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# Thermodynamic assessment of the In-Ir system in the In rich part

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# 1. Introduction

The last few years, the binary indium compounds (such as InP, InAs, and InSb) have been largely investigated due to their important technological properties. Belonging to the A<sup>III</sup>-B<sup>V</sup> semiconductors, they have applications in electronic and optoelectronic devices. In order to found out which elements are stable in contact with the III-V semi-conductor, ternary M-III-V (with M = metal) phase diagrams such as In-As-Ir, In-Sb-Ir are necessary to be assessed. Yet before, the low-order systems must be mandatory determined. The In-Ir binary system has not been genuinely studied experimentally [1–5]. The phase diagram available in the literature is not complete [6–8]. The In rich part, up to x(Ir) = 0.5, has been reviewed since 1998 [9-12]. Two intermetallic compounds have been identified as In<sub>3</sub>Ir and In<sub>2</sub>Ir. Their crystal structures, determined by refinement of X-ray diffraction diagrams are reliable. In<sub>2</sub>Ir has two crystallographic independent iridium networks with stronger interaction within and weaker one between the networks. It is a good metallic conductor and Pauli paramagnet [13]. Thermodynamic properties have been determined in particular for the liquid phase [11,12]. As regards the two intermetallic compounds, only the enthalpy of formation of In<sub>3</sub>Ir measured by high temperature drop calorimetry [14] is reliable. Because of the large differences in the melting temperatures of In (429K) and Ir (2723 K), the evaporation of In must be accurately controlled

# ABSTRACT

Optimization by the CALPHAD method of the thermodynamic parameters of the In–Ir system has been carried out using the experimental phase diagram data and thermodynamic properties. The numerous experimental data of the liquid phase determined in the 0 < x(Ir) < 0.35 composition range by two authors are coherent and associated with the scarce enthalpies of formation of the two intermetallic compounds allowed to optimize a set of coherent thermodynamic parameters in order to calculate the phase diagram in the In rich part. In the  $0.40 < x(Ir) \le 1$  composition range, the phase diagram seems more complex than the schematic part extrapolated at high temperature and the agreement between the calculated diagram and this extrapolated experimental part is not satisfactory. Further experimental investigations are needed to improve the calculation in this composition range, but which are difficult because hampered by different phenomena.

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and taken into account during the experimental determinations. In addition, the sluggishness of the equilibration may hamper these experiments. As no thermodynamic assessment was performed before, the aim of the present work was to optimize a set of consistent thermodynamic parameters of the different phases of the In–Ir system by the CALPHAD method [15] which will serve later to assess ternary systems M–In–Ir.

#### 2. Experimental data

#### 2.1. Phase diagram data

The shape of the phase diagram has first been drawn by Moffat [6] in comparison to the one of the Co–In system which displays two definite compounds CoIn<sub>3</sub> and CoIn<sub>2</sub> melting incongruently and a miscibility gap with a very high critical temperature. The liquidus part Lig/Lig + In<sub>3</sub>Ir was determined using differential calorimetry by Schubert et al. [1,2] between 600 and 1250 K, as well as the existence of two intermetallic compounds In<sub>3</sub>Ir and In<sub>2</sub>Ir, Table 1, reported later by Ellner and Bhan [5]. Schubert et al. [1,2] also determined a eutectic reaction Liq  $\leftrightarrow$  In tetragonal\_A6+In<sub>3</sub>Ir and two peritectic reactions  $\text{Liq} + \text{In}_2\text{Ir} \leftrightarrow \text{In}_3\text{Ir}$  and  $\text{Liq} + (\text{Ir}) \leftrightarrow \text{In}_2\text{Ir}$  in the  $0 \le x(Ir) < 0.5$  composition range. The solubility of iridium in indium in the temperature range 600-1240 K has been measured by Dieva [4]. Two data of the Liq/Liq + In<sub>3</sub>Ir liquidus part were assessed by Anres et al. [11] by calorimetric measurements in good agreement with the data of Schubert [1,2], and three data of the Liq/Liq + In<sub>2</sub>Ir liquidus part. By differential thermal analysis Anres et al. [11] measured the temperatures of the eutectic (about 1258 K) and peritectic

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Table 1	
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Symbols and crystal structures of the solid phases in the In–Ir al	oys.
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Diagram symbol	Composition at % Ir	Symbol use in Thermo-Calc data file	Pearson symbol [24]	Space group	Strukturbericht designation	Prototype
In	0	Tetragonal_A6	tl2	I4/mmm	A6	In
In₃Ir_HT	25	In <sub>3</sub> Ir_HT	tP16	$P4_2/mnm$		FeGa <sub>3</sub>
In <sub>3</sub> Ir_LT	25	In <sub>3</sub> Ir_LT	oP16	Pnma		CrFe <sub>3</sub>
In <sub>2</sub> Ir	33.33	In <sub>2</sub> Ir	oF48	Fddd		CuMg <sub>2</sub>
In <sub>54</sub> Ir <sub>46</sub>	46	Metastable				
Ir	100	FCC_A1	cF4	Fm3m	A1	Cu

(about 1463 K) reactions and pointed out the difficulty to reach the (solid + liquid) equilibrium. A change of structure LT  $\leftrightarrow$  HT was noticed at 625 K for In<sub>3</sub>Ir.

New experimental phase diagram data assessed by Flandorfer et al. [12] based on X-ray diffraction, Electron Probe Microscopy Analysis (EPMA) and Differential Thermal Analysis (DTA) was published in 2002. A metastable phase  $In_{54}Ir_{46}$  was found. A small homogeneity range was determined for the  $In_2Ir$  and  $In_3Ir$  phases. For this latter phase, a metatectic reaction was suggested as  $In_3Ir_HT <->$  Liq+ $In_3Ir_LT$ , at temperatures below 625 K [11] or  $620 \pm 3$  K [12], as well as a peritectoïd reaction  $In_2Ir + In_3Ir_HT <->$  $In_3Ir_LT$  at  $636 \pm 3$  K [12]. The temperatures of all the invariant reactions were indicated for  $0 \le x$  (Ir)  $\le 0.5$ . A (Ir) fcc solid solution with a very small amount of In (0.01%) was also mentioned. The new phase diagram drawn by [12] with the above more recent experimental data is shown in Fig. 1. Beyond x(Ir) > 0.4, the liquidus is unknown and drawn with a dashed line as well as the two-phase domain (Liq+(Ir)).

