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# **INTERACTION OF CYCLOPENTANE WITH BENZENE,**  CARBON TETRACHLORIDE AND CYCLOHEXANE

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#### **ABSTRACT**

Heats of mixing cyclopentane + benzene, + carbon tetrachloride, + cyclo**hexane** at 308-15 K and for cyclohexane + carbon tetrachloride at 298.15 K have been determined in an adiabatic calorimeter. The data have been examined for current theories **(hlcGlasfian,** Flory and Barker) of solutions and show that McGlashan's theory predicts values for  $H^E$  and  $G^E$  that are in good agreement with their corresponding experimental values. Interaction energy between the components of these mixtures has also been determined.

## **INTRODUCTION**

Cyclopentane forms interesting binary systems with benzene, carbon tetrachloride and cydohexane as these involve cnIy a minimum number of interaction pairs. There is thus adequate scope **for a systematic theoretical interpretation** of **excess data in terms of the contemporary theories of solutions. The present work reports heats of mixing for these systems and examines the data** in terms of these theories.

#### EXPERIMENTAL

Benzene, carbon teirachloride and cyclohexane were purified and their purity was checked as reported earlier<sup>1</sup>. Cyclopentane (Fluka) was distilled a number of times and a constant boiling fraction (b.p. 48.9°C at 750 Torr) was used for our present study. The purity of this sampIe **was checked by measuring its density at 298.15 K** which agreed to within 0.00005 g cm<sup> $-1$ </sup> with those in the literature<sup>2</sup>. Heats **of mixing measurements were made in an adiabatic calorimeter described earIier3.** 

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#### **RESULTS**

Heats of mixing values for various systems are recorded in Table 1. The results were fitted to the expression

$$
H^{\mathsf{E}}/\mathsf{x}_1(1-\mathsf{x}_1) \mathbf{J} \,\mathrm{mol}^{-1} = h_0 + h_1(2\mathsf{x}_1 - 1) + h_2(2\mathsf{x}_1 - 1)^2 \tag{1}
$$

where  $x_1$  is the mole fraction of component 1. The constants  $h_0$ ,  $h_1$  and  $h_2$  were evaluated by fitting  $H^E/x_1(1-x_1)$  to eqn (1) by the method of least squares. They are recorded in Table 2 together with the standard deviations  $\sigma(H^E)$ .

#### TABLE 1

### MEASURED HEATS OF MIXING,  $H^E$  AND COMPARISON OF VALUES CALCULATED ACCORDING TO VARIOUS THEORIES WITH VALUES INTERPOLATED FROM THE MEASURED VALUES AT MOLE FRACTIONS x<sub>1</sub> OF COMPONENT 1



# TABLE 1 (continued)



#### TABLE 2

**PARAMETERS OF EON (1) TOGETHER WITH THE STANDARD DEVIATIONS**  $\sigma(H^E)$ **AXD INTERACTION ENERGY u** 

System	ho	$\bm{h}_1$	h,	$\sigma H^{E}(J\, mol^{-1})$	$\mu(J$ mol <sup>-1</sup> )
$Cyclopentanc(1) + benzenc(2)$	2390.38	151.62	349.82	5.30	104.70
$Cyclopentane(1) + carbon$ tetrachloride(2)	296.40	$-29.81$	$-2.45$	1.00	12.55
$Cyclopentane(1) + cyclohexane(2)$ 131.98		22.30	$-66.125$	1.24	6.28
$Cyclohexane(1) + ccrbon$ tetrachloride(2)	660.02	45.21	$-35.40$	3.30	28.03

# **DISCUSSION**

# *Comparison with earlier results*

 $H<sup>E</sup>$  values for carbon tetrachloride + cyclohexane at 298.15 K and + cyclopentane at 308.15 K are in excellent agreement (within  $1 \text{ J mol}^{-1}$ ) with those of Ewing and Marsh<sup>4</sup>. However, our  $H^E$  values at 308.15 K for cyclopentane + cyclohexane are consistently more positive than those of Ewing and Marsh<sup>4</sup>, the deviation being 14 J mol<sup>-1</sup> for an equimolar composition. We are unaware of any  $H^E$  data at  $308.15$  K with which to compare our results for cyclopentane  $+$  benzene; however, they are comparable to the  $H^E$  values<sup>5</sup> at 298.15 K.

