B}^{\rm 0} \right)
$$
  
+  $(h_{\rm A}\bar{U}_{\rm A} + h_{\rm AC}U_{\rm A}) \frac{r_{\rm A}K_{\rm AC}\Phi_{\rm C}r_{\rm A}\Phi_{\rm A}}{\Phi_{\rm A}}$   
+  $(h_{\rm B}\bar{U}_{\rm B} + h_{\rm BC}U_{\rm B}) \frac{r_{\rm B}K_{\rm BC}\Phi_{\rm C}r_{\rm A}\Phi_{\rm B}}{\Phi_{\rm B}}$   
+  $\left[ h_{\rm A} \left( \frac{\bar{U}_{\rm A}x_{\rm A}\Phi_{\rm A}}{\Phi_{\rm A}} (2 - r_{\rm A}r_{\rm B}K_{\rm AB}^2\Phi_{\rm A}r_{\rm B} \Phi_{\rm B}r_{\rm A}U_{\rm B})(1 + r_{\rm A}K_{\rm AC}\Phi_{\rm C}) \right) \right]$   
+  $\frac{\bar{U}_{\rm A}}{U_{\rm A}K_{\rm AB}} \left[ \frac{x_{\rm A}}{r_{\rm B}\Phi_{\rm A}} (1 + r_{\rm A}K_{\rm AC}\Phi_{\rm C}r_{\rm A}) + \frac{x_{\rm B}}{r_{\rm A}\Phi_{\rm B}} (1 + r_{\rm B}K_{\rm BC}\Phi_{\rm C}r_{\rm A}) \right]$   
+  $h_{\rm B} \left\{ \frac{\bar{U}_{\rm B}x_{\rm B}\Phi_{\rm B}}{\Phi_{\rm B}} (2 - r_{\rm A}r_{\rm B}K_{\rm AB}^2\Phi_{\rm A}r_{\rm B} \Phi_{\rm B}r_{\rm A}U_{\rm A}U_{\rm B})(1 + r_{\rm B}K_{\rm BC}\Phi_{\rm C}r_{\rm A}) \right\}$   
+  $\frac{\bar{U}_{\rm B}}{U_{\rm B}K_{\rm AB}} \left[ \frac{x_{\rm A}}{r_{\rm B}\Phi_{\rm A}} (1 + r_{\rm$ 

$$
+ h_{AB} \Biggl\{ \Biggl[ \frac{x_{A}}{r_{B} \Phi_{A}} (1 + r_{A} K_{AC} \Phi_{C_{1}}) + \frac{x_{B}}{r_{A} \Phi_{B}} (1 + r_{B} K_{BC} \Phi_{C_{1}}) \Biggr] \times \frac{(1 + r_{A} r_{B} K_{AB}^{2} \Phi_{A_{1}} \Phi_{B_{1}} U_{A} U_{B})}{K_{AB}} + \frac{2 U_{A} x_{A} \Phi_{A_{1}}}{\Phi_{A}} (1 + r_{A} K_{AC} \Phi_{C_{1}}) + \frac{2 U_{B} x_{B} \Phi_{B_{1}}}{\Phi_{B}} (1 + r_{B} K_{BC} \Phi_{C_{1}}) \Biggr\} + \Biggl\{ h_{AC} r_{A} K_{AC} \Phi_{C_{1}} \Biggl( \frac{U_{A} x_{A} \Phi_{A_{1}}}{\Phi_{A}} + \frac{x_{A}}{r_{A} K_{AB} \Phi_{A}} \Biggr) + h_{BC} r_{B} K_{BC} \Phi_{C_{1}} \Biggl( \frac{U_{B} x_{B} \Phi_{B_{1}}}{\Phi_{B}} + \frac{x_{B}}{r_{B} K_{AB} \Phi_{B}} \Biggr) \Biggr\} \times (1 - r_{A} r_{B} K_{AB}^{2} \Phi_{A_{1}} \Phi_{B_{1}} U_{A} U_{B}) \Biggr] \frac{r_{A} r_{B} K_{AB}^{2} \Phi_{A_{1}} \Phi_{B_{1}} U_{A} U_{B}}{(1 - r_{A} r_{B} K_{AB}^{2} \Phi_{A_{1}} \Phi_{B_{1}} U_{A} U_{B})^{2}} - R \sum_{i}^{3} \frac{y}{q_{i} x_{i}} \frac{\partial r_{i \mu}}{\partial (1/T)} \frac{y}{q_{i} \partial_{i} \tau_{i \mu}} (12)
$$

