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# Crystallization kinetics and nucleation parameters of Nylon 6 and poly(ethylene-co-glycidyl methacrylate) blend

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#### Abstract

Blend of Nylon 6 and poly(ethylene-co-glycidyl methacrylate) (PEGMA) were prepared by a twin-screw extruder. Morphology observed with scanning electron microscopies (SEM) show PEGMA is well dispersed in Nylon 6 matrix. Isothermal and nonisothermal crystallization of the blend was investigated by differential scanning calorimeter (DSC) and crystallization kinetics was described by Avrami and Tobin models. Equilibrium melting temperatures were estimated from linear Hoffman–Weeks relationship. All analyses showed that the reaction between PEGMA and Nylon 6 reduced the molecular mobility and reduced the crystallization rate. Expand  $K_g$  and  $U^*$  in the Hoffman–Lauritzen equation by Vyazovkin's method demonstrated that Nylon 6/PEGMA had higher  $K_g$  and  $U^*$  values and provided another supportive evidence to the above interpretation. © 2007 Elsevier B.V. All rights reserved.

Keywords: Nylon 6; Isothermal crystallization; Nonisothermal crystallization Hoffman-Lauritzen; Vyazovkin

# 1. Introduction

Miscibility between components in a polymer blend is a critical factor, which influences properties of the blend [1,2]. Reactive compatibilization is an approach that allows one to compatibilize immiscible blends by generating interfacial agents in situ via a chemical reaction between the constituent components during mixing process. These in situ formed agents tend to stay at the interface, as the reaction between functional groups occurs at the interface, and thus can act as effective compatibilizers between two immiscible polymers.

Nylon 6 is one of the important classes of engineering plastics with excellent solvent resistance and good processibility. However, most polyamides have a number of drawbacks, including

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low heat deflection temperature, poor dimensional stability, and low impact strength.

Poly(ethylene-co-glycidyl methacrylate) (PEGMA) is a copolymer of ethylene and glycidyl methacrylate with epoxy groups. The epoxy groups can react with functional groups of carboxyl, hydroxyl, or amines and PEGMA has been processed as compatibilizer for polar–nonpolar blends such as PBT/polypropylene [7], PET/polyethylene [8–11] and Nylon 6/PP [12]. Rubbery PEGMA has also been extensively used as an impact modifier for engineering plastic because of its good miscibility with the matrix such as poly(butylene terephthalate) (PBT) [3], poly(ethylene terephthalate) (PET) [4], poly(phenylene sulfide) (PPS) [5] and polyamides [6].

The presence of a second component in a blend affects not only the mechanical properties but also crystallization kinetics of the blend. In this article, isothermal and nonisothermal crystallization kinetics of Nylon 6 and PEGMA blend were studied by Avrami [15–17] and Tobin [18–20] mod-

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els. The equilibrium melting temperature  $(T_m^o)$  was calculated by linear Hoffman–Weeks equation [14]. The parameters of Hoffman–Lauritzen equation [13] were estimated by Kishore and Vasanthakumari [21], Lim et al. [22], and Vyazovkin's et al. [23,24] methods.

# 2. Experimental

# 2.1. Materials

Commercial grade Nylon 6 was supplied by BASF (Ultramid<sup>®</sup> B35) which had a number-average molecular weight of 24,000 and relative viscosity of 3.3 (1 g/dl in sulfuric acid). PEGMA was purchased from Sumitomo Chemical Co Ltd. (CG5004) which contained 81 wt% ethylene and 19 wt% glycidyl methacrylate, and had a melting flow index (MFI) of 180 g (2.16 kgf/190 °C, ASTM D1238). All materials were used as received without purification.

