



## Thermodynamics of mixtures containing oxaalkanes. 6. Random mixing in ether + benzene, or + toluene systems

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### ABSTRACT

The Flory model has been applied to linear or cyclic ether+benzene, or +toluene mixtures. In addition, the relative variation of the molar excess enthalpy,  $H_m^E$ , along homologous series of the considered systems, has been discussed taking into account the contributions to  $H_m^E$  from the ether–ether, aromatic–aromatic and ether–aromatic interactions. It has been shown that in  $\text{CH}_3(\text{CH}_2)_{u-1}\text{O}(\text{CH}_2\text{CH}_2\text{O})_v(\text{CH}_2)_{u-1}\text{CH}_3$  + benzene mixtures, the  $u$  increase ( $v$  fixed) leads to a weakening of interactions between unlike molecules, and that proximity effects also weaken this type of interactions. In contrast, the  $v$  increase ( $u$  fixed) or cyclization lead to stronger interactions between unlike molecules. From the application of the model, it is concluded that the random mixing hypothesis may be considered to be valid to a large extent for many of the investigated solutions. Erroneously, strong orientational effects are predicted for 1,3-dioxolane, or 1,4-dioxane + benzene systems, but this has been attributed to the model can not describe asymmetric  $H_m^E$  curves when the mixture compounds show close values for  $V_i$  (molar volume) and for  $V_i^*$  (reduction parameter for volume). Previous calculations on the basis of the Kirkwood–Buff integrals formalism confirm that the mixture structure is close to random mixing. Flory results on the excess molar volumes have been discussed taking into account the so-called curvature and  $P^*$  contributions to this excess function.

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### 1. Introduction

It is known that the Flory model [1] is commonly used to describe simultaneously, excess molar enthalpies,  $H_m^E$ , and excess molar volumes,  $V_m^E$ , of systems formed by non-polar (benzene [2]) or slightly polar compound (N,N,N-trialkylamine [3] or monoether [4]) and alkane, or involving two polar compounds as 1-alkanol + 1-alkanol [5] or 2-methoxyethanol + hydroxyether [6]. The good agreement between experimental and theoretical results implies that the random mixing hypothesis, a basic assumption of the Flory model, is attained in large extent for these systems. It may be due to such solutions are characterized by dispersive interactions (benzene + alkane), or by weak dipolar interactions (monoether + alkane) or to the identical chemical nature of the two mixture compounds (1-alkanol + 1-alkanol). In addition, the Flory model has also been widely used to investigate order creation and order destruction processes in binary mixtures formed by one alkane and one non-polar or slightly polar compound, with spherical or plate like shape [7–10]. As any order effects are ignored in the theory (random mixing hypothesis), differences between experimental values for the magnitudes  $H_m^E$ ,  $V_m^E$ ,  $C_{pm}^E$ ,  $(\partial V_m^E/\partial T)_p$ ,

or  $-(\partial V_m^E/\partial P)_T$  and the corresponding Flory results are ascribed to order effects. The main conclusion of these studies is the existence of a short orientational order in long chain alkanes, which does not appear in highly branched isomeric alkanes, or short chain alkanes.

The theory has been also applied to predict isobaric expansion coefficient,  $\alpha_p$  isentropic,  $\kappa_S$ , or isothermal,  $\kappa_T$  compressibilities and speeds of sound,  $u$ , of simple systems, as those involving two alkanes, or of the type cyclohexane or benzene +  $n$ -alkane [2,11,12]. We have shown that the model application can be extended in two ways. Firstly, the theory provides rather accurate predictions on  $\alpha_p$ ,  $\kappa_S$ ,  $\kappa_T$  and  $u$  of complex mixtures as alkoxyethanol + dibutylether, or +1-butanol [13]. Secondly, it is possible to investigate the existence of orientational effects in complex mixtures by studying the variation of the interaction parameter,  $X_{12}$ , with the composition [14,15]. Here, in order to gain insight into the interactions and structure of ether + aromatic compound mixtures, the same method is applied to investigate the validity of the random mixing hypothesis in ether + benzene or + toluene mixtures. Previously, as similar research has been presented for ether + alkane systems [16].

From a practical point of view, this type of studies is particularly interesting as precise molecular recognition is essential to living systems [17]. Thus, biological discriminations as enzyme–substrate or antigen–antibody are well known. In chemical systems, molecular recognition has been extensively studied using a variety of model compounds such as 1,3-dioxane or crown ethers [17,18].

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Actually, it is accepted that molecular recognition, biological or chemical, is due to specific weak interactions between the interacting groups of the respective molecules [17]. Mixtures containing ethers are also important because they are increasingly used as additives to gasoline owing to their octane-enhancing and pollution-reducing properties [19,20]. In addition, cyclic polyethers have attracted interest as model substances for bio-systems (see above), separation techniques, chemical analysis or in relation to their use in synthetic methods in organic chemistry [21,22]. In the case of crown ethers, this is due to the fact that they can selectively form strong electrostatic complexes with a large variety of ligands in different solvents [23–25].

## 2. The Flory model

In this section, a brief summary of the model is presented. More details are given in the original works [1,26–29]. The main features of the theory are as follows: (i) molecules are divided into segments. A segment is an arbitrarily chosen isomeric portion of the molecule. The number of segments per molecule of component  $i$  is denoted by  $r_i$  and the number of intermolecular contact sites per segment by  $s_i$ . (ii) The mean intermolecular energy per contact is proportional to  $-\eta/v_s$  (where  $\eta$  is a positive constant characterizing the energy of interaction for a pair of neighbouring sites and  $v_s$  is the volume of a segment). (iii) When stating the configurational partition function, it is assumed that the number of external degrees of freedom of the segments is lower than 3, in order to take into account the restrictions on the precise location of a given segment by its neighbours in the same chain. (iv) Random mixing is assumed: the probability of having species of kind  $i$  neighbours to any given site is equal to the site fraction,  $\theta_i$  ( $\theta_i = s_i r_i N_i / srN$ ; where  $N = N_1 + N_2$  is the total number of molecules and  $r$  and  $s$  are the total number of intermolecular segments and contact sites per segment, respectively). For very large total number of contact sites, the probability of formation of an interaction between contacts sites belonging to different liquids is  $\theta_1\theta_2$ . Under these hypotheses, the Flory equation of state is given by:

$$\frac{\bar{p}\bar{V}}{\bar{T}} = \frac{\bar{V}^{1/3}}{\bar{V}^{1/3} - 1} - \frac{1}{\bar{V}\bar{T}} \quad (1)$$

where  $\bar{V} = V/V^*$ ;  $\bar{P} = P/P^*$  and  $\bar{T} = T/T^*$  are the reduced volume, pressure and temperature, respectively. Eq. (1) is valid for pure liquids and liquid mixtures. For pure liquids, the reduction parameters,  $V_i^*$ ,  $P_i^*$  and  $T_i^*$  can be obtained from experimental data, such as  $\alpha_{pi}$  and  $\kappa_{Ti}$ . For mixtures, the corresponding parameters are calculated as follows:

$$V^* = x_1 V_1^* + x_2 V_2^* \quad (2)$$

$$T^* = \frac{\varphi_1 P_1^* + \varphi_2 P_2^* - \varphi_1 \theta_2 X_{12}}{\varphi_1 P_1^*/T_1^* + \varphi_2 P_2^*/T_2^*} \quad (3)$$

$$P^* = \varphi_1 P_1^* + \varphi_2 P_2^* - \varphi_1 \theta_2 X_{12} \quad (4)$$