where the quantities  $\bar{U}_I$  and  $U_I$  are defined as

$$
\bar{U}_I = K_I \Phi_{I_1} / (1 - K_I \Phi_{I_1})^2
$$
\n(13)

$$
U_{I} = 1/(1 - K_{I} \Phi_{I_{1}}) \tag{14}
$$

and the value of  $\bar{U}_l$  at pure alcohol states  $\bar{U}_l^0$  is

$$
\bar{U}_I^0 = K_I \Phi_{I_1}^0 / (1 - K_I \Phi_{I_1}^0)^2
$$
\n(15)

The monomer segment fractions of the components,  $\Phi_{A_1}$ ,  $\Phi_{B_1}$  and  $\Phi_{C_1}$ , are solved simultaneously from eqns. (16)-(18)

$$
\Phi_{A} = (1 + r_{A}K_{AC}\Phi_{C_{1}})\bar{S}_{A} + \frac{r_{A}K_{AB}\bar{S}_{A}\bar{S}_{B}}{(1 - r_{A}r_{B}K_{AB}^{2}\bar{S}_{A}\bar{S}_{B})^{2}}\times \{2 + r_{B}K_{AB}\bar{S}_{A}(2 - r_{A}r_{B}K_{AB}^{2}\bar{S}_{A}\bar{S}_{B}) + r_{A}K_{AB}\bar{S}_{B}\n+ \Phi_{C_{1}}[(r_{A}K_{AC} + r_{B}K_{BC}) + r_{A}r_{B}K_{AB}K_{AC}\bar{S}_{A}\n\times (2 - r_{A}r_{B}K_{AB}^{2}\bar{S}_{A}\bar{S}_{B}) + r_{A}r_{B}K_{AB}K_{BC}\bar{S}_{B}]\}\n(16)
$$

$$
\Phi_{\rm B} = (1 + r_{\rm B} K_{\rm BC} \Phi_{\rm C_1}) \bar{S}_{\rm B} + \frac{r_{\rm B} K_{\rm AB} S_{\rm A} S_{\rm B}}{(1 - r_{\rm A} r_{\rm B} K_{\rm AB}^2 S_{\rm A} S_{\rm B})^2} \times \{2 + r_{\rm A} K_{\rm AB} S_{\rm B} (2 - r_{\rm A} r_{\rm B} K_{\rm AB}^2 S_{\rm A} S_{\rm B}) + r_{\rm B} K_{\rm AB} S_{\rm A} \n+ \Phi_{\rm C_1} [(r_{\rm A} K_{\rm AC} + r_{\rm B} K_{\rm BC}) + r_{\rm A} r_{\rm B} K_{\rm AB} K_{\rm BC} S_{\rm B} \n\times (2 - r_{\rm A} r_{\rm B} K_{\rm AB}^2 S_{\rm A} S_{\rm B}) + r_{\rm A} r_{\rm B} K_{\rm AB} K_{\rm AC} S_{\rm A}] \}
$$
\n(17)