# Comparison with theory

We now examine our results for the corresponding state theory of McGlashan<sup>6</sup>. Following Marsh et al.<sup>7</sup> we calculated  $H^E$  using the one fluid approximation and van der Waals combining rules together with the van der Waals equation of state, from the relations

$$
H^{E} = -\langle a \rangle / \langle v \rangle + x_1 a_1 / v_1 + x_2 a_2 v_2^{-1}
$$
 (2)

$$
V_{i} = (a_{i}/2RT)\left[1 - \left\{1 - 4b_{i}RT/a_{i}\right\}^{1/2}\right]
$$
\n(3)

where  $a_i$  and  $b_i$  are the usual van der Waals constants and  $x_1$  is the mole fraction of component 1. The averaged quantities were evaluated from the following expression:

$$
\langle a \rangle = a_1 x_1^2 + 2a_{12} x_1 x_2 + a_2 x_2^2 \tag{4}
$$

$$
\langle b \rangle = b_1 x_1^2 + 2 b_{12} x_1 x_2 + b_2 x_2^2 \tag{5}
$$

where  $a_{12} = \xi (a_1 a_2)^{1/2} (b_1^2 / b_1 b_2)^{1/2}$  (6)

$$
b_{12} = (b_1^{1/3} + b_2^{1/3})/8 \tag{7}
$$

and  $\xi$  is a number close to unity. In principle  $\xi$  can be obtained from second virial

coefficient data but the practice in all the theories has been to devise an experimental excess function like  $H^E$  or  $G^E$  which agrees with the calculated value at one specified composition and then to calculate the other function. As  $G<sup>E</sup>$  data are available for benzene  $+$  cyclopentane and carbon tetrachloride  $+$  cyclohexane mixtures only, we evaluated  $\xi$  from a forced fit of  $H_{\kappa,n}^E$  for an equimolar composition and then calculated  $^7$ the corresponding  $G<sup>E</sup>$  values. The calculated  $G<sup>E</sup>$  values are recorded in Table 3 and considering the simplified nature of this theory, they are in satisfactory agreement with their corresponding experimental values<sup>8,9</sup>.  $H^E$  values were then recalculated at  $x_1 = 0.3, 0.4, 0.6$  and 0.7 for all the mixtures and these values (Table 1) are in good agreement with their corresponding experimental values. The van der Waal's constants were evaluated from critical data<sup>10</sup>.

### **TABLE 3**

**COMPARISON OF CALCULATED AND EXPERIMENTAL GE VALUES** 



At the time this paper was drafted, the authors' attention was drawn to a recent publication<sup> $11$ </sup> which incorporates the contributions of the difference in intermolecular energy  $\theta$ , in size  $\phi$ , and deviations from Berthelot's rule to this theory and expresses  $H<sup>E</sup>$  by the expression<sup>11</sup>

$$
H^{E}/x_{1}(1-x_{1}) = [2(1-\xi)(1+\theta/2)+\theta^{2}/4-\theta\phi/2][-u+TC_{p}]
$$
  

$$
\approx [2(1-\xi)-\theta\phi/2][-u+TC_{p}]
$$
 (8)

where  $u$  and  $C_p$  are the configurational energy and heat capacity of component 1 taken as reference. For a liquid foliowing the van der Waals equation of state

$$
-u + TC_p = (a/V)(2 - V/b)^{-1} \approx a/V
$$
 (9)

and the energy and size difference parameters  $\theta$  and  $\phi$  are given by

$$
1+\theta = T_{c,2}/T_{c,1} \tag{10}
$$

$$
1 + \phi = V_{c,2}/V_{c,1} \tag{11}
$$

In examining our data in terms of expression (8) we calculated  $\zeta$  from  $H_{\text{exp}}^{\text{E}}$  and calculated the corresponding  $G^E$  values for benzene + cyclopentane and carbon tetrachloride  $\div$  cyclohexane mixtures. The data indicate that  $G^E$  values thus calculated do not improve those evaluated from McGlashan's original theory, although the predicted  $H^E$  values at  $x_1 = 0.3, 0.4, 0.6$  and 0.7 are comparable to values calculated from expression (2).

It would now be instructive to consider our results for Flory's theory<sup>12</sup>. Flory supposes that a molecule in a liquid is **made up of segments each havirg a "hard**core" volume  $\mathbf{r}^*$  but occupying an effective volume  $\mathbf{r}$  in the liquid so that the reduced volume  $\bar{v}_i = v_i/r_i^*$  for a pure substance i can be calculated from its expansivity  $\alpha_i$ **according to the relation"** 

$$
\tilde{v}_i = [1 + \alpha_i T/3 (1 + \alpha_i T)]^3 \qquad (i = 1, 2)
$$
\n(12)

