

## APPLICATION OF THE FLORY THEORY OF LIQUID MIXTURES TO EXCESS VOLUMES AND ENTHALPIES OF BENZENE + CYCLOALKANE AND + *n*-ALKANE MIXTURES

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### ABSTRACT

The molar excess volumes of benzene + *n*-pentane, + *n*-dodecane and + *n*-hexadecane and the molar excess enthalpies of benzene + cycloheptane, + cyclooctane and + cyclodecane have been measured over the whole composition range at 25°C. These results, together with literature values, have been analysed using the Flory theory of liquid mixtures.

### INTRODUCTION

The Flory theory of liquid mixtures has previously been fitted by Benson and Singh [1] to the molar excess volumes and enthalpies of benzene + cycloalkane (cyclopentane, cyclohexane, cycloheptane and cyclooctane) mixtures. In this work, these calculations are repeated using improved experimental results together with literature values [2–4] and the work is extended to include calculations on benzene + cyclodecane using new data. The work is further extended to include calculations on benzene + *n*-alkane (*n*-pentane, *n*-hexane, *n*-heptane, *n*-octane, *n*-dodecane and *n*-hexadecane) mixtures using new results reported here together with reliable literature values [5–8].

### EXPERIMENTAL

The benzene (BDH, Analar grade) was fractionally crystallised four times, dried over sodium and stored. The purity, as judged by GLC was better than 99.9 mol%. The *n*-pentane (Riedel de Haën, A.G., spectral grade) and cycloheptane (Aldrich Chemical Co., Gold label 99 + % grade) was fractionally distilled and dried over sodium. The *n*-dodecane, *n*-hexadecane and cyclooctane (all from Aldrich Chemical Co., Gold label 99 + % grade) were fractionally crystallised and also dried under sodium. The cyclodecane (Fluka, purum grade) was used without further purification. Analysis of

TABLE I

Molar excess volume,  $V_m^E$ , for  $x C_6H_6 + (1-x) C_5H_{12}$  and the deviations  $\delta V_m^E$  calculated from eqn. (1) and Table 3 at 25°C

$x$	$V_m^E$ ( $cm^3 mol^{-1}$ )	$10^{-4} \delta V_m^E$ ( $cm^3 mol^{-1}$ )	$x$	$V_m^E$ ( $cm^3 mol^{-1}$ )	$10^{-4} \delta V_m^E$ ( $cm^3 mol^{-1}$ )	$x$	$V_m^E$ ( $cm^3 mol^{-1}$ )	$10^{-4} \delta V_m^E$ ( $cm^3 mol^{-1}$ )
$n-C_5H_{12}$								
0.0786	0.0297	0.7	0.4072	0.1128	9.4	0.6801	0.1018	23.3
0.1206	0.0452	6.7	0.4831	0.1153	-11.5	0.6934	0.0984	15.2
0.1983	0.0685	-9.3	0.5217	0.1149	-15.0	0.7715	0.0773	-11.0
0.2548	0.0848	-0.1	0.5952	0.1124	5.8	0.8987	0.0378	-3.2
0.3115	0.0964	-10.9						
$n-C_{12}H_{26}$								
0.0755	0.1917	-12.2	0.4911	0.9142	16.3	0.6586	0.9527	-5.5
0.1272	0.3156	-10.5	0.5374	0.9456	37.5	0.7419	0.8893	-7.5
0.2179	0.5150	-39.1	0.5503	0.9485	7.3	0.8275	0.7332	-51.9
0.3984	0.6707	-5.5	0.5947	0.9602	1.0	0.8992	0.5197	23.6
0.3920	0.8135	22.1						
$n-C_{16}H_{34}$								
0.1481	0.3812	-13.9	0.4981	1.0194	-23.7	0.6971	1.0802	-32.2
0.2205	0.5643	52.9	0.5507	1.0692	40.8	0.7849	0.9823	-35.1
0.2854	0.6974	-25.9	0.6176	1.0988	37.9	0.8783	0.7266	-2.4
0.3587	0.8352	-8.1	0.6496	1.1025	51.1	0.9248	0.5137	6.0
0.4224	0.9283	-47.5						

TABLE 2  
 Molar excess enthalpy  $H_m^E$  for  $x C_8H_6 + (1-x) C_7H_8$ , and the deviations  $\delta H_m^E$  calculated from eqn. (2) and Table 4 at 25°C