#### 2.2. Thermodynamic data

The integral and partial molar enthalpies of mixing of the liquid phase have been first determined by Anres et al. [11] using the direct drop method with a high temperature calorimeter in the



Fig. 1. The In-Ir phase diagram drawn by Flandorfer et al. [12].

temperature range 1175-1589 K for 0 < x(Ir) < 0.26, and at 1154 K and for  $0 < x(Ir) \le 0.02$ . In and Ir purities were 99.99 wt %. The errors in the enthalpies of mixing and in the molar fraction x(Ir) were, respectively, assessed at about  $\pm 4\%$  and less than  $\pm 1\%$ . They indicated that the enthalpy of mixing of the liquid phase seems not be temperature dependent within the experimental error in the temperature and molar fraction ranges studied. They found that at 1154 K the limiting partial molar enthalpy of mixing of hypothetically supercooled liquid iridium in liquid indium is equal to  $-50 \pm 2$  kJ/mol.

Later on, Flandorfer et al. [12] determined the integral enthalpies of mixing of the liquid phase by means of a high temperature drop calorimeter in the 1463-1663 K temperature range. They claimed that the limiting partial enthalpy of mixing of liquid Ir in liquid In (about -50 kJ/mol) does not depend significantly on temperature, while the integral enthalpy of mixing of the liquid phase, which reaches -12 to -15 kJ/mol, depends on temperature. A liquid miscibility gap, as earlier suggested in the literature [6], which would need that the Gibbs energy of mixing of the liquid phase becomes positive, was excluded. On the other hand, authors of [11] indicated the possibility of the existence of a liquid-liquid miscibility gap because the extremum of the curve  $\Delta_{mix}H_m^0 = f(x_{(Ir)})$  is one of the less exothermic ones for the alloy series consisting of a group VIII transition metal and a sp metal (Ga or In essentially) and moreover of the great similarity observed between the Co-In and In-Ir systems.

The theoretical values predicted by the Miedema's model were 0J/mol for the integral enthalpy of mixing of the liquid phase for x(Ir) = 0.5 and -1 J/mol for the limiting partial molar enthalpy of dissolution of Ir in In and In in Ir [16]. Molar enthalpies of formation of the intermetallic compounds have been determined by [11] on the basis of the plots of the integral enthalpies of mixing of the liquid phase versus x(Ir) drawn at 1175 K for In<sub>3</sub>Ir, and at 1204, 1282 and 1359 K for In<sub>2</sub>Ir, according to the respective reactions:

 $3In(liq) + Ir(liq) \rightarrow In_3Ir (sol)$  $2In(liq) + Ir(liq) \rightarrow In_2Ir (sol).$ 

The values were  $-9 \pm 2 \text{ kJ/mol}$  and  $-14 \pm 2 \text{ kJ/mol}$ , respectively. Another measurement of the molar enthalpy of formation of In<sub>3</sub>Ir was made in 2002 by Meschel and Kleppa [14] in the case of the determination of standard enthalpies of formation of some transition metal-indium compounds by high temperature direct synthesis calorimetry. For In<sub>3</sub>Ir\_HT the average value of six or seven consecutive measurements with the appropriate standard deviation obtained was  $-23.8 \pm 2.4$  kJ/mol of atoms at  $1273 \pm 2$  K. The pattern of In<sub>3</sub>Ir matched well with the generated pattern by Xray diffraction. No unreacted metals or secondary phases were detected [14]. So, this experimental procedure is more reliable that the extrapolation method used by Anres et al. [11] (data derived on the basis of the precipitation of solid compounds from the liquid marked by kinks on the curve of the integral enthalpy of mixing of the liquid phase versus x(Ir) which can have an important uncertainty.

Let us remind that the theoretical values predicted by the semi-empirical model of Miedema and co-workers [16] at 298.15 K were, respectively, -10 kJ and -13 kJ/mol of atoms for  $\text{In}_3\text{Ir}$  and  $\text{In}_2\text{Ir}$ .

Anres et al. [11] also determined the molar heat capacities between 423 and 763 K for three alloys of x(Ir) composition equal to 0.186, 0.25 and 0.33.

## 3. Thermodynamic models

#### 3.1. Pure elements

The Gibbs energy function (298.15 K) for the element *i* (*i* = In, Ir) in the  $\phi$  phase ( $\phi$  = liquid, tetragonal\_A6 or FCC\_A1) is described by an equation of the following form:

$$G_i^{\phi}(T) = a + bT + cT \ln T + dT^2 + eT^3 + fT^7 + gT^{-1} + hT^{-9}$$
(1)

In this paper, the Gibbs energy functions are taken from the SGTE compilation of Dinsdale [17]. These functions are, respectively, valid up to T = 3800 K and 4000 K for In and Ir.

#### 3.2. Solution phases

The Gibbs energy of one mole of formula unit is expressed as the sum of three terms:

$$G^{\text{liq}} - H^{\text{SER}} = {}^{\text{ref}}G^{\text{liq}} + {}^{\text{id}}G^{\text{liq}} + {}^{\text{ex}}G^{\text{liq}}$$
(2)

$${}^{\text{ref}}G_{\text{liq}} = x_{\text{ln}} \left[ {}^{0}G_{\text{ln}}^{\text{liq}} - H_{\text{ln}}^{\text{SER}} \right] + x_{\text{lr}} \left[ {}^{0}G_{\text{lr}}^{\text{liq}} - H_{\text{lr}}^{\text{SER}} \right]$$
(3)

where  $H_i^{\text{SER}}$  (298.15K) is the molar enthalpy of the *i* element at 298.15K in its Standard Element Reference (SER) state, tetragonal\_A6 for In and FCC\_A1 for Ir.

$${}^{10}G_{liq} = RT(y_{ln} \ln y_{ln} + y_{lr} \ln y_{lr})$$
(4)

where *R* is the ideal gas constant; *T* is the temperature, in Kelvin;  $x_{In}$  and  $x_{Ir}$  are the mole fraction of the elements In and Ir, respectively.