# 2.2. Sample preparation

All materials were dried at 323 K in a vacuum oven for 48 h before compounding. Nylon 6 and 20 wt% PEGMA were compounded with a twin-screw extruder (Continent Machinery Company, Model CM-MTE, L/D = 32, D = 40 mm) at 523 K with 300 rpm to make blends of Nylon 6/PEGMA. Twenty percent of PEGMA was chosen to make wide enough difference from neat Nylon 6 to have measurable effects. But, at the same time, not to change the processing condition too much so that a meaning-ful comparison can be made. For comparison, the neat Nylon 6 was also compounded by the extruder and went through similar thermal condition.

#### 2.3. Morphology

Samples were fractured in liquid nitrogen to examine the morphology roughly normal to the extrusion direction with scanning electron microscope (HITACHI, S-3500).

#### 2.4. Characterizations

The differential scanning calorimeter (DSC), PerkinElmer Pyris 1 DSC was calibrated by using indium standard and with a sample weight of 8–10 mg. All operations were executed in a nitrogen atmosphere. Before collecting the data of isothermal crystallization, the samples were heated to 523 K and held in the molten state for 5 min to eliminate the influence of thermal history. The sample melts were then subsequently quenched at a rate of 100 K/min to reach the specific temperatures. After the completion of isothermal crystallization, the samples were heated to 523 K at a rate of 10 °C/min to measure the melting temperatures. Nonisothermal crystallization was carried out by heating the samples to 523 K and held in the molten state for 5 min to eliminate the influence of thermal history. The sample melts were then subsequently cooled to 323 K at a heating rate of 10, 20, 30 and 40 K/min.



15KU 1.00KX 10.0P 6389

Fig. 1. SEM micrograph of Nylon 6/PEGMA blend. (a) Original specimen, (b) etched by toluene.

# 3. Results and discussion

#### 3.1. Morphology

The fractured surface of the Nylon 6/PEGMA blend is shown in Fig. 1. The fine particles of PEGMA are well dispersed in



Fig. 2. IR spectrum of PEGMA and Nylon 6/PEGMA.

Nylon 6 with particle size smaller than 1  $\mu$ m (Fig. 1a). There is no obvious discontinuity at interface and the two phases are difficult to identify with SEM. For further characterization, the surfaces were etched with hot toluene to remove the unreacted PEGMA (Fig. 1b). The reaction at interface between the epoxy group of PEGMA and end group of Nylon 6 is the factor which improves the compatibility between Nylon 6 and PEGMA.

The epoxy groups of PEGMA can react with amine or carboxylic acid end group of Nylon 6 through the following simplified equations [25,26,7]:

![](_page_2_Figure_3.jpeg)

tively. The  $T_{\rm m}^{\rm o}$  value of neat Nylon 6 in the present study is in the ranges (501–512 K) reported in the literature [27–29]. The addition of PEGMA does not seem to alter the  $T_{\rm m}^{\rm o}$  of Nylon 6 significantly.

#### 3.3. Isothermal crystallization kinetics

Fig. 4a shows representative exothermic traces of Nylon 6/PEGMA isothermal crystallized at different temperature. The isothermal fraction of crystallinity,  $X_t^i$ , was calculated as

$$\begin{array}{c} \begin{array}{c} \begin{array}{c} CH_{2}CH_{2} \\ \hline \\ CH_{2}CH_{2} \\ \hline \\ CH_{2}C \\ CH_{2}C \\ \hline CH_{2}C \\ \hline \\ CH_{2}C \\ \hline CH_{2}C \\ \hline \\ CH_{2}C \\ \hline CH_{2}C \\ \hline C$$

The IR peaks at 846, 910, and  $997 \text{ cm}^{-1}$  are characteristic peaks of epoxy groups [7] in PEGMA as shown in Fig. 2. Disappearance of those peaks after melt blending indicates that epoxy ring-opening reactions have occurred, but it was difficult to identify the chemical structures of the reaction products from the spectra. Relative viscosity, measured at a concentration of 1 g/dl in sulfuric acid, also increased from 3.3 (neat Nylon 6) to 3.8 (Nylon 6/PEGMA).