In Eqs. (3) and (4),  $\varphi_i = x_i V_i^* / \sum x_i V_i^*$  is the segment fraction and  $\theta_2$  is alternatively calculated as:  $\theta_2 = \varphi_2 / (\varphi_2 + S_{12} \varphi_1)$ .  $S_{12}$  is the so-called geometrical parameter of the mixture, which, assuming that the molecules are spherical, is calculated as  $S_{12} = (V_1^*/V_2^*)^{-1/3}$ . The energetic parameter,  $X_{12}$ , also present in Eqs. (3) and (4), is defined by similarity with:

$$P_i^* = \frac{s_i \eta_{ii}}{2v_s^2} \quad (5)$$

as

$$X_{12} = \frac{s_1 \Delta \eta}{2v_s^2} \quad (6)$$

where  $\Delta \eta = \eta_{11} + \eta_{22} - 2\eta_{12}$ . In Eqs. (5) and (6),  $v_s^*$  (reduction volume for segment) and  $\eta_{ij}$  are changed from molecular units to molar units per segments.  $H_m^E$  is determined from:

$$H_m^E = \frac{x_1 V_1^* \theta_2 X_{12}}{\bar{V}} + x_1 V_1^* P_1^* \left( \frac{1}{\bar{V}_1} - \frac{1}{\bar{V}} \right) + x_2 V_2^* P_2^* \left( \frac{1}{\bar{V}_2} - \frac{1}{\bar{V}} \right) \quad (7)$$

which can be also written as:

$$H_m^E = \frac{x_1 V_1^* \theta_2 X_{12}}{\bar{V}} + x_1 V_1^* \varphi_2 \left( \frac{\bar{V}_1 - \bar{V}_2}{\bar{V}_0} \right) \left( \frac{P_2^*}{\bar{V}_2} - \frac{P_1^*}{\bar{V}_1} \right) + \frac{V_m^E}{(\bar{V}_0)^2 (\varphi_1 P_1^* + \varphi_2 P_2^*)} \quad (8)$$

where  $\bar{V}_0 = \varphi_1 \bar{V}_1 + \varphi_2 \bar{V}_2$ . The term which depends directly on  $X_{12}$  in Eq. (8) is usually named the interaction contribution [26] to  $H_m^E$ . The remaining terms are the so-called equation of state contribution [26] to  $H_m^E$ . The reduced volume of the mixture,  $\bar{V}$ , in Eqs. (7) and (8) is obtained from the equation of state. Therefore, the molar excess volume can be also calculated:

$$V_m^E = (x_1 V_1^* + x_2 V_2^*) (\bar{V} - \varphi_1 \bar{V}_1 - \varphi_2 \bar{V}_2) \quad (9)$$

## 3. Estimation of the Flory interaction parameter

$X_{12}$  can be determined from a  $H_m^E$  measurement at a given composition from the equation [14,15]:

$$X_{12} = \frac{x_1 P_1^* V_1^* (1 - \bar{T}_1/\bar{T}) + x_2 P_2^* V_2^* (1 - \bar{T}_2/\bar{T})}{x_1 V_1^* \theta_2} \quad (10)$$

For the use of this expression, it must be taken into account that  $\bar{V}\bar{T}$  is a function of  $H_m^E$ :

$$H_m^E = \frac{x_1 P_1^* V_1^*}{\bar{V}_1} + \frac{x_2 P_2^* V_2^*}{\bar{V}_2} + \frac{1}{\bar{V}\bar{T}} (x_1 P_1^* V_1^* \bar{T}_1 + x_2 P_2^* V_2^* \bar{T}_2) \quad (11)$$

and that, from the equation of state,  $\bar{V} = \bar{V}(\bar{T})$ . For normal applications, it is possible to use the so-called  $\bar{p} \approx 0$  approximation of the equation of state, which is a good approximation at atmospheric pressure. More details have been given elsewhere [14,15]. Eq. (10) generalizes that previously given to calculate  $X_{12}$  from  $H_m^E$  at  $x_1 = 0.5$  [30]. Properties of the pure compounds at 298.15 K, molar volumes,  $\alpha_{pi}$  and  $\kappa_{Ti}$ , and the corresponding reduction parameters,  $P_i^*$  and  $V_i^*$  ( $i = 1, 2$ ), needed for calculations are listed in Table 1. Values of these properties at  $T \neq 298.15$  K were estimated according to the method used previously [16].  $X_{12}$  values determined from experimental  $H_m^E$  data at  $x_1 = 0.5$  are collected in Table 2.

## 4. Results

Results on  $H_m^E$  and  $V_m^E$  obtained from the Flory model using  $X_{12}$  values at  $x_1 = 0.5$  are listed in Tables 2 and 3, respectively. A comparison between experimental and theoretical values for  $H_m^E$  and  $V_m^E$  are shown graphically in Figs. 1–4. For the sake of clarity, Table 2 also includes the relative standard deviations for  $H_m^E$  defined as:

$$\sigma_r(H_m^E) = \left[ \frac{1}{N} \sum \left( \frac{H_{m, \text{exp}}^E - H_{m, \text{calc}}^E}{H_{m, \text{exp}}^E} \right)^2 \right]^{1/2} \quad (12)$$

where  $N = 19$  is the number of data points, and  $H_{m, \text{exp}}^E$  represents smoothed  $H_m^E$  values calculated at  $\Delta x_1 = 0.05$  in the composition range [0.05, 0.95] from polynomial expansions given in the original works. In order to obtain detailed information on the concentration dependence of  $X_{12}$ , this magnitude has been determined using Eq.

**Table 1**Flory parameters<sup>a</sup> of pure compounds at  $T = 298.15$  K.

Compound <sup>b</sup>	$V_i$ (cm <sup>3</sup> mol <sup>-1</sup> )	$\alpha_p \times 10^{-3}$ K <sup>-1</sup>	$\kappa_T \times 10^{-12}$ Pa <sup>-1</sup>	$V_i^*$ (cm <sup>3</sup> mol <sup>-1</sup> )	$P_i^*$ (J cm <sup>-3</sup> )
101	69.67 <sup>c</sup>	1.996 <sup>c</sup>	2514.6 <sup>d</sup>	49.02	478.1
202	104.74 <sup>e</sup>	1.654 <sup>e</sup>	1967 <sup>e</sup>	76.57	469.1
303	137.68 <sup>f</sup>	1.261 <sup>f</sup>	1440 <sup>f</sup>	106	440.7
404	170.45 <sup>g</sup>	1.1336 <sup>g</sup>	1205.9 <sup>g</sup>	133.74	455.2
505	203.40 <sup>h</sup>	1.027 <sup>h</sup>	1067 <sup>h</sup>	162.02	450.8
606	235.81 <sup>i</sup>	0.906 <sup>i</sup>	865 <sup>i</sup>	192.01	471
808	302.09 <sup>k</sup>	0.68 <sup>j</sup>	580 <sup>j</sup>	236.59	485
10201	104.34 <sup>c</sup>	1.268 <sup>l</sup>	1114.5 <sup>l</sup>	80.25	573.4
20202	141.33 <sup>m</sup>	1.225 <sup>m</sup>	1140.5 <sup>m</sup>	109.38	534.6
10101	89.49 <sup>n</sup>	1.495 <sup>n</sup>	1485 <sup>n</sup>	66.3	574.2
20102	126.38 <sup>n</sup>	1.281 <sup>n</sup>	1411 <sup>n</sup>	97.0	465.3
1020201	142.93 <sup>l</sup>	1.060 <sup>l</sup>	821.6 <sup>l</sup>	118.25	610.6
2020202	179.56 <sup>o</sup>	1.11 <sup>o</sup>	909.9 <sup>o</sup>	141.4	586.5
THF	81.76 <sup>p</sup>	1.2265 <sup>p</sup>	962.3 <sup>p</sup>	63.26	634.7
THP	98.19 <sup>c</sup>	1.156 <sup>q</sup>	990 <sup>r</sup>	76.78	569.4
1,3-Dioxolane	69.98 <sup>s</sup>	1.164 <sup>s</sup>	758.3 <sup>s</sup>	54.65	750.3
1,3-Dioxane	85.64 <sup>t</sup>	1.05 <sup>t</sup>	733 <sup>t</sup>	68.08	675.7
1,4-Dioxane	85.71 <sup>c</sup>	1.115 <sup>c</sup>	738 <sup>c</sup>	67.44	727.5
Benzene	89.44 <sup>c</sup>	1.213 <sup>c</sup>	966 <sup>c</sup>	69.34	622.8
Toluene	106.89 <sup>c</sup>	1.067 <sup>c</sup>	912 <sup>c</sup>	84.74	554.9