$$
\Phi_{\rm C} = \Phi_{\rm C_1} \{ 1 + r_{\rm C} K_{\rm AC} S_{\rm A} + r_{\rm C} K_{\rm BC} S_{\rm B} + \frac{r_{\rm A} r_{\rm B} r_{\rm C} K_{\rm AB}^2 S_{\rm A} S_{\rm B}}{(1 - r_{\rm A} r_{\rm B} K_{\rm AB}^2 S_{\rm A} S_{\rm B})} \times \left[ \frac{K_{\rm AC}}{r_{\rm B} K_{\rm AB}} + \frac{K_{\rm BC}}{r_{\rm A} K_{\rm AB}} + K_{\rm AC} S_{\rm A} + K_{\rm BC} S_{\rm B} \right] \}
$$
(18)

where the sums  $\overline{S}_i$  and  $S_i$  are defined as

$$
\bar{S}_I = \Phi_{I_1}/(1 - K_I \Phi_{I_1})^2
$$
\n(19)

$$
S_{\rm I} = \Phi_{I_1}/(1 - K_1 \Phi_{I_1})
$$
\n(20)

### CALCULATED RESULTS

TABLE 1

Table 1 shows the association parameters and molecular structural parameters for the pure components. We used two sets of association parameters: **I**, association constants at 50°C,  $K_A^*$ , were taken from Brandani [18] and a single value of  $h<sub>A</sub> = -23.2$  kJ mol<sup>-1</sup> was taken for all alcohols [19]; **II,**  $K^*$  and  $h_A$  were obtained from Nagata [5]. The pure-component molecular structural parameters  $r$  and  $q$  were calculated by the method of Vera et al. [20]. Table 2 gives the solvation constants and enthalpies of complex formation used in this work. Table 3 presents the binary calculated results and the calculated values are compared with the experimental results in Figs.  $1-3$ .

Figures  $\overline{4}$  and 5 compare selected experimental  $H^E$  results with theoretical calculations based on the **ERAS, NRTL** [12] and **UNIQUAC**  associated-solution models for 1-propanol + triethylamine +  $n$ -heptane. The solid lines through the triangles depicted in Figs. 4 and 5 represent the compositions for which experimental results were taken. Bender et al. [12] stated that predictions of  $H^E$  made by the **ERAS** model and the **NRTL** model are of comparable quality in the case of curves A, C, D and E in Figs. 4 and

Component	Type <sup>a</sup>	$K_{\rm A}^{*}$ (50°C)	$-h_A/(kJ \text{ mol}^{-1})$	r	$\boldsymbol{q}$
1-Propanol		87.0	23.2	2.23	1.98
	$\mathbf{I}$	89.9	23.6		
1-Hexanol		40.8	23.2	3.85	3.28
	П	59.6	22.4		
1-Heptanol		40.7	23.2	4.39	3.71
	П	49.8	22.1		
$n$ -Heptane				4.15	3.52
3-Pentanone				3.14	2.72
Triethylamine				4.02	3.41

Association parameters and molecular structural parameters for pure components

<sup>a</sup> **I**, association constants were taken from Brandani [18], and  $h<sub>A</sub> = -23.2$  kJ mol<sup>-1</sup> was used for all alcohols [19]; **II**,  $K_A^*$  and  $h_A$  were taken from Nagata [5].



#### TABLE 2

Solvation constants and enthalpies of complex formation

<sup>a</sup> I, association constants were taken from Brandani [18], and  $h_A = -23.2$  kJ mol  $\degree$  was used for all alcohols [19]; **II**,  $K_A^*$  and  $h_A$  were taken from Nagata [5] and  $h_{AB} = (h_A + h_B)/2$ .



Fig. 1. Molar excess enthalpies for the three binary systems at  $25^{\circ}$ C. Experimental data:  $\bullet$ , 1-propanol + n-heptane [12] (smoothed data);  $\blacktriangle$ , triethylamine + n-heptane [12];  $\blacksquare$ , 1-propanol + triethylamine [12]; -, calculated using  $K_A^*$  (50°C) = 89.9 and  $h_A = -23.6$  kJ mol<sup>-1</sup>.