The  $e^{x}G^{liq}$  energy part in Eq. (2) is given by the Redlich–Kister polynomial [18]

$${}^{\text{ex}}G_{\text{liq}} = y_i y_j \sum_{\lambda=0}^{\lambda} {}^{\lambda} L_{i,j}^{\text{Liq}} (y_i - y_j)^{\lambda}$$
(5)

with *i* and *j* are indices which correspond to the two species In and Ir.

The binary interaction parameters of the  ${}^{\lambda}L_{i,j}^{\text{Liq}}$  type, assessed in the present work, were temperature dependent as follows:

$$^{\lambda}L_{i\,i}^{\mathrm{Liq}} = a_{\lambda} + b_{\lambda}T\tag{6}$$

 $a_{\lambda}$  and  $b_{\lambda}$  are the coefficients to be optimized.

The tetragonal A6 and FCC A1 phases were, respectively, modelled as pure In because of the unknown and certainly very low solubility of Ir in In and as a solution phase (Ir).

#### 3.3. Stoichiometric compounds and intermediate phases

In<sub>3</sub>Ir and In<sub>2</sub>Ir were first considered as stoichiometric compounds, their Gibbs energy noted as  ${}^{0}G_{ApBq}$  was expressed as follows:

$${}^{0}G_{ApBq} = \frac{p}{p+q} {}^{0}G_{A} + \frac{q}{p+q} {}^{0}G_{B} + a + bT$$
(7)

where  ${}^{0}G_{A}$  and  ${}^{0}G_{B}$  are the Gibbs energy of the pure elements In and Ir, respectively; *a* and *b* are parameters to be determined.

As the  $In_3Ir$  and  $In_2Ir$  intermetallic compounds have an experimental small homogeneity range [12], in a second step, they were treated by a two-sublattice model. The experimental extension of  $In_3Ir$  is towards the In rich part (substoichiometric compound) while the one of  $In_2Ir$  is from one part to another of the stoichiometric composition, so the respective modelling were as follows:  $(In)_{0.75}(In,Ir\%)_{0.25}$  and  $(In\%,Ir)_{0.6667}(In,Ir\%)_{0.3333}$ . The symbol % denotes the major component in the considered sublattice.

The Gibbs energy function per mole (m) of the formula unit  $(In)_{0.75}(In,Ir\%)_{0.25}$  is the following:

$$G^{0.75\ln 0.25 \text{Ir}} - H^{\text{SER}}_{0.75\ln 0.25 \text{Ir}} = y^{1}_{\text{In}} y^{2}_{\text{In}} G^{\ln:\ln} + y^{1}_{\text{In}} y^{2}_{\text{Ir}} G^{\ln:\ln} + RT \left[ 0.75 y^{1}_{\text{In}} \ln y^{1}_{\text{In}} + 0.25 (y^{2}_{\text{In}} \ln y^{2}_{\text{In}} + y^{2}_{\text{Ir}} \ln y^{2}_{\text{Ir}}) \right] + {}^{\text{xs}}G_{\text{m}}$$
(8)

$$H_{\text{In0.75Ir0.25}}^{\text{SER}} = 0.75H_{\text{In}}^{\text{SER}} + 0.25H_{\text{Ir}}^{\text{SER}}$$
(9)

where  $y_{In}^1 = 1$  denotes the site fraction of Indium in the first sublattice,  $y_{In}^2$  and  $y_{Ir}^2$  the site fractions of indium and iridium in the second sublattice,  ${}^0G^{In0.75In0.25}$  is the Gibbs energy of the hypothetical compound In<sub>0.75</sub>In<sub>0.25</sub>.

 ${}^{xs}{G}^{\lambda}_m$  is the excess Gibbs energy expressed by the following expression:

$${}^{KS}G_{\rm m}^{\lambda} = y_{\rm In}^2 y_{\rm Ir}^2 (L_{\rm In:In,Ir}^{\lambda})$$
 (10)

where  $L_{\text{In:In,Ir}}^{\lambda}$  represents the interaction parameters between the elements In and Ir in the second sublattice while the first sublattice is only occupied by the element In. These excess parameters are temperature dependent as:

$$L_{\rm In:In,Ir}^{\lambda} = a_{\lambda} + b_{\lambda}T \tag{11}$$

In order to avoid the occurrence of the hypothetical compound  $In_pIn_q$  or  $Ir_pIr_q$  during the phase diagram calculation, the value +5000 J/mol of atoms was added to the functions GHSERIn and GHSERIr, see Tables 2 and 4.

The Gibbs energy function per mole (m) of the formula unit  $(In\%,Ir)_{0.6667}(In,Ir\%)_{0.3333}$  is the following:

$$G^{0.6667\ln 0.3333 \text{lr}} - H^{\text{SER}}_{0.6667\ln 0.3333 \text{lr}} = y^{1}_{\ln} y^{2}_{\Gamma} G^{\ln:: \ln} + y^{1}_{\ln} y^{2}_{\Gamma} G^{\text{c} \text{lr}: 1r} + y^{1}_{\ln} y^{2}_{\ln} G^{\text{c} \text{lr}: 1r} + y^{1}_{\ln} y^{2}_{\ln} G^{\text{c} \text{lr}: 1r} + y^{1}_{\ln} y^{2}_{\ln} G^{\text{c} \text{lr}: 1r} + RT \left[ 0.6667 \left( y^{1}_{\ln} \ln y^{1}_{\ln} + y^{1}_{\ln} \ln y^{1}_{\ln} \right) + 0.3333 \left( y^{2}_{\ln} \ln y^{2}_{\ln} + y^{2}_{\ln} \ln y^{2}_{\ln} \right) \right] + {}^{\text{xs}}G_{\text{m}}$$
(12)

with the same symbols as in [Eq. (8)].