<sup>a</sup>  $V_i$ , molar volume,  $\alpha_p$ , isobaric thermal expansion coefficient;  $\kappa_T$ , isothermal compressibility;  $V_i^*$ , reduction parameter for volume and  $P_i^*$ , reduction parameter for pressure.<sup>b</sup> The figures represent the number of aliphatic groups attached to the O atoms, e.g. 101 is dimethylether and 1020201 is 2,5,8-trioxanonane; THF, tetrahydrofuran; THP, tetrahydropyran.<sup>c</sup> [65].<sup>d</sup> Estimated according to the method reported in Ref. [66].<sup>e</sup> [67].<sup>f</sup> [68].<sup>g</sup> [69].<sup>h</sup> [70].<sup>i</sup> [71].<sup>j</sup> Estimated value.<sup>k</sup> [44].<sup>l</sup> [72].<sup>m</sup> [73].<sup>n</sup> [74].<sup>o</sup> [75].<sup>p</sup> [76].<sup>q</sup> [77].<sup>r</sup> [78].<sup>s</sup> [79].<sup>t</sup> [56].

(10) and the mentioned  $H_{m,exp}^E$  values at  $\Delta x_1 = 0.05$ . The  $X_{12}$  ( $x_1$ ) variation is estimated from the equation:

$$\Delta_i = \frac{|\Delta X_{12}|_i^{\max}}{X_{12}(x_1 = 0.5)} \quad (13)$$

where  $|\Delta X_{12}|_i^{\max}$  is the maximum absolute value of the  $X_{12}(x_1) - X_{12}(x_1 = 0.5)$  difference in the ranges [0.05, 0.45] ( $i = 1$ ) and [0.55, 0.95] ( $i = 2$ ). The corresponding values are listed in Table 4 (see also Figs. 5–7).

## 5. Discussion

Previously, it has been already pointed out that, in oxaalkane + aromatic compound mixtures, specific interactions of the  $n-\pi$  type between unlike molecules exist [31–33]. Thus, the exothermic  $H_m^E$  values of the 2,5-dioxahehexane + benzene system [34] could be explained on the basis of such interactions. In order, to evaluate the strength of the ether–aromatic interactions, a method widely applied is the following [35–37]. Let us denote the positive contributions to  $H_m^E$  from the disruption of the ether–ether and aromatic–aromatic interactions by  $\Delta H_{O-O}$  and  $\Delta H_{aro-aro}$ , respectively, and by  $\Delta H_{O-aro}$ , the negative contribution from the creation of the ether–aromatic interactions. Then, we can

write:

$$H_m^E = \Delta H_{O-O} + \Delta H_{aro-aro} + \Delta H_{O-aro} \quad (14)$$

This equation can be extended to  $x_1 \rightarrow 0$  [38,39] to evaluate  $\Delta H_{O-aro}$ , the strength of the interactions between ether and the aromatic compound in the studied solutions. In such case,  $\Delta H_{O-O}$  and  $\Delta H_{aro-aro}$  can be replaced by  $H_1^{E,\infty}$  (partial excess molar enthalpy at infinite dilution of the first component) of ether or benzene, or toluene + alkane systems. Thus,

$$\begin{aligned} \Delta H_{O-aro} = & H_1^{E,\infty}(\text{ether} + \text{aromatic compound}) \\ & - H_1^{E,\infty}(\text{ether} + \text{alkane}) - H_1^{E,\infty}(\text{aromatic compound} \\ & + \text{alkane}) \end{aligned} \quad (15)$$

In mixtures with linear ethers, the considered alkane is heptane, while in cyclic ether solutions is cyclohexane. Table 5 lists  $\Delta H_{O-aro}$  values for some selected mixtures. Below, we are referring to values of the excess functions at equimolar composition and 298.15 K.

### 5.1. $CH_3(CH_2)_{u-1}O(CH_2)_{u-1}CH_3$ + benzene

Here,  $H_m^E$  increases with  $u$  (Table 2). This may be explained on the basis of the following effects. (i) A weakening of the ether–benzene interactions, as the decrease of the  $|\Delta H_{O-aro}|$  term for increased

**Table 2**  
Molar excess enthalpies,  $H_m^E$ , at 298.15 K and equimolar composition for ether + benzene, or + toluene systems. The Flory interaction parameter,  $X_{12}$ , calculated from  $H_m^E$  at equimolar composition, and the interactional and equation of state contributions,  $H_{m,int}^E$  and  $H_{m,EOS}^E$ , respectively, are also included.

Ether <sup>a</sup>	$H_m^E$ (J mol <sup>-1</sup> )	$X_{12}$ (J cm <sup>-3</sup> )	$H_{m,int}^E$ (J mol <sup>-1</sup> )	$H_{m,EOS}^E$ (J mol <sup>-1</sup> )	$\sigma_r(H_m^E)^b$	Ref.
Solvent: benzene						
101	-194 <sup>c</sup>	-8.23	-82	-112	0.081	[80]
202	-8.7	0.772	10.8	-19.6	1.30	[81]
303	175	7.28	128	47	0.157	[82]
404	320	11.63	238	82	0.125	[83]
	304 <sup>d</sup>	10.97	220	84	0.129	[84]
505	403	13.33	308	95	0.142	[71]
606	425	13.36	345	80	0.135	[71]
10201	-179	-8.84	-130	-49	0.036	[34]
20202	-281	-11.46	-207	-75	0.010	[71]
1020201	-286	-9.78	-193	-93	0.057	[82]
2020202	-428	-14.95	-318	-110	0.069	[82]
10101	56	3.59	46	10	0.067	[85]
20102	72	3.19	53	19	0.280	[85]
THF	-364	-21.16	-268	-96	0.029	[31]
THP	-253	-12.93	-187	-66	0.052	[86]
1,3-Dioxolane	79	4.53	52	17	0.670	[87]
1,3-Dioxane	-157	-8.47	-114	-43	0.104	[32]
1,4-Dioxane	-31	-1.63	-21.7	-9.3	7.3	[32]
Solvent: toluene						
101	-221 <sup>c</sup>	-7.25	-78	-143	0.011	[80]
404	80 <sup>e</sup>	2.72	61	19	0.136	[88]
THF	-363	-19.69	-269	-94	0.030	[58]
THP	-250	-11.96	-187	-63	0.082	[58]
1,3-Dioxolane	184	11.32	139	45	0.103	[58]
1,4-Dioxane	122	6.45	92	30	0.178	[58]

<sup>a</sup> For symbols, see Table 1.

<sup>b</sup> Eq. (12).

<sup>c</sup>  $T=323.15$  K.

