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### article info

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#### ABSTRACT

[A calorimetric](http://www.sciencedirect.com/science/journal/00406031) study of the kinetics and thermodynamics of the attack of a phosph region (Tunisia) by phosphoric acid and by a mixture of phosphoric acid and sulfuric at different temperatures. Two samples of the same ore having different grain size 25 °C, the dissolution enthalpy in phosphoric acid solution equals −233.6 ± 2.2 J/g for ples. Attack by the mixture of acids is strongly dependent on the solid granulometr the calorimetric results by Avrami model shows the existence of three domains attril ore dissolution/H<sub>2</sub>PO<sub>4</sub>  $-$  neutralisation, hemihydrate (HH) precipitation and hemihydi transformation. The attack by the acid mixture was performed at higher temperatures a tion the transitional formation of the anhydrous sulfate (AH) at  $T \geq 55$  °C, which transforms into diffusional formation of the anhydrous sulfate (AH) at  $T \geq 55$  °C, which transforms into diffusional forms in the tran after the HH/DH transformation.

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#### **1. Introduction**

Phosphate fertilizers are produced from phosphate ore. Attack of natural phosphate ores by sulfuric and/or phosphoric acid solution is the basic process for producing phosphoric acid and inorganic phosphorus fertilizers, such as superphosphate. In the wet production process, the raw phosphate ore is converted into phosphoric acid and calcium sulfate by adding solutions of sulfuric and phosphoric acid in the reactor [1]. These acids are introduced simultaneously or successively [2]. In the latter case two processes occur which are dissolution of the ore and precipitation of calcium sulfate [3].

Several kinetic and thermodynamic studies have proposed mechanisms for the digestion of phosphates in either phosphoric or sulfuric acid [3–16]. But only Dorozhkin [11] has studied the dissolution of a natural fluorapatite in a mixture of these acids. Recently Abdel-Aal et al. [17] have studied the crystallization of calcium sulfate dihydrate in solutions having different supersaturation ratios and free sulfate concentrations. These authors added various amount of a solution containing calcium dibasic orthophosphate (CaHPO<sub>4</sub>) in phosphoric acid (20%) to sulfuric acid solution.

In a series of works [13-15], we have conducted modynamic studies of the attack of synthetic f  $Ca_{10}(PO_4)_6F_2$ , by a mixture of sulfuric and phosp ferent temperatures. The aim of the present w the kinetics and thermodynamics of the attacl ore (PN) from Gafsa region (Tunisia) by phosphore and by a mixture of phosphoric and sulfuric  $a$ temperatures.

### **2. Experimental**

A SETARAM C-80 calorimeter operating in isothermal used. The reversal cells of the calorimeter have provided with electrical resistors in order to per in the reaction cell, so time constants have been o same conditions as for the chemical process.

Experiments have been carried out by mixing  $(17.07-511.42 \text{ mg})$  of solid with  $4.5 \text{ mL}$  of acid solution. recorded thermograms were integrated to give the enthalpy. For kinetic investigation, the recorded cessed according to the procedure developed in [9–10], to give the deconvoluted curves.

The ore was supplied by the "Groupe Chimique after aqueous enrichment and sifting.

Two samples of the ore have been used. The fi a grain size <500  $\mu$ m, and the second (PN2) is obt.

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dard methods. The results are converted into P2O5 and CaO (Table S2 in Supplementary data). Calcite amount is determined by an increment method which consists in recording the X-ray diffractograms of mixtures of the ore with known amounts of calcite. The intensity of the most intense peak of calcite (2 $\theta$  = 29°) as a function of the  $CaCO<sub>3</sub>$  added is represented by a straight line, and the intercept on the mass axis gives the amount of calcite in the original ore. The result is reported in Table S2 in Supplementary data.

Assuming the apatitic phase is pure Fap, and contains the whole amount of phosphorus, the percentage of Fap in the ore is 55.81. This value leads to the amount of calcium in the apatitic phase. Taking into account the calcite, the total amount of calcium in the ore as CaO is 38.43%, slightly lower than the experimental 39.62% (Table S2 in Supplementary data). The discrepancy results from the existence of small amounts of other phases containing calcium, such as dolomite.