#### 4. Results and discussions

The optimization of the interaction parameters were carried out by taking into account all the relevant experimental data which are detailed in Section 2. But, in order to avoid the occurrence of an unwanted inverted miscibility gap in the liquid phase during the calculation of the phase diagram, additional constraints  $\partial^2 G/\partial x^2 > 0$ in the whole Ir composition range (every  $\Delta x(Ir) = 0.025$ ) and at different temperatures (every  $\Delta T = 25$  K) between 1200 and 4000 K were imposed as previously in other systems [19–21]. The hypothesis of no miscibility gap in the In–Ir system was supported by the reasons argued by [12]. The modelling of the system was performed according to the CALPHAD method [15] with the Thermo-Calc software [22] and the assessment was carried out using the Parrot module [23] of this package.

The optimization was made in several steps.

1. *First* the thermodynamic parameters of the liquid phase were optimized using the numerous and negative integral and scarce partial experimental enthalpies of mixing [11,12]. In the Parrot module, we attributed the weight of 1 to all the experimental data measured up to x(Ir)=0.35. The other data were discarded because they concerned a two-phase (liquid + compound) domain. Four excess parameters of the Redlich–Kister equation [18] were optimized. The minimum of the curve of the integral enthalpy of mixing of the liquid phase versus the Ir molar fraction was calculated at about -20 kJ/mol and x(Ir)=0.5. We concluded than no