<sup>d</sup>  $T=313.15$  K.

<sup>e</sup>  $T=303.15$  K.

$u$  values indicates, which predominates over the lower positive  $\Delta H_{O-O}$  contribution (Table 5). This is due to the decrease of the effective dipole moment,  $\bar{\mu}$  [40–42], of the ether: 0.599 ( $u=1$ ) > 0.488 ( $u=2$ ) > 0.393 ( $u=3$ ) > 0.353 ( $u=4$ ) > 0.323 ( $u=5$ ) [42]. Note that interactions of the type dipole-induced dipole, like ether–benzene, can be represented by an average potential pro-

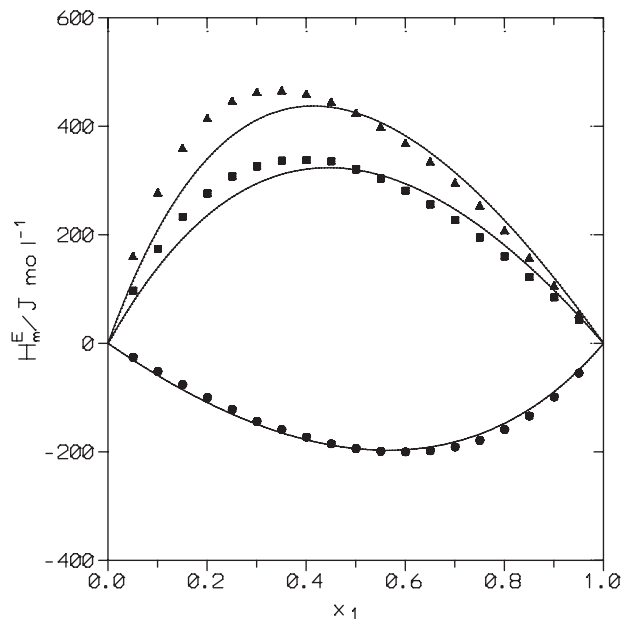
portional to  $\alpha_i \mu_j^2$  and inversely proportional to  $r^6$  ( $\alpha_i$  is the polarizability of the non-polar compound (benzene);  $\mu_j$  is the dipole moment of the polar component (ether) and  $r$  is the intermolecular distance) [43]. Therefore, one could expect then that the higher  $\bar{\mu}$  of the oxaalkane is, the stronger are the interactions between unlike molecules and also those between ether molecules

**Table 3**  
Molar excess volumes,  $V_m^E$  at 298.15 K and equimolar composition for ether + benzene or + toluene systems. Comparison of experimental (exp.) results with Flory calculations.

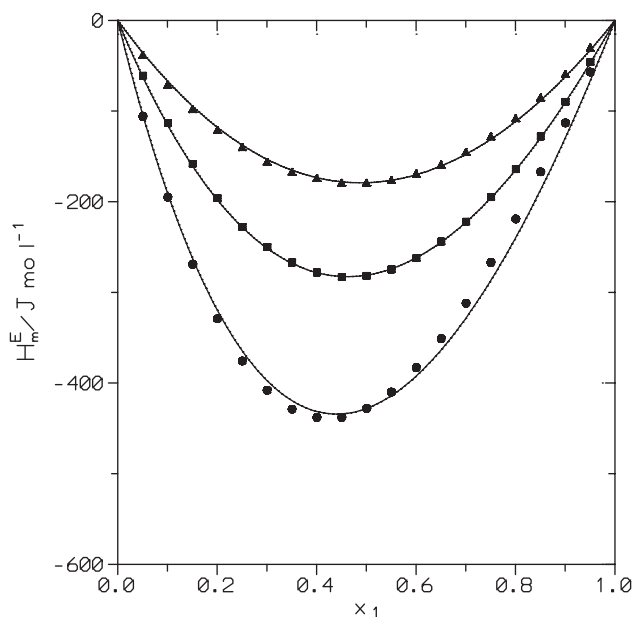
System <sup>a</sup>	$V_m^E$ (cm <sup>3</sup> mol <sup>-1</sup> )		Ref.
	Exp.	Flory	
404 + benzene	0.1298	0.375	[83]
	0.158		[89]
	0.158		[90]
10201 + benzene	-0.017	-0.154	[34]
THF + benzene	-0.252	-0.254	[91]
	-0.253		[92]
	-0.216		[93]
THP + benzene	-0.166	-0.166	[91]
	-0.163		[94]
	-0.191		[94]
1,3-Dioxane + benzene	-0.191		[94]
	-0.200		[95]
1,4-Dioxane + benzene	-0.065	-0.078	[94]
	-0.065		[95]
404 + toluene	-0.153	-0.012 <sup>b</sup>	[96]
	-0.369	-0.198	[97]
THF + toluene	-0.344		[93]
	-0.367		[98]
	-0.162	-0.162	[97]
THP + toluene	-0.159		[98]
	-0.124	0.208	[98]
1,3-Dioxolane + toluene	-0.124		[98]
1,4-Dioxane + toluene	-0.015	-0.015	[98]

<sup>a</sup> For symbols, see Table 1.

<sup>b</sup> Calculated at 303.15 K.



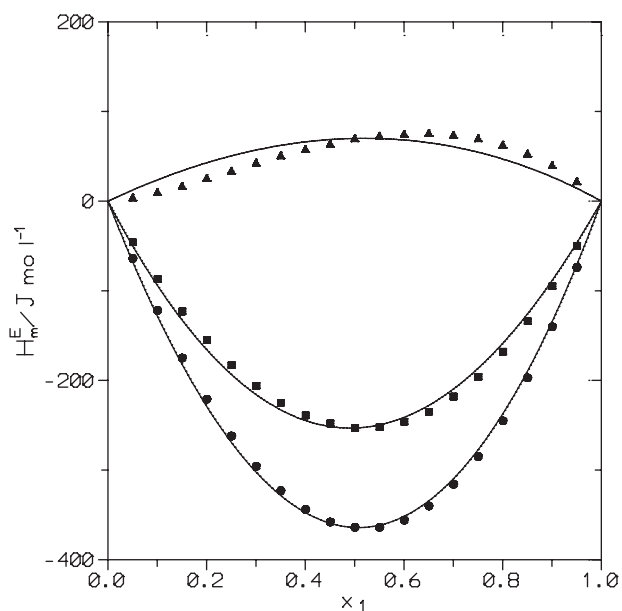
**Fig. 1.**  $H_m^E$  for linear monoether (1) + benzene (2) mixtures. Points, experimental results: (●) dimethylether ( $T=323.15$  K) [80]; (■) dibutylether ( $T=298.15$  K) [83]; (▲) dihexylether ( $T=298.15$  K) [71]. Solid lines, Flory calculations.



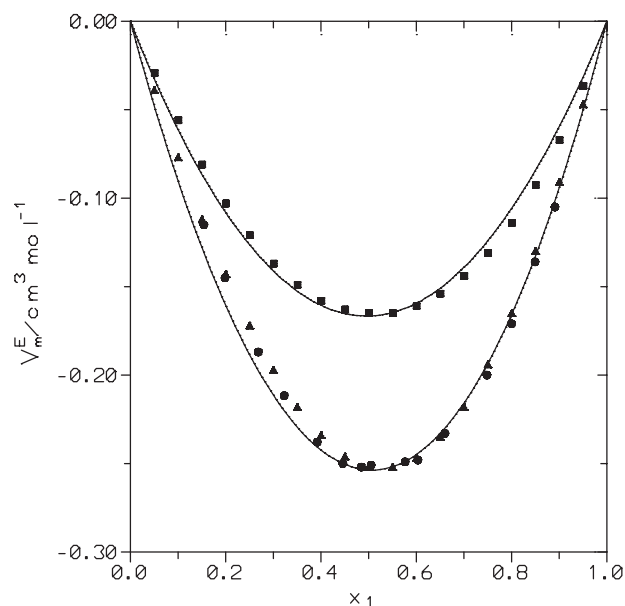
**Fig. 2.**  $H_m^E$  for linear polyether (1)+benzene (2) at 298.15 K. Points, experimental results: ( $\blacktriangle$ ) 2,5-dioxahexane [34]; ( $\blacksquare$ ) 3,6-dioxaoctane [71]; ( $\bullet$ ) 3,6,8-trioxaundecane [82]. Solid lines, Flory calculations.

