

Note

NON-ISOTHERMAL KINETICS WITH NON-LINEAR TEMPERATURE PROGRAMME. PART III

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Being required by a mathematical treatment closer to reality, non-linear temperature programmes are more and more used [1–3]. They have been established not only to minimize the deviation of the sample temperature from the programmed temperature [3], but also to solve exactly the temperature integral. This paper aims to establish a general equation from which a particular non-linear temperature programme, able to solve exactly the temperature integral, can be derived.

If the required experimental conditions are met, the rate equation of heterogeneous reaction is supposed to be [4]

$$\frac{d\alpha}{dt} = f(\alpha) g(T) \quad (1)$$

where α is the degree of conversion, t is time and T is the temperature (K). $f(\alpha)$ in the simplest form can be taken as

$$f(\alpha) = (1-\alpha)^n \quad (2)$$

n being the reaction order.

The function $g(T)$ is considered to follow the Arrhenius relationship

$$g(T) = A \exp(-E/RT) \quad (3)$$

where A is the pre-exponential factor ($dA/dT = 0$, as is general admitted), E is the activation energy, and $R = 1.987 \text{ cal mole}^{-1} \text{ K}^{-1}$.

Using, also, the reciprocal heating rate

$$L(T) = \frac{1}{\beta} = \frac{dt}{dT} \quad (4)$$

and introducing eqns. (2)–(4) into eqn. (1) gives

$$\frac{d}{(1-\alpha)^n} = AL(T) \exp(-E/RT) \quad (1a)$$

which on integration leads to

$$A \int_{T_0}^T L(T) \exp(-E/RT) dT = \begin{cases} \frac{1 - (1-\alpha)^{1-n}}{1-n} & \text{for } n \neq 1 \\ -\ln(1-\alpha) & \text{for } n = 1 \end{cases} \quad (1b)$$

Problems arise with the left-hand side of this equation, i.e. the temperature integral

$$F(T) = A \int_{T_0}^T L(T) \exp(-E/RT) dT \quad (5)$$

due to the unknown form of $L(T)$.

The simplest case is to presume $L(T) = a_0$, which means a linear heating programme, but then $F(T)$ will be expressed by an asymptotic series [5] and the result will always be approximate [5,6]. This is one of the reasons for the search for non-linear programmes.

The second reason is that, during an experiment, some endothermic and/or exothermic effects of the studied reaction cause deviation from linearity of the $T(t)$ graph, and the mathematical model has to represent them. We discuss here two of the ways to obtain $F(T)$.

(a) Assuming temperature programmes of the general form [7]

$$L(T) = \frac{1}{T^2} \sum_i b_i T^i \quad (6)$$

The problem, in this form, was studied by Smutek for thermal desorption. From eqn. (6) he gets, by integration

$$\Delta t = b_1 \ln \frac{T}{T_0} + \sum_{i \neq 1}^z \frac{b_i}{i-1} \Delta T^{i-1} \quad (7)$$

where $\Delta t = t - t_0$ and $\Delta T^k = T^k - T_0^k$ and also obtains $F(T)$ for the general heating regime

$$F(T) = \frac{A}{T} \sum_i^z b_i T^i \left[E_{i(x)} - \left(\frac{T_0}{T} \right)^{i-1} E_{i(x_0)} \right] \quad (8)$$

where

$$E_{i(x)} = \int_1^\infty t^{-i} e^{-xt} dt \quad \text{and} \quad x = E/RT.$$

For positive integer values of i and large values of x , $E_{i(x)}$ becomes

$$E_{0(x)} = \frac{e^{-x}}{x}$$

which allows us to write the exact solution of $F(T)$ in the form

$$F(T) = A \frac{R}{E} \sum_i^z b_i T^{i-1} \exp(-E/RT) \quad (9)$$

(b) By generalization of a method earlier described by Marcu and Segal [2]

$$F(T) = A \sum_i^z a_i T^i \exp(-E/RT) \quad (10)$$

This method selects from the beginning the solutions which fulfil the

condition of solving exactly eqn. (5).

Noting

$$l(T) = \sum_i^z a_i T^i \quad (11)$$

$$F(T) = \int_{T_0}^T L(T) \exp(-E/RT) dT = Al(T) \exp(-E/RT)$$

which, by derivation and substituting eqn. (4) for $L(T)$ leads to

$$dt = \left(l' + \frac{E}{RT^2} l \right) dT \quad (12)$$

The integration of eqn. (12) using eqn. (11) give us the heating programmes as follows.

$$\Delta t = a_1 \left(\Delta T + \frac{E}{R} \ln \frac{T}{T_0} \right) + \sum_{i \neq 1}^z a_i \Delta T^{i-1} \left(\frac{E}{R} \cdot \frac{1}{i-1} + \Delta T \right) \quad (13)$$

Comparing eqn. (7) with eqn. (13), it is obvious that for small ΔT and $a_i(E/R) = b_i$ the two equations give the same solution.

With these results eqn. (1b) becomes

$$A \sum_i^z a_i T^i \exp(-E/RT) = \begin{cases} \frac{1 - (1 - \alpha)^{1-n}}{1 - n} & \text{for } n \neq 1 \\ -\ln(1 - \alpha) & \text{for } n = 1 \end{cases} \quad (1c)$$

which allows kinetic parameters to be determined.

Using equation (1c) for $z = 1$, the kinetic parameters of $\text{Ca}(\text{COO})_2 \cdot \text{H}_2\text{O}$ dehydration were determined. The results ($n = 0.95$; $E = 24.5 \text{ kcal mole}^{-1}$; $A = 10^6 \text{ sec}^{-1}$) are in good agreement with those found in the literature [1].

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