

## Note

### COMPUTER-DETERMINED KINETIC PARAMETERS FROM TG CURVES. PART XVI

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In a previous communication [1], expressions were developed which were utilized to analyze data from non-isothermal TG (NITG) curves, at relatively low conversions, for activation energy ( $E$ ). Such an analysis led to the estimation of  $E$  alone, virtually independent of reaction order ( $n$ ) values. In this paper, expressions have been developed with the same goal in mind, to determine values of  $E$  irrespective of the  $n$ -values. To this end, rational approximations and an iterative computer procedure were employed.

#### THEORY

It was previously reported [2-4] that the integral of the Arrhenius function could be satisfactorily represented by rational expressions such as,

$$T \exp(-x) \frac{(x^2 + 10x + 18)}{(x^3 + 12x^2 + 36x + 24)} \quad (1)$$

$$T \exp(-x) \frac{(x^3 + 18x^2 + 88x + 96)}{(x^4 + 20x^3 + 120x^2 + 240x + 120)} \quad (2)$$

as well as the equation which was derived using integration by parts,

$$T \exp(-x) \frac{1}{x} \left[ 1 - \frac{2!}{x} + \frac{3!}{x^2} + \dots + \frac{(-1)^N (N+1)!}{x^N} \right], \quad N = 2 \quad (3)$$

where  $x = E/RT$ . The suitability of eqns. (1)-(3) as well as of other expressions for the estimation of  $E$  and  $n$  has been reported [2,3]. By employing any of eqns. (1)-(3), we may readily write for an  $n$ -type unimolecular or pseudo-unimolecular decomposition by means of NITG, at relatively low conversions [1]

$$\ln \left[ \frac{(\alpha/T)}{(RA)} \right] = -\frac{E}{RT} + \ln \left( \frac{A}{\beta} \right) \quad (4)$$

where  $A$  = pre-exponential factor,  $\beta$  = constant heating rate, and  $\alpha$  = degree

of conversion. The term  $RA$  can denote any of the moieties in eqns. (1)–(3) which follow the term  $T \exp(-x)$ .

## RESULTS AND DISCUSSION

A computer program was devised which allowed the determination of  $E/R$  from eqn. (4) by means of iteration. Since values of  $x$  are invariably larger than 5, an initial value of  $x = 5$  was arbitrarily assumed. Using a least squares treatment (LSQ), where the left-hand side of eqn. (4) was the dependent variable and the independent variable  $-1/T$ ,  $\alpha-T$  data provided an initial value of  $E/R$ . This value of  $E/R$  was then used in the  $RA$ -term so that another value of  $E/R$  could be obtained by means of LSQ. This iterative procedure was rapid and continued until the absolute value of the difference between a value of  $E/R$  and its previous value divided by the value of  $E/R$  was less than 0.0001. When this limiting condition was met, the value of  $E/R$  was considered to be the proper value (generally, less than 4 iterations were required). Along with  $E/R$ , a correlation coefficient (CR) was obtained. The preceding method was applied to low conversion data for octamethylcyclotetrasiloxane (OMCS) [5], teflon [5], magnesium hydroxide [6], as well as theoretical data [7].

In the case of OMCS, 5 pairs of  $\alpha-T$  data were used where  $\alpha$  varied from 0.005 to 0.106. A value of  $E = 10.3 \text{ kcal mol}^{-1}$  was obtained along with  $CR = 0.9955$  (lit. [5,8],  $E = 11.7$  and  $12.7 \pm 1.5$ ). For teflon, 5 pairs of data afforded values of  $E = 65.1 \text{ kcal mol}^{-1}$ ,  $CR = 0.9997$  (lit. [5],  $E = 66-68 \text{ kcal mol}^{-1}$ ). The procedure was also applied to NITG data for magnesium hydroxide to test the effect of an apparent high value of  $n$ , ca. 1.5. For 7  $\alpha$ -values ranging from 0.03 to 0.12 (trace 1),  $E = 58.4 \text{ kcal mol}^{-1}$  and  $CR = 0.9967$  (lit. [2,3,6,8-11],  $E = 53-57 \text{ kcal mol}^{-1}$ ). Finally, employing 12 pairs of theoretical  $\alpha-T$  data where  $\alpha$  ranged from 0.007 to 0.1001,  $E = 29.8$  and  $CR = 0.9999$  (lit. [7],  $E = 30 \text{ kcal mol}^{-1}$ ). From the preceding, it can be seen that the method employed was rapid and provided reasonably satisfactory values of  $E$  even though  $n$ -values ranged from ca. 0.3 to 1.5.

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