Fable	2		

	The optimized th	hermodynamic pa	ameters of the In-Ir	system (second	l optimization,	Section 2.2
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Phase	Thermodynamic model	Parameters (units in J/mol atom and J/mol atom K)
Liquid	(ln,lr) <sub>1</sub>	${}^{0}L = -78500$ ${}^{1}L = +16000$ ${}^{2}L = +22000$ ${}^{3}L = -11000$
FCC_A1	(In,Ir)1 (Va)1	${}^{0}L_{\text{In,Ir:Va}}^{\text{FCC-A1}} = -10000$ ${}^{1}L_{\text{FCC-A1}}^{\text{FCC-A1}} = 500$
In <sub>3</sub> Ir_LT	(In) <sub>0.75</sub> :(In,Ir) <sub>0.25</sub>	$G_{\ln n \ln}^{\ln n + LT} - H_{\ln}^{\text{Tetragonal} - A6} = \text{GHSERIn} + 5000$
		$G_{\text{ln:lr}}^{\text{ln}_{2}\text{lr}_{-}\text{LT}} - 0.75*H_{\text{ln}}^{\text{Tetragonal_A6}} - 0.25*H_{\text{lr}}^{\text{FCC_A1}} = 0.75*\text{GHSERIn} + 0.25*\text{GHSERIr} - 24900 + 4.378*T_{\text{ln}} + 0.25*\text{GHSERIr} + 0.25$
		${}^{0}L_{\text{In:In,Ir}}^{\text{In}} = -2000$
In <sub>3</sub> Ir_HT	(In) <sub>0.75</sub> :(In,Ir) <sub>0.25</sub>	$G_{\text{ln:ln}}^{\text{ln_2Ir},\text{HT}} - H_{\text{ln}}^{\text{Tetragonal},\text{A6}} = \text{GHSERIn} + 5000$
		$G_{\text{ln:lr}}^{\text{ln}_2\text{lr},\text{HT}} - 0.75 * H_{\text{ln}}^{\text{Tetragonal},\text{A6}} - 0.25 * H_{\text{lr}}^{\text{FCC},\text{A1}} = 0.75 * \text{GHSERIn} + 0.25 * \text{GHSERIr} - 23800 + 2.645 * T$
		${}^{0}L_{\text{In:In,Ir}}^{\text{in:Jir.HT}} = -2700$
In <sub>2</sub> Ir	(In,Ir) <sub>0.6667</sub> :(In,Ir) <sub>0.3333</sub>	$G_{\text{ln:In}}^{\text{In}} - H_{\text{ln}}^{\text{Tetragonal}\_A6} = \text{GHSERIn} + 5000$
		$G_{\mathrm{lr};\mathrm{lr}}^{\mathrm{ln}_{2}\mathrm{lr}} - H_{\mathrm{lr}}^{\mathrm{FCCA1}} = \mathrm{GHSERIr} + 5000$
		$G_{ln;lr}^{ln_2lr} - 0.6667 * H_{lr}^{Tetragonal\_A6} - 0.3333 * H_{lr}^{FCC\_A1} = 0.6667 * GHSERIn + 0.3333 * GHSERIr - 26500 + 1.681 * T_{lr}^{Tetragonal\_A6} - 0.3333 * H_{lr}^{FCC\_A1} = 0.6667 * GHSERIn + 0.3333 * GHSERIr - 26500 + 1.681 * T_{lr}^{Tetragonal\_A6} - 0.3333 * H_{lr}^{FCC\_A1} = 0.6667 * GHSERIn + 0.3333 * GHSERIr - 26500 + 1.681 * T_{lr}^{Tetragonal\_A6} - 0.3333 * H_{lr}^{FCC\_A1} = 0.6667 * GHSERIn + 0.3333 * GHSERIr - 26500 + 1.681 * T_{lr}^{Tetragonal\_A6} - 0.3333 * H_{lr}^{FCC\_A1} = 0.6667 * GHSERIn + 0.3333 * GHSERIr - 26500 + 1.681 * T_{lr}^{Tetragonal\_A6} - 0.3333 * H_{lr}^{FCC\_A1} = 0.6667 * GHSERIn + 0.3333 * GHSERIr - 26500 + 1.681 * T_{lr}^{Tetragonal\_A6} - 0.3333 * GHSERIr + 0.3333 * GHSERIr + 0.3333 * GHSERIr + 0.6667 * GHSERIn + 0.3333 * GHSERIr + 0.6607 * GHSERIr + 0.6667 * GHSERIr + 0.667 * GHSERIr + 0.6667 * GHSERIr + 0.667 * GHSERIr + 0.6667 * GHSERIr + 0.667 * GHSERIr + 0.6667 * GHSERIr + 0.667 * GHSERIr + 0.6667 * GHSERIr + 0.667 * GHSERIr + 0.667 * 0.667 * 0.667 * 0.667 * 0.667 * 0.667 * 0.667 * 0.667 * 0.667 * 0.667 * 0.667 * 0.667 * 0.667 * 0.667 * 0.667 * 0.667 * 0.667 * 0.667 * 0.667 * 0.677 * 0$
		$G_{\rm lr;In}^{\rm ln_2lr} - 0.6667 * H_{\rm lr}^{\rm FCC\_A1} - 0.3333 * H_{\rm ln}^{\rm Tetragonal\_A6} = 0.6667 * {\rm GHSERIr} + 0.3333 * {\rm GHSERIn} + 10000 + 26500 - 1.681 * T_{\rm ln}^{\rm CC\_A1} - 0.3333 * H_{\rm ln}^{\rm Tetragonal\_A6} = 0.6667 * {\rm GHSERIr} + 0.3333 * {\rm GHSERIn} + 10000 + 26500 - 1.681 * T_{\rm ln}^{\rm CC\_A1} - 0.3333 * H_{\rm ln}^{\rm Tetragonal\_A6} = 0.6667 * {\rm GHSERIr} + 0.3333 * {\rm GHSERIn} + 10000 + 26500 - 1.681 * T_{\rm ln}^{\rm CC\_A1} - 0.3333 * H_{\rm ln}^{\rm Tetragonal\_A6} = 0.6667 * {\rm GHSERIr} + 0.3333 * {\rm GHSERIn} + 10000 + 26500 - 1.681 * T_{\rm ln}^{\rm CC\_A1} - 0.3333 * {\rm GHSERIn} + 10000 + 26500 - 1.681 * T_{\rm ln}^{\rm CC\_A1} - 0.3333 * {\rm GHSERIn} + 10000 + 26500 - 1.681 * T_{\rm ln}^{\rm CC\_A1} - 0.3333 * {\rm GHSERIn} + 10000 + 26500 - 1.681 * T_{\rm ln}^{\rm CC\_A1} - 0.3333 * {\rm GHSERIn} + 10000 + 26500 - 1.681 * T_{\rm ln}^{\rm CC\_A1} - 0.3333 * {\rm GHSERIn} + 10000 + 26500 - 1.681 * T_{\rm ln}^{\rm CC\_A1} - 0.3333 * {\rm GHSERIn} + 10000 + 26500 - 1.681 * T_{\rm ln}^{\rm CC\_A1} - 0.3333 * {\rm GHSERIn} + 10000 + 26500 - 1.681 * T_{\rm ln}^{\rm CC\_A1} - 0.3333 * {\rm GHSERIn} + 10000 + 26500 - 1.681 * T_{\rm ln}^{\rm CC\_A1} - 0.3333 * {\rm GHSERIn} + 10000 + 26500 - 1.681 * T_{\rm ln}^{\rm CC\_A1} - 0.3333 * {\rm GHSERIn} + 10000 + 26500 - 1.681 * T_{\rm ln}^{\rm CC\_A1} - 0.3333 * {\rm GHSERIn} + 10000 + 26500 - 1.681 * T_{\rm ln}^{\rm CC\_A1} - 0.3333 * {\rm GHSERIn} + 10000 + 26500 - 1.681 * T_{\rm ln}^{\rm CC\_A1} - 0.3333 * {\rm GHSERIn} + 10000 + 26500 - 1.681 * T_{\rm ln}^{\rm CC\_A1} - 0.3333 * {\rm GHSERIn} + 10000 + 26500 - 1.681 * T_{\rm ln}^{\rm CC\_A1} - 0.3333 * {\rm GHSERIn} + 10000 + 26500 - 1.681 * T_{\rm ln}^{\rm CC\_A1} - 0.3333 * {\rm GHSERIn} + 0.3333 * {\rm GHS$
		${}^{0}L_{\text{In-lin,Ir}}^{\text{In-2}\text{Ir}} = -14000 + 6 * T$
		${}^{0}L_{\text{In,Ir:Ir}}^{\text{In}} = +16200 + 1 * T$

(Va) for vacancy.

temperature dependence was necessary as previously indicated by Anres et al. [11].

Fig. 2 shows the very good agreement between the calculated integral enthalpies of mixing of the liquid phase and experimental data of [11,12] up to x(Ir) equal to about 0.35 where only the liquid phase exists. Indeed, when x(Ir) > 0.35 the difference between the calculated integral enthalpies of mixing of the liquid phase and the experimental data of Refs. [11,12] increases. This is due to the precipitation of a solid phase [11,12] revealed by kinks on some experimental curves and then the measured data concern a two-phase domain (liquid + In<sub>3</sub>Ir) or (liquid + In<sub>2</sub>Ir). The temperatures and compositions of these kinks were identified as liquidus data information by [12].

The four excess parameters of the liquid phase optimized in the present work are similar to the ones by [11] but slightly different because in addition of the data of [11], we took into account the data determined by [12]. Fig. 3 shows the reasonable agreement, within the experimental error bar, between the calculated partial enthalpies of formation of the liquid phase and the experimental data. No temperature dependence is noticed. The calculated limiting partial molar enthalpy of mixing of liquid iridium in liquid indium is equal to -50 kJ/mol.

2. The second step of the optimization was relative to the optimization of the enthalpies of formation of the intermetallic compounds. As the experimental data are different from one another, we had to test each one separately. No composition range was first assumed for  $In_3Ir$  and  $In_2Ir$ . We used the liquidus data



**Fig. 2.** Calculated and experimental integral molar enthalpies of mixing of the liquid phase. The error bar is  $\pm 4\%$  (|) for  $\Delta_{mix}H_m^0$  and  $\pm 1\%$  (–) for  $x_{lr}$ .