$x$	$H_m^E$ (J mol <sup>-1</sup> )	$\delta H_m^E$ (J mol <sup>-1</sup> )	$x$	$H^E$ (J mol <sup>-1</sup> )	$\delta H_m^E$ (J mol <sup>-1</sup> )	$x$	$H_m^E$ (J mol <sup>-1</sup> )	$\delta H_m^E$ (J mol <sup>-1</sup> )
<i>Cyclo-C<sub>7</sub>H<sub>8</sub></i>								
0.1727	431.6	-1.7	0.4829	801.1	3.4	0.6956	721.7	-6.2
0.2385	552.6	-1.0	0.5458	807.0	0.0	0.8072	559.9	-1.6
0.3156	666.1	1.0	0.5828	800.6	0.6	0.9105	310.7	-1.7
0.4017	759.2	6.9	0.6015	793.2	-1.8			
<i>Cyclo-C<sub>8</sub>H<sub>6</sub></i>								
0.1430	368.4	-5.1	0.4810	805.7	4.2	0.7137	718.4	-4.2
0.2156	517.6	1.5	0.5132	813.9	3.1	0.8262	536.1	-3.3
0.2748	616.7	5.4	0.5503	812.2	-1.8	0.9180	294.2	-4.3
0.3433	704.7	5.8	0.6346	785.2	-4.6	0.9455	212.1	4.2
0.4464	784.1	-1.0						
<i>Cyclo-C<sub>10</sub>H<sub>20</sub></i>								
0.0924	252.1	-3.5	0.4556	801.5	3.3	0.7058	736.7	-6.3
0.1851	461.4	1.4	0.5436	827.4	3.1	0.7680	654.9	-4.0
0.3526	586.3	6.6	0.5893	814.7	-4.8	0.8602	453.4	-2.9
0.3687	733.8	3.1	0.6506	785.4	-6.1	0.9178	307.7	3.0
0.3805	746.4	4.2						

TABLE 3

Smoothing coefficients for  $x \text{C}_6\text{H}_6 + (1-x) \text{C}_y\text{H}_{2y+2}$  at  $25^\circ\text{C}$  determined from the results of Table 1

<i>n</i> -Alkane	$A_0$ ( $\text{cm}^3 \text{mol}^{-1}$ )	$A_1$ ( $\text{cm}^3 \text{mol}^{-1}$ )	$A_2$ ( $\text{cm}^3 \text{mol}^{-1}$ )	$A_3$ ( $\text{cm}^3 \text{mol}^{-1}$ )
<i>n</i> -C <sub>5</sub> H <sub>12</sub>	0.4665	-0.0023	-0.0780	0.0
<i>n</i> -C <sub>12</sub> H <sub>26</sub>	3.6766	-1.4268	0.8984	-0.6273
<i>n</i> -C <sub>16</sub> H <sub>34</sub>	4.0944	-1.9251	1.3578	-1.0891

these compounds by GLC showed purity levels ranging between 99.6 (for *n*-hexadecane and cyclodecane) and 99.9 mol%.

The  $V_m^E$  measurements were done using a Paar (DMA 601) vibrating tube densitometer. The method has been described elsewhere [9]. The  $H_m^E$  measurements were done using an LKB 2107 microcalorimeter. The method has also been described elsewhere [10].

## RESULTS

Excess molar volumes at 298.15 K are reported for systems for which such data is not available in the literature (e.g., benzene + *n*-pentane) and also where the results differ significantly from the literature (e.g., benzene + *n*-dodecane and + *n*-hexadecane). Excess molar enthalpies are also given on mixtures for which data is not available (e.g., benzene + cyclodecane) and on mixtures where the results differ significantly from the literature (e.g., benzene + cycloheptane and + cyclooctane). The  $V_m^E$  and  $H_m^E$  results are given in Tables 1 and 2, together with the deviations,  $\delta V_m^E$  and  $\delta H_m^E$ , calculated from the following smoothing equations

$$\delta V_m^E / (\text{cm}^3 \text{mol}^{-1}) = V_m^E / (\text{cm}^3 \text{mol}^{-1}) - x(1-x) \sum_{r=0}^r A_r (1-2x)^r \quad (1)$$

and

$$\delta H_m^E / (\text{J mol}^{-1}) = H_m^E / (\text{J mol}^{-1}) - x(1-x) \sum_{r=0}^r B_r (1-2x)^r \quad (2)$$

TABLE 4

Smoothing coefficients for  $x \text{C}_6\text{H}_6 + (1-x) \text{C}_y\text{H}_{2y}$  at  $25^\circ\text{C}$  determined from the results of Table 2

Cycloalkane	$B_0$ ( $\text{J mol}^{-1}$ )	$B_1$ ( $\text{J mol}^{-1}$ )	$B_2$ ( $\text{J mol}^{-1}$ )
Cyclo-C <sub>7</sub> H <sub>14</sub>	3210.1	-465.1	297.3
Cyclo-C <sub>8</sub> H <sub>16</sub>	3230.7	-543.3	401.8
Cyclo-C <sub>10</sub> H <sub>20</sub>	3267.8	-593.0	391.9

where  $x$  denotes the mole fraction. The coefficients  $A_i$  and  $B_i$  are given in Tables 3 and 4.