#### 3.2. Equilibrium melting temperature

The equilibrium melting temperature  $(T_{\rm m}^{\rm o})$  of a polymer is defined as the melting temperature of an infinite stack of extended chain crystals, large in directions perpendicular to the chain axis and where the chain ends have established an equilibrium state of pairing. The equilibrium temperature is a true reflection of the microstructure and morphology of a blend, and it is a reference temperature from which the driving force for crystallization is measured [14].

Hoffman–Weeks relation [14] has been widely accepted to estimate equilibrium melting temperature  $(T_m^o)$ , which is determined by extrapolation of  $T_m$  versus  $T_c$  to  $T_m = T_c$  (referred to as linear H–W; LHW):

$$T'_{\rm m} = T^{\rm o}_{\rm m} \left(1 - \frac{1}{\gamma}\right) + \frac{T_{\rm c}}{\gamma} \tag{1}$$

The thickening coefficient  $\gamma = l/l^*$ , where *l* and *l*<sup>\*</sup> are the lamellar thickness at the time of melting and the thickness of the critical nucleus at  $T_c$ , respectively. The results of  $T_m^o$ ,  $\gamma$ , and regression of the linear H–W are shown in Fig. 3. The  $T_m^o$  of neat Nylon 6 and Nylon 6/PEGMA is 501.96 and 502.41 K, respec-

the ratio of the exothermic peak areas at time t and infinite time [17-19]:

$$X_{t}^{i} = \frac{\int_{0}^{t} (\mathrm{d}H_{c}^{i}/\mathrm{d}t) \,\mathrm{d}t}{\int_{0}^{\infty} (\mathrm{d}H_{c}^{i}/\mathrm{d}t) \,\mathrm{d}t}$$
(2)

where  $dH_c^i$  is the enthalpy of crystallization released during an infinitesimal time interval dt. Fig. 4b shows a typical relative crystallinity of Nylon 6/PEGMA. From these curves, the half-time of crystallization  $t_{1/2}^i$  defined as the time required to reach half of the final crystallinity ( $X_t^i = 0.5$ ) can be calculated. In general,  $t_{1/2}^i$  or  $1/t_{1/2}^i$ , is taken as a measure of the overall rate of crystallization of a polymer as shown in Fig. 5. It can be seen

![](_page_2_Figure_17.jpeg)

Fig. 3. Comparisons of linear H–W and nonlinear H–W plots for Nylon 6 and Nylon 6/PEGMA.

![](_page_3_Figure_1.jpeg)

Fig. 4. DSC isothermal measurement. (a) Heat flow, and (b) relative crystallinity as a function of crystallization time and fitted by Avrami models.

that  $1/t_{1/2}^i$  of Nylon 6 decreased when PEGMA was added. Such a decrease in crystallization rate may be accounted for by the increase of the blend viscosity due to reactions between Nylon 6 and PEGMA and the concurrent reduction of the molecular mobility.

![](_page_3_Figure_4.jpeg)

Fig. 5.  $1/t_{1/2}^i$  as a function of isothermal crystallization temperature.

![](_page_3_Figure_6.jpeg)

Fig. 6. Relation of undercooling and isothermal rate constants evaluated from Avrami model.

### 3.3.1. Avrami analysis

The Avrami equation was applied to analyze the isothermal crystallization process of polymers [17–19]:

$$X_t = 1 - \exp(-(K_a t)^{n_a})$$
(3)

where  $X_t$  is the relative crystallinity, t is the crystallization time,  $K_a$  is the Avrami crystallization rate constant and  $n_a$  is the Avrami exponent.  $X_t$  can be calculated as the ratio between the area of the exothermic peak at time t and the total measured area of crystallization. Under isothermal crystallization, crystallization rate constant  $(K_a^i)$  and Avrami exponent  $(n_a^i)$  were found by fitting experimental data of  $X_t^i$  to Eq. (3) and the results are shown in Fig. 6. Reconstruction of Eq. (3) from the calculated  $K_a^i$  and  $n_a^i$  values (Fig. 4b) shows that Avrami model provides a good fitting.