**Fig. 3.** Calculated and experimental partial enthalpies of mixing of the liquid phase. The error bar on the partial enthalpy of mixing was evaluated at about  $\pm 4\%$  by [11].



**Fig. 4.** Comparison of the complete In–Ir phase diagram calculated with the thermodynamic parameters optimized during the second step of the optimization, Table 2, with experimental data.

[1,2,11,12], the temperature and the Ir composition of the liquid phase involved in the eutectic and peritectic invariant reactions, the experimental enthalpies of formation of  $In_3Ir$  and  $In_2Ir$  as well as the Cp values determined by Anres et al. [11].

We kept as valuable the values of the excess parameters of the liquid phase optimized in the first step.

#### 4.1. Test of the data of Anres et al. [11]

We first used as initial values (at 298.15 K with the reference state In tetragonal\_A6, Ir FCC\_A1), the values  $[a_i, Eq. (7)]$  of the respective enthalpies of formation (-0.651 and -5.735 kJ/mol) of the two intermetallic compounds recalculated on the basis of the available molar ones of the In<sub>3</sub>Ir and In<sub>2</sub>Ir compounds (-9 and -14 kJ.mol, extrapolated at T = 1175 K by Anres et al. [11] with the reference state In and Ir liquid at 1175 K). No temperature parameter  $[b_i, Eq.$ (7)] was considered. The above enthalpies of formation of the two intermetallic compounds In<sub>3</sub>Ir and In<sub>2</sub>Ir used to describe the phase diagram are not enough negative to allow their stability at high temperatures, and the liquid was stable down to 0 °C in the central part of the diagram.

#### Table 3

Invariant reactions in the In-Ir system calculated after the second step of optimization (Section 2.2).



**Fig. 5.** Comparison of the In–Ir phase diagram in the In rich part (calculated on the basis of the thermodynamic parameters optimized during the second step of the optimization, Table 2) with the experimental data.

Then we used as initial values  $[a_i, Eq. (7)]$ , the recalculated values at 298.15K (-2.651 and -7.397 kJ/mol) from the higher negative values of the respective enthalpies of formation of the two compounds within the error bar ( $\pm 2 \text{ kJ/mol}$ ) indicated by Anres et al. [11], i.e. -11 (In<sub>3</sub>Ir) and -16 kJ/mol (In<sub>2</sub>Ir), and no temperature dependence  $[b_i, Eq. (7)]$  was assumed. Once again, the liquid was stable down to 0 °C in the central part of the diagram. Only one invariant reaction was calculated (Liq  $\leftrightarrow \ln + \ln_2 \ln$ ). As mentioned above in the paragraph, the enthalpies of formation of In<sub>3</sub>Ir and In<sub>2</sub>Ir are not yet enough negative to allow their stability at high temperatures.

## 4.2. Test of the data of Meschel and Kleppa [14]

We used the enthalpy of formation of the In<sub>3</sub>Ir\_HT compound  $(-23.8 \pm 2.4 \text{ kJ/mol}, \text{ reference states SER at 298.15 K})$  measured by Meschel and Kleppa [14] and optimized the ones of In<sub>3</sub>Ir\_LT and In<sub>2</sub>Ir. We took into account the small homogeneity range determined by EPMA [12], for the In<sub>3</sub>Ir (0.238–0.25 Ir) and In<sub>2</sub>Ir (0.314–0.343 Ir) phases. In addition, the experimental structural transformation In<sub>3</sub>Ir\_LT  $\leftrightarrow$  In<sub>3</sub>Ir\_HT at 625 K was assumed. A coher-

	*	,		
Reactions	<i>T</i> (°C)	Phase <i>x</i> (Ir)	T (°C)	Phase <i>x</i> (Ir)
	[Ref.]	[Ref.]	Thiswork	This work
$Liq \Leftrightarrow In + In_3 Ir_LT$	156±2[12]	In <sub>3</sub> Ir_LT	156.8	Liq 3.41E-08
	$156.64 \pm 0.02$ [11]	0.238-0.25 [12]		In 0.0000
				In <sub>3</sub> Ir_LT 0.2424
In₃Ir_HT ⇔ Liq + In₃Ir_LT	347±3[12]	In <sub>2</sub> Ir	347.0	Liq 3.71E-05
	352 [11]	0.314-0.343		In <sub>3</sub> Ir_LT 0.2425
		[12]		In3Ir_HT 0.2386
$In_2Ir + In_3Ir_HT \Leftrightarrow In_3Ir_LT$	363±3[12]		361.7	In <sub>2</sub> Ir 0.3278
				In <sub>3</sub> Ir_HT 0.2500
				In <sub>3</sub> Ir_LT 0.2500
$Liq + In_2Ir \Leftrightarrow In_3Ir_HT$	981±3[12]		981	Liq 0.0976
	985 [11]			In <sub>2</sub> Ir 0.2934
				In3Ir_HT 0.2442
$Liq \Leftrightarrow In_2Ir$			1190	Liq 0.3300
				In <sub>2</sub> Ir 0.3300
$Liq \Leftrightarrow In_2Ir + (Ir)$	$1188 \pm 5$ [12]		621.1	Liq 0.5984
	1190 [11]			In <sub>2</sub> Ir 0.3414
				(Ir) 0.9752

#### Table 4

Optimized thermodynamic parameters to reproduce the experimental phase diagram drawn by Flandorfer et al. [12], third optimization.