(larger  $\Delta H_{O-O}$  values, Table 5). (ii) Moreover, interactions between unlike molecules are less probable for mixtures with ethers of larger  $u$  values as their etheric surface is smaller, and it is more sterically hindered by the longer adjacent alkyl groups (steric effect). On the other hand, a higher positive  $\Delta H_{aro-aro}$  contribution is expected due to the larger aliphatic surface of these ethers. Note that  $H_m^E$  of benzene +  $n$ -alkane increases with the chain length of the alkane (Table A.1, Appendix A).

It is remarkable that, although  $X_{12}(x_1=0.5)$  increases with  $u$  (Table 2), solutions including ethers with  $u=5$  or 6 are characterized by close  $X_{12}(x_1=0.5)$  values. This suggests that the mentioned systems mainly differ by geometrical factors. We have



**Fig. 3.**  $H_m^E$  for cyclic ether (1)+benzene (2) mixtures at 298.15 K. Points, experimental results: ( $\bullet$ ) tetrahydrofuran [31]; ( $\blacksquare$ ) tetrahydropyran [86]; ( $\blacktriangle$ ) 1,3-dioxolane [87]. Solid lines, Flory calculations.



**Fig. 4.**  $V_m^E$  for cyclic monoether (1)+benzene (2) mixtures at 298.15 K. Points, experimental results: ( $\bullet$ ) [92] or ( $\blacktriangle$ ) [91], tetrahydrofuran; ( $\blacksquare$ ) tetrahydropyran [91]. Solid lines, Flory calculations.

used  $X_{12}(x_1=0.5) = 13.36 \text{ J cm}^{-3}$  (the value for the solution containing dihexyl ether) to predict  $V_m^E$  of the system with dioctyl ether. The result ( $0.506 \text{ cm}^3 \text{ mol}^{-1}$ ) is in reasonable agreement with the experimental one ( $0.550 \text{ cm}^3 \text{ mol}^{-1}$  [44]). It seems that the so-called Patterson effect [45], an extra positive contribution to  $H_m^E$  from the disruption of the order in longer  $n$ -alkanes by globular or plate like shape molecules, such benzene or cyclohexane [45,46], is not present in these systems.

**Table 4**

Variations of the  $X_{12}$  values,  $\Delta_1$ , obtained from  $H_m^E$  data at 298.15 of ether + benzene, or + toluene mixtures in the concentration ranges [0.05, 0.5] ( $i=1$ ) and [0.5, 0.95] ( $i=2$ ) calculated according to Eq. (13).

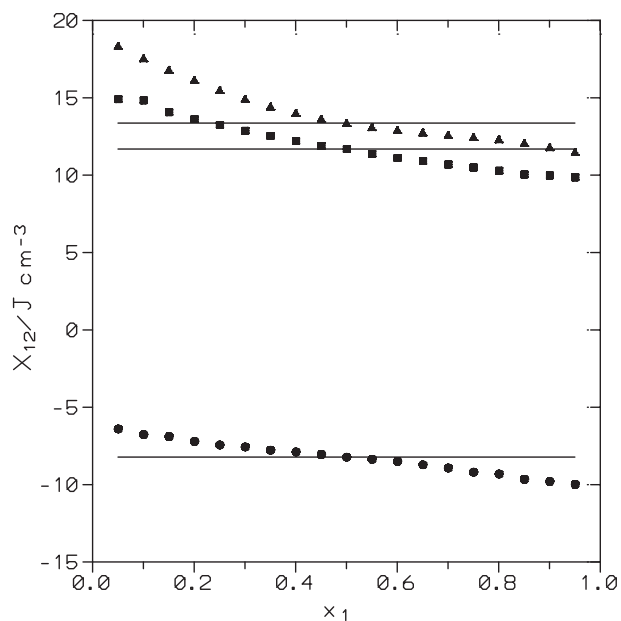
System <sup>a</sup>	$\Delta_1$	$\Delta_2$	Ref.
101 + benzene	0.222 <sup>b</sup>	0.214 <sup>b</sup>	[80]
202 + benzene	3.74	2.63	[81]
303 + benzene	0.184	0.255	[82]
404 + benzene	0.282	0.152	[83]
	0.278 <sup>c</sup>	0.189 <sup>c</sup>	[84]
505 + benzene	0.331	0.211	[71]
606 + benzene	0.373	0.140	[71]
10201 + benzene	0.070	0.081	[34]
20202 + benzene	0.012	0.022	[71]
2020202 + benzene	0.030	0.151	[82]
10101 + benzene	0.042	0.061	[85]
20102 + benzene	0.511	0.354	[85]
THF + benzene	0.050	0.039	[31]
THP + benzene	0.075	0.073	[86]
1,3-Dioxolane + benzene	0.675	0.534	[87]
1,3-Dioxane + benzene	0.107	0.200	[32]
1,4-Dioxane + benzene	2.38	1.77	[32]
101 + toluene	0.030 <sup>b</sup>	0.052 <sup>b</sup>	[80]
404 + toluene	0.195 <sup>d</sup>	0.250 <sup>d</sup>	[88]
THF + toluene	0.013	0.067	[58]
THP + toluene	0.010	0.022	[58]
1,3-Dioxolane + toluene	0.219	0.081	[58]
1,4-Dioxane + toluene	0.307	0.203	[58]

<sup>a</sup> For symbols, see Table 1.

<sup>b</sup> Data at 323.15 K.

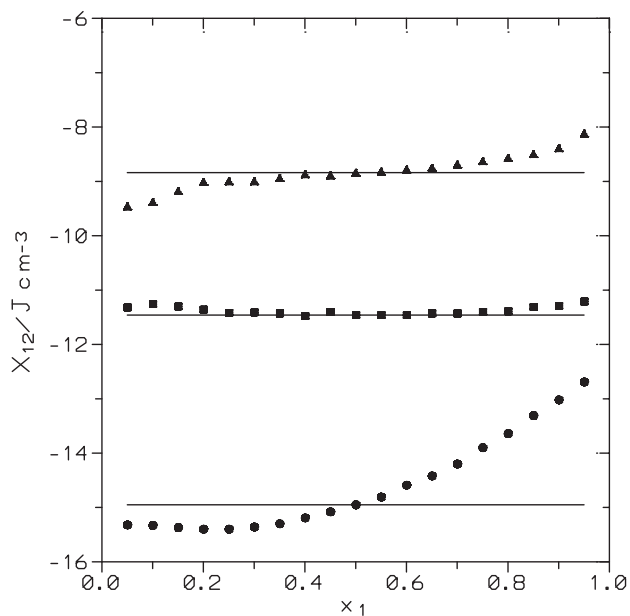
<sup>c</sup> Data at 313.15 K.

<sup>d</sup> Data at 303.15 K.