Avrami exponent represents a parameter revealing the nucleation mechanism and growth dimension. The  $n_a^i$  values are around 2.04–2.37 for Nylon 6 and 2.03–2.23 for Nylon 6/PEGMA blend. The  $n_a^i$  values are close to the results (2.1–2.3) reported by literature [30], which is a two-dimensional growth of a spherulite. No significant changes of the values of  $n_a^i$  were found with the addition of PEGMA and thus the addition of PEGMA may not affect the geometric dimension of Nylon 6 crystal growth.

While  $n_a^i$  may be recognized as a constant with crystallization temperatures  $(T_c)$ ,  $K_a^i$  depends strongly on  $T_c$ . The isothermal rate constants,  $K_a^i$ , are also shown in Fig. 6 as a function of  $T_c$  for these two samples. The values  $K_a^i$  increased with decreasing  $T_c$ .

To compare crystallizability of Nylon 6 and Nylon 6/PEGMA blend, the undercooling and crystallization rate constants calculated from Avrami model are shown in Fig. 6. To reach an assigned value of rate constant, the blend needed to be imposed a higher undercooling than Nylon 6; it indicated that the crystallization rate of Nylon 6 is greater than Nylon 6/PEGMA [31]. The overall crystallization rate is governed by nucleation and diffusion [32]. The reaction between Nylon 6 and PEGMA would reduce the molecular mobility and crystallization rate due to an increasing in melt viscosity.

# 3.3.2. Activation energy $(\Delta E_a^i)$ from isothermal crystallization

The crystallization process is assumed to be thermally activated and the crystallization rate constant  $K_a$  can be approximately described as follows:

$$\ln K_{\rm a}^{i} = \ln K_{\rm o} - \frac{\Delta E_{\rm a}^{i}}{RT_{\rm c}} \tag{4}$$

where  $K_0$  is the temperature-dependent pre-exponential factor, R is the gas constant and  $\Delta E_a^i$  is the activation energy for the primary crystallization process which consists of the transport activation energy and the nucleation activation energy [33,34]. The  $\Delta E_a^i$  are estimated from the slopes of linear plots of  $\ln K_a$  against  $1/T_c$  and shown in Fig. 7. The  $\Delta E_a^i$  values are -76.9 and -81.0 kJ/mole for Nylon 6 and Nylon 6/PEGMA, respectively. The apparent activation energy,  $\Delta E_a^i$ , cannot be further proportioned into its transport and nucleation components.

# *3.3.3. Nucleation parameter from isothermal thermal analysis*

The overall crystallization rate should be interpreted by the combination of nucleation and growth phenomena. Hoffman–Lauritzen [13] proposed the following equation:

$$G = G_0 \exp\left[\frac{-U^*}{R(T_c - T_\infty)} - \frac{K_g}{T_c(\Delta T)f}\right]$$
(5)

where *G* is the crystallization rate parameter and *G*<sub>o</sub> is a preexponential term;  $U^* = 1500$  cal/mole is the diffusional activation energy for the transport of crystallizable segments at the liquid–solid interface; *R* is the gas constant;  $T_{\infty} = T_g - 30$  K and  $T_g = 323$  K [33] is the hypothetical temperature below which viscous flow ceases;  $\Delta T = T_m^o - T_c$ ;  $f = 2T_c/(T_m^o + T_c)$  is a correction factor;  $K_g$  is the nucleation parameter which can

![](_page_4_Figure_10.jpeg)

Fig. 7. Activation Energy ( $\Delta E_a^i$ ) from isothermal crystallization.

