

## Note

### COMPUTER-DETERMINED KINETIC PARAMETERS FROM TG CURVES. PART XV

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In previous publications, values of reaction order ( $n$ ) were estimated for “ $n$ -type” unimolecular or pseudo-unimolecular decompositions without the need for any initial determination of activation energy ( $E$ ) [1–5]. The procedures described involved the estimation of slopes of TG curves ( $RT$ ) at various degrees of conversion ( $\alpha$ ) and corresponding temperatures ( $T$ , K) [data from DTA (and DSC) traces can also be readily utilized]. Then values of  $n$  could be determined directly by graphical procedures [2–4] or indirectly by iterative methods [5]. The aim of this paper is to extend previously reported procedures so that the value of  $n$  can now be determined directly by means of cubic equations which use data from TG or DTA (or DSC) traces.

#### THEORY

It can be readily shown (cf. ref. 1) that

$$\text{LH} = [(1 - \alpha_1)^n - (1 - \alpha_1)] / [(1 - \alpha_2)^n - (1 - \alpha_2)] \quad (1)$$

where  $\text{LH} = [(RT)_1 / (RT)_2] (T_1 / T_2)^2$ , and  $RT = d\alpha / dT$ . From eqn. (1), for various fixed values of  $\alpha_1$  and  $\alpha_2$ , values of LH can be calculated for various values of  $n$ . In this manner, the following arbitrary values of  $\alpha_1 / \alpha_2$  were used: 0.2/0.8, 0.2/0.9, 0.25/0.75, 0.3/0.6, 0.3/0.7, 0.3/0.8, 0.4/0.7, 0.4/0.8, and 0.5/0.8 while the values of  $n$  used ranged from 0.1 to 2. Then the calculated values of LH and  $n$  were correlated by means of a cubic expression such as

$$n = A0 + A1(\text{LH}) + A2(\text{LH})^2 + A3(\text{LH})^3 \quad (2)$$

Correlation coefficients ranged from 0.9998 to 0.9999 and standard error of estimate values ranged from 0.00016 to 0.013.

## TESTING THE METHOD

In the Appendix a computer program (CP) is presented whereby values of  $n$  can be rapidly calculated from values of  $T_1$ ,  $(RT)_1$  [or  $(\Delta T)_1$  in the case of DTA],  $T_2$ , and  $(RT)_2$ , once values of  $\alpha_1/\alpha_2$  have been specified. In the CP, line numbers (LN) 110–190 depict values of  $A_0$ ,  $A_1$ ,  $A_2$ , and  $A_3$  which correspond to the ratios of  $\alpha_1/\alpha_2$  in LN 10. The CP was tested in the following cases: (1) theoretical TG data for  $n = 0.5$ ; (2) theoretical TG data for  $n = 1$  [6]; (3) experimental DTA data for benzenediazonium chloride (BDC) in aqueous solution [7]; (4) experimental TG data for magnesium hydroxide (MH) [8]; (5) experimental DTA data for bulk polypropylene (PP) [9]. Values corresponding to the ratios in LN 10 of the CP were obtained by interpolation where necessary.

In cases 1 and 2, all the nine  $\alpha$  ratios in LN 10 of the CP were tested and the average  $n$ -values and their corresponding mean deviations were, respectively:  $0.50 \pm 0.00$  and  $1.01 \pm 0.00$ . In case 3, six  $\alpha$  ratios were tested for BDC and afforded an average value of  $n = 0.98 \pm 0.02$  (lit. [3–5,7], 1–1.1). In case 4, four  $\alpha$  ratios were utilized from data for the dehydroxylation of MH to afford a value of  $n = 1.8 \pm 0.05$  for Trace 1 and  $n = 1.7 \pm 0.22$  for Trace 2 (lit. [8], 1.5–1.7). Finally, in case 5, four  $\alpha$  ratios were tested for PP and yielded  $n = 0.81 \pm 0.02$  (lit. [3],  $0.88 \pm 0.11$ ).

From the preceding, it can be seen that the calculated values of  $n$  for the various cases were in reasonably good agreement with anticipated or reported values. A possible limitation of the method in the case of TG is the difficulty of measuring accurately large values of slope from a primary thermogram ( $RT$ ). (However, where available, DTG equipment should be able to manage such measurements.) On the other hand, DTA (or DSC) can afford accurate values of slope ( $\Delta T$  can be used since ratios are employed) but much interpolation would probably be needed since specified values of  $\alpha$ , determined by area measurements, would be difficult to obtain readily. Of course, once values of  $n$  are determined, values of  $E$  can then be obtained.

## APPENDIX

A computer program to calculate reaction order ( $n$ ) using a cubic equation.

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2  ***CALCN. OF 'N' USING CUBIC ECU.***
3  '
5  CLS
8  '
10 INPUT"WHICH RATIO: 2/8 (1), 2/9 (2), 2.5/7.5 (3), 3/6 (4), 3/7 (5), 3/8 (6),
4/7 (7), 4/8 (8), 5/8 (9) ";A
15 '
20 ON A GOSUB 110,120,130,140,150,160,170,180,190
25 '
30 PRINT:INPUT"ENTER IN ORDER: T1, RT1, T2 & RT2 ";T1,R1,T2,R2
35 '
40 LH=(R1/R2)*(T1/T2)^2
45 '
50 N=A0+ A1*LH+A2*(LH)^2+A3*(LH)^3
55 '
60 PRINT:PRINT"THE VALUE OF REACTION ORDER= ";CENS(N)
65 '
70 END
100 '
110 A0=-1.21469:A1=5.88051:A2=-4.29979:A3=1.63847:RETURN
115 '
120 A0=-.554837:A1=2.96582:A2=-1.50471:A3=.36425:RETURN
125 '
130 A0=-1.6883:A1=6.280628:A2=-4.058854:A3=1.47885:RETURN
135 '
140 A0=-3.89949:A1=10.41649:A2=-6.60883:A3=2.75432:RETURN
145 '
150 A0=-2.35935:A1=7.02524:A2=-4.17492:A3=1.51003:RETURN
155 '
160 A0=-1.361512:A1=4.431316:A2=-2.306174:A3=.672883:RETURN
165 '
170 A0=-2.9409:A1=6.80851:A2=-3.634:A3=1.27719:RETURN
175 '
180 A0=-1.59965:A1=3.9671:A2=-1.73755:A3=.462325:RETURN
185 '
190 A0=-2.00998:A1=4.1452:A2=-1.79115:A3=.499774:RETURN

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