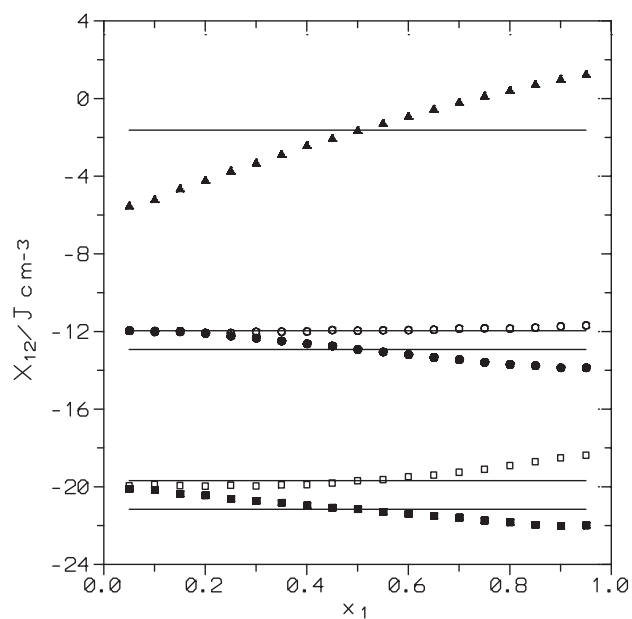


**Fig. 5.** Flory interaction parameters,  $X_{12}$ , for linear monoether (1)+benzene (2) mixtures. Points, values determined from  $H_m^E$  at  $\Delta x_1 = 0.05$ : (●) dimethylether ( $T = 323.15\text{ K}$ ) [80]; (■) dibutylether ( $T = 298.15\text{ K}$ ) [83]; (▲) dihexylether ( $T = 298.15\text{ K}$ ) [71]. Solid lines,  $X_{12}$  values calculated from  $H_m^E$  at  $x_1 = 0.5$ .

The  $\sigma_r(H_m^E)$  values determined from the Flory model for  $\text{CH}_3(\text{CH}_2)_{u-1}\text{O}(\text{CH}_2)_{u-1}\text{CH}_3$  + heptane mixtures, are 0.053 ( $u = 2$ ); 0.021 ( $u = 3$ ); 0.020 ( $u = 3$ ); 0.059 ( $u = 5$ ) [16]; while  $\sigma_r(H_m^E) = 0.047$  for the benzene + octane system (Table A.1, Appendix A). The  $\sigma_r(H_m^E)$  results for the present solutions are higher (Table 2), indicating that orientational effects are stronger. However, the rather moderate  $\sigma_r(H_m^E)$  values obtained suggest that these effects are weak, which is supported by low  $C_{pm}^E$  negative values. So, for the dibutylether system,  $C_{pm}^E \approx -1\text{ J mol}^{-1}\text{ K}^{-1}$ , value calcu-



**Fig. 6.** Flory interaction parameters,  $X_{12}$ , for linear polyether (1)+benzene (2) mixtures at 298.15 K. Points, values determined from  $H_m^E$  at  $\Delta x_1 = 0.05$ : (▲) 2,5-dioxahexane [34]; (■) 3,6-dioxaoctane [71]; (●) 3,6,8-trioxoundecane [82]. Solid lines,  $X_{12}$  values calculated from  $H_m^E$  at  $x_1 = 0.5$ .



**Fig. 7.** Flory interaction parameters,  $X_{12}$ , for cyclic ether (1)+benzene (2), or +toluene (2) mixtures at 298.15 K. Points, values determined from  $H_m^E$  at  $\Delta x_1 = 0.05$ : (●) tetrahydrofuran + benzene [31]; (■) tetrahydropyran + benzene [86]; (▲) 1,4-dioxane + benzene [32]; (□) tetrahydrofuran + toluene [58]; (○) tetrahydropyran + toluene [58]. Solid lines,  $X_{12}$  values calculated from  $H_m^E$  at  $x_1 = 0.5$ .

**Table 5**

Partial excess molar enthalpies at infinite dilution of the first compound,  $H_1^{E,\infty}$ , at  $T = 298.15\text{ K}$  for solute (1)+organic solvent (2) mixtures, and enthalpy of aromatic–ether interaction,  $\Delta H_{(\text{aromatic-O})}$ , for ether (1)+aromatic compound (2) systems.

System <sup>a</sup>	$H_1^{E,\infty}/\text{kJ mol}^{-1}$	$\Delta H_{(\text{aromatic-O})}/\text{kJ mol}^{-1}$
$\text{C}_6\text{H}_6 + n\text{-C}_7$	3.66 [99]	
$\text{C}_6\text{H}_6 + n\text{-C}_6^b$	3.97 [100]	
$\text{C}_6\text{H}_6 + \text{C}_6\text{H}_{12}$	3.74 [101]	
$\text{C}_7\text{H}_8 + \text{C}_6\text{H}_{12}$	2.10 [102]	
$1\text{O}1 + n\text{-C}_{10}^b$	1.92 [80]	
$2\text{O}2 + n\text{-C}_7$	1.60 [103]	
$3\text{O}3 + n\text{-C}_7$	0.84 [104]	
$4\text{O}4 + n\text{-C}_7$	0.531 [105]	
$5\text{O}5 + n\text{-C}_7$	0.496 [70]	
$1\text{O}2\text{O} + n\text{-C}_7$	5.48 [50]	
$2\text{O}2\text{O}2 + n\text{-C}_7$	4.53 [49]	
$2\text{O}1\text{O}2 + n\text{-C}_7$	2.42 [85]	
THF + $\text{C}_6\text{H}_{12}$	3.37 [58]	
THP + $\text{C}_6\text{H}_{12}$	2.22 [58]	
1,3-Dioxolane + $\text{C}_6\text{H}_{12}$	8.99 [58]	
1,3-Dioxane + $\text{C}_6\text{H}_{12}$	7.74 [32]	
1,4-Dioxane + $\text{C}_6\text{H}_{12}$	7.85 [32]	
$1\text{O}1 + \text{C}_6\text{H}_6^b$	-0.535 [80]	-6.11
$2\text{O}2 + \text{C}_6\text{H}_6$	0.246 [81]	-5.01
$3\text{O}3 + \text{C}_6\text{H}_6$	1.15 [82]	-3.35
$4\text{O}4 + \text{C}_6\text{H}_6$	2.17 [83]	-2.02
$5\text{O}5 + \text{C}_6\text{H}_6$	2.92 [71]	-1.23
$1\text{O}2\text{O}1 + \text{C}_6\text{H}_6$	-0.815 [34]	-9.95
$2\text{O}2\text{O}2 + \text{C}_6\text{H}_6$	-1.25 [71]	-9.44
$2\text{O}1\text{O}2 + \text{C}_6\text{H}_6$	0.525 [85]	-5.45
THF + $\text{C}_6\text{H}_6$	-1.40 [91]	-8.51
THP + $\text{C}_6\text{H}_6$	-0.816 [91]	-6.78
1,3-Dioxane + $\text{C}_6\text{H}_6$	-0.694 [32]	-12.17
1,4-Dioxane + $\text{C}_6\text{H}_6$	-0.444 [32]	-12.03
THF + $\text{C}_7\text{H}_8$	-1.33 [58]	-6.8
THP + $\text{C}_7\text{H}_8$	-0.98 [58]	-5.3
1,3-Dioxolane + $\text{C}_7\text{H}_8$	0.463 [58]	-10.63
1,4-Dioxane + $\text{C}_7\text{H}_8$	0.206 [58]	-9.74

<sup>a</sup> For symbols, see Table 1.