![](_page_4_Figure_12.jpeg)

Fig. 8. Plot of  $\ln(1/t^i) + (U^*/R(T_c - T_\infty))$  as a function of  $\ln \psi_0 - (K_g/T_c(\Delta T)f)$ .

be related to the product of lateral and folding surface free energy.

The crystallization rate parameter G is considered proportional to  $t_{1/2}^i$ , Eq. (5) is rewritten as:

$$\frac{1}{t^i} = G_0 \exp\left[\frac{-U^*}{R(T_c - T_\infty)} - \frac{K_g}{T_c(\Delta T)f}\right]$$
(6a)

or

$$\ln\left(\frac{1}{t_{1/2}^{i}}\right) + \frac{U^{*}}{R(T_{c} - T_{\infty})} = \ln G_{o} - \frac{K_{g}}{T_{c}(\Delta T)f}$$
(6b)

Fig. 8 demonstrates the plot of Eq. (6b) for Nylon 6 and Nylon 6/PEGMA, and the  $K_g$  values are estimated from the slope and intercept of Fig. 8. The  $K_g$  value ( $1.08 \times 10^5$ ) of neat Nylon 6 is close to the value ( $0.737-1.53 \times 10^5$ ) reported in literatures [29,30].

The nucleation parameter  $(K_g)$  represents the free energy necessary to form a nucleus of critical size. Higher value of  $K_g$  in Nylon 6/PEGMA blend than neat Nylon 6 indicated that the motion of the Nylon 6 chains is more difficult in the blend. The result is consistent with the conclusion provided by the crystallization rate constant.

## 3.4. Nonisothermal crystallization kinetics

Fig. 9a shows representative DSC thermograms of nonisothermal crystallization of Nylon 6/PEGMA at different cooling rates. The exothermic peaks became wider and shifted towards lower temperature with increasing cooling rate. Table 1 lists some characteristic parameters for nonisothermal melt crystallization. For both samples, the onset of crystallization temperature ( $T_{o}$ ) and temperature ( $T_{p}$ ) and end of crystallization temperature ( $T_{\infty}$ ) all shifted towards lower temperature with increasing cooling rate. The onset temperature of crystallization ( $T_{o}$ ) and peak crystallization temperature ( $T_{p}$ ) of Nylon 6 shift to a lower temperature, which indicates the addition of PEGMA retards the crystallization. The reciprocal half-time of

6/PEGMA

![](_page_5_Figure_1.jpeg)

Fig. 9. DSC nonisothermal measurement. (a) Heat flow, and (b) relative crystallinity as a function of crystallization time and fitted by Avrami and Tobin models.

crystallization  $(t_{1/2}^n)$  is also a measure of the overall rate of nonisothermal crystallization. It also indicates the crystallization rate is reduced with the addition of PEGMA.

The relative degree of crystallinity,  $X_T^n$ , of nonisothermal crystallization was calculated as the ratio of the exothermic peak areas [35,36]:

$$X_T^n = \frac{\int_{T_0}^T [\mathrm{d}H_c^n/\mathrm{d}T] \,\mathrm{d}T}{\int_{T_0}^{T_\infty} [\mathrm{d}H_c^n/\mathrm{d}T] \,\mathrm{d}T}$$
(7)

where *T* is an arbitrary temperature,  $dH_c^n$  is the enthalpy of crystallization released during an infinitesimal temperature interval *dT*; the relative crystallinity  $X_T^n$  is a function of temperature

Table 2 Nonisothermal Avrami and Tobin kinetics parameters

30

40

2.86

2.62

				· · · · · · · · · · · · · · · · · · ·					
	10	3.11	0.955	0.990	0.996	4.76	1.104	0.999	
Nylon	20	3.19	1.577	1.023	0.994	4.85	1.816	0.999	
6	30	2.83	2.172	1.026	0.996	4.33	2.583	0.999	
	40	2.68	2.869	1.026	0.995	4.12	3.339	0.999	
	10	2.86	0.865	0.985	0.992	4.34	1.011	0.999	
Nylon	20	3.28	1.408	1.017	0.994	4.96	1.616	0.999	