The  $H_m^E$  and  $V_m^E$  results together with literature data [2–8] have been fitted to the Flory theory of liquid mixtures as previously reported [10]. The properties of the pure liquids used in the calculations are given in Table 5 together with literature references to the properties. In a few cases the properties have been obtained by extrapolation. The results of Flory calculations, performed as previously [10], are given in Table 6. The quantities in this table have been defined previously [10].

## DISCUSSION

No measurements for  $V_m^E$  at 25°C for benzene + *n*-pentane have been reported in the literature. The present results at 25°C are, however, within experimental error of the extrapolated results of Mahl et al. [18] who measured  $V_m^E$  for this system at 15 and 20°C.

Díaz Peña and Nuñez Delgado measured  $V_m^E$  for benzene + dodecane and + hexadecane at 25°C [19]; the results reported here are significantly different to these. No other workers have reported measurements at 25°C on these two systems.  $V_m^E$  was also measured for benzene + *n*-hexane, + *n*-heptane, + *n*-octane, + cyclopentane, + cyclohexane, + cycloheptane, + cyclooctane and + cyclodecane. The results in all cases are within the experimental errors of the data available in the literature [2,7] and have not, therefore, been reported here.

The only reported measurements of  $H_m^E$  on benzene + cycloheptane are

TABLE 5

Properties of the pure liquids at 25°C used in the Flory theory (the estimated values were extrapolated from the data of the relevant homologue series)

Hydrocarbon	$\rho$ (g cm <sup>-3</sup> )	Ref.	$10^3\alpha$ (K <sup>-1</sup> )	Ref.	$10^{12}k$ (Pa <sup>-1</sup> )	Ref.
C <sub>6</sub> H <sub>6</sub>	0.8736	11	1.260	12	966	13
C <sub>5</sub> H <sub>10</sub>	0.7404	11	1.347	14	1331	14
C <sub>6</sub> H <sub>12</sub>	0.7739	11	1.217	15	1136	16
C <sub>7</sub> H <sub>14</sub>	0.8073	11	1.00	17	967	17
C <sub>8</sub> H <sub>16</sub>	0.8315	11	0.979	14	803	14
C <sub>10</sub> H <sub>20</sub>	0.8550	This work	0.740	This work	530	(Estimate)
C <sub>5</sub> H <sub>12</sub>	0.6212	11	1.643	(Estimate)	2120	(Estimate)
C <sub>6</sub> H <sub>14</sub>	0.6548	11	1.375	12	1669	12
C <sub>7</sub> H <sub>16</sub>	0.6795	11	1.245	12	1438	12
C <sub>8</sub> H <sub>18</sub>	0.6985	11	1.150	12	1282	12
C <sub>12</sub> H <sub>26</sub>	0.7452	11	0.970	12	988	12
C <sub>16</sub> H <sub>34</sub>	0.7699	11	0.898	12	857	12

TABLE 6

The results of fitting the Flory theory to mixtures of  $x C_6H_6 + (1-x)$  cyclo- $C_yH_{2y}$  and  $(1-x) n-C_yH_{2y+2}$ 

Hydrocarbon	Ref. to the $V_m^E$ data	Ref. to the $H_m^E$ data	$10^7 \chi_{12}(H_m^E)$ ( $J m^{-3}$ )	$\sigma(H_m^E)$ ( $J mol^{-1}$ )	$\sigma^*(V_m^E)$ ( $cm^3 mol^{-1}$ )	$10^7 \chi_{12}(V_m^E)$ ( $J m^{-3}$ )	$\sigma(V_m^E)$ ( $cm^3 mol^{-1}$ )	$\sigma^*(H_m^E)$ ( $J mol^{-1}$ )
$C_5H_{10}$	2	3	3.294	13.5	0.065	2.727	0.008	95.1
$C_6H_{12}$	2	4	4.155	6.4	0.006	4.118	0.004	7.5
$C_7H_{14}$	2	This work	4.109	8.1	0.167	2.600	0.005	151.1
$C_8H_{16}$	2	This work	4.036	9.6	0.034	3.828	0.027	13.9
$C_{10}H_{20}$	2	This work	4.099	14.0	0.167	5.796	0.062	293.8
$C_5H_{12}$	This work	5	4.471	44.4	0.100	3.862	0.036	223.6
$C_6H_{14}$	7	6	4.427	24.9	0.192	3.117	0.027	241.3
$C_7H_{16}$	7	8	4.495	45.4	0.215	3.000	0.034	230.3
$C_8H_{18}$	7	5	4.496	24.1	0.226	2.887	0.031	214.5
$C_{12}H_{26}$	This work	5	4.811	38.1	0.272	2.833	0.035	227.4
$C_{16}H_{34}$	This work	5	5.339	46.2	0.265	3.379	0.028	223.8