<sup>b</sup>  $T = 323.15\text{ K}$ .



lated from  $H_m^E$  data at 298.15 K and 313.15 K (see Table 2). Negative  $C_{pm}^E$  values are typical of mixtures characterized by dispersive interactions (e.g.,  $C_{pm}^E = -3.34 \text{ J mol}^{-1} \text{ K}^{-1}$  for the benzene + heptane system [47]). On the other hand, Table 4 reveals that orientational effects are more important at  $x_1 < 0.5$ , where  $X_{12}(x_1) > X_{12}(x_1 = 0.5)$  and the model overestimates interactions between unlike molecules. The opposite trend is encountered at  $x_1 > 0.5$ . In  $\text{CH}_3(\text{CH}_2)_{u-1}\text{O}(\text{CH}_2)_{v-1}\text{CH}_3$  or benzene + *n*-alkane mixtures, orientational effects are more relevant at low concentration of the ether and at high concentration of benzene, respectively. This could explain the large values (Table 4). The large  $\sigma_r(H_m^E)$  and  $\Delta_i$  values obtained for the diethylether mixture merely reflects that the model can not represent very asymmetric curves, as s-shaped ones, when the mixture compounds show close  $V_i$  and  $V_i^*$  values. The same occurs for the 1,4-dioxane + benzene system. This is a shortcoming of the model.

### 5.2. Linear polyether or acetal + benzene

The replacement of a linear monoether by a linear polyether of similar size leads to a  $H_m^E$  decrease which may be ascribed to interactions between unlike molecules become stronger in the latter mixtures (higher  $|\Delta H_{O-\text{aro}}|$  values, Table 5), in such way that the more negative  $\Delta H_{O-\text{aro}}$  contribution is prevalent over the more positive  $\Delta H_{O-O}$  term. This is consistent with the higher  $\bar{\mu}$  values of polyethers in comparison to those of monoethers. For example,  $\bar{\mu}$  (2,5-dioxahexane) = 0.653 [42]. The stronger ether–ether interactions in systems with polyethers are also supported by the fact that, at 298.15 K, the systems 2,5,8,11-tetraoxadodecane + dodecane or 2,5,8,11,14-pentaoxapentadecane + decane are close to their upper critical solution temperatures (280.81 K and 291.98 K respectively [48]). In addition, the larger etheric surface of polyethers makes easier the creation of the new ether–aromatic interactions upon mixing.

$H_m^E$  of solutions including  $\text{CH}_3(\text{CH}_2)_{u-1}\text{O}(\text{CH}_2\text{CH}_2\text{O})_v(\text{CH}_2)_{u-1}\text{CH}_3$ , decreases when  $u$  is increased for a given  $v$  value (Table 2). In the case of the longer ethers, this may be ascribed to a lower  $\Delta H_{O-O}$  contribution to  $H_m^E$  and not to stronger ether–benzene interactions. In fact,  $\bar{\mu}$  (3,6-dioxaoctane) = 0.525 [42]; in heptane solutions  $H_m^E(\text{J mol}^{-1}) = 889$  (3,6-dioxaoctane) [49] < 1285 (2,5-dioxahexane) [50], and  $\Delta H_{O-O}(\text{kJ mol}^{-1}) = 4.53$  (3,6-dioxaoctane), < 5.48 (2,5-dioxahexane) (Table 5). Similarly it may be explained the observed decrease of  $H_m^E$  when  $v$  is increased for a fixed  $u$  value.

It is known that proximity effects lead to a weakening of the interactions between ether molecules in mixtures with alkanes [51], as  $\bar{\mu}(\text{acetal}) < \bar{\mu}(\text{diether})$  (e.g.,  $\bar{\mu}$  (3,5-dioxahexane) = 0.421 [42]) and then  $\Delta H_{O-O}$  (3,6-dioxaoctane) >  $\Delta H_{O-O}$  (3,5-dioxahexane) = 2.42  $\text{kJ mol}^{-1}$  (Table 5). In solutions containing benzene, interactions between unlike molecules also become weaker when an acetal is replaced by a diether of similar size (Table 5). In this case, the lower  $|\Delta H_{O-\text{aro}}|$  term overcompensates the decrease of the  $\Delta H_{O-O}$  contribution and  $H_m^E$  increases (Table 2).

For linear polyether + heptane systems, we have previously obtained using Flory  $\sigma_r(H_m^E) = 0.055$  (2,5-dioxahexane); 0.065 (2,5,8-trioxanonane); 0.065 (3,6-dioxaoctane); 0.058 (2,4-dioxapentane); 0.039 (3,5-dioxahexane) = 0.039 [16]. These results are similar to those determined here for the benzene solutions (Table 2). Therefore, it may be concluded that the mixture structure is newly close to random mixing. Note that the  $\Delta_i$  values are lower than for the systems with linear monoethers (Table 4). The observed discrepancies for the 3,5-dioxahexane + benzene mixture may be related to experimental inaccuracies as the  $H_m^E$  curve is very shifted towards low  $x_1$  values of the acetal when is compared to that of the 2,4-dioxapentane solution.

### 5.3. Cyclic ether + benzene

For monoethers, cyclization, that is, the replacement of a linear ether by a homomorphic cyclic one, also implies decreased  $H_m^E$  values, which may be explained in the same terms as above. Ether–benzene interactions are stronger in solutions with cyclic ethers, and the more negative  $\Delta H_{O-\text{aro}}$  (Table 5) contribution is prevalent over the more positive  $\Delta H_{O-O}$  term. This is due to the  $\bar{\mu}$  values of tetrahydrofuran, 0.723, and of tetrahydropyran, 0.619, are larger than those of homomorphic linear ethers [42], and to the oxygen atom is less sterically hindered in cyclic molecules. Systems with diethers behave differently, depending on the considered oxaalkane. Note that  $H_m^E(\text{J mol}^{-1}) = -31$  (1,4-dioxane) [32] > -179 (2,5-dioxahexane) [34], which might be due to the  $\Delta H_{O-O}$  contribution becomes here more relevant. However, this seems to be no the case for the 1,3-dioxane mixture as the corresponding  $H_m^E$  value (-157  $\text{J mol}^{-1}$  [32] is expected to be lower than that of the homomorphic acetal. (See  $H_m^E$  values for mixtures with 2,4-dioxapentane, or 3,5-dioxahexane listed in Table 2.) This merely remarks the complex behaviour of systems with cyclic diethers. In terms of the classical UNIFAC model, it has been shown, on the basis on principles of unchanging geometry and approximate group electroneutrality, that new groups must be introduced to a correct description of systems with cyclic ethers [52–54]. A similar conclusion has been stated using DISQUAC [16,55].

Results from the Flory model for heptane mixtures are:  $\sigma_r(H_m^E) = 0.064$  (tetrahydrofuran); 0.062 (tetrahydropyran); 0.094 (1,3-dioxolane); 0.159 (1,3-dioxane); 0.071 (1,4-dioxane) [16]. For the systems with benzene,  $\sigma_r(H_m^E)$  substantially differs for systems including cyclic monoethers or cyclic diethers. For the former, orientational effects are weak, as it is indicated by low  $\sigma_r(H_m^E)$  and  $\Delta_i$  values (Tables 2 and 4), and then the random mixing hypothesis may be considered to be valid to a large extent. In contrast, the model predicts strong orientational effects in systems with 1,3-dioxolane or 1,4-dioxane. However, such effects are weak as it is revealed by low  $|H_m^E|$  (Table 2) and  $C_{pm}^E$  values. So,  $C_{pm}^E(\text{J mol}^{-1} \text{ K}^{-1}) = 1.18$  (1,3-dioxolane), 0.41 (1,4-dioxane) [33]. Moreover, the corresponding molar excess isochoric heat capacities,  $C_{vm}^E$ , are also low and positive, 0.70 and 0.55  $\text{J mol}^{-1} \text{ K}^{-1}$ , respectively [56]. This allows to conclude that the random mixing hypothesis is also a reasonable approximation for such solutions as, in terms of the Flory theory,  $C_{vm}^E = 0$  [57].