1.926

2.454

for Nylon 6 and Nylon 6/PEGMA. During the nonisothermal crystallization process, the time, *t*, and temperature exhibit the following relationship:

1.022

1.022

0.992

0.990

4.36

4.03

2.300

2.854

$$t = \left| \frac{T_{\rm o} - T}{\varphi} \right| \tag{8}$$

where  $\varphi$  is the cooling rate. A typical relative crystallinity  $(X_t^n)$  of Nylon 6/PEGMA as a function of time is illustrated in Fig. 9b. The higher the cooling rate results in the shorter the time for completing the crystallization.

#### 3.4.1. Avrami analysis

Avrami equation [15–17] was also employed to describe the primary stage of nonisothermal crystallization. Nonisothermal crystallization rate constant  $(K_a^n)$  and Avrami exponent  $(n_a^n)$  were found by fitting experimental data of  $X_t$  to Eq. (3) and the results are shown in Table 2.

In nonisothermal crystallization  $K_a^n$  and  $n_a^n$  do not have the same physical significance as in the isothermal crystallization because the temperature changes constantly. Assuming constant or approximately constant cooling rate, Jeziorny [37] suggested the modified Avrami to characterize the kinetics of nonisothermal crystallization:

$$\ln K_{\rm J} = \frac{\ln K_{\rm a}}{\varphi} \tag{9}$$

The results obtained from Jeziorny method are listed in Table 2.

Using the values thus obtained, the theoretical Eq. (4) was used and simulation results are compared to experimental data for all cooling rates examined in Fig. 9b. Deviation from the experimental data at high relative crystallinity is generally attributed to spherulite impinging effect.

Table 1

Characteristic data of nonisothermal melt crystallization exotherms for Nylon 6 and Nylon 6/PEGMA

Cooling rate $\varphi$ (K/min)	Nylon 6				Nylon 6/PEGMA			
	<i>T</i> <sub>o</sub> (K)	<i>T</i> <sub>p</sub> (K)	$T_{\infty}$ (K)	$t_{1/2}^{n}$ (min)	<i>T</i> <sub>o</sub> (K)	<i>T</i> <sub>p</sub> (K)	$T_{\infty}$ (K)	$t_{1/2}^{n}$ (min)
10	473.9	466.4	447.2	0.90	471.0	461.0	435.1	0.97
20	470.6	460.6	436.9	0.54	467.2	455.9	429.9	0.61
30	467.5	457.6	426.1	0.38	463.5	452.1	418.2	0.42
40	465.2	454.1	420.2	0.29	461.2	450.3	407.5	0.34

0.999

0.999

![](_page_6_Figure_1.jpeg)

Fig. 10. Dependence of undercooling,  $T_{\rm m}^{\rm o} - T_{1/2}$ , on cooling rate.

#### 3.4.2. Tobin analysis

Tobin [18–20] proposed the following expression to describe phase transformation kinetics with growth site impingement in order to improve the Avrami model which is suitable for the early stages of crystallization.

$$X_t = \frac{(K_t t)^{n_t}}{1 + (K_t t)^{n_t}} \tag{10}$$

where  $K_t$  is the Tobin rate constant, and  $n_t$  is the Tobin exponent. Tobin exponent  $n_t$  is not necessary an integer and is mainly governed by different types of nucleation and growth mechanism. Tobin parameters ( $K_t$  and  $n_t$ ) of Eq. (10) under nonisothermal crystallization can be found by directly fitting the  $X_t^n$  data obtained from each cooling rate to equation and the results are shown in Table 2. The Tobin exponent ( $n_t$ ) was found to increase with cooling rate from 4.03 to 4.96 and it was always higher than the Avrami exponent ( $n_a$ ). The reconstructed relative crystallization as a function of time by adapting Tobin models, as shown in Fig. 9b, demonstrates a better fitting than Avrami model. Both Avrami and Tobin model should only be used to "describe" the nonisothermal crystallization since they are assumed to be under isothermal conditions.