### **3. Thermodynamics of the ore attack by phosphoric acid solution at 25 ◦C**

Fig. S2 in Supplementary data gives the variation of measured enthalpy deduced by integrating the calorimetric signal as a function of PN dissolved masses (PN1 sample). The slope of the straight line gives a global enthalpy:  $\Delta H = -233.6 \pm 2.2$  J/g (PN1). This value corresponds to the total dissolution of the PN in the phosphoric acid solution, since the X-ray diffraction diagram of the residue isolated at the end of the attack, Fig. S3 in Supplementary data, shows only a halo corresponding to silica. Moreover, the attack of the grinded sample PN2 by the same solution leads to the same dissolution enthalpy  $\Delta H = -233.7 \pm 2.0$  J/g. The intercept  $1.0832 \pm 1.0602$  has an interval definition round zero value.

Fap and calcium carbonate are the major components of the mineral ore, so their contribution to the dissolution enthalpy can be calculated. Dissolution enthalpy of synthetic Fap in phosphoric acid solution (20%  $P_2O_5$ ) was measured in previous works [9,12] (−178.6 J/Fap g). We have measured the dissolution enthalpy of  $CaCO<sub>3</sub>$  in the same experimental conditions by dissolving various amounts of calcite (CaCO<sub>3</sub> Normapur, purity >99%) in 4.5 mL of phosphoric acid solution (20%  $P_2O_5$ ). Fig. S4 in Supplementary data shows the variation of measured enthalpy, as a [funct](#page-3-0)ion of calcium carbonate mass. The enthalpy resulting from the slope equals  $-303.6 \pm 3.1$  J/g.

Taking into account the percentage of Fap and calcite, 55.81% and 15.07%, respectively, the calculated enthalpy is  $-145.5 \pm 3.3$  J/PN1 g. It differs widely from the measured −233.6 ± 2.2 J/g. Discrepancy between these values results probably from the presence of silica, organic substances and possible other carbonates in the ore sample.

Similar experiments have been carried out on the PN2 sample and led to an enthalpy of  $-350.3 \pm 2.7$  J/g, which ative than the one obtained with PN1. The tra the mixture of acids seems to be strongly dep granulometry.

Fig. S7 in Supplementary data shows examp thermograms obtained for different masses of I two overlapped peaks having the same shape ously obtained by the attack of synthetic Fap temperatures between 35 and 55 $°C$  [15]. As the X-ray difference  $X$ of the solid isolated after the first peak  $(t = 120$ ence of HH and apatite, we can ascribe, as wit first peak to the PN dissolution and HH precip second one corresponds to the HH into DH transformation. ever, in the case of PN1, the latter transformation achieved and the thermograms did not reach after 8 h.

The transitional formation of hemihydra was not previously observed with pure Fap less soluble in the acid solution resulting f PN (industrial conditions) than in the one thetic Fap  $[13]$ . Fig. S7 in Supplementary  $\alpha$ PN1 mass decreases a better separation bet observed and the second peak starts later. It seems PN1 mass increases, the dihydrate solubility earlier and so the transformation of hemihydrate into an occurs at a shorter time than with smaller ore.

## 4.2. Determination of the enthalpy of the complete **PN** *the [acid](#page-3-0) [m](#page-3-0)ixture at 25* ◦*C*

As with synthetic Fap  $[14]$  $[14]$ , the enthalpy the total attack of the PN by the acid mixture calculated by adding the enthalpy dissolutior ric acid solution, previously determined (−23 precipitation-neutralisation enthalpy. In order  $t$ ter, two experimental series were carried out. The first one consistent in dissolving various amounts of a  $PN/H_3PO_4$ : acid mixture at 25 °C. The  $PN/H_3PO_4$  solution v solving 548.53 mg of PN in  $11.4508$  g of a phos (20%  $P_2O_5$ ). These quantities have been chosen final solution an  $\rm H_2PO_4^-$  concentration in the sa tude as that obtained by dissolving PN in the aci the PN dissolution in phosphoric acid leads to a dispersed colloidal particles, consequently the was energetically shaken before sampling. The (Fig. S8a in Supplementary data) can be express equation:

 $\Delta H_1 = 8 10^{-6}$  m<sup>2</sup> – 0.0298 m + 0.3430

 $\mu$ mount. The plot of this difference  $\mu_{\rm J}$  as a function of the PN mass (mg) in the  $PN/H_3PO_4$  solution, calculated in the latter solution, is represented by a straight line, Fig. S9 in Supplementary data, having 0.144 J/mg as a slope, from which the precipitation-neutralisation enthalpy can be deduced as  $-144.0 \pm 3.3$  J/PN1 g. Adding this quantity to the  $\Delta H$  corresponding to PN dissolution in the phosphoric acid solution  $(-233.6 \pm 2.2$  J/g) leads to  $-377.6 \pm 4.0$  J/PN g. This latter value corresponds to the total PN attack by acid mixture solution leading to DH precipitation. X-ray diffraction pattern, Fig. S10 in Supplementary data, of the isolated solid at the end of these experiments shows only dihydrate and silica. This value differs from the one corresponding to PN2 (350.3  $\pm$  2.7) by about [7%](#page-3-0) [a](#page-3-0)nd is far from that determined for the attack of PN1 ( $-161.5 \pm 1.2$  J/g). The advancement of reaction is significantly dependent on the grain size of the solid particles.