Phase	Thermodynamic model	Parameters (units in J/mol atom and J/mol atom K)
Liquid	(In,Ir) <sub>1</sub>	${}^{0}L = -6500$ ${}^{1}L = -15000$ ${}^{2}L = -7000$ ${}^{3}L = -2000$
FCC_A1	$(In,Ir)_1 (Va)_1$	${}^{0}L_{\text{In,Ir,VA}}^{\text{FCC.A1}} = 35000 + 8 * T$
		$L_{\rm In, Ir; Va}^{\rm recard} = 25000$
In <sub>3</sub> Ir_LT	(In) <sub>0.75</sub> :(In,Ir) <sub>0.25</sub>	$G_{\text{In:In}}^{\text{In}_{3}\text{Ir}_{-}\text{LT}} - H_{\text{In}}^{\text{Tetragonal}_{-}\text{A6}} = \text{GHSERIn} + 5000$
		$G_{\text{ln}:lr}^{\text{ln}_3\text{lr}\_LT} - 0.75 * H_{\text{ln}}^{\text{Tetragonal\_A6}} - 0.25 * H_{\text{lr}}^{\text{FCC\_A1}} = 0.75 * \text{GHSERIn} + 0.25 * \text{GHSERIr} - 24900 + 11.303 * T$
		${}^{0}L_{\text{In};\text{ln};\text{lr}}^{\text{In}_{2}\text{lr},\text{LT}} = -2500$
In₃Ir_HT	(In) <sub>0.75</sub> :(In,Ir) <sub>0.25</sub>	$G_{\text{ln:ln}}^{\text{ln}_3\text{lr},\text{HT}} - H_{\text{ln}}^{\text{Tetragonal}_A6} = \text{GHSERIn} + 5000$
		$G_{\text{ln:lr}}^{\text{ln_3lr},\text{HT}} - 0.75*H_{\text{ln}}^{\text{Tetragonal},\text{A6}} - 0.25*H_{\text{lr}}^{\text{FCC},\text{A1}} = 0.75*\text{GHSERIn} + 0.25*\text{GHSERIr} - 23800 + 9.568*T$
		${}^{0}L_{\text{In};\text{In},\text{Ir}}^{\text{In}_{3}\text{Ir},\text{HT}} = -3000$
		$G_{\text{ln},\text{ln}}^{\text{ln},\text{lr}} - H_{\text{ln}}^{\text{Tetragonal},\text{A6}} = \text{GHSERIn} + 5000$
In <sub>2</sub> Ir	(In,Ir) <sub>0.6667</sub> :(In,Ir) <sub>0.3333</sub>	$G_{\text{lr;lr}}^{\text{ln}_2\text{lr}} - H_{\text{lr}}^{\text{FCC}-A1} = \text{GHSERIr} + 5000$
		$G_{\text{In}2\text{Ir}}^{\text{In}_2\text{Ir}} - 0.6667 * H_{\text{In}}^{\text{Tetragonal}\_A6} - 0.3333 * H_{\text{Ir}}^{\text{FCC}\_A1} = 0.6667 * \text{GHSERIn} + 0.3333 * \text{GHSERIr} - 26700 + 11.135 * T_{\text{In}}^{\text{CO}} + 1$
		$G_{\rm lr,ln}^{\rm ln_2lr} - 0.6667 * H_{\rm lr}^{\rm FCC\_A1} - 0.3333 * H_{\rm ln}^{\rm Tetragonal\_A6} = 0.6667 * {\rm GHSERIr} + 0.3333 * {\rm GHSERIn} + 10000 + 26700 - 11.135 * T_{\rm ln}^{\rm CO} + 10000 + 26700 - 11.135 * T_{\rm ln}^{\rm CO} + 10000 + 2000 + 10000 + 2000 + 100000 + 100000 + 10000 + 10000 + 10000 + 1000000 + 1000000 + 1000000 + 100000000$
		${}^{0}L_{\mathrm{In};\mathrm{ln},\mathrm{lr}}^{\mathrm{In}} = -18700 + 10.8 * T$
		${}^{0}L_{\mathrm{In},\mathrm{Ir};\mathrm{Ir}}^{\mathrm{In}} = +16200 + 1.0 * T$

(Va) for vacancy.

ent set of optimized parameters was obtained. Table 2. Fig. 4 gives the complete calculated phase diagram compared to the experimental data. The temperature and composition of the eutectic reaction: Liq  $\leftrightarrow$  In + In<sub>3</sub>Ir<sub>-</sub>LT are well reproduced, Table 3. Its temperature 429.8 K is within the error bar  $429 \pm 2$  K given by Flandorfer et al. [12]. Thus the calculated temperature 1254K of the peritectic invariant reaction Liq +  $In_2Ir \leftrightarrow In_3Ir_-HT$  is also in good agreement with the experimental  $1254 \pm 3 \text{ K}$  [12] or 1258 K one [11]; the Ir composition of the liquid phase (0.097 Ir) is quite in agreement with the one (0.10 Ir) mentioned in [12], Table 3. In<sub>2</sub>Ir shows a congruent melting at 1463 K. The calculated In<sub>2</sub>Ir liquidus reproduced the experimental data very well especially in the high Ir part. In the low Ir part, the agreement is somehow less good but taking into account the difference between the results from calorimetric measurements (1200 K) and DTA (1258 K) for the peritectic reaction: Liq +  $In_2Ir \leftrightarrow In_3Ir_HT$  [12], the composition of liquid participating in the reaction may be somehow uncertain. In fact in the composition range  $0.35 \le x(Ir) \le 1$ , instead of the peritectic reaction Liq + (Ir)  $\leftrightarrow$  In<sub>2</sub>Ir a eutectic reaction (Liq  $\leftrightarrow$  In<sub>2</sub>Ir + (Ir)) was observed at T = 894.1 K for x(Liq, Ir) = 0.598, Fig. 4 and Table 3. The solubility limit (about 0.98 lr) of the FCC\_A1 (lr) solid solution at T = 850 K and 1250 K [12] is well calculated.

A zoom of Fig. 4 in shown in Fig. 5 in the In rich part. It will be noted that the transformation Liq + In<sub>3</sub>Ir\_LT  $\leftrightarrow$  In<sub>3</sub>Ir\_HT occurs at 620.0 K while the In<sub>2</sub>Ir + In<sub>3</sub>Ir\_HT  $\leftrightarrow$  In<sub>3</sub>Ir\_LT reaction takes place at 634.7 K. These results are in good agreement with the experimental data of Flandorfer et al. [12] and his two suggestions of a possibly metatectic transformation at 620±3 K and a peritectoïd one at 636±3 K.