### 5.4. Ether + toluene

Ether–aromatic interactions are weaker in toluene mixtures, as the formation of such interactions is more difficult due to the smaller aromatic surface of toluene (Table 5). This means an increase of  $H_m^E$  which, in systems with cyclic monoethers, seems to be compensated by the decrease related to a lower  $\Delta H_{\text{aro-aro}}$  contribution in such way that  $H_m^E$  is practically independent of the aromatic compound, benzene or toluene. For cyclic diether + toluene systems  $H_m^E$  is higher as the decrease of the  $|\Delta H_{O-\text{aro}}|$  term is not compensated by the lower  $\Delta H_{\text{aro-aro}}$  contribution.

The  $\sigma_r(H_m^E)$  values show that the orientational effects are weak and that the mixture structure is here also similar to that of the systems examined above. Accordingly,  $C_{pm}^E$  is low for these solutions (1.59, 1.34, 1.98 and 1.10  $\text{J mol}^{-1} \text{ K}^{-1}$  for the systems with tetrahydrofuran tetrahydropyran, 1,3-dioxolane and 1,4-dioxane, respectively [58]).

Finally, it should be mentioned that the Kirkwood–Buff formalism [59–61] has been applied to determine the Kirkwood–Buff integrals,  $G_{ij}$ , and related magnitudes as linear coefficients of preferential solvation,  $\delta_{ij}$ , or local mole fractions,  $x_{ij}$ , for tetrahydrofuran

**Table A.1**

Molar excess enthalpies,  $H_m^E$ , at 298.15 K and equimolar composition for benzene + *n*-alkane systems. The Flory interaction parameter  $X_{12}$  calculated from  $H_m^E$  at equimolar composition, the interactional contribution,  $H_{m,int}^E$ , and variations of the  $X_{12}$  values,  $\Delta_1$  (Eq. (13)), obtained from  $H_m^E$  data at 298.15 are also included.

Alkane <sup>a</sup>	$H_m^E$ (J mol <sup>-1</sup> )	$X_{12}$ (J cm <sup>-3</sup> )	$H_{m,int}^E$ (J mol <sup>-1</sup> )	$\sigma_r(H_m^E)^b$	$\Delta_1$	$\Delta_2$
Hexane <sup>c</sup>	897	43.64	644	0.026	0.054	0.022
Octane <sup>d</sup>	969	44.13	710	0.047	0.048	0.098
Dodecane <sup>d</sup>	1101	46.90	846	0.063	0.073	0.102
Hexadecane <sup>d</sup>	1256	51.26	992	0.177	0.070	0.176

<sup>a</sup> Flory parameters for pure alkanes are taken from [3].

<sup>b</sup> Eq. (12).

<sup>c</sup> L. Romaní, M.I. Paz-Andrade, *An. Quim.* 70 (1974) 422–425.

<sup>d</sup> M. Díaz Peña, C. Mendiña, *J. Chem. Thermodyn.* 6 (1974) 387–393.

or 1,4-dioxane + benzene, or +toluene mixtures [32,62,63]. The low  $|G_{ij}|$  and  $|\delta_{ij}|$  values obtained lead to  $x_{ij}$  values which are very close to the bulk ones. Thus, the main conclusion of these studies is that such solutions hardly show any preferential solvation [32,62,63], which confirms our conclusions.

### 5.5. Molar excess volumes

For most of the systems listed in Table 3,  $V_m^E$  is negative indicating that the negative contributions to this excess function from interactions between unlike molecules and/or from structural effects are predominant over the positive contribution from the breaking of interactions between like molecules. We note that both magnitudes  $H_m^E$  and  $V_m^E$  show the same sign (negative) and change in the same sequence for cyclic ether + benzene mixtures: tetrahydrofuran < tetrahydropyran < 1,3-dioxane < 1,4-dioxane. This suggests that the contribution to  $V_m^E$  from interactions between unlike molecules is the more important. In contrast,  $H_m^E$  and  $V_m^E$  are both positive for dibutyl, or dioctyl ether + benzene systems, and the contribution to  $V_m^E$  from the disruption of interactions between like molecules becomes predominant. For 1,3-dioxolane or 1,4-dioxane + toluene,  $H_m^E > 0$  and  $V_m^E < 0$ , which points out that here structural effects are more relevant.

The observed discrepancies between experimental and calculated values could be rather easily analyzed in terms of the Prigogine–Flory version of the theory [64]. In this version of the model, the curvature term of  $V_m^E$  is proportional to  $-(\bar{V}_1 - \bar{V}_2)^2$ , and the so-called  $P^*$  term is proportional to  $(P_1^* - P_2^*)(\bar{V}_1 - \bar{V}_2)$ . Inspection of Table 3 shows that large discrepancies between theory and experiment are usually encountered when the  $P^*$  term is high in absolute value as for dibutylether + benzene, or tetrahydrofuran 1,3-dioxolane or 1,4-dioxane + toluene mixtures. In this case, the  $P^*$  contribution is positive and the theoretical  $V_m^E$  is higher than the experimental value. For the 2,5-dioxahexane, or 1,4-dioxane + benzene mixtures, the mentioned contribution is negative and the Flory results are lower than the experimental ones.

## 6. Conclusions

The relative variation of  $H_m^E$ , along homologous series, for ether + benzene, or +toluene systems has been discussed taking into account the contributions to  $H_m^E$  from ether–ether, aromatic–aromatic and ether–aromatic interactions. It has been shown that the increase of  $u$  ( $v$  fixed) in  $\text{CH}_3(\text{CH}_2)_{u-1}\text{O}(\text{CH}_2\text{CH}_2\text{O})_v(\text{CH}_2)_{u-1}\text{CH}_3$  + benzene mixtures leads to a weakening of interactions between unlike molecules. These interactions are also weakened by proximity effects. In contrast, the  $v$  increase ( $u$  fixed) or cyclization lead to stronger interactions between unlike molecules. From the application of the Flory model, it is concluded that orientational effects are weak in the investigated systems, in such way that the mixture structure is close to random mixing. The theory predicts strong orientational

effects for 1,3-dioxolane, or 1,4-dioxane + benzene solutions, but this has been attributed to the theory cannot describe asymmetric  $H_m^E$  curves when the mixture compounds show close  $V_i$  and  $V_i^*$  values. Conclusions are confirmed by previous calculations on the basis of the Kirkwood–Buff integrals formalism.

## 7. List of symbols

$C_p$	heat capacity at constant pressure
$H$	molar enthalpy
$\Delta H$	contribution to the molar excess enthalpy (three types are considered; ether–ether, aromatic–aromatic and ether–aromatic)
$P$	pressure
$P^*$	reduction parameter for pressure in the Flory theory
$T$	temperature
$T^*$	reduction parameter for temperature in the Flory theory
$V$	molar volume
$V^*$	reduction parameter for volume in the Flory theory
$x$	mole fraction
$X_{12}$	interaction parameter in the Flory theory

### Greek letters

$\bar{\mu}$	effective dipole moment
$\sigma_r$	relative standard deviation (Eq. (12))

### Superscripts

E	excess property
$\infty$	property at infinite dilution

### Subscripts

$i$	mixture compound ( $i = 1, 2$ )
m	molar property

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## Appendix A.

See Table A.1.

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