System $(A + B)$	Type <sup>a</sup>	No. of data points	Abs. arith. mean dev./ $(J mol^{-1})$	<b>Parameters</b>				Ref.
				$C_{BA}/K$	$D_{BA}$	$C_{AB}/K$	$D_{AB}$	
1-Propanol $+$ triethylamine	I	13	8.61	987.73	1.7722	$-156.75$	0.0974	12
	П		7.11	766.99	1.3933	$-183.97$	0.0511	
1-Propanol $+ n$ -heptane		19	4.44	191.66	0.7144	150.34	0.4789	12
	$\mathbf{H}$		4.47	214.36	0.7924	165.64	0.5360	
Triethylamine $+ n$ -heptane		12	0.60	264.52	0.9504	63.19	0.1798	12
1-Propanol + 1-hexanol	I	16	0.62	$-59.08$	$-0.4566$	67.78	0.5175	16
	П		0.15	$-64.83$	$-0.1702$	94.07	0.2377	
1-Propanol $+1$ -Heptanol		18	0.51	34.73	$-0.8317$	$-22.50$	0.7835	16
	П		0.81	35.48	$-0.6744$	$-15.00$	0.6535	
1-Propanol $+3$ -pentanone	I	22	8.22	300.60	0.4061	381.80	$-0.2969$	15
	п		7.21	260.41	0.2982	411.21	$-0.1738$	
1-Hexanol $+3$ -pentanone		20	8.49	313.60	0.4868	418.68	$-0.2963$	16
	п		8.62	272.43	0.2369	439.02	$-0.1321$	
1-Heptanol $+3$ -pentanone	I	20	5.94	297.24	0.3656	465.42	$-0.1866$	16
	п		8.16	308.11	0.3068	449.46	$-0.2184$	

TABLE 3

Calculated results of excess molar enthalpies for binary systems at 25°C

<sup>a</sup> I, association constants were taken from Brandani [18], and  $h_A = -23.2 \text{ kJ mol}^{-1}$  was used for all alcohols [19]; **II**,  $K_A^*$  and  $h_A$  were taken from Nagata [5].



Fig. 2. Molar excess enthalpies for two alcohol + alcohol systems at 25°C. Experimental data:  $\bullet$ , 1-propanol + 1-heptanol [16];  $\blacktriangle$ , 1-propanol + 1-hexanol [16]; -, calculated using  $K_A^*$  (1-propanol) = 87.0,  $K_B^*$  (1-hexanol) = 40.8 and  $K_B^*$  (1-heptanol) = 40.7 at 50°C, and  $h_A = h_B = -23.2$  kJ mol<sup>-1</sup>.



Fig. 3. Molar excess enthalpies for three binary systems at  $25^{\circ}$ C. Experimental data:  $\bullet$ , 1-heptanol + 3-pentanone [16];  $\blacktriangle$ , 1-hexanol + 3-pentanone [16];  $\blacksquare$ , 1-propanol + 3pentanone [15];  $-\frac{1}{2}$ , calculated using  $K_A^*$  (1-propanol) = 87.0,  $K_B^*$  (1-hexanol) = 40.8 and *K*<sub>B</sub><sup>\*</sup> (1-heptanol) = 40.7 at 50°C, and  $h_A = h_B = -23.2 \text{ kJ} \text{ mol}^{-1}$ .

5, and the **ERAS** model is superior in the case of curve B. In contrast, the **UNIQUAC** associated-solution model is superior to the **ERAS** model in all cases.

Figures 6 and 7 also compare experimental  $H<sup>E</sup>$  results with predicted values obtained from the Nitta-Chao [17] and **UNIQUAC** associated-solution models for **1-propanol +** 1-hexanol or 1-heptanol + 3-pentanone. Again the **UNIQUAC** associated-solution model works better than the Nitta-Chao model.

Table 4 gives the ternary predicted results for the three systems. The two sets of parameters give nearly the same results.