Enthalpies of neutralisation of  $\rm H_2PO_4^-$  and precipitation of DH from Ca<sup>2+</sup> and SO<sub>4</sub><sup>2-</sup> ions were determined, at 55 °C, in a previous work [13] and the values are  $+55.15 \pm 1.30$  and −239.88 ± 2.61 J/Fap g, respectively. Neglecting their variation with temperature, we can calculate the enthalpy of neutralisation/precipitation taking into account the amount of phosphorus and calcium in PN. The value obtained,  $-159.3 \pm 2.9$  J/PN g, differs from the one determined experimentally  $(-144.0 \pm 3.3$  J/g) by 9.5%. The difference is probably due to the above approximation and mainly to the dispersion of the experimental values around the least square line, Fig. S9 in Supplementary data (*R*<sup>2</sup> = 0.98) resulting from a lack of homogeneity of the  $PN/H_3PO_4$  samples.

### *4.3. Kinetics of the PN dissolution in the acid mixture solution at 25* ◦*C*

Due to the presence of various components in PN, it was not possible to derive a kinetic model from deconvoluted thermograms, as with pure Fap [13,14]. However, applying the Avrami model [19–21] shows the succession of processes leading at the end to precipitation of gypsum. According to this model the fraction reacted *x* is related to time through the following relationship: <sup>−</sup>ln(1 <sup>−</sup> *<sup>x</sup>*) *= ktn*, with *n* and *k* as constants. At the beginning this model has been developed for phase transitions, then it was applied to chemical processes, and the shift of the curve representing ln[−ln(1 <sup>−</sup> *<sup>x</sup>*)] over ln(*t*) has been assigned to a change in the crystallization [22–24] or reaction process [25–29]. In the case of PN the transformed fraction equals the quotient of the heat quantity (*q*) released from the beginning of the peak until time *t*, over the total heat (*Q*) corresponding to the transformation of total mass of PN. These quantities are calculated by integrating the corresponding surface under the peak. Fig. S11 in Supplementary data shows Avrami curves for various amounts of PN1. The curves exhibit three domains I, II and III, which can be assigned to PN dissolution/H $_2$ PO $_4^-$  neutralisation, hemihydrate precipitation and hemihydrate/dihydrate transformation, respectively. Fig. S11 in Supplementary data allows earlier.

Table S3 in Supplementary data gathers Avra and  $n$ ) deduced from the Avrami representation masses. This table shows that *k* and *n* paramete values in every domain for various amounts of P tion corroborates the predominance of one prod domain. The Avrami parameter "n" for dissolution, cannot be explained because for  $n > 3$  the mecha interpretable [24]. However, for two other doma 0.7 and 1. These values indicate that the correspor seem to be controlled by diffusion [30].

## **5. Attack of the PN by acid mixture at different temperatures**

In the wet process the acid solution has a con the mixed acid solution and the exothermic effect the mixing of acids and the attack maintains th 80 °C. Fig. S12 in Supplementary data shows deconvolutiongrams obtained at different temperatures with masses to 40 mg. As the temperature increases, the sec sponding to hemihydrate/dihydrate transformation, and  $\alpha$ the first one, and the thermogram contains only 55  $\degree$ C; when a third peak appears. The same phen observed with PN2.

Application of the Avrami model to the ther at 55 $\degree$ C, Fig. S13 in Supplementary data, shows t three domains separated by the shifts of the cur and 60 000 s. X-Ray patterns obtained from the these times as well as at the end of the attack, Fig. p[lemen](#page-3-0)tary data show the apatite  $(Ap)$  rays in a together with that of one or two of the sulfates. successively to a mixture of  $(Ap + AH + HH)$ ,  $(Ap + AH + HH)$  $(Ap + DH)$ . So the first domain corresponds to PI simultaneous precipitation of hemihydrate and The second domain corresponds to the HH into tion and the third one to the AH into DH transfo seems to begin after about 19h from the begini the attack is not finished even after 45 h matur shaking.