In Fig. 6a and b the molar heat capacities calculated between 300 and 800 K for the In<sub>3</sub>Ir\_LT and In<sub>2</sub>Ir phases are compared at once with the data of Anres et al. [11] and the ones obtained from the Neumann and Kopp rule from the Cp values of pure In and Ir taken from Dinsdale [17]. The agreement is more satisfactory for In<sub>2</sub>Ir than for In<sub>3</sub>Ir\_LT. In order to avoid the anomaly of the heat capacity of In (bump at T = 429.75 K occurring when the GHSERIn Gibbs energy is represented as the power series in terms of temperature described by [17] in the 429.75 K < T < 3800 K range), the power series of the 298.15 K < T < 429.15 K range was used for temperatures higher than 429.75 K.

Table 5

Invariant reactions in the In-Ir system calculated after the third step of optimization (calculation of the interpolated phase diagram by Flandorfer et al. [12]).

Reactions	T (°C) [Ref.]	Phase x(Ir) [Ref.]	T(°C) This work	Phase x(Ir) This work
$Liq \Leftrightarrow ln + ln_3 lr\_LT$	$156 \pm 2$ [12] $156.64 \pm 0.02$ [11]	ln <sub>3</sub> lr_LT 0.238-0.25 [12]	156.8	Liq 2.6E–09 In 0.0000 In₃Ir_LT 0.2382
In₃Ir_HT ⇔ Liq + In₃Ir_LT	347±3 [12]	ln <sub>2</sub> lr 0.314-0.343 [12]	347.6	Liq 1.8E–05 In <sub>3</sub> Ir_LT 0.2400 In <sub>2</sub> Ir HT 0.2366
$In_2Ir + In_3Ir_HT \Leftrightarrow In_3Ir_LT$	363±3[12]		361.0	In <sub>2</sub> Ir 0.3208 In <sub>3</sub> Ir_HT 0.2500 In <sub>3</sub> Ir_LT 0.2500
Liq + In₂Ir ⇔ In₃Ir_HT	981±3[12] 985[11]		981	Liq 0.1012 In <sub>2</sub> Ir 0.3080 In <sub>2</sub> Ir HT 0.2452
$Liq \Leftrightarrow In_2 Ir + (Ir)$	1188±5 [12] 1190 [11]		1188	Liq 0.3057 In <sub>2</sub> Ir 0.3837 (Ir) 0.9621



**Fig. 6.** (a) Molar heat capacities calculated between 300 and 800 K (continuous line) for the  $In_2Ir$  phase and compared with the data of Anres et al. [11] ( $\Delta$ ) and the Neumann and Kopp rule (dashed line). (b) Molar heat capacities calculated between 300 and 800 K (continuous line) for the  $In_3Ir$ .LT phase and compared with the data of Anres et al. [11] ( $\Delta$ ) and the Neumann and Kopp rule (dashed line).

3. Finally, in a third optimization step, we tried to reproduce the liquidus interpolated by Flandorfer et al. [12] in the composition range  $0.35 \le x(\ln) \le 1$  and obtained a second set of optimized thermodynamic parameters.

Compared to the first set, the two negative excess parameters of the liquid phase ( ${}^{0}L$  and  ${}^{3}L$ ) were lowered very much (in absolute value) in order to diminish its stability at low temperatures, Table 4. So no agreement could be found with the coherent integral and partial experimental data of enthalpies of mixing of the liquid phase determined by [11,12]. In this last step of the process, a homogeneity range was also assumed for the two intermetallic compounds, Fig. 7. In addition the structural change at about T = 625 K (LT  $\leftrightarrow$  HT) of the In<sub>3</sub>Ir phase [11,12] was taken into account, Fig. 8. The eutectic reaction: Liquid  $\leftrightarrow$  In + In<sub>3</sub>Ir\_LT, and the two peritectic reactions: Liq + In<sub>2</sub>Ir  $\leftrightarrow$  In<sub>3</sub>Ir\_HT and Liq + (Ir)  $\leftrightarrow$  In<sub>2</sub>Ir) at 1461 K is in



**Fig. 7.** Comparison of the In–Ir phase diagram calculated with the thermodynamic parameters optimized during the third procedure, Table 4, with the experimental data.



**Fig. 8.** Part of the In–Ir phase diagram in the In rich part calculated with the thermodynamic parameters optimized during the third procedure, Table 4, and compared with the experimental data.

agreement with the predicted one  $(1461 \pm 5 \text{ K})$  by [12] or 1463 K [11].

#### 5. Conclusion

A coherent set of thermodynamic parameters was optimized based on the CALPHAD approach, which led to the calculation of a phase diagram which is in good agreement with the experimental part determined up to about x(Ir) = 0.35.

Beyond this value and up to  $x(Ir) \le 1$ , no experimental liquidus data has been determined. In this interpolated part of the phase diagram by [12], our optimization led to the calculation of a eutectic reaction Liq  $\leftrightarrow In_2Ir + (Ir)$  instead of a predicted peritectic one Liq  $+ (Ir) \leftrightarrow In_2Ir$ .

The calculated integral and partial enthalpies of mixing of the liquid phase of the In–Ir system are in good agreement, within the

experimental error, with the numerous and coherent experimental data up to about x(Ir) = 0.35. Beyond this value, the agreement is not satisfactory due to the precipitation of solid phases in the liquid.

The phase diagram proposed by [12] can only be calculated with a new set of optimized excess thermodynamic parameters of the liquid phase but which cannot give account of the reliable integral and partial enthalpies of mixing determined by [11,12].

Consequently, in the  $0.35 \le x(\ln) \le 1$  composition range, the In–Ir phase diagram seems to be more complex than the predicted one as attested by the determination of a new phase  $\ln_{54}\ln_{46}$  by [12] which has been first assumed as metastable and further experimental determinations are therefore needed in the Ir rich part of the phase diagram.

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