Heats of mixing,  $H^E$  were then calculated from Flory's formula<sup>11</sup>

$$
H^{\mathsf{E}} = \mathbf{x}_1 P_1^* V_1 \tilde{v}_1^{-1} (\tilde{v}_1^{-1} - \tilde{v}_{\text{calc.}}^{-1}) + \mathbf{x}_2 P_2^* V_2 \tilde{v}_2^{-1} (\tilde{v}_2^{-1} - \tilde{v}_{\text{calc.}}^{-1}) + + \mathbf{x}_1 V_1 \tilde{v}_1^{-1} \theta_2 \chi_{12} \tilde{v}_{\text{calc.}}^{-1}
$$
 (13)

**where** 

$$
\begin{split} \bar{v}_{\text{calc}} &= (\phi_1 \bar{v}_1 + \phi_2 \bar{v}_2) + (\phi_1 \bar{v}_1 + \phi_2 \bar{v}_2)^{7/3} \left[ \frac{4}{3} - (\phi_1 \bar{v}_1 + \phi_2 \bar{v}_2) \right]^{-1} \times \\ &\times \left[ (\phi_1 P_1^* \bar{T}_1^0 + \phi_2 P_2^* \bar{T}_2^0) \left( \phi_1 P_1^* + \phi_2 P_2^* \right)^{-1} \left\{ 1 - \phi_1 \theta_2 \chi_{12} (\phi_1 P_1^* + \phi_2 P_2^*)^{-1} \right\} - \\ &\quad - \left\{ (\phi_1 \bar{v}_1 + \phi_2 \bar{v}_2)^{1/3} - 1 \right\} \left( \phi_1 \bar{v}_1 + \phi_2 \bar{v}_2 \right)^{-4/3} \right] \end{split} \tag{14}
$$

The various terms have their usual significance<sup>12</sup> and were calculated as described earlier<sup>1</sup>. Evaluation of  $H^E$  by this theory requires a knowledge of  $\theta_2 \chi_{12}$  which was obtained by fitting  $H_{\text{ern}}^{\text{E}}$  to expression 13 for an equimolar mixture. This value of  $\theta_{2} \chi_{12}$ was next used to calculate the corresponding  $G^E$  value for benzene + cyclopentane and carbon tetrachloride + cyclohexane mixtures. These calculated  $G<sup>E</sup>$  values do agree equally well with their corresponding experimental values as the ones calculated from McGIashan's original theory. The theory nevertheless gives a good reproduction of  $H^E$  values for all the mixtures at  $x_1 = 0.3, 0.4, 0.6$  and 0.7. However, any satisfactory theory of solutions of non-electrolytes should be in a position to predict reasonably well the values of  $H^E$ ,  $G^E$  and  $V^E$  and the present study on simple mixtures gives credit to McGIashan's theory.

In an alternate attempt to understand the nature of interaction between the components of these mixtures, we examined our results for Barker's theory<sup>13</sup>. This generalized lattice mode1 theory allows a molecule to have contact points of several types; each type having a definite interaction energy. The total number of contacts, which a molecule occupying  $r<sub>A</sub>$  sites on a Z-coordinated lattice, is capable of making, is given by

$$
q_A Z = r_A Z - 2r_A + 2 \tag{15}
$$

**As** the components of these binary mixtures are aI1 non-polar, the theory prescribed that they have only one type of contact point. The heats of mixing values were then calculated from the relation

$$
H^{\text{E}} = -4RTX_{\text{S}}X_{\text{A}}\eta_1 \ln \eta_1 \tag{16}
$$

where  $X_A$  and  $X_S$  can be solved from:

$$
X_A[X_A \eta_{A-A} + X_S \eta_{A-S}] = q_A Z x_A/2
$$
  
\n
$$
\eta_1 = \eta_{A-S} = e^{-u_1/kT}
$$
\n(17)

$$
X_{s}[X_{A}\eta_{A-S}+X_{S}\eta_{S-S}] = q_{s}Z x_{s}/2
$$
\n(18)

A value of  $Z = 4$ ,  $r_A = 2$  for cyclopentane, and  $r_S = 2$  for carbon tetrachloride, benzene and cyclohexane used throughout. It is further supposed that interaction between molecules of the same type have zero interaction energy so that  $\eta_{A-A} = \eta_{S-A} = e^{-u=0/kT}$  $= 1$ .  $H<sup>E</sup>$  values calculated in this manner for the various systems are recorded in Table 1 and they reproduce well the experimental curves of  $H<sup>E</sup>$  fcr all the systems. The interaction energy of cyclopentane with benzene, carbon tetrachloride and cyclo**hexane are recorded in Table 2, these are also repulsive in character and vary in the order benzene, carbon tetrachloride > cyclohexane.** 

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