within experimental error of the extrapolated results of Mahl et al. [18]. They used a batch calorimeter which had a small vapour space. The present results for the cycloheptane system in the equimolar regions are of the order of  $50 \text{ J mol}^{-1}$  lower than those of Watson et al. [20]. For the cyclooctane system, the  $H_m^E$  results are consistently lower than those of Watson et al., and in the equimolar region the discrepancy is greater than  $20 \text{ J mol}^{-1}$ . The present  $H_m^E$  results for the benzene + cyclopentane and cyclohexane are within the combined experimental errors of this work and that recorded in the literature [3,4], and have therefore, not been reported here. No measurements on benzene + cyclodecane have been previously reported.

The  $H_m^E$  measurements on benzene + *n*-pentane, + *n*-hexane, + *n*-heptane, + *n*-octane, + *n*-dodecane and + *n*-hexadecane are within the experimental errors of the literature values [5,6,8] and have, therefore, not been reported here. In comparing the results, it is evident that there are errors in sign for the coefficients in table 3 of ref. 5. These have been corrected in a recent compilation of  $H_m^E$  data [21].

The present results of Flory calculations for the benzene + cycloalkane mixtures are very similar to those obtained by Benson and Singh [1] and support the remarkable success of this simple theory in fitting  $V_m^E$  and  $H_m^E$  data for binary systems of differing molecular size and nature. The poor fit for the benzene + cyclodecane system may be due to errors in the prediction of the properties of cyclodecane.

The application of this theory to benzene + *n*-alkane mixtures is also remarkably good although inferior to that obtained for the benzene + cycloalkane mixtures. This is remarkable considering the differences in size, shape and nature of the benzene and *n*-alkane molecules.

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#### REFERENCES

- 1 G.C. Benson and J. Singh, *J. Phys. Chem.*, 72 (1968) 1345.
- 2 J.L. Poveda Vilches, M.C. Alonso, M.A.C. Medina and J. Nuñez Delgado, *Thermochim. Acta*, 59 (1982) 73.
- 3 P.S. Arora, R.C. Phutela and P.D. Singh, *Thermochim. Acta*, 10 (1974) 47.
- 4 R.J. Hill and F.L. Swinton, *J. Chem. Thermodyn.*, 12 (1980) 489.
- 5 M. Diaz Peña and C. Menduiña, *J. Chem. Thermodyn.*, 6 (1974) 387.
- 6 B.D. Smith, O. Muthu and A. Dewan, *J. Phys. Chem. Ref. Data*, 12 (1983) 389.
- 7 K.R. Harris and P.J. Dunlop, *J. Chem. Thermodyn.*, 2 (1970) 813.
- 8 E. Müncsch, *Thermochim. Acta*, 22 (1978) 237.

- 9 T.M. Letcher and B.W.H. Scoones, *J. Chem. Thermodyn.*, 14 (1982) 185.
- 10 W.L. Spiteri and T.M. Letcher, *Thermochim. Acta*, 59 (1982) 73.
- 11 A.P.I., *Selected Values of Properties of Hydrocarbons and Related Compounds*. American Petroleum Institute, Research Project 44, Carnegie Press, Pittsburg, PA, 1967.
- 12 M. Diaz Peña and G. Tardajos, *J. Chem. Thermodyn.*, 10 (1978) 19.
- 13 M. Diaz Peña, G. Tardajos, C. Menduiña and R.L. Arenosa, *J. Chem. Thermodyn.*, 11 (1979) 67.
- 14 M.B. Ewing and K.N. Marsh, *J. Chem. Thermodyn.*, 9 (1977) 371.
- 15 G.C. Benson, A. Murakami, V.T. Lam and J. Sing, *Can. J. Chem.*, 48 (1970) 211.
- 16 E. Alcart, G. Tardajos and M. Diaz Peña, *J. Chem. Eng. Data*, 26 (1981) 22.
- 17 I.A. McLure, J.E. Bennett, A.E.P. Watson and C.G. Benson, *J. Phys. Chem.*, 69 (1965) 2759.
- 18 B.S. Mahl, R.K. Nigam, S.L. Chopra and P.P. Singh, *J. Chem. Thermodyn.*, 3 (1971) 363.
- 19 M. Diaz Peña and J. Nuñez Delgado, *J. An. Quim.*, 70 (1974) 678.
- 20 A.E.P. Watson, I.A. McLure, J.E. Bennett and G.C. Benson, *J. Phys. Chem.*, 69 (1965) 2753.
- 21 J.J. Christensen, R.W. Hanks and R.M. Izatt, *Handbook of Heats of Mixing*, Wiley, New York, 1982, 207 pp.