Crystallizability can be compared at the same degree of undercooling. Fig. 10 shows the undercooling needed to reach 50% relative crystallization ( $X_t = 0.5$ ), that is  $T_m^0 - T_{1/2}$ . Higher undercooling would suggest a lower crystallizability and Fig. 10 indicated that the crystallizability of Nylon 6 is higher than the blend [32]. The results suggest that the addition of PEGMA slowed down the kinetics.

### 3.4.3. Effective activation energy

Several methods have been suggested to estimate the effective energy barrier in nonisothermal crystallization [38–40]. However, to ignore the negative sign in cooling process may result in errors [41]. The Friedman equation [42] is applied to nonisothermal crystallization for estimating the dependence of the effective activation energy on conversion and temperature. The Friedman equation can be expressed as follows:

$$\ln\left(\frac{\mathrm{d}X_t^n}{\mathrm{d}t}\right)_{X_t^n} = \mathrm{constant} - \frac{\Delta E_{X_t^n}}{RT_{X^n}} \tag{11}$$

where  $dX_t^n/dt$  is the instantaneous crystallization rate as a function of time for a given value of the relative crystallinity, R is the universal gas constant, and  $\Delta E_{X^n}$  is the effective energy barrier of the process for a given value of  $X_t^n$ . At various cooling rates, the values of  $dX_t^n/dt$  at a specific  $X_t^n$  are correlated to the corresponding crystallization temperature at this  $X_t^n$ , that is,  $T_{X^n}$ , a straight line can be obtained by plotting  $dX_t^n/dt$  versus  $1/T_{X^n}$ and the slope is  $-\Delta E_{X^n}/R$ .

The dependence of the effective activation energy and temperature on conversion based on Friedman equation is shown in Fig. 11. The activation energy increases with the increasing relative crystallinity in both samples, and Nylon 6/PEGMA had higher activation energy than neat Nylon 6. Nonisothermal crystallization becomes more difficult with increasing  $X_t^n$ . It also indicated that PEGMA reduced the crystallization rate.

# *3.4.4. Nucleation parameter from nonisothermal thermal analysis*

Kishore and Vasanthakumari [21] used  $G = dX_t^n/dt$  and rearranged Eq. (5) to get the following equation:

$$\frac{\mathrm{d}X_t^n}{\mathrm{d}t} = \frac{G_{\mathrm{o}}}{\varphi} \exp\left[\frac{-U^*}{R(T-T_{\infty})}\right] \exp\left[\frac{-K_{\mathrm{g}}(T_{\mathrm{m}}^{\mathrm{o}}-T)}{2T^2(T_{\mathrm{m}}^{\mathrm{o}}-T)}\right]$$
(12)

 $T_p$  is the maximum rate which could be obtained by differenating Eq. (12) with respect to *T* and equating it to zero, yielding Eq. (13):

$$K_{\rm g} = \frac{U^* T_{\rm p}^3 (T_{\rm m}^{\rm o} - T_{\rm p})^2}{R(T_{\rm p} T_{\rm m}^{\rm o} - T_{\rm m}^{\rm o2} + T_{\rm p}^2)(T_{\rm p} - T_{\infty})^2}$$
(13)

Fig. 12 shows the dependence of  $K_g$  values on  $T_p$  values resulted from different cooling rate. The  $K_g$  values increases with decreasing  $T_p$ , i.e. increases with increasing cooling rate. The values are much lower than those results obtained from isothermal crystallization and literatures [29,30]. It seems inapplicable in neat Nylon 6 and Nylon 6/PEGMA.

![](_page_6_Figure_20.jpeg)

Fig. 11. Dependence of the effective energy barrier and average temperature on the extent of relative crystallinity  $(X_t^n)$ .