**Remark.** Errors on the slopes and intercepts according to the standard least square processing on the sum was determined by applying the form the statistical treatment developed by Guedens e

# **Appendix A. Supplementary data**

Supplementary data associated with this arti in the online version, at doi:10.1016/j.tca.2008.05

#### <span id="page-3-0"></span>**References**

- [1] M. Jansen, A. Waller, J. Verbiest, R.C. Van Landschoot, G.M. Van Rosmalen, Ind. Crystallization 84 (1984) 171–176.
- [2] P. Becker, Phosphates and Phosphoric Acid, Marcel Dekker, 1989.
- [3] S.V. Sluis, Y. Meszaros, M. Gerda, V. Rosmalen, Ind. Eng. Chem. Res. 26 (1987) 2501–2505.
- [4] E.O. Huffmann, W.E. Cate, M.E. Deming, K. Elmore, J. Agric. Food Chem. 5 (4) (1957) 266.
- [5] F. Ben Brahim, M. Mgaidi, M. El Maaoui, Can. J. Chem. Eng. 77 (1999) 136.
- [6] F. Gioia, G. Mura, A. Viola, Ind. Eng. Chem. Process Des. Dev. 16 (3) (1977) 390.
- [7] K. Shakourzadeh, R. Bloise, F. Baratin, Ind. Miner. Technol. 9 (1984) 443.
- [8] K. Ardhaoui, A. Ben Cherifa, M. Jemal, J. Therm. Anal. Cal. 81 (2005) 251–254.
- [9] K. Brahim, I. Khattech, J.D. Dubes, M. Jemal, Thermochim. Acta 436 (2005) ` 43–50.
- [10] K. Brahim, K. Antar, I. Khattech, M. Jemal, Ann. Chim. Sci. Mat. 31 (5) (2006) 611–620.
- [11] S.V. Dorozhkin, J. Prakt. Chem. 338 (1996) 620.
- [12] K. Brahim, Thèse de Doctorat en Chimie, Faculté des Sciences de Tunis, Juillet, 2006.
- [13] K. Antar, M. Jemal, Thermochim. Acta 452 (2007) 71–75.
- [14] K. Antar, K. Brahim, M. Jemal, Thermochim. Acta 449 (2006) 35–41.
- [15] K. Antar, Thèse de Doctorat en Chimie, Faculté des Sciences de Tunis, Juin, 2007.
- [16] K. Brahim, K. Antar, I. Khattech, M. Jemal, Sci. Res. Essays 3 (1) (2008) 35–39.
- [17] E.A. Abdel-Aal, M.M. Rashed, H. El-Shall, Cryst. Res. Technol. 39 (2004) 313–321.
- [18] V.M. Mireille, Thèse d'État: Physico-Chimie des Solides, INP Toulouse, Juillet, 1984.
- [19] M. Avrami, Kinetics of phase change I, J. Chem. Phys. 7 (1939) 1103.
- [20] M. Avrami, Kinetics of phase change II, J. Chem. Phys. 8 (1940) 212.
- [21] M. Avrami, Kinetics of phase change III, J. Chem. Phys. 9 (1941) 177.
- [22] M. Liu, Q. Zhao, Polymer 44 (2003) 2537–2545.
- [23] M. Yavuz, H. Maedo, J. Alloys Compd. 28 (1998) 280–289.
- [24] G.L. Perlovich, A. Bauer-Brandl, J. Therm. Anal. Calorim. 63 (2001) 653–661.
- [25] J. Kabai, Acta Chim. Acad. Sci. Hung. 78 (1973) 57.
- [26] M.A. Wells, R.J. Gilkes, R.W. Fitzpatrick, Clays Clay Miner. 49 (2001) 60–72.
- [27] M. Miyake, M. Maeda, Metall. Mater. Transform. B 37B (2006) 181.
- [28] H. Okur, T. Tekin, A.K. Ozer, M. Bayramoglu, Hydrometallurgy 67 (2002) 79–86.
- [29] F. Sevim, H. Saraç, M.M. Kocakerim, A. Yartasi, Ind. Eng. Chem. Res. 42 (2003) 2052.
- [30] C.N.R. Rao, K.J. Rao, Phase Transitions in Solids, Mc Graw-Hill, 1978, p. 93.
- [31] W.J. Guedens, J. Yperman, J. Mullens, L.C. Van Poucke, J. Chem. Educ. 70 (9) (1993) 776–779.