Fig. 4. Comparison between experimental and calculated excess enthalpies for ternary mixtures of  $x_1$ 1-propanol +  $x_2$ triethylamine +  $x_3$ n-heptane prepared by mixing pure triethylamine with constant ratios of  $x_1/x_3$  at 25°C.  $\bullet$ ,  $\blacktriangle$ : Experimental data of Bender et al. [12]. Calculated:  $\frac{1}{\sqrt{2}}$  UNIQUAC associated-solution model using  $K_A^* = 89.9$  (50°C) and  $h_A = -23.6$  kJ mol<sup>-1</sup>; ---, **ERAS** model; ---, **NRTL** model.



Fig. 5. Comparison between experimental and calculated excess enthalpies for ternary mixtures of  $x_1$ 1-propanol +  $x_2$ triethylamine +  $x_3$ n-heptane prepared by mixing pure 1propanol with constant ratios of  $x_2/x_3$  at 25°C.  $\bullet$ ,  $\blacktriangle$ ,  $\blacksquare$ : Experimental data of Bender et al. [12]. Calculated:  $\longrightarrow$ , UNIQUAC associated-solution model using  $K_2^* = 89.9$  (50°C) and *h*<sub>A</sub> = -23.6 kJ mol<sup>-1</sup>; ---, ERAS model; ----, NRTL model



Fig. *6.* Comparison between experimental and calculated excess enthalpies at 25°C of the pseudo-binary. Experimental data of López et al. [16]:  $\bullet$ ,  $(x_1 + x_2)(0.2495$  1propanol + 0.7505 3-pentanone) +  $x_3$ 1-hexanol;  $(x_1 + x_2)(0.5000$  1-propanol + 0.5000 3-pentanone) +  $x_3$ 1-hexanol;  $\triangle$ ,  $(x_1 + x_2)(0.7505$  1-propanol + 0.2495 3-pentanone) +  $x_3$ 1hexanol. Calculated:  $-\rightarrow$ , **UNIQUAC** associated-solution model using  $K_A^* = 87.0$  (50°C) and  $h_A = -23.2 \text{ kJ mol}^{-1}$  for 1-propanol, and  $K_B^* = 40.8 \text{ kJ mol}^{-1}$  and  $h_B = -23.2 \text{ kJ mol}^{-1}$  for 1-hexanol; ---, Nitta-Chao model.

### TABLE 4

Predicted results of ternary excess molar enthalpies at 25°C



<sup>a</sup> **I**, association constants were taken from Brandani [18], and  $h<sub>A</sub> = 23.2$  kJ mol<sup>-1</sup> was used for all alcohols [19]; II, association parameters were taken from Nagata [5].

<sup>b</sup> AAD, absolute arithmetic mean deviation; ARD, absolute relative deviation.



Fig. 7. Comparison between experimental and calculated excess enthalpies at 25°C of the pseudo-binary. Experimental data of López et al. [16]:  $\bullet$ ,  $(x_1 + x_2)(0.2495$  1propanol + 0.7505 3-pentanone) +  $x_3$ 1-heptanol;  $\blacksquare$ ,  $(x_1 + x_2)(0.5000$  1-propanol + 0.5000 3-pentanone) +  $x_3$ 1-heptanol;  $\blacktriangle$ ,  $(x_1 + x_2)(0.7505$  1-propanol + 0.2495 3-pentanone) +  $x_3$ 1-heptanol. Calculated:  $\frac{1}{\sqrt{2}}$ , UNIQUAC associated-solution model using  $K_A^* = 87.0$  (50°C) and  $h_A = -23.2 \text{ kJ mol}^{-1}$  for 1-propanol, and  $K_B^* = 40.7 \text{ kJ mol}^{-1}$  and  $h_B = -23.2 \text{ kJ mol}^{-1}$ for 1-heptanol; ---, Nitta-Chao model.

We may conclude that the UNIQUAC associated-solution model is better than the **ERAS, NRTL** and Nitta-Chao models in predicting ternary  $H^E$  values for the three systems studied here.

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