![](_page_7_Figure_1.jpeg)

Fig. 12.  $K_g$  values calculated by Kishore, Lim, and Vyazovkin method.

Lim et al. [22] modified the Lauritzen–Hoffman equation by substituting  $T_c$  with  $(T_o - \varphi t)$  to measure the spherulite growth rate as a function of temperature and cooling rate in nonisothermal crystallization as following equation:

$$\ln G + \frac{U^{*}}{R(T_{o} - \varphi t - T_{\infty})}$$
  
=  $\ln G_{o} - \frac{K_{g}}{(T_{o} - \varphi t)[T_{m}^{o} - (T_{o} - \varphi t)]f}$  (14a)

$$f = \frac{2(T_{\rm o} - \varphi t)}{T_{\rm m}^{\rm o} + (T_{\rm o} - \varphi t)} \tag{14b}$$

*G* is the growth rate and *G* is the inversely proportional to the time to achieve a specific relative degree of crystallinity, i.e.  $G \approx 1/t_{x_t^n}$  [41]. The  $K_g$  could be obtained from the slope with similar method as isothermal crystallization. Fig. 12 shows the  $K_g$  values does not show significantly change with  $X_t^n$ . The  $K_g$  values of neat Nylon 6 are 1.09–1.17 × 10<sup>5</sup> which are close to above result obtained from isothermal crystallization and literatures [29,30].

However, to assume a constant  $U^*$  for both samples does not seem reasonable because the addition of PEGMA would influence the molecular mobility. Vyazovkin et al. [23,24] used the dependence of the effective activation energy on temperature to estimate the parameters ( $K_g$  and  $U^*$ ) of the Lauritzen–Hoffman theory [43] and derived the following equation:

$$\Delta E_{X_t} = -R \frac{(\ln G)}{d(1/T)} = U^* \frac{T^2}{(T - T_\infty)^2} + K_g R \frac{(T_m^o)^2 - T^2 - T_m^o T}{(T_m^o - T)^2 T}$$
(15)

Fig. 12 shows the dependence of the effective activation energy on temperature evaluated by replacing  $X_t$  with an average temperature, according to Vyazovkin's method [42,43]. The values  $K_g$  and  $U^*$  can be estimated by fitting Eq. (15) with the dependence of the effective activation energy on temperature, and the results are shown in Fig. 12. The  $K_g$  values obtained from Eq. (15) are close to above results and literatures [30,31]. The higher  $U^*$  value (7863 J/mole) of Nylon 6/PEGMA than that (7263 J/mole) of neat Nylon 6 also means the addition of PEGMA retards the chain mobility and reduces the crystallization rate.

#### 4. Conclusion

Blend of Nylon 6 and poly(ethylene-co-glycidyl methacrylate) (PEGMA) were prepared by compounding in a twin-screw extruder. The PEGMA was well dispersed in Nylon 6 from SEM morphology. Crystallization of neat Nylon 6 and Nylon 6/PEGMA was described by Avrami and Tobin models. The introduction of PEGMA slowed the kinetics of both isothermal and nonisothermal crystallization of Nylon 6 due to reduction in chain mobility because of the reaction between the epoxy groups in PEGMA and the end groups of Nylon 6 (-NH<sub>2</sub> or -COOH groups). Reduction of Nylon 6 mobility also led to an increase in  $T_{\rm m}^{\rm o}$ . Determination of  $K_{\rm g}$  and  $U^*$  values in the Hoffman-Lauritzen equation by Vyazovkin's method demonstrated that Nylon 6/PEGMA had higher  $K_g$  and  $U^*$  values indicating that the addition of PEGMA reduced the Nylon 6 mobility and decreased the crystallization rate. Vyazovkin's method is a powerful technique to study polymer crystallization and gives supportive evidence consistent with the kinetics